



Statewide Hatchery Evaluation

New Hampshire Fish and Game Department

New Hampshire December 13, 2023

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Abbreviations

| AACE | Association for the Advancement of Cost Engineering |
|-------|---|
| EPA | Environmental Protection Agency |
| HVAC | Heating, Ventilation and Air Conditioning |
| NHDES | New Hampshire Department of Environmental Services |
| NHFGD | New Hampshire Fish and Game Department |
| NPDES | National Pollution Discharge Elimination System |
| NPV | Net Present Value |
| O&M | Operation and Maintenance |
| OPCC | Opinion of Probable Construction Cost |
| PRAS | Partially Recirculating Aquaculture System |
| RAS | Recirculating Aquaculture System |
| SFH | State Fish Hatchery |
| TP | Total Phosphorus |
| UV | Ultraviolet Light |

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Executive Summary

New Hampshire Fish and Game Department (NHFGD) operates six fish hatcheries in the State of New Hampshire: Powder Mill, Berlin, New Hampton, Milford, Twin Mountain, and Warren. This system of facilities produces approximately 400,000 lbs of fish annually to serve the State's demand. The largest of the State's producers is Powder Mill with 120,000 lbs annually. Berlin, New Hampton, and Milford all produce roughly 70,000 to 75,000 lbs annually, and Twin and Warren combined produce roughly 45,000 lbs annually.

Total phosphorus (TP) effluent limits imposed on the Powder Mill State Fish Hatchery in 2021 were the driving factor for this comprehensive study. These limits were given to Powder Mill due to the receiving water body (several impoundments on the Merrymeeting River) having been listed on New Hampshire's 303(d) list as impaired due to cyanobacteria in the preceding years. Cyanobacteria is harmful to human health and fueled by excess phosphorus, thus leading to what is one of the lowest TP effluent limits in the country faced by a fish hatchery at 12 μ g/L TP.

In addition, the Berlin State Fish Hatchery (SFH) is currently facing a new discharge permit; however, the limits have not yet been finalized by the EPA for this facility. Although exact limits are currently unknown, it is likely that this facility will be required to decrease current production numbers to meet the new effluent permit requirements.

Due to this regulatory pressure on two of the State's major hatcheries, NHFGD retained HDR Engineering Inc. (HDR) to evaluate existing conditions, develop modernization alternatives for each individual hatchery, and look at the entire system as a whole to find the most efficient way to meet production and stocking goals while maintaining permit compliance. In 2022-2023, HDR completed the condition assessments, a piloting effort at Powder Mill, and modernization evaluations for each of the six hatcheries.

Characterization of the speciation of total phosphorus in hatchery effluent was undertaken at Powder Mill and Berlin given the concentrations of each species significantly influences the treatment mechanism necessary when such a low TP target is desired. Data on phosphorous speciation in hatchery effluent is not readily available in literature since such a low TP effluent limit has never been faced by a hatchery before. It was found that Powder Mill's effluent contained all three phosphorous species that comprise total phosphorus in roughly equivalent values. Each individual species was found in levels higher than the permitted total limit. Since each species requires a different form of treatment, this means three different treatment methods are required to approach meeting such low limits.

A pilot effluent treatment study was executed at Powder Mill to determine if it was even technologically achievable to meet the required TP limits. The study found that the limits could be achieved by ultrafiltration, chemical addition, and ion exchange processes in series. However, the cost to implement these technologies at Powder Mill was not the most efficient way to meet production and stocking goals and cost more than current available funding.

Concurrently, evaluations of each of the hatcheries were conducted and utilized to develop system wide alternatives to evaluate how production can be relocated within the existing system to meet both effluent permit limits and the state's production demand. Given the mission of NHFGD, it is desirable that most of the available funding be expended on modernizing fish production facilities that discharge less TP rather than construct advanced effluent treatment facilities to serve outdated and failing hatchery technology.

Three key issues drive achieving 400,000 lbs of production within the State's system of six hatcheries; permit compliance, water supply (quantity and quality), and the condition of the existing infrastructure.

- Permit Compliance The low limits already in place for Powder Mill and the potential for similar at Berlin dictate the need for any of the larger hatcheries to include effluent treatment. The scale and complexity of the treatment will be determined by the location of the facility, the amount of treated recirculation water, and existing or potential future limits. Production capabilities that have been estimated in this document outline potentials based on fish rearing and infrastructure requirements but the ultimate levels of production achievable at each location will be driven by permit compliance.
- Water Supply Powder Mill is the only facility within the state with ample water supply. All
 other sites have limited water supplies that are currently being utilized to the maximum
 extent possible for the existing systems which were designed for flow through with multiple
 passes. Thus, for any of the other five facilities, recirculating aquaculture systems (RAS)
 that include water treatment are required. Additionally, Milford has limits on the amount of
 water that can be withdrawn, and that water is high in iron and manganese causing
 increased maintenance within the facility. However, some facilities such as Twin Mountain,
 while small, has a high-quality water supply that would be suitable for broodstock use.
- Infrastructure Existing infrastructure has been driven to the end of its useful life. Major investments to maintain permit compliance, efficient operation, and address water supply issues should be done in conjunction with modernized rearing facilities to maximize the investment of the state's dollars and protect the production capabilities of the system.

After review of multiple alternatives at all six facilities, as well as development and evaluation of statewide alternatives, an approach to the improvements required to continue to support NHFGD's production goals in the interim is clear. Immediate investments should occur at New Hampton to construct a new recirculating aquaculture system (RAS) facility to accommodate 150,000 lbs in production plus house Brook and Brown Trout broodstock and Landlocked Atlantic Salmon egg rearing. The centralized location of the facility, capability to complete major renovation within the existing footprint, and the ability to utilize RAS make the location ideal for major infrastructure investments. This project increases production by 108% based on lbs per year at New Hampton. With additional future funding, this facility has the potential to increase production up to 250,000 lbs per year with the use of higher rearing densities and a relocation of the effluent discharge to the Pemigewasset River.

Investment to construct a Rainbow Trout broodstock facility at Twin Mountain should be executed concurrently or shortly after completion of construction at New Hampton. A new biosecure building

capable of housing an internal Rainbow Trout program would eliminate the need to import poor quality eggs from other programs outside of New Hampshire, resulting in a huge cost savings in labor and operation in addition to better control of egg quality.

These two recommended projects at New Hampton and Twin Mountain allow NHFGD to meet 359,000 lbs of production after consideration of the anticipated losses required at Powder Mill and Berlin. There are multiple pathways available to meet the overall statewide production goals that have been determined as part of this study:

- New Hampton Phase 2 Relocation of the effluent discharge from Dickerman Brook to the Pemigewasset River could allow this facility to produce up to 250,000 lbs with minimal rearing system improvements by carrying an increased density within the existing rearing units.
- Milford Rehabilitation Rebuild of Milford including source water treatment to reach 100,000 lbs in production.
- Powder Mill Re-Evaluation Evaluate use of a dilution zone coupled with recirculating technology. Additional evaluation of less advanced forms of TP removal may also be justified.
- Berlin/New Northern Facility Depending on the regulatory pressure on Berlin, reevaluation of a new Northern Facility may be justified.

However, given the uncertainty remaining regarding the regulatory environment as well as further engineering study required to determine the most cost-effective path forward, additional evaluation should be undertaken prior to implementing a long-term plan to meet the states entire 400,000 lb goal for production.

While major projects at New Hampton and Twin Mountain are recommended as part of the interim plan and multiple other pathways exist to reach the State's 400,000 lb production goal, it is critical to understand that reinvestment into the entire statewide system is overdue. The State's existing hatcheries have provided an enormous environmental, social, and economic impact over their life span. Per year, the New Hampshire Hatchery System produces roughly 1.5 million fish for stocking. Extrapolating that by the average 20-year lifespan of a facility typically assigned in engineering studies, results in roughly 30 million fish! These systems have served New Hampshire for significantly longer than 20 years, having an average age of 88 years, and now need significant reinvestment to continue to provide these benefits.

The implementation timeline for the interim plan is extremely condensed and will require significant capital investment within the State's hatchery systems over the course of the next five years to maintain production goals, with even more investment necessary to reach the long-term goals. The recommended timeline for the interim plan is as follows:

- <u>Phase 1 2025</u>:
 - Powder Mill Reduction in annual production from 118,000 lbs to 30,000 lbs (75% reduction) to meet effluent TP limits.

- Berlin Slight reduction in annual production from 74,000 lbs to roughly 64,000 lbs (13.5% reduction). If further reduction is deemed necessary after receiving the final EPA discharge permit this facility may shift its focus to Brook Trout broodstock only as a viable alternative to meet new effluent TP limits.
- <u>Phase 2 2025/2026</u>:
 - New Hampton New RAS facility to accommodate 150,000 lbs in production plus house Brook and Brown Trout broodstock and Landlocked Atlantic Salmon egg rearing.
- <u>Phase 3 2026/2027</u>:
 - Twin Mountain Slight reduction in production to focus on Rainbow Trout broodstock.
- <u>Phase 4 2027-2030</u>:
 - Reevaluation of the statewide system to determine the best way to meet production goals. Depending on the selected long-term approach, major rehabilitation at other facilities should be undertaken to maintain production capabilities at existing facilities.

The opinion of probable construction costs (OPCC) summary for each phase of implementation of the interim plan are shown below in Table ES-1.

| | Phase 1 2025 | Phase 2 2025/2026 | Phase 3 2026/2027 |
|-------------|-----------------|----------------------|----------------------|
| Powder Mill | \$2,800,000 | | |
| Belin | | | |
| New Hampton | | \$50,900,000 | |
| Milford | | | |
| Twin | | | \$ 4,000,000 |
| Warren | | | |
| Total | \$2,800,000 | \$50,900,000 | \$4,000,000 |

Table ES-1: Recommended Interim Plan OPPCs by Phase

Notes: 1. Opinion of Probable Construction Costs do not include required design engineering and design services during construction fees. Determination of project funding requirements will necessitate the inclusion of these fees.

Implementing significant improvements to New Hampton and Twin Mountain will allow NHFGD to continue to effectively carry out its mission of conserving, managing, and protecting the State's fish and wildlife resources and their habitats; informing and educating the public about these resources; and providing the public with opportunities to use and appreciate these resources until further information is known. Furthermore, reevaluation of the remaining alternatives to reach the State's goal of 400,000 lbs ensures that the best overall long-term solution is implemented so that NHFGD can continue to provide the enormous environmental, social, and economic impact in the most cost-effective way for the next 25 to 50 years.

1 Introduction

The State of New Hampshire utilizes fish stocking as one of several essential tools to provide statewide fisheries resource management and recreational opportunity. These are two of the many functions of the New Hampshire Fish and Game Department (NHFGD), and it is accomplished by the operation of fish hatcheries and rearing stations. The major objective of these facilities is to produce the requested number of trout and Landlocked Atlantic Salmon to support recreational sport fishing in the state. Species produced, transferred, and stocked include Brown Trout, Rainbow Trout, Brook Trout, and Landlocked Atlantic Salmon. Other objectives of these facilities include:

- Supplementation in public waters where natural recruitment is low.
- Reintroductions of populations following fish kills.
- Restoration of various fish populations where human-influenced factors caused declines in fish abundance.
- Increase angler opportunities for higher-than-average catch rates or larger-than-average sized trout.

Six state-operated facilities focus on providing high quality fish to meet State objectives: Powder Mill, Berlin, New Hampton, Milford, Twin Mountain, and Warren. (Figure 2-1). Lack of investment in these facilities has occurred over the last several decades resulting in significant deferred necessary maintenance, costly emergency repairs, ineffective infrastructure, and labor-intensive operations. The average age of the facilities is 88 years and the last major infrastructure improvement to these facilities was to consolidate outfalls and provide better removal and storage of solids. However, the consistent lack of investment in these facilities has resulted in all six facilities requiring significant rehabilitation to meet the State's recreational sport fishing goals. In addition, some of these facilities are facing stricter effluent limits which will also require significant investment to attain permit compliance.

Powder Mill Fish Hatchery, the largest in the State's system (in pounds of fish produced), received a new NPDES (National Pollution Discharge Elimination System) Permit in January 2021 with concentration and load-based total phosphorus (TP) limits for the hatchery effluent discharged to Merrymeeting River. A monthly average TP discharge concentration limit of 12 μ g/L was established for each of Powder Mills outfalls along with cumulative load-based limits of 227 lb/year and 19 lb/month. It is important to note that this limit is believed to be one of the lowest in the country for a fish hatchery. While treatment of the existing hatchery effluent to this limit has been shown to be technically achievable, it is significantly cost prohibitive. Additionally, the Berlin Fish Hatchery is anticipated to receive new effluent limits for TP in 2024 which could also pose compliance challenges.

To maximize fish production while minimizing impacts to the environment, modernization within the system must occur. In general terms modernization involves upgrading fish culture infrastructure, utilizing fish production water efficiently, providing healthy fish rearing environments, enhancing effluent treatment, and improving the fish culturist's work environment. A comprehensive evaluation of the NHFGD system was undertaken to determine how to best meet stocking and production goals and comply with total phosphorous (TP) effluent limits at Powder Mill and Berlin through the following efforts:

- Review of current production and stocking levels.
- Condition assessments of all six facilities.
- Bench scale and pilot testing for effluent TP removal.
- Modernization evaluations of all six facilities.

The following pages discuss the results from these efforts and present alternative approaches for meeting statewide objectives through different combinations of improvements at each individual hatchery.

2 Existing Facilities Summary

The NHFGD hatchery system consists of six hatcheries: Powder Mill, Berlin, New Hampton, Milford, Twin Mountain, and Warren. The Nashua National Fish Hatchery supports the six NHFGD facilities. A general overview of the production levels and locations of these hatcheries is provided in Table 2-1 and Figure 2-1.

| Facility | Number | Pounds | % of Total Pounds Produced |
|------------------|-----------|---------|----------------------------------|
| Powder Mill | 344,007 | 117,590 | 31 |
| Berlin | 292,033 | 74,165 | 20 |
| New Hampton | 424,809 | 72,123 | 19 |
| Milford | 158,275 | 68,108 | 18 |
| Warren | 166,695 | 23,685 | 6 |
| Twin Mountain | 57,112 | 20,838 | 5 |
| Nashua * | 26,544 | 4,441 | 1 |
| System Totals | 1,469,475 | 380,950 | 100 |

Table 2-1: Statewide Fish Production Averages fromNHFGD Hatcheries Between 2016 and 2021

*Currently, the Nashua National Fish Hatchery rears half of the statewide Landlocked Atlantic Salmon.

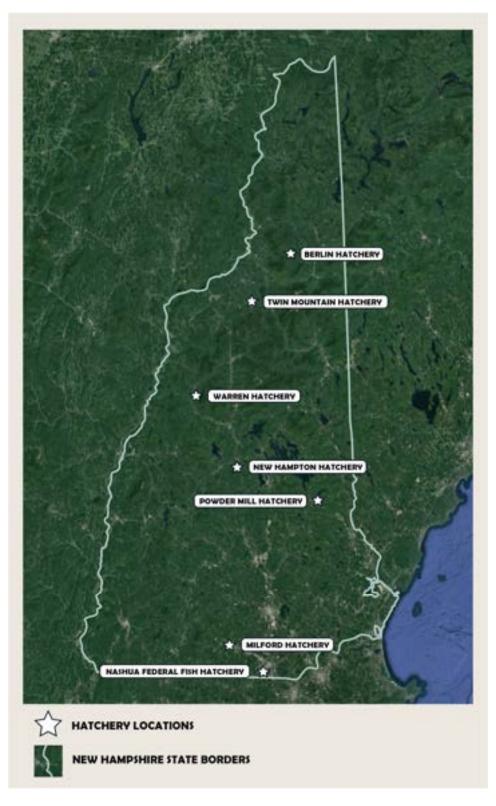


Figure 2-1: New Hampshire Fish and Game Department Statewide Hatcheries.

2.1 Powder Mill State Fish Hatchery

Powder Mill State Fish Hatchery (SFH) is in the Town of New Durham on the southern tip of Merrymeeting Lake in Strafford County, New Hampshire (Figure 2-2). The hatchery resides on approximately 95.55 acres of state-owned land. It consists of 99 exterior ponds/raceways, a hatchery building, and several support buildings. The facility currently manages only early rearing and final growout phases of fish rearing. Powder Mill no longer utilizes its hatchery building for its intended purpose. Infrastructure available for production includes seven primary areas:

- 1. Indoor hatchery building
- 2. Outdoor 25' circular tanks
- 3. A-D Series outdoor linear raceways
- 4. E-F Series outdoor linear raceways
- 5. Outdoor Woods Ponds
- 6. Outdoor Show Ponds
- 7. Outdoor Bass Ponds

Water is supplied by gravity flow from Merrymeeting Lake (1,111 surface acres) located just north of the facility. Water temperature varies monthly and throughout the hatchery. The average yearly water temperature for the entire site is 48°F. Water temperatures for December through March are below 38°F, and limited fish growth occurs during this period. In summer months, temperatures can reach 59°F, which often results in less oxygen carrying capacity. Two recently installed flow meters exist at this facility, one at discharge 001 and the other at discharge 002. Monthly water usage ranges from 3,800 to 4,065 gallons per minute (gpm), with an average monthly use of 3,950 gpm, not to exceed 4,500 gpm.

The hatchery building is not currently utilized for incubation or early rearing. The building houses Heath incubator trays and 10 circular rearing units. Each circular tank is 5' diameter with an operating depth of 1.6'. The water flow to each tank is 10 gpm, and the circular tanks are being used as mixing tanks for lime addition to the culture water for series E, F, and G to assist in stabilizing pH and meeting effluent limits.

The hatchery maintains 99 concrete and earthen rearing units. The upper portion of the facility contains seven banks of raceways (labeled Series A through G). These concrete raceways utilize serial reuse and are fed source water at two locations, the east of Series E and the west of Series A. The raceways do not currently have integral aeration systems but do contain electrical distribution. On average, the flow through each series of raceways is as follows: Series A - 150 gpm, Series B - 800 gpm, Series C - 600 gpm, Series D - 300 gpm, Series E - 300 gpm, and Series F - 300 gpm. The upper portion of the facility also contains four earthen ponds called the Show Ponds, which are used for rearing large yearling fish. The water supply for the Show Ponds is the discharge from the Series A through D raceways.

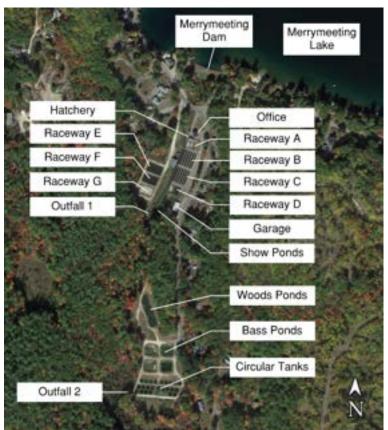


Figure 2-2: Powder Mill State Fish Hatchery Aerial Image.

The lower portion of the facility contains four earthen ponds called the Woods Ponds, four earthen ponds called Bass Ponds, and 27 circular 25' diameter rearing units. Discharge from the Show Ponds is serially reused in the Woods Ponds, Bass Ponds, and 25' circular rearing units. The Woods Ponds are no longer utilized due to the extreme level of predation experienced. The Bass Ponds were previously used for broodstock holding, but they have recently been serving as settling and storage basins for vacuumed fish waste. Each 25' circular rearing unit is 2.25 feet deep on average with the deepest point in the middle. The flow into each unit is approximately 18 gpm. Four of the circular tanks are currently being utilized for storage and solids settling of the vacuumed fish waste. All rearing units for Powder Mill SFH are summarized in Table 2-2.

| Rearing Unit | Quantity | Unit Volume (ft³) ¹ | Total Volume (ft³)1 |
|-----------------------------|----------|-----------------------------------|---------------------------|
| Indoor Facility | | | |
| 5' Circular Tank | 10 | 29 | 290 |
| Subtotal | | | 290 |
| Outdoor Facility | | | |
| Series A Linear Raceways | 10 | 233 | 2,330 |
| Series B Linear Raceways | 6 | 1,920 | 11,520 |
| Series C Linear Raceways | 6 | 1,920 | 11,520 |
| Series D Linear Raceways | 8 | 612 | 4,896 |
| Series E Linear Raceways | 10 | 681 | 6,810 |
| Series F Linear Raceways | 10 | 681 | 6,810 |
| Series G Linear Raceways | 10 | 681 | 6,810 |
| Show Pond | 4 | 1,426 | 5,707 |
| Woods Pond | 4 | 5,560 | 21,839 |
| Bass Pond | 4 | 18,315 | 73,260 |
| 25' Circular Tanks | 27 | 860 | 23,220 |
| Subtotal | | | 167,912 |
| Total | | | 168,202 |

1) Unit Volume and Total Volume refer to the total available volume, not the operating volume.

2.2 Berlin State Fish Hatchery

Berlin State Fish Hatchery (SFH) is in the Town of Berlin located within the Kilkenny Valley in the White Mountain National Forest in Coos County, New Hampshire (Figure 2-3). The hatchery resides on an approximately 365 acres of federally owned land. The site is leased and operated by NHFGD. The facility consists of groundwater and surface water supplies, 51 outdoor concrete rectangular raceways, a hatchery building with 24 concrete rectangular raceways and 48 aluminum rearing troughs, and numerous support buildings. The facility manages the following phases of rearing: broodstock management, egg incubation, early rearing, and final grow out, which is accomplished utilizing an indoor hatchery building and outdoor concrete raceways.



Figure 2-3: Berlin State Fish Hatchery Aerial Image.

The water supplies for Berlin SFH are Cold Brook, Diversion Pond, the West Branch of the Upper Ammonoosuc River, Third Brook, No. 9 Brook, and two production wells. Hatchery personnel report that flow rates can be estimated over weirs at the facility. Currently, no flow meters exist. The flow rates from the surface water supplies vary seasonally, ranging between 400 and 2,800 gpm depending on the water source. The production wells produce between 200 and 400 gpm. Surface waters supply most of the water, while the wells supplement Cold Brook both in the summer, when flows are low, and in the winter, when water is too cold or frozen. HDR completed additional preliminary phosphorus sampling on the source waters and effluent at Berlin SFH between March and April of 2022. Results from three sampling events showed large variations in total phosphorus (TP) and phosphorus (P) speciation between each of the sources and each of the sampling events. These results suggested that there is enough TP in the sources to impact the TP in the effluent at a significant level and further sampling should be undertaken.

Cold Brook and the wells supply the Hatchery Building, Young's Raceway, and Foster's Raceway. The West Branch of the Upper Ammonoosuc River and Third Brook supply the Upper Canal

Raceways. Overflow from the Canal Raceways and No. 9 Brook feed Diversion Pond, which supplies the West Branch Raceways. Appendix B provides a proposed site layout for Berlin including an overview the water sources, flow splits, and outfalls.

The Hatchery Building uses an average flow of 50 gpm, not to exceed 100 gpm. It contains 24 concrete raceways and 48 aluminum troughs for early rearing, as well as trough inserts for egg incubation. The concrete raceways each measure 26.6' x 2.6' x 1.7', and the aluminum troughs each measure 13' x 1.1.6' x 0.38' at operating depth. The average water flow per trough is 20 gpm. The average water flow per raceway is 30 gpm, with a maximum rate of 75 gpm.

The hatchery maintains 51 concrete raceways that are split into four series: Young's Raceways, Foster's Raceways, West Branch Raceways, and the Upper Canals. Young's Raceways consist of 12 raceways that each measure 76' x 8' x 1.8' at operating depth and average a flow of 480 gpm, with a maximum flow of 600 gpm. Foster's Raceways consist of 16 raceways that each measure 73' x 8' x 1.7' at operating depth and average a flow of 450 gpm, with a maximum flow of 600 gpm. The West Branch Raceways are a set of 20 raceways that each measure 107' x 8' x 1.8' at operating depth and average a flow of 1,050 gpm. The Upper Canals consist of three raceways that each measure 335' x 12' x 2.7' at operating depth and average a flow of 2,800 gpm. All rearing units for Berlin SFH are summarized in Table 2-3.

| Rearing Unit | Quantity | Unit Volume (ft³) ¹ | Total Volume (ft³) ¹ |
|--------------------------|----------|-----------------------------------|------------------------------------|
| Indoor Facility | | | |
| Concrete Raceways | 24 | 118 | 2,832 |
| Aluminum Troughs | 48 | 6 | 288 |
| Subtotal | | | 3,120 |
| Outdoor Facility | | | |
| Foster's Raceways | 16 | 1,200 | 19,200 |
| Young's Raceways | 12 | 1,162 | 13,944 |
| West Branch Raceways* | 20 | 1,715 | 34,300 |
| Upper Canals | 3 | 4,100 | 12,301 |
| Subtotal | | | 79,745 |
| Total | | | 82,865 |

Table 2-3: Berlin Rearing Unit Summary

1 Unit Volume and Total Volume refer to the volume available at operating depths.

* Currently empty

2.3 New Hampton State Fish Hatchery

New Hampton State Fish Hatchery (SFH) is in the Town of New Hampton on the western edge of Belknap County, New Hampshire (Figure 2-4). The hatchery resides on approximately 163 acres of state-owned land and consists of 75 rearing units, a hatchery building, a water supply pond, and various springs with driven well heads. The facility manages the following phases of rearing: brood production, egg incubation, early rearing, and final grow out, which is accomplished utilizing five primary areas that include:

- 1. Indoor hatchery building
- 2. Outdoor 25' circular tanks
- 3. Outdoor 46' rearing rectangular raceways
- 4. Outdoor 50' rearing rectangular raceways
- 5. Outdoor 100' rearing rectangular raceways

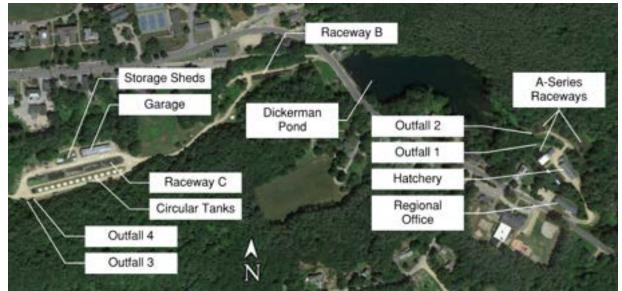


Figure 2-4: New Hampton State Fish Hatchery Aerial Image.

Various artesian springs and a small creek impoundment supply water to the hatchery via gravity flow. Located at the east end of the hatchery property, these springs supply water to the upper portion of the station, including the hatchery building. The main supply of water for the lower portion of the station is Dickerman Pond. In general, water temperatures in the upper series are consistently between 45°F and 49°F, while temperatures in the lower series are much more variable, between 36°F and 59°F. No flow meter exists for the measurement of hatchery water supply flow rates. It is estimated that the hatchery utilizes a flow rate of approximately 600 to 1,800 gpm, with an average flow of 1,200 gpm.

The hatchery building contains 160 Heath vertical incubation trays and 28 concrete rearing tanks. The Heath trays are divided into stacks of eight. The 14 upper tanks are 15' x 2.75' x 1.75' and flow serially into the 14 lower tanks, which measure 12' x $2.75' \times 1.6'$.

The hatchery maintains 60 concrete rectangular raceways (Series A, B, and C) and 15 circular tanks. Series A consists of 27 raceways, but they are not currently used for rearing fish due to their poor structural condition. Series B contains 13 concrete raceways (8' x 63' x 2'). The peak water flow to Series B is approximately 400 gpm that flows serially through the raceways and reaches a maximum water temperature of $58^{\circ}F$. Series C consists of 20 raceways (5' x 100' x 1.5') and 15 circular tanks (25' x 1.3'). Water flow is serially reused throughout the concrete raceways. All rearing units for New Hampton SFH are summarized in Table 2-4.

| Rearing Unit | Quantity | Unit Volume (ft ³) ¹ | Total Volume (ft ³) ¹ |
|---------------------------|----------|--|---|
| Indoor Facility | | | |
| Heath Incubation Trays | 160 | 1 | 160 |
| 12' Rearing Tanks | 14 | 63 | 885 |
| 15' Rearing Tanks | 14 | 90 | 1,260 |
| Subtotal | | | 2,145 |
| Outdoor Facility | | | |
| A-2 Raceways | 14 | 412 | 5,768 |
| A-3 Raceways | 5 | 600 | 3,000 |
| A-5 Raceways | 8 | 752 | 6,016 |
| B Raceways | 13 | 600 | 7,800 |
| C Raceways | 20 | 735 | 14,700 |
| 25' Circular Tanks | 15 | 627 | 9,405 |
| Subtotal | | | 46,689 |
| Total | | | 48,834 |

Table 2-4: New Hampton Rearing Unit Summary

1) Unit Volume and Total Volume will vary based on operating depths.

2.4 Milford State Fish Hatchery

Milford State Fish Hatchery (SFH) is in the Town of Milford on the northwest edge of Hillsborough County, New Hampshire (Figure 2-5). The hatchery resides on approximately 165 acres of stateowned land and consists of sixty (60) 25' diameter circular tanks, earthen ponds, a hatchery building, support buildings, and production water supply wells. The facility manages the following phases of rearing: egg incubation, early rearing, and final grow out.

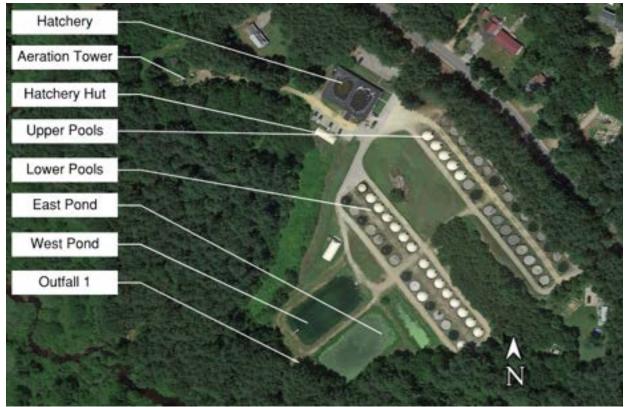


Figure 2-5: Milford State Fish Hatchery Aerial Image.

Water is supplied to the hatchery via two production wells, which are located southwest of the hatchery. A total of five production wells have been installed and used over the years; however, only two of the wells (Field and River) are currently in operation. The remaining have been discontinued due to iron and manganese problems. For aeration and degassing, water from the two wells is piped independently to a pair of towers acting as packed columns atop elevated head tanks with overflow standpipes inside. The towers were built in 2011 for a combined typical flow of 1,325 gpm and maximum of 1,700 gpm. The River Well provides up to 1,150 gpm, and the Field Well provides approximately 550 gpm. River Well water historically was high in manganese and moderately high in iron, which would foul the column packing. The well is now throttled in the well vault resulting in a reduction in manganese, but unfortunately, the manganese is not low enough to be considered non-influential. Field Well water appears to be higher in iron due to the column packing getting orange faster. Because of the minerals, both packed columns should be cleaned every one to two years. Historically, this only occurs as often as funding allows. When the well pumps are restarted after having been off for a time, such as for well cleaning, the piping is flushed to deter surging depositional material from the wells or their force-mains into the columns.

There is currently no flow meter installed at Milford SFH, and a weir system is currently used to collect flow data for NPDES reporting. A new flow meter was purchased in 2022, but the design of the West Pond discharge pipe complicates installation and requires engineering. According to 2021 data, peak flow rates vary from 1,000 to 1,400 gpm, although no data were available during some months.

The hatchery building contains 128 Heath vertical incubation trays, 4 circular tanks, and 20 concrete rectangular rearing tanks. There is an outdoor nursery building with 12 circular tanks, which has been abandoned due to corrosion of the galvanized tanks. The Heath trays are divided into stacks of eight, and the average flow rate per tray is 5 gpm. The 12 circular tanks are 8' in diameter and are operated at depths between 2-2.5'. The average water flow per circular tank varies from 1 to 6 gpm with a maximum rate of 20 gpm. The 20 concrete rearing tanks measure 26' x 2.2' x 2.4' but are typically operated at depths of 1.7'. Water flow per concrete tank varies from 18 to 20 gpm.

The hatchery maintains sixty (60) 25' diameter circular tanks that typically operate at 1.5' water depth. The units are divided into an upper and lower area, with 30 units in each area. Maximum flow to the circular units is 50 to 60 gpm. These circular tanks are operated at two-thirds the recommended flow rate of one exchange per hour, or 82 gpm. A West Pond and East Pond are located below the 25' circular tanks. Both ponds were originally installed as waste settling ponds, but the West Pond is now utilized for rearing space. All rearing units for Milford SFH are summarized in Table 2-5.

| Rearing Unit | Quantity | Unit Volume (ft³) | Total Volume (ft³) | |
|--------------------------------|----------|----------------------|-----------------------|--|
| Indoor Facility | | | | |
| Heath Incubation Trays | 128 | 1 | 128 | |
| 6' Circular Tanks | 4 | 56 | 224 | |
| Raceways | 20 | 95 | 1,900 | |
| Outdoor Nursery (Abandoned) | 12 | 100 | 1,200 | |
| Subtotal | | | 3,452 | |
| Outdoor Facility | | | | |
| 25' Circular Tank | 60 | 736.3 | 44,178 | |
| West Pond | 1 | 61,800 | 61,800 | |
| Subtotal | | | 105,978 | |
| Total | | | 109,430 | |

Table 2-5: Milford Rearing Unit Summary

1) Unit Volume and Total Volume will vary based on operating depths.

2.5 Twin Mountain State Fish Hatchery

Twin Mountain State Fish Hatchery (SFH) is located about a mile north of Twin Mountain in the Town of Carroll, along Route 3 in Coos County, New Hampshire (Figure 2-6). The hatchery resides on approximately 28 acres of state-owned land and consists of 22 outdoor rectangular concrete raceways, three covered broodstock circular tanks, a brood house, a hatchery building with 11 concrete raceways, and Heath egg incubators. The facility manages the following phases of rearing: egg incubation, early rearing, and final grow out. The program is accomplished utilizing two primary areas that include an indoor hatchery building and outdoor concrete raceways.



Figure 2-6: Twin Mountain State Fish Hatchery Aerial Image.

Production water for Twin Mountain SFH is provided by several springs. The springs are located on the west side of Route 3 in three separate clusters of artesian well points. A 6" diameter production well yields about 300 gpm and directly influences the flow from the springs. Another spring located near the brood house yields 45 gpm that is used in the broodstock holding tanks.

In total, the well and springs yield about 820 gpm. The temperature of the spring and production well waters vary from 42°F to 52°F.

The hatchery building contains Heath vertical incubation trays and 11 concrete rectangular rearing raceways. Five of the raceways measure $33' \times 2.7' \times 1.25'$ at operating depth and average a flow of 6 to 20 gpm, with a maximum flow of 60 gpm. The other six raceways measure $33' \times 2.75' \times 1.25'$ at operating depth and average a flow of 6 to 20 gpm, with a maximum flow of 60 gpm.

The hatchery has 22 outdoor concrete raceways that are split into Series A and Series B. Series A, which consists of 12 raceways, is no longer in use due to the failing condition of the concrete. The 10 raceways in Series B each measure 50' x 10' x 1.75' at operating depth, with an average flow of 280 to 480 gpm. Series B operates under a 10-pass serial reuse system. All rearing units for Twin Mountain SFH are summarized in Table 2-6.

| Rearing Unit | Quantity Unit Volume (ft ³) ¹ | | Total Volume (ft³) ¹ |
|----------------------|--|-----------|------------------------------------|
| Indoor Facility | | | |
| Raceways 1-11 | 11 | 110 | 1,210 |
| Subtotal | | | 1,210 |
| Outdoor Facility | | | |
| Series A Raceways | 12 | Abandoned | Abandoned |
| Series B Raceways | 10 | 875 | 8,750 |
| Subtotal | | | 8,750 |
| Total | | | 9,960 |

Table 2-6: Twin Mountain Rearing Unit Summary

1) Unit Volume and Total Volume will vary based on operating depths.

2.6 Warren State Fish Hatchery

Warren State Fish Hatchery (SFH) is in the Town of Warren about a mile to the south of the center of town along Old Route 25 in Grafton County, New Hampshire (Figure 2-7). The hatchery resides on approximately 134 acres of state-owned land and consists of 13 rearing units, display ponds, and a hatchery building with five concrete rectangular raceways and 80 Heath vertical tray egg incubators. The facility manages the early rearing and final grow out. The hatchery building is no longer utilized due to past flooding events and resulting unresolved mold issues.



Figure 2-7: Warren State Fish Hatchery Aerial Image.

Supply water for Warren SFH is provided by several springs and three production wells. The springs are free flowing (artesian) and produce between 200 gpm and 400 gpm. Wells 1, 2, and 3 produce up to 100, 200, and 500 gpm respectively. The temperature of production wells varies from 38°F to 60°F.

The hatchery building contains 6 concrete raceways and 80 Heath vertical incubation trays. The Heath trays average a total flow of 150 gpm. Four of the concrete raceways measure 15' x 3' x 1.5' at operating depth, and the other two measure 25' x 3' x 1.5' at operating depth.

The hatchery maintains 13 outdoor raceways, which are mostly concrete, and a few earthen ponds that now have concrete bottoms. All operate under serial reuse. The raceways are divided into three blocks, and the dimensions of each raceway vary; volumes can be found below in Table

2-7. The average flow rate of the outdoor raceways is 325 gpm but can vary between 250 to 500 gpm. All rearing units for Warren SFH are summarized in Table 2-7.

| Rearing Unit | Quantity | Unit Volume (ft³) ¹ | Total Volume (ft³) ¹ | | | |
|---------------------------|----------|-----------------------------------|------------------------------------|--|--|--|
| Indoor Facility | | | | | | |
| Raceways 1-4 | 4 | 135 | 540 | | | |
| Raceways 5-6 | 2 | 112 | 224 | | | |
| Heath Incubation Trays | 80 | - | - | | | |
| Subtotal | | | 764 | | | |
| Outdoor Facility | | | | | | |
| Upper Reservoir (A) | 1 | 5,472 | 5,472 | | | |
| Middle Reservoir (B) | 1 | 2,325 | 2,325 | | | |
| Lower Reservoir (C) | 1 | 5,280 | 5,280 | | | |
| Above Bridge (D) | 1 | 2,787 | 2,787 | | | |
| Bridge (E) | 1 | 2,226 | 2,226 | | | |
| Below Bridge (F) | 1 | 2,112 | 2,112 | | | |
| No. 8 (G) | 1 | 2,944 | 2,944 | | | |
| Long (M) | 1 | 2,565 | 2,565 | | | |
| Spring (K) | 1 | 2,563 | 2,563 | | | |
| Round (L) | 1 | 2,226 | 2,226 | | | |
| First Little (H) | 1 | 1,400 | 1,400 | | | |
| Second Little (I) | 1 | 1,393 | 1,393 | | | |
| Rainbow (J) | 1 | 2,520 | 2,520 | | | |
| Subtotal | | | 35,813 | | | |
| Total | | | 36,577 | | | |

Table 2-7: Warren Rearing Unit Summary

1) Unit Volume and Total Volume refer to the volume available at operating depths.

3 Existing Stocking and Production Summary

The State of New Hampshire annually produces and stocks an average of 1.4 million fish weighing approximately 380,950 pounds (2016-2021 average). The goal for the statewide program is to stock fish between 8 and 10 inches, at a minimum. A maximum of 583 waterbodies receive fish produced by the State's six hatcheries. Four primary salmonid species are stocked in New Hampshire including Rainbow Trout, Brook Trout, Brown Trout, and Landlocked Atlantic Salmon. Landlocked Atlantic Salmon were formerly produced at Powder Mill, but because of the new TP limits, a portion of the salmon are now produced at the Nashua National Fish Hatchery through a cooperative agreement in addition to New Hampton. While Nashua is not a facility operated by NHFGD, the salmon numbers are included to reflect the overall program needs for the State. Table 3-1 shows the six-year annual average for total number and total pounds produced from 2016-2021. The table also displays the percentage of total pounds that each six-year facility average contributed to the entire system.

| | Rainbow Trout Brown Trout Brook Tro | | Trout | Landlocked Atlantic Salmon | | Facility Total | | | | | |
|------------------|-------------------------------------|---------|---------|-------------------------------|---------|----------------|--------|--------|-----------|---------|-----------------------|
| Facility | Number | Pounds | Number | Pounds | Number | Pounds | Number | Pounds | Number | Pounds | % of Total Lbs. |
| Powder Mill | 91,447 | 42,622 | 47,970 | 18,275 | 164,032 | 52,062 | 40,558 | 4,631 | 344,007 | 117,590 | 31 |
| Berlin | 87,536 | 27,910 | 46,925 | 17,070 | 157,572 | 29,185 | - | - | 292,033 | 74,165 | 20 |
| New Hampton | 37,132 | 19,040 | 177,045 | 12,745 | 204,583 | 39,596 | 6,049 | 742 | 424,809 | 72,123 | 19 |
| Milford | 54,118 | 28,741 | 33,204 | 15,925 | 70,953 | 23,442 | - | - | 158,275 | 68,108 | 18 |
| Warren | 18,303 | 7,421 | 11,098 | 4,146 | 135,094 | 11,520 | 2,200 | 598 | 166,695 | 23,685 | 6 |
| Twin Mountain | 34,858 | 11,467 | - | - | 22,254 | 9,371 | - | - | 57,112 | 20,838 | 5 |
| Nashua | - | - | - | - | - | - | 26,544 | 4,441 | 26,544 | 4,441 | 1 |
| Species Total | 323,394 | 137,201 | 316,242 | 68,161 | 754,488 | 165,176 | 75,351 | 10,412 | 1,469,475 | 380,950 | 100 |

 Table 3-1: Statewide Yearly Production Averages from NHFGD Hatcheries During 2016-2021.

¹ – The Nashua National Fish Hatchery is currently producing all Landlocked Atlantic Salmon for The State of New Hampshire but is not a NHFGD facility.

As seen in Table 3-1, production amounts vary among NHFGD hatcheries and can vary slightly year to year. Powder Mill SFH and Berlin SFH account for the highest production totals over a six-year period, producing over 117,000 and 74,000 pounds of fish, respectively. New Hampton SFH very closely follows Berlin's average pounds produced, with over 72,000 pounds of fish produced from 2016-2021. It should be noted that the difference in production between Berlin and New Hampton are negligible, and in some years reviewed, New Hampton's production exceeded Berlin's. Twin Mountain and Warren had the lowest production totals from 2016-2021, with slightly more than 44,500 pounds produced.

Stocking also varies between NHFGD hatcheries. Based on data from the 2016-2021 stocking season, a total of 583 bodies of water (BOW) are stocked by NHFGD staff (Table 3-2). Based on the six-year production totals, Powder Mill stocks the most BOW, followed by New Hampton, Milford, Berlin, Warren, and Twin Mountain, respectively. Despite having the second-highest production total, Berlin SFH only stocks the fourth most BOW (151). Fish stocked at Berlin in 2022 were predominately Brook Trout. Twin Mountain stocks the least number of BOWs, as well as the fewest number of Rainbow Trout, Brown Trout, and Brook Trout when compared to the other NHFGD hatcheries.

| Facility | Rainbow Trout | Brown Trout | Brook Trout | Landlocked Atlantic Salmon | Average BOW Stocked per Year |
|------------------------------------|---------------|-------------|-------------|----------------------------------|------------------------------------|
| Powder Mill | 65 | 34 | 150 | 9 | 258 |
| New Hampton | 4 | 2 | 27 | 2 | 34 |
| Milford | 3 | 3 | 15 | - | 20 |
| Berlin | 3 | 1 | 14 | - | 18 |
| Warren | 1 | 2 | 15 | 1 | 20 |
| Twin Mountain | 1 | - | 5 | - | 6 |
| Nashua ¹ | - | - | 2 | 7 | 9 |
| Average BOW Stocked per Year | 77 | 42 | 228 | 19 | 365 |

Table 3-2: Average Number of Waterbodies Stocked by Each NHFGD State Fish Hatchery from 2016-2021.

¹ – The Nashua National Fish Hatchery is producing Landlocked Atlantic Salmon for Powder Mill SFH

Table 3-3 shows the total BOW stocked for each hatchery location, as well as the total number of square miles that each hatchery covers. In addition to stocking the largest number of BOW, Powder Mill also covers the largest area at 5,972 square miles which is indicative of the activity for the hatchery. Milford SFH covers more square miles than New Hampton SFH, despite New Hampton stocking a larger number of BOW. Twin Mountain covers the smallest area.

Travel distances are farthest from Powder Mill SFH and Berlin SFH to their respective stocking points, with Powder Mill SFH having two stocking locations that are between three and three and a half hours roundtrip and Berlin SFH having one stocking location that is approximately four hours round trip. All other stocking locations are within two hours or less of their respective hatcheries. The travel distances from each NHFGD hatchery and their respective stocking points were found to be within acceptable timeframes with the types of trucks and oxygen supplementation utilized by NHFGD staff. Figure 3-1 shows the NHFGD hatcheries, their stocking locations throughout the state, and is color coded based on the hatchery that stocks the water body.

| Facility | Areas Stocked/Covered (sq. miles) |
|-----------------------|-----------------------------------|
| Powder Mill | 5,972 |
| Milford | 3,338 |
| New Hampton | 3,295 |
| Berlin | 2,903 |
| Warren | 959 |
| Twin Mountain | 529 |
| Nashua ^{1,2} | See Powder Mill |
| Total | 16,996 |

Table 3-3: Size of Areas Stocked by Each NHFGD State Fish Hatchery.

¹ – The Nashua National Fish Hatchery is producing Landlocked Atlantic Salmon for Powder Mill SFH

² - The Nashua trips were completed by Powder Mill and are within the total area covered by Powder Mill

While the six-year average of production across all NHFGD facilities is just below 381,000 pounds, the peak production across all hatcheries during this same period is approximately 470,500 pounds. Nevertheless, the maximum carrying capacity of the NHFGD system is roughly 773,000 pounds. Powder Mill SFH produces the most fish out of the six state hatcheries, with Berlin SFH being capable of the second-most production and Twin Mountain being capable of the least production. While these facilities have the capacity to produce more than the current production amounts by way of rearing volume, the facilities are limited primarily by flow rate, as well as hatchery effluent.

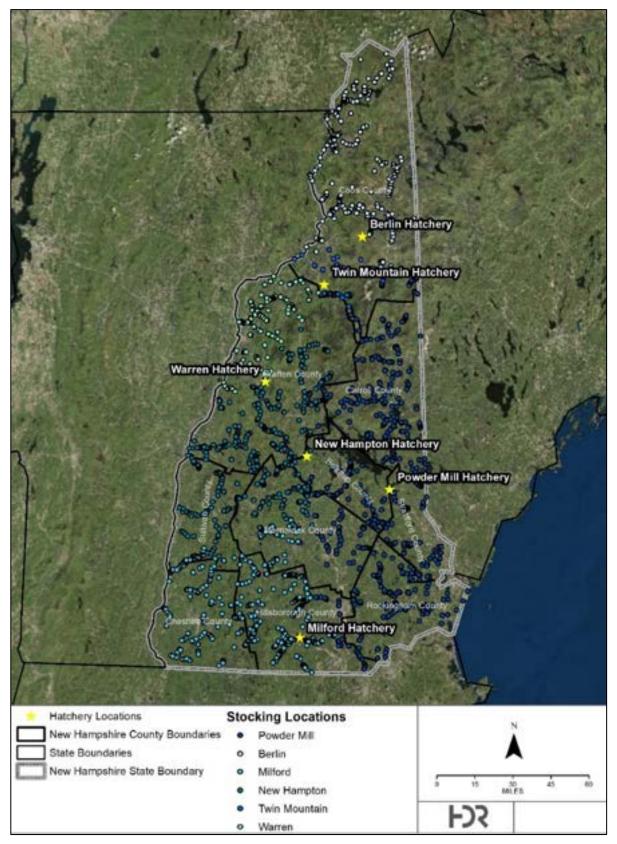


Figure 3-1: New Hampshire Stocking Locations.

3.1 Broodstock, Egg Transfers, and Fish Transfers

The NHFGD hatcheries do not operate independently but rather as a single system, with fish and resources shared between the facilities at key points throughout the year. Providing quality eggs in sufficient quantity to support the NHFGD program is vital for hatchery managers to produce a consistent product in time for stocking waterbodies in New Hampshire with quality trout. Currently, NHFGD maintains broodstock for Brown Trout and Brook Trout but does not actively maintain broodstock for Rainbow Trout. Some light-controlled indoor spaces were available for broodstock spawning operations, but dedicated, biosecure broodstock facilities are not consistently provided at each broodstock location.

Rainbow Trout eggs are acquired from other states to support the program. The eggs available to New Hampshire are often poorer quality, surplus, or eggs that become available outside of ideal production timing. For these reasons, it is difficult for NHFGD staff to properly plan for Rainbow Trout production. In addition to unpredictable timing of the surplus eggs, the poor quality often leads to unpredictable, insufficient results and increased labor costs.

The facility-to-facility fish transfers are also a vital part of the system-wide operation. Fingerling fish may be moved between facilities to optimize rearing space or take advantage of water quality conditions that are more favorable for fish growth at one facility versus another. The interrelationship of the facilities is not reflected in the annual production totals but is tracked and accounted for within the records kept by NHFGD. In 2022, more than 530,000 fingerlings were transferred between the facilities to support the growout of trout. The transfers also allow growout to be conducted in closer proximity to BOWs that will be stocked by a specific hatchery. Most transfers are produced at New Hampton. Without these transfers to other facilities to maximize the rearing space, the State's program goals could not be met.

4 Existing Statewide Hatchery Drivers

There are four main drivers that determine the suitability of an existing site for expansion: permit compliance (with the current emphasis being TP), source water quality and availability, production and stocking goals, and geographic location. These drivers are further discussed in the following sections.

4.1 Permit Compliance (Total Phosphorus Emphasis)

The total phosphorus effluent limit imposed on Powder Mill State Fish Hatchery was the driving factor for this comprehensive study. These limits were given to Powder Mill because, since its last permit cycle, the receiving waters (several impoundments on the Merrymeeting River) have been listed on New Hampshire's 303(d) list as impaired due to cyanobacteria, which is fueled by excess phosphorus. The Berlin State Fish Hatchery will most likely face new TP effluent limits in its new NPDES permit which is currently in the process of renewal. Berlin SFH's outfall to York Pond is anticipated to receive limits low enough to require elimination of this outfall. This is because York Pond has also been classified, since the facility's last permit cycle, as an impaired water body on the State's Department of Environmental Services (NHDES) 303(d) list due to chlorophyll-a, total phosphorus, and cyanobacteria. Combining all the effluent outfalls and moving them to the West Branch of the Upper Ammonoosuc will likely allow for an increase in TP effluent limits above those required for York Pond, but that water body is classified as an Outstanding State Water Resource given its location in a national forest (NHDES). Given these two facilities are the largest fish producers in the system and these effluent limits cannot be reliably met without advanced effluent treatment systems that are too capital intensive to justify downstream of aging infrastructure, expansions must occur at locations within the state that are less environmentally sensitive to meet production and stocking goals statewide.

Table 4-1 summarizes the current receiving water body for each hatchery, along with the anticipated TP effluent limit likely required for that water body. Anticipated TP effluent limits were calculated and provided to New Hampshire Fish and Game Department (NHFGD) by New Hampshire Department of Environmental Services (NHDES) for use as guidance during this statewide study and evaluation. It is important to note that, currently, Powder Mill SFH is the only facility known to have a TP limit as low as 12 μ g/L. However, effluent limits could be modified for various reasons including increases in fish production, changes to discharge location, and water quality standards. Potential effluent limits associated with the characteristics of each receiving water body need to be considered so capital investments remain viable facilities long-term. As can be seen from this information, New Hampton SFH, Milford SFH, and Warren SFH are the three existing facilities that will likely have the greatest ability for expansion based solely on the effluent TP levels.

| Facility | Receiving Water(s) | Anticipated TP Limit | |
|---------------|-------------------------------------|----------------------|--|
| Powder Mill | Merrymeeting River | 12 µg/L | |
| Berlin | West Branch of the Upper Ammonoosuc | Unknown | |
| Now Hometon | Dickerman Brook | No Increases | |
| New Hampton | Pemigewasset River ¹ | 600 μg/L¹ | |
| NATION 1 | Purgatory Brook | No Increases | |
| Milford | Souhegan River ¹ | 140 μg/L¹ | |
| Twin Mountain | Carroll Stream | No Increases | |
| Warren | Patch Brook | No Increases | |
| | Baker River ¹ | 128 μg/L¹ | |

Table 4-1: Hatchery Discharge Receiving Body Summary

¹ – Not the current receiving water rather a nearby possible alternative.

Feeding the fish at each facility is the central mechanism for fish production in the state. The pounds of feed introduced to the system are consumed by the fish, and the result is an increase in fish biomass. Feeding and subsequent fish growth are the primary sources of generated waste parameters that leave each facility and enter the receiving waterbody. For this reason, the feeding levels, and the rate at which the fish consume the feed, are the primary points of discussion when summarizing hatchery impacts to receiving waterbodies. Table 4-2 shows the calculated annual feeding totals, mass loadings for total phosphorus, and mass loadings total suspended solids for each of the six NHFGD hatcheries.

| Facility | Annual Feed Fed (lbs.) | Peak Flow (gpm) ¹ | Annual Total Phosphorus (lbs.) | Annual Total Suspended Solids (lbs.) |
|---------------|---------------------------|---------------------------------|-----------------------------------|---|
| Powder Mill | 103,781 | 4,065 | 373.6 | 31,134.3 |
| Berlin | 63,480 | 2,838 | 228.5 | 19,044.0 |
| New Hampton | 25,272 | 4,363 | 91.0 | 7,581.6 |
| Milford | 67,011 | 1,400 | 241.2 | 20,103.3 |
| Warren | 19,944 | 1,224 | 71.8 | 5,983.2 |
| Twin Mountain | 18,413 | 650 | 66.3 | 5,523.9 |
| Total | 297,901 | 19,198 | 1,072.4 | 89,370.3 |

Table 4-2: Annual Statewide Effluent Totals from NHFGD Hatcheries (2021).

¹ – The peak rearing volume demands represent the highest demand month of the year; rearing volume requirements may be less than the peak during other times of the year.

The efficiency of converting dry fish food to wet biomass of fish is known as the feed conversion (FC) or feed conversion rate (FCR). A 1:1 ratio would mean that, for each pound of food fed, the fish gained one pound. The measure is used to determine feeding efficiency and to limit overfeeding of the fish that would result in wasted food and increased effluent TP concentrations. The amount of feed administered at each facility is determined by the size of the fish and by

utilizing feed tables provided by fish food manufacturers. The feeding rates can also be calculated utilizing fish culture standards.

Each hatchery in the system measures the feed conversion ratios and adjusts the feeding levels accordingly. The ratios observed in the NHFGD system were within the expected levels for fish being fed by manufacturers' recommended feeding levels, meaning that the hatchery managers are following the guidelines provided by the feed manufactures and not overfeeding by their tables. It was noted at some facilities, however, that fish growth rates were faster than expected, meaning the consumption of food was generating fish biomass ahead of schedule. For these instances, the hatchery managers have adjusted feeding levels below manufacturers' tables to avoid overfeeding.

As expected, based on the production totals in Table 3-1, Powder Mill SFH has the highest pounds of feed fed per year, highest annual TP loads, and highest annual total suspended solids loads. It should be noted that the annual TP pounds produced at Powder Mill SFH is higher than the proposed effluent limit for the facility (227 pounds annually), based on current production levels and with no treatment.

When concentration-based limits are discussed, the peak flows are important to determine the anticipated effluent concentrations in mg/L. Low-flow facilities or low-flow times of the year will generally result in higher effluent concentrations. For these reasons, the peak and low-flow periods at the point of discharge are important to review.

4.2 Source Water Quality and Availability

Another driver affecting each hatchery is source water quality and availability. The maximum allowable loading that can be realized at each hatchery depends on many factors; the most important ones are:

- Species and weight of fish.
- Target size for the produced fish.
- Source water quality characteristics including dissolved oxygen, temperature, pH, alkalinity, and other contaminates like iron and manganese.
- Tolerance towards metabolic waste product build-up in the rearing water. Ammonia nitrogen, carbon dioxide, and particulate and dissolved solids are of special importance.

In general, source water availability is the primary factor limiting carrying capacity at each facility in New Hampshire. Additional considerations impacting the actual carrying capacity include the degree of water reuse within each system, day-to-day operations, volume of rearing space, water quality, dissolved oxygen levels, and the knowledge of the hatchery manager. Nonetheless, general carrying capacity of the system can be determined by the available flow rate at each facility.

The NHFGD hatchery managers match the loading rates and carrying capacity to the available source water flows. This is standard practice for well-managed systems. However, as a system,

significant reuse of water without treatment reduces the overall carrying capacity at each facility. Water is used by the fish and then serially reused multiple times at all facilities in the NHFGD system. With each reuse of water without treatment, the water quality degrades, and fish stress increases. To manage for the poorer water quality, most NHFGD facilities operate lower carrying capacities to account for the lack of sufficient water quality and flow.

Table 4-3 demonstrates the approximate carrying capacity of each facility based on density. The table assumes that all listed rearing volumes at each facility are available and does not account for the condition of the rearing units. Peak values represent the highest demand month of the year based simply on total pounds of all fish. Hatcheries may experience lower values than the peak throughout the year as fish are growing to target size. The table was generated to show the theoretical carrying capacity based strictly on the available infrastructure within the existing system. A density of 1.9 lbs/ft³ for a 9.5" fish (density index of 0.2) was assumed for all facilities. This density was observed during the site visits and discussed with hatcheries. While the value can vary depending on the phase of rearing and between hatcheries, the generalized number provides an appropriate base.

As outlined by Westers (2001), non-salmonids in conservation-based hatcheries like the NHFGD system operate between 1.8 lbs/ft³ and 5 lbs/ft³, putting the NHFGD system on the lower end of the density spectrum. The density-only method provides a maximum ceiling for production and does not consider space requirements to house multiple species simultaneously and water quality factors such as dissolved oxygen and ammonia toxicity. It does provide a benchmark for production capacity based on available infrastructure.

| Facility | Peak Production Level (Ibs.) from 2016-2021 | Peak Flow (gpm) | Peak Carrying Capacity (lbs.) |
|---------------|---|-----------------|----------------------------------|
| Powder Mill | 146,802 | 4,065 | 325,889 |
| Berlin | 89,648 | 2,838 | 176,286 |
| New Hampton | 91,928 | 4,363 | 106,920 |
| Milford | 89,891 | 1,400 | 83,880 |
| Warren | 27,877 | 1,224 | 63,166 |
| Twin Mountain | 24,408 | 650 | 16,620 |
| Total | 470,554 | | 772,761 |

Table 4-3: Carrying Capacities for Each Facility Using the Density-Based Models.

As demonstrated above, the production levels at most NHFGD facilities are below the densitybased carrying capacity, indicating the water quality and water reuse are the limiting factors. If more water flow or oxygen supplementation was available within the system, a higher-production poundage could be carried within the existing infrastructure. It should be noted that density-based carrying capacity does not account for other factors such as peak fish loading, ammonia, and dissolved oxygen levels. However, improvements to the current facilities would theoretically allow for an increase in production more aligned with the estimated maximum carrying capacities if sufficient water were available. In a system with good water quality, appropriate temperatures, good management, and adequate flow rates, densities of 3.0 lbs/ft³, 4.0 lbs/ft³, and even 5.0 lbs/ft³ can be achieved (Westers, 2001). Table 4-4 below includes existing water available and quality of the source water at each hatchery.

| Facility | Source Water | Min ¹ Flow (GPM) | Max ¹ Flow (GPM) | Source Water Quality |
|---------------|--------------------------------|-----------------------------------|-----------------------------------|---|
| Powder Mill | Merrymeeting Lake | - | 4,500 | Partially treated surface water with potential for ichthyophthirius multifiliis |
| Berlin | Cold Brook Diversion Dam | 400 | 1,400 | Untreated surface water with low seasonal flows |
| | Production Wells | 200 | 450 | Untreated TP impaired groundwater with declining production |
| | West Branch Diversion Dam | 500 | 2,838 | Untreated surface water with low seasonal flows |
| | Diversion Pond | 634 | 2,063 | Untreated surface water with low seasonal flows |
| New Hampton | Major Springs | 250 | 800 | Untreated spring water stored in uncovered pools |
| | Minor Springs | 100 | 200 | Untreated spring water stored in uncovered pools |
| | Dickerman Pond | - | 1,500 | Untreated surface water and the dam is in poor condition |
| Milford | Field Well | - | 550 | Aerated ground water with declining production and iron and manganese contamination |
| | River Well | - | 1,150 | Aerated ground water with declining production and iron and manganese contamination |
| Warren | Well 1 | 90 | 100 | Untreated ground water stored in uncovered aerated pools |
| | Well 2 | - | 200 | Untreated ground water stored in uncovered aerated pools |
| | Well 3 | - | 500 | Untreated ground water stored in uncovered pools |
| | Springs | 200 | 400 | Untreated spring water stored in uncovered pools |
| Twin Mountain | Springs and Production Well | - | 820 | Untreated spring/ground water stored in uncovered pools |

| Table 4-4: Hatcher | v Source Water | Availability | / and Qualit | v Summarv |
|---------------------|-------------------------|--------------|--------------|-------------------|
| Table I II Hateller | , o ouloo llutol | ,a | | , c annary |

¹ – Reliable flow measurement is not available at the facilities. These values represent best estimates based on permitted limits, historic operating records, and prior reports.

4.3 Production and Stocking Goals

Production and stocking goals are desired to be maintained in the future and not reduced because of effluent total phosphorus (TP) limitations or source water challenges. As such, the State of New Hampshire desires to continue the current annual production and stocking of an average of 1.4 million fish weighing approximately 380,950 pounds, with the goal to stock fish between 8 and 10 inches, minimum. Additional discussion on production and stocking goals is in Section 3.

4.4 Geographical Considerations

Geographical considerations with respect to the goals of NHFGD have two distinct impacts:

- 1. Travel time from hatchery to waterbody and the stress on the fish during that transit time.
- 2. Climate change and its impact on the water bodies in the state that can continue to support salmonid species in the long-term, particularly in the southernmost portion of the state.

4.4.1 Stocking Logistics

The State's current production and stocking practices are summarized in Section 3. Significant changes to the stocking practices are not currently desired. Table 4-5 below details the number of water bodies stocked, square miles covered by stocking, and the approximate time for the furthest stocking trip for each hatchery. When looking at alternatives for continuing to meet the State's existing production and stocking goals, it is important to consider ways of increasing stocking efficiency by producing fish closer to the BOW where they are stocked.

Table 4-5 and Figure 4-1 present the State's production and stocking data in a slightly different way from that presented in Section 3, breaking the state into three sections: Northern, Central, and Southern. While the boundaries of these three sections are arbitrary, this gives a more tangible understanding for what the production and stocking in each section would need to be to meet the State's existing goals. While it is not necessarily required that fish production match the stocking goals within these arbitrary boundaries, it provides an overview of what an ideal production and stocking scenario would look like.

| Hatchery | # BOW | Square Miles | Furthest Roundtrip |
|---------------|-------------|--------------|--------------------|
| Powder Mill | 326 (32.5%) | 5,972 (35%) | 3.5 hrs. North |
| New Hampton | 326 (32.5%) | 3,295 (19%) | 2.5 hrs. South |
| Milford | 183 (18.3%) | 3,338 (20%) | 2.5 hrs. South |
| Berlin | 151 (15.1%) | 2,903 (17%) | 4 hrs. North |
| Warren | 63 (6.3%) | 959 (6%) | 2 hrs. North |
| Twin Mountain | 26 (2.6%) | 529 (3%) | 2 hrs. East |
| Nashua | 17 (1.7%) | 2 (<1%) | NA |
| Total | 1,200 | 16,998 | |

Table 4-5: Hatchery Service Area Characteristics

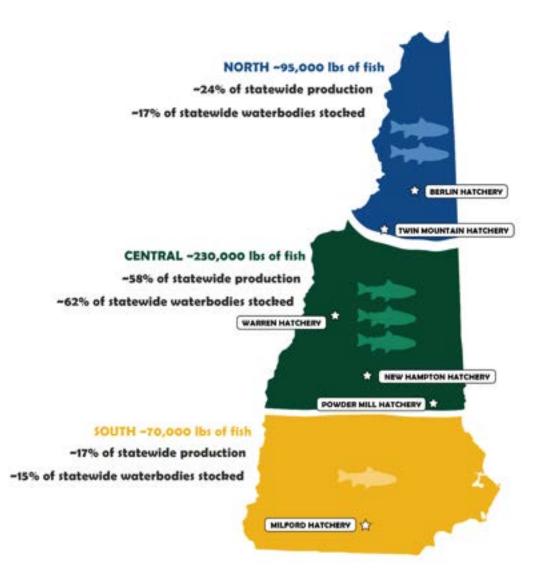


Figure 4-1: NHF&G Proposed Regional Production Map.

4.4.2 Climate Uncertainty

The primary impacts of climate uncertainty on hatchery operations and fisheries management involve impacts to water supplies that are critical for hatchery and fisheries management. Water flows, temperature, and quality can all be affected by a changing climate. These impacts occur through the following mechanisms:

- Warming surface waters and increased evaporation.
- Warming groundwater (shallow aquifers).
- Higher potential for thermal and wind impacts to hypolimnetic withdrawals from reservoirs.
- Increased rate of severe events like drought and flooding:
 - Direct flood impacts on hatcheries.
 - Indirect flood impacts due to reduced water quality if water sources receive sediment and other runoff.
 - Reduced recharge rates of groundwater aquifers due to higher rates of surface runoff during stronger storms (less infiltration opportunity for recharge).

While drought and flooding should be taken into consideration, the focus of this discussion is on warming surface and ground waters. Warming surface and ground water impact hatchery source water but can generally be corrected by adding additional raw water conditioning processes to the impacted hatchery. However, warming surface waters that serve as critical habitat for fisheries directly affect stocking suitability of impacted waters. Thus, as climate change worsens over time, adaption strategies will need to be incorporated into the State's production and stocking plan. These strategies should be considered when developing the statewide system alternatives to ensure capital investments made are able to provide the most benefit over the longest period. To do this, it is important to understand the continuum of temperature sensitivity among the most common salmonid species:

Lake Trout \rightarrow Brook Trout \rightarrow Rainbow Trout \rightarrow Landlocked Atlantic Salmon \rightarrow Brown Trout

It is important that hatchery managers consider these temperature sensitivities for both stocking and production plans. This means that species produced and stocked may need to be modified as the State experiences more impactful temperature effects on water resources. Thus, a progression of Brook – Rainbow – Brown Trout, in increasing order of tolerance to temperature and water quality declines over time should be anticipated. Figure 4-2 notes what this might look like based on dividing the state into three sections, as presented in Section 4.4.1. Other species for consideration include Atlantic Salmon (including landlocked subspecies) and hybrids such as tiger trout or splake. NHFGD has already implemented winter and early spring put and take fisheries in waters that may become marginal for coldwater species but where there is still angler demand for coldwater fisheries. NHFGD is now working toward removing the season end date to allow for longer angler opportunities.

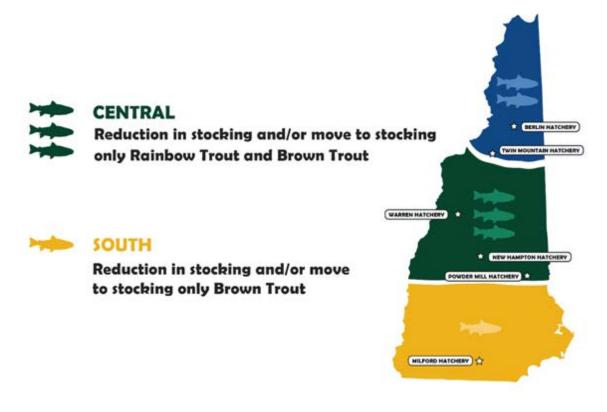


Figure 4-2: Proposed Species Stocking Regional Map

5 Hatchery Improvement and Repurposing Alternatives

As part of this overall study effort, condition assessments were undertaken at each hatchery to determine the general condition of existing infrastructure. Next, alternatives for improvements or modernization at each facility were determined, evaluation of the alternatives were performed, and recommendations were provided for the four largest hatcheries on an independent basis. At this point, enough information and understanding about the State's hatchery system as a whole was available to develop statewide alternatives that would reach the State's stocking and production goals within the constraints imposed by the drivers discussed in Section 4. The statewide alternatives then defined the alternatives that would be evaluated for the remaining two low-production hatcheries (Twin and Warren). A review of the alternatives evaluated for each hatchery is provided below. For more details regarding each of these alternatives, reference the associated modernization reports including:

- Hatchery Modernization Development and Effluent Treatment Alternatives Evaluation Powder Mill Fish Hatchery. HDR, 2023.
- Hatchery Modernization Development and Effluent Treatment Evaluation Berlin Fish Hatchery. HDR, 2023.
- Hatchery Modernization Evaluation New Hampton & Milford Fish Hatcheries. HDR, 2023.
- Hatchery Modernization Evaluation Twin & Warren Fish Hatcheries. HDR, 2023.

5.1 Powder Mill

With the primary driver of this study focused on effluent treatment for phosphorus reduction, the costs of treating the effluent to meet the extremely low permit limits is the primary consideration. Two effluent treatment alternatives were evaluated and discussed in *Hatchery Modernization Development and Effluent Treatment Alternatives Evaluation Powder Mill Fish Hatchery* (HDR, 2023) and include Alternatives A (membrane filtration with chemical dosing) and B (membrane filtration with adsorption). These effluent treatment alternatives were found to have a cost difference of less than 10 percent, with both alternatives being able to achieve compliance limits. Given the effluent treatment evaluation shows only a small difference between the two treatment alternatives, the following discussion focuses on the hatchery infrastructure alternative evaluations.

Three main alternatives were considered, along with a separate repurposing alternative:

- Alternative 1: Reuse existing rearing units with aquaculture upgrades and advanced effluent treatment (reuse existing hatchery infrastructure).
- Alternative 2: New circular rearing tanks with 75% recirculation and advanced effluent treatment (75% partial recirculation).
- Alternative 3: New circular rearing tanks with 95% recirculation and advanced effluent treatment (95% recirculation).
- Repurposing Alternative: Re-purposed approach to meeting statewide production and stocking goals (Limit production to up to 30,000 lbs annually to remain in permit compliance).

Based on the results of the evaluation performed in *Hatchery Modernization Development and Effluent Treatment Alternatives Evaluation Powder Mill Fish Hatchery* (HDR, 2023) Alternative 2 will not be considered moving forward. The goal for Powder Mill is to maintain a level of production that does not cause an exceedance of effluent permit limits, but also to consider alternatives for repurposing the hatchery to provide other critical functions for the state-wide production system. Upon careful consideration, the alternative best suited for Powder Mill is use for limited production for up to 30,000 pounds annually dependent upon remaining within permit compliance. Each of the viable alternatives are summarized and discussed in the sections below.

5.1.1 Alternative 1 – Reuse Existing Facility Infrastructure

Alternative 1 includes a new 3,750 gpm (5.4 MGD) effluent treatment plant to service the existing hatchery with minimal upgrades to the fish rearing systems. This alternative has the lowest capital cost. However, 85 percent of the investment (roughly \$30 million) is directly associated with effluent treatment requirements, and about 7 percent of the investment (roughly \$2.5 million) is directly associated with rearing improvements. The remaining 8 percent of costs are largely attributed to site work/improvements. This alternative does not modernize the existing conditions of the hatchery and only provides minor upgrades to sustain failing infrastructure. As is discussed in *Existing Conditions and Facility Evaluations Powder Mill Fish Hatchery Feasibility Study* (HDR, 2022), there are many deficiencies at the existing facility due primarily to the age of the

infrastructure and the outdated fish culture technology in use. Most deficiencies pertain to aging buildings and fish rearing infrastructure that does not permit the staff to operate efficiently. Additional investment will be required to extend the useful life of the hatchery in addition to making investments in effluent treatment technology.

Due to its age, many "modern retrofits" to the rearing facilities are likely not feasible due to structural integrity and hydraulic grade concerns. Additionally, this alternative has the highest O&M cost of the alternatives evaluated. For comparison, the required effluent treatment plant would be similar in capacity to Portsmouth's Pierce Island Wastewater Treatment Facility (3,333 gpm or 4.8 MGD, as reported on their website). While designed average flows would be similar, the wastewater characteristics and limits at a Powder Mill facility would necessitate a different design than Pierce Island. NHFGD is not currently equipped to own and operate a treatment plant of the size and complexity required. While this alternative meets the effluent limits and fish production goals on paper, the decision to make a large investment in effluent treatment downstream of a facility at the end of its useful life is not justifiable.

5.1.2 Alternative 2 – 75% Partial Recirculation

Alternative 2 was not considered for further evaluation because it has much higher costs. This alternative included very similar rearing infrastructure upgrades to alternative 3 and very similar effluent treatment infrastructure as alternative 1. In effect, this alternative includes the most expensive rearing upgrades paired with the most expensive effluent treatment upgrades to raise the same number of fish. While partially recirculating aquaculture systems (PRAS) are a viable fish rearing method, it does not make sense for this application.

5.1.3 Alternative 3 – 95% Recirculation

Alternative 3 includes a new 95% Recirculating Aquaculture System (RAS) hatchery building, as well as a new 693 gpm (1.0 MGD) effluent treatment plant. Alternative 3 has the highest capital cost with about 25 percent of the investment (roughly \$14 million) being directly associated with the effluent treatment plant and 60 percent of the investment (roughly \$34 million) being associated with the new rearing facilities. The remaining 15 percent of costs are largely attributed to site work/improvements. This alternative replaces the existing hatchery rearing units and aims to provide improved flexibility within current production levels. The alternative also has the ability to slightly increase production levels over the current average production. The key concept is utilizing recirculation technology to raise fish in less first-use water from the lake, which in turn generates less effluent to be treated. The new rearing facilities would be within a single enclosed and biosecure building, occupying a fraction of the currently utilized footprint. Since this alternative has a low water demand from Merrymeeting Lake (693 gpm) and compact site layout, the new hatchery does not need to be built on the currently developed site and could be built on undisturbed land. This alternative still requires advanced effluent treatment, albeit a much smaller treatment plant would be required in comparison to alternative 1. The staffing and operation of the treatment facility would still be a significant challenge for the NHFGD. While this alternative also meets the effluent limits and fish production goals on paper, the decision to make such a large investment to save this facility should be considered against siting a new facility at a new location not as susceptible to strict effluent requirements.

5.1.4 Alternative Comparisons of Capital, O&M, and 20-Year NPV Costs

A comparison of the capital, O&M, and 20-year net present value (NPV) costs for each alternative is shown in Table 5-1. For the purposes of this report, each hatchery infrastructure alternative is presented with the membrane filtration with adsorption alternative for effluent treatment. As discussed above, the cost differences between the effluent treatment alternatives were under 10 percent, and each alternative scales in the same fashion with respect to flow. These opinions were prepared to a variation of the standards of the Association for the Advancement of Cost Engineering (AACE) International Class 4 estimate, which outlines an added construction contingency of 50 percent for conceptual-level studies of this nature. The contingency was applied as an escalation at the individual line-item level in lieu of adding contingencies at the construction cost level, and the associated construction fees are assumed to be included in the escalation.

| Alternative | Capital Cost | O&M Cost | 20-Year NPV |
|---------------|---------------|--------------|----------------|
| Alternative 1 | \$ 43,388,000 | \$ 2,631,000 | \$ 100,092,000 |
| Alternative 2 | \$ 78,284,000 | \$ 3,288,000 | \$ 147,073,000 |
| Alternative 3 | \$ 60,406,000 | \$ 2,114,000 | \$ 103,600,000 |

Table 5-1: Comparative Capital, O&M, and 20-Year NPV Costs

5.1.5 Repurposing – Limited Production

Alternatives exist for Powder Mill to contribute to the overall NHFGD fish production program if the costs for other alternatives are deemed too high for the return on investment. That repurposed role is providing a reduced level of production. Reducing the level of production by up to 75% of the current levels would still allow for much needed production to occur but at a level low enough to achieve permit compliance.

As stated previously, Powder Mill provides the largest amount of fish for NHFGD's public stocking program in addition to stocking the most bodies of water, so the loss of production from this facility has the largest impact to the fishing public. Without compensation for the lost production, a significant reduction of stocked fish state-wide would occur. Two potential locations to replace some of this lost production are New Hampton and Milford. New water sources and discharge points would need to be analyzed to confirm suitable conditions, but locations outside of the existing discharge points utilizing river water, which must be treated for incoming debris and pathogens via UV, potentially exist in these two locations. If considered for development, most available dollars could be expended on fish production facilities rather than effluent treatment facilities.

5.2 Berlin

Berlin State Fish Hatchery may also be facing tighter total phosphorus (TP) limits. Although the future limits are currently unknown, specific effluent TP limits to the West Branch of the Upper Ammonoosuc River and York Pond may be slightly higher or lower. Neither limit is expected to significantly impact the required treatment technologies. Thus, treatment alternatives studied for Berlin were also focused on effluent treatment. The costs of treating effluent to required permit

limits is the primary focus. Effluent treatment options for Berlin are the same as those developed for Powder Mill.

Two main alternatives were considered, along with a separate repurposing alternative:

- Alternative 1: Reuse existing rearing units with aquaculture upgrades and advanced effluent treatment (reuse existing hatchery infrastructure).
- Alternative 2: New circular rearing tanks with 95% recirculation and advanced effluent treatment (95% recirculation).
- Repurposing Alternative: Re-purposed approach to meeting statewide production and stocking goals (broodstock, egg take, and limited fingerling production facility only).

5.2.1 Alternative 1 – Reuse Existing Hatchery Infrastructure

Alternative 1 includes a new 3,570 gpm (5.1 MGD) effluent treatment plant to service the existing hatchery with minimal upgrades to the rearing systems. The Canal Raceways are abandoned due to their isolated location and minimal rearing capacity. Extending a collection system to convey their effluent to the treatment plant does not provide good value. Alternative 1 has the lowest capital cost, with 81 percent of the investment (roughly \$38 million) directly associated with the effluent treatment requirements and about 12 percent of the investment (roughly \$6 million) directly associated with rearing related improvements. The remaining 7 percent of costs are largely attributed to site work/improvements. This alternative does not modernize the existing rearing processes and only provides minor upgrades to sustain failing infrastructure. As is discussed in Existing Conditions and Facility Evaluation Berlin Fish Hatchery Feasibility Study (HDR, 2022), there are many deficiencies at the existing facility due primarily to the age of the infrastructure in place, lack of investment in maintenance, and the outdated fish culture technology in use. Most deficiencies pertain to aging buildings and fish rearing infrastructure that do not allow staff to operate efficiently. Additional investment associated with the deficiencies discussed will be required, in addition to the costs presented here to extend the hatchery's useful life.

Due to its age, many "modern retrofits" to the rearing facilities are likely not feasible due to structural integrity and hydraulic grade concerns. Additionally, this alternative has the highest O&M cost of the alternatives evaluated. For comparison and similar to Powder Mill, the required effluent treatment plant would be similar in capacity to Portsmouth's Pierce Island Wastewater Treatment Facility (3,333 gpm or 4.8 MGD, as reported on their website). While designed average flows would be similar, the wastewater characteristics and limits at a Berlin facility would necessitate a different design than Pierce Island. NHFGD is not currently equipped to own and operate a treatment plant of the size and complexity required. While this alternative meets the effluent limits and fish production goals on paper, the decision to make a large investment in effluent treatment downstream of a facility at the end of its useful life is not justifiable.

5.2.2 Alternative 2 – 95% Recirculation

Alternative 2 includes a new 95% RAS hatchery building as well as a new 693 gpm (1.0 MGD) effluent treatment plant. Alternative 2 has the highest capital cost, with 24 percent of the

investment (roughly \$14 million) directly associated with effluent treatment and 70 percent of the investment (roughly \$39 million) associated with the new rearing facilities. The remaining 5 percent of costs are largely attributed to site work/improvements. This alternative replaces the existing hatchery rearing units and aims to increase production capacity and provide improved flexibility. The key concept is utilizing recirculation technology to raise fish in less water, which in turn generates less effluent to be treated. For this application, a high rate of recirculation (95%) was chosen due to source water availability and to minimize the requirements for source water/effluent treatment systems. The new rearing facilities represent an expansion of production at Berlin and would be housed within a single enclosed and biosecure building occupying a fraction of the currently utilized footprint. Since this alternative has a low water demand from Cold Brook/New Wells (693 gpm) and compact site layout, the new hatchery does not need to be built on the currently developed site and could be built on undisturbed land. This alternative still requires advanced effluent treatment, albeit a much smaller treatment plant would be required in comparison to alternative 1. The staffing and operation of the treatment facility would still be a significant challenge for the NHFGD. While this alternative also meets the effluent limits and fish production goals on paper, the decision to make such a large investment to save this facility should be considered against siting a new facility at a new location not as susceptible to strict effluent requirements. Additionally, major investments in infrastructure more centrally located could benefit fish movement state-wide.

5.2.3 Alternative Comparisons of Capital, O&M, and 20-Year NPV Costs

A comparison of the capital, O&M, and 20-year net present value (NPV) costs for each alternative is shown in Table 5-2. These opinions were prepared to a variation of the standards of the Association for the Advancement of Cost Engineering (AACE) International Class 4 estimate, which outlines an added construction contingency of 50 percent for conceptual level studies of this nature. The contingency was applied as an escalation at the individual line-item level in lieu of adding contingencies at the construction cost level, and the associated construction fees are assumed to be included in the escalation.

| Alternative | Capital Cost | O&M Cost | 20-Year NPV |
|----------------------------|---------------|--------------|----------------|
| Alternative 1 | \$ 46,422,000 | \$ 3,232,000 | \$ 116,441,000 |
| Alternative 2 (130,000 lb) | \$ 56,224,000 | \$ 2,455,000 | \$ 107,416,000 |

5.2.4 Repurposing – Broodstock, Egg Take, and Limited Fingerling Production

In this alternative, the existing hatchery building remains in operation, and the facility serves as the primary Brook Trout (EBT) broodstock, egg take, and fingerling production location for the state, continuing part of its current function that is critical to the overall state-wide program. Fouryear classes of broodstock are maintained (EBT0, EBT1, EBT2, and EBT3) annually. The facility spawns fish and incubates Brook Trout eggs in a biosecure environment as its primary purpose. Two alternatives are possible under this scenario:

- 1. Eggs could be shipped to other facilities once they reach the eyed egg stage from Berlin.
- 2. Berlin could maintain broodstock, produce eggs, and also take fish to a fingerling stage of approximately two to three inches for transfer to other facilities for growout.

For alternative 1, the Young's Raceways and Foster's Raceways are maintained and utilized for the broodstock program year classes, along with the hatchery building. Existing raceway covers would be replaced to provide a biosecure area for broodstock. Enhancements to the facility could be made that include improving incoming water quality for better biosecurity. The end goal should be focused on making enhancements to provide the most biosecure broodstock facility possible within the budget available at Berlin. The remaining rearing infrastructure at Berlin is abandoned in place.

Assuming average fecundity levels for Brook Trout (400-600 per female) and acknowledging variability based on size of broodstock, the facility could nominally produce 600,000 Brook Trout eggs annually. Incubation and early rearing space would still require evaluation for suitability. Table 5-3 was developed to show the potential phosphorus loading from a broodstock operation. The numbers utilized do not reference a particular water supply and are provided only as a guideline to estimate potential impacts. This data shows that maintaining the Brook Trout broodstock program within proposed permit levels is feasible.

| Species | Number | Pounds | FPP | Fish Length | Space Required (cf) | Required Flow (gpm) | Temp (F) | %BW Feed | Feed per Day (Ibs.) | Total Phos (μg/L) |
|------------|--------|--------|------|----------------|---------------------------|---------------------------|-------------|-------------|---------------------------|-------------------------|
| EBT Year 3 | 1000 | 4,000 | 0.25 | 18 | 2,222 | 889 | 50 | 0.4% | 17 | |
| EBT Year 2 | 1,500 | 1,500 | 1.00 | 14 | 1,071 | 429 | 50 | 0.6% | 8 | |
| EBT Year 1 | 1,800 | 909 | 2.0 | 11 | 826 | 331 | 50 | 0.7% | 7 | |
| EBT Year 0 | 3,000 | 73 | 41.0 | 4 | 183 | 37 | 50 | 2.0% | 1 | |
| Total | 7,300 | 6,482 | | | 4,303 | 1,685 | | | 34 | 19.7 |

Table 5-3: Brook Trout Adult Space Example

For alternative 2, a modern hatchery building complete with broodstock, egg incubation, early rearing, and office spaces could be constructed to house the broodstock program for Brook Trout. If recirculation is utilized, this concept could even be expanded to include Rainbow Trout and Brown Trout. General concepts for a large broodstock building that can house Brook Trout, Rainbow Trout, and Brown Trout are provided in Appendix F for reference and future consideration.

This enhancement would modernize the office space, incubation capabilities, and provide space for early rearing facilities while still utilizing Young's and Foster's Raceways as needed within permit limits to stage fish or hold fingerling prior to transfer to other facilities. It may be possible that some production could still occur at Berlin, provided the phosphorus generated to maintain the four broodstock year classes and the fingerling production remains under the proposed limit or if an economical effluent treatment process can be added.

5.3 New Hampton

The New Hampton State Fish Hatchery provides the best current location for infrastructure expenditures and expansion of production out of the six facilities operated by the State. This position is based on site characteristics such as geographic location, water supplies, effluent discharge flexibility, likely total phosphorus (TP) effluent limits, and space available to accommodate a production increase. With the likely reductions in production at Powder Mill and Berlin due to new, low effluent phosphorus limits, additional rearing space within the state will be required to maintain statewide production levels.

Two main alternatives were considered:

- Alternative 1A: 95% recirculation.
- Alternative 1B: 95% recirculation and rehabilitate Series B and C.

5.3.1 Alternative 1A - 95% Recirculation

In this alternative, the existing hatchery infrastructure is abandoned in place, and new infrastructure is added that can more efficiently utilize the water supply available at New Hampton. A new incoming water treatment building, enclosed rearing building, and associated infrastructure for effluent treatment are constructed within the existing properties owned by NHFGD. The new facilities utilize recirculating aquaculture systems (RAS), which treat and reuse 95% of culture water. The recirculation systems reduce the required water supply demand and water supply treatment for pathogens compared to systems that do not treat and recirculate fish production water.

Flows were estimated based on fish rearing requirements and the initial layout of a modular type of facility. The initial layout provides for four independent RAS modules in the growout phase and two RAS modules for intermediate rearing. This layout has the potential to produce 130,000 pounds annually, which would be an increase over current production with a smaller overall water demand. The poundage outlined for New Hampton must also include the Brown Trout broodstock and Landlocked Atlantic Salmon program.

Dickerman Pond has been a reliable source of water throughout the historic operation of the facility. However, given that it is surface water, it is susceptible to diseases, contamination by debris, and temperature fluctuations, treatment is needed. It should be noted that water could be collected more efficiently within the A-Series and could bypass Dickerman Pond with appropriate design considerations. This could limit disease and temperature concerns. To be utilized as water supply for a new 95% recirculating aquaculture facility with or without Dickerman Pond bypass, filtration and UV disinfection are recommended. Well water is typically preferable for fish rearing if it is readily available in sufficient quantity and uncontaminated by heavy metals like iron and manganese. An investigation into production wells and groundwater quality is recommended as the preferred source water for any new facility to rule out the availability of a good groundwater source.

Alternative 1A provides the state with a facility renovation capable of increasing production over current levels, provided the use of RAS is implemented. The facilities can produce more fish with

similar levels of water with the use of water treatment equipment associated with the RAS and with the use of modern circular rearing units.

5.3.2 Alternative 1B - 95% Recirculation and Rehabilitate Series B and C

The lower area of New Hampton provides a logical area for NHFGD to invest and expand production. This area includes the existing B-Series and C-Series but also adjacent, undeveloped land. It is possible NHFGD could utilize some of the existing infrastructure in B-Series and C-Series to continue operations and produce fish in the 50,000 lbs to 70,000 lb range with an additional production in a new RAS facility (up to 150,000 to 200,000 lbs pending permit level determinations) These numbers would include maintaining the Brown Trout broodstock. When modernized rearing environments are provided through renovations and new construction, as outlined in this document, fish rearing densities can be increased over current densities maintained at the current configuration of New Hampton and infrastructure is available to produce up to half of the NHFGD required fish production goals with one major infrastructure investment location.

5.3.3 Alternative Comparisons of Capital, O&M, and 20-Year NPV Costs

A comparison of the capital, O&M, and 20-year NPV costs for each Alternative is shown in Table 5-4. These opinions were prepared to a variation of the standards of the Association for the Advancement of Cost Engineering (AACE) International Class 4 estimate, which outlines an added construction contingency of fifty percent (50%) for conceptual level studies of this nature. The contingency was applied as an escalation at the individual line-item level in lieu of adding contingencies at the construction cost level, and the associated construction fees are assumed to be included in the escalation.

| Alternative | Capital Cost | O&M Cost | 20-Year NPV |
|----------------|---------------|--------------|---------------|
| Alternative 1A | \$ 46,565,000 | \$ 1,428,000 | \$ 76,170,000 |
| Alternative 1B | \$ 49,861,000 | \$ 1,558,000 | \$ 78,409,000 |

Table 5-4: Comparative Capital, O&M, and 20-Year NPV Costs

5.4 Milford

The Milford State Fish Hatchery may also provide a good location for infrastructure expenditures but does have several limitations. This position is based on site characteristics such as geographic location, effluent discharge flexibility, likely total phosphorus (TP) effluent limits, and space available to accommodate a production increase. However, limitations include poor water quality. With the likely reductions in production at Powder Mill and Berlin due to new and tight phosphorus discharges, additional rearing space at Milford may be required to maintain historic production levels. A single alternative was considered: new circular rearing tanks with 95% recirculation.

5.4.1 Alternative 1 - 95% Recirculation

In this alternative, the existing hatchery infrastructure is abandoned in place, and new infrastructure is added that can more efficiently utilize the available water supply for Milford. A new incoming water treatment building, enclosed rearing building, and associated infrastructure for effluent treatment are constructed within the existing properties owned by NHFGD. The new facilities utilize recirculating aquaculture systems (RAS), which treat and reuse 95% of culture water. The recirculation systems reduce the required water supply demand and required water supply treatment for pathogens or metal concerns, such as iron at Milford.

Flows were estimated based on fish rearing requirements and the initial layout of a modular type of facility. The initial layout provides for four independent RAS modules in the growout phase and two RAS modules for intermediate rearing. This layout has the potential to produce 130,000 pounds or more annually, which would be an increase over current production with a smaller overall water demand. By carrying slightly higher rearing densities and adding additional rearing modules, the facility could support up to 200,000 lb of production within the proposed RAS concepts.

This alternative provides the State with facility renovations capable of increasing production over current levels, provided the use of RAS is implemented. The facilities can produce more fish with similar levels of water with the use of water treatment equipment associated with the RAS and with the use of modern circular rearing units.

5.4.2 Capital, O&M, and 20-Year NPV Costs

The capital, O&M, and 20-year net present value (NPV) costs for alternative 1 is shown in Table 5-5. These opinions were prepared to a variation of the standards of the Association for the Advancement of Cost Engineering (AACE) International Class 4 estimate, which outlines an added construction contingency of 50 percent for conceptual level studies of this nature. The contingency was applied as an escalation at the individual line-item level in lieu of adding contingencies at the construction cost level, and the associated construction fees are assumed to be included in the escalation.

| Alternative | Capital Cost | O&M Cost | 20-Year NPV |
|---------------|---------------|--------------|---------------|
| Alternative 1 | \$ 47,390,000 | \$ 1,591,000 | \$ 80,835,000 |

| Table 5-5: Comparative Capital, O&M | I, and 20-Year NPV Costs |
|-------------------------------------|--------------------------|
|-------------------------------------|--------------------------|

5.5 Twin Mountain

The available water volume and hatchery space at Twin Mountain State Fish Hatchery does not present an opportunity for major expansion. Maintaining the existing infrastructure at these facilities is the best way for these facilities to continue contributing to statewide goals and is the only alternative evaluated. The good water quality at Twin Mountain, as well as the existing infrastructure, does provide an opportunity to bring a Rainbow Trout broodstock back into New Hampshire. The existing production at Twin Mountain could be altered slightly to include

broodstock in place of some of the general production currently occurring. Currently, NHFGD is producing approximately 323,000 Rainbow Trout weighing approximately 137,200 lbs. An in-state broodstock program capable of producing the eggs to supply the program could be implemented at Twin Mountain, which has a water supply conducive to good Rainbow Trout production.

One alternative was considered for this facility, along with a separate repurposing alternative:

- Alternative 1: Infrastructure rehabilitation to include Rainbow Trout broodstock and egg take facility.
- Repurposing Alternative: New broodstock and egg take facility for Rainbow Trout.

5.5.1 Alternative 1 - Infrastructure Rehabilitation

In this alternative, the existing fish rearing units are left in place, and most of the facilities remain unchanged. Repairs to the existing concrete rearing units and selected buildings would be made to the extent possible to extend their useful lives. If a broodstock is maintained, a portion of the existing raceways must be changed from catchable production to broodstock production. This has an impact on the overall pounds produced for stocking but has a positive addition to the capabilities for maintain broodstock in state. The program will need to accommodate multiple year classes of Rainbow Trout broodstock, with Year 0, 1, 2, and 3 ages likely kept isolated from each other. Year 0 would be housed in the existing building, with years 1, 2, and 3 occupying outdoor space in the pools. The priority for the site would be housing broodstock with some additional space supporting catchable production, as available. Utilizing the existing units is not ideal from a biosecurity perspective, given the open nature of the system. Predation control strategies utilizing netting or tension fabric structures could be considered.

It would be worthwhile to seriously investigate reuse of the old broodstock building, which has been abandoned for over a decade due to a collapsed roof. Efforts to rehabilitate the building would include structural, electrical, and architectural assessments as well as re-establishment of the source water and effluent discharge, since it was not picked up in the drain line consolidation project and has not been included in NPDES permits since before 2012. If this infrastructure could be rehabilitated and put back into service, additional catchable production could be achieved.

5.5.2 Opinion of Probable Construction Cost

A conceptual Opinion of Probable Construction Cost (OPCC) was developed for alternative 1 of roughly \$2,300,000. Cost and quantities for equipment and repairs were developed based on information obtained from suppliers and historical reports. Costs for contingencies are included in the estimate for each individual process area, and cost of escalation to midpoint of construction and market volatility adjustment are included in subtotal cost of all process areas. There are no new ongoing O&M costs (chemical, electrical, labor, or replacement) associated with the proposed upgrades at either facility.

5.5.3 Repurposing Alternative - New Broodstock and Egg Take Facility

An ideal scenario for broodstock management would be the construction of a new dedicated broodstock building for Rainbow Trout. Unlike the general scenario for a centralized NHFGD

broodstock facility, the alternative for Twin Mountain would be a building and space dedicated exclusively to Rainbow Trout. An enclosed building would allow for predation control, light control, and would provide a more biosecure location for holding broodstock. The building could also be sized to house a small amount of backup broodstock for Brook Trout and Brown Trout, if desired, for safe keeping in the event of issues with Berlin or New Hampton brood. Existing areas of the hatchery could continue to be utilized for a limited amount of production to support the statewide goals in addition to the broodstock facility.

5.6 Warren

Warren State Fish Hatchery does not have adequate receiving waters to support expansion. With the discharge from this facility into a small brook with no allowable increases in TP discharges, the need to buy property in order to relocate the discharge to the Baker River, and the increase in flooding this facility experiences, maintaining the existing infrastructure at this facility is the best way to continue contributing to statewide goals. Thus, the only alternative evaluated is infrastructure rehabilitation.

5.6.1 Alternative 1 - Infrastructure Rehabilitation

In this alternative, the existing fish rearing units are left in place, and most of the facilities remain unchanged. Repairs to the existing rearing units and selected buildings would be made to the extent possible to extend their useful lives. Eventually, the hatchery building will be abandoned in place, as flooding will likely occur more often over time, making this building nearly impossible to utilize consistently.

5.6.2 Opinion of Probable Construction Cost

A conceptual Opinion of Probable Construction Cost (OPCC) was developed for the recommended repairs of roughly \$2,300,000. Cost and quantities for equipment and repairs were developed based on information obtained from suppliers and historical reports. Costs for contingencies are included in the estimate for each individual process area, and cost of escalation to midpoint of construction and market volatility adjustment are included in subtotal cost of all process area. There are no new ongoing O&M costs (chemical, electrical, labor, or replacement) associated with the proposed upgrades at either facility.

5.7 Overall Summary of Alternatives by Hatchery

To summarize the alternatives and their costs presented in the preceding sections by hatchery so comparisons can be made at a glance, see Table 5-6 below.

\$/pound (1)

\$ 42.41

| Capital Cost | NPV |
|---------------|----------------|
| \$ 43,388,000 | \$ 100,092,000 |

NPV

\$80,835,000

Capital Cost

\$47,390,000

Table 5-6: Summary of Hatcheries' Alternatives

Description

Reuse Existing Hatchery

Infrastructure

Description

95% Recirculation

Powder Mill

Alternative

Alternative 1

Milford

Alternative

Alternative

1A

| Alternative 2 | 75% Partial Recirculation | 130,000 | \$ 78,284,000 | \$ 147,073,000 | \$ 56.57 |
|-------------------|---|-----------------------------|-------------------|-------------------|-------------------|
| Alternative 3 | 95% Recirculation | 130,000 | \$ 60,406,000 | \$ 103,600,000 | \$ 39.85 |
| Repurpose | Broodstock and Egg Take Facility | 30,000 | Not Yet Costed | Not Yet Costed | Not Yet Costed |
| Berlin | | | | | |
| Alternative | Description | Production (pounds/year) | Capital Cost | NPV | \$/pound (1) |
| Alternative 1 | Reuse Existing Hatchery Infrastructure | 64,000 | \$ 46,422,000 | \$ 116,441,000 | \$ 95.44 |
| Alternative 2 | 95% Recirculation | 130,000 | \$ 56,224,000 | \$ 107,416,000 | \$ 41.31 |
| Repurpose | Broodstock, Egg Take, and Fingerling Production Facility | 16,000 | Not Yet Costed | Not Yet Costed | N/A |
| New Hampton | | | | | |
| Alternative | Description | Production (pounds/year) | Capital Cost | NPV | \$/pound (1) |
| Alternative 1A | 95% Recirculation | 130,000 | \$ 46,565,000 | \$ 76,170,000 | \$ 29.30 |
| Alternative 1B | 95% Recirculation and Rehabilitate Series B and C. | 202,000 | \$ 49,861,000 | \$ 78,409,000 | \$ 19.41 |

Production

130,000

(pounds/year)

Production (pounds/year)

118,000

\$/pound (1)

\$ 31.09

Table 5-6 (cont'ed)

| Twin Mountain | | | | | | |
|---------------|-------------------------------------|-----------------------------|-------------------|--|--|--|
| Alternative | Description | Production (pounds/year) | Capital Cost | | | |
| Alternative 1 | Infrastructure Rehabilitation | 21,000 | \$ 2,300,000 | | | |
| Alternative 2 | Broodstock and Egg Take Facility | Not Yet Estimated | Not Yet Costed | | | |
| Warren | Warren | | | | | |
| Alternative | Description | Production (pounds/year) | Capital Cost | | | |
| Alternative 1 | Infrastructure Rehabilitation | 24,000 | \$ 2,300,000 | | | |

(1) \$/pound calculated by dividing the 20-year NPV by 20 years of production.

6 Considerations for Future Investigation

There are several moving pieces regarding regulatory issues affecting these facilities, the time frame in which the chosen alternative will be implemented, and additional work that could be conducted to assist in finding potentially better, more cost-effective alternatives to reaching the State's production and stocking goals.

6.1 Addition of a Dilution Zone in Powder Mill's Permit

EPA has set the instream target for total phosphorus in Merrymeeting River at 12 μ g/L. Current practice at the hatchery is that almost all flow from the source water (Merrymeeting Lake) to the river is utilized by the hatchery to rear fish. Thus, there is no dilution factor that can be considered, making the effluent limits the same as the instream target.

Two of the proposed upstream hatchery modernization alternatives being considered are to implement a recirculating aquaculture system. This type of system would significantly reduce the flow rate required from the source water and thus the effluent discharge. The recirculated water used for fish rearing is conditioned before reuse by treating for solids and ammonia. In effect, the total source water flow through in the hatchery would reduce from 6 MGD to approximately 1 MGD. This opens an opportunity for the NPDES to be modified to allow for a minimum dilution factor of 2, where the hatchery effluent could be diluted with the lake water in a dilution zone before being discharged to the river. Thus, the instream target would be disconnected from the effluent limit and could allow for potential permit modification to increase the hatchery average monthly effluent limit up to 24 μ g/L. Consequently, the required TP removal would decrease from 90% to 70% in peak loadings summer months, eliminating the need for ion exchange or adsorption unit and reducing metal salt addition significantly. With such permit modification, more sustainable and cost-effective treatment solution would be possible.

6.2 Potential Additional Pilots

Many different filtration technologies are available on the market that can potentially be deployed in the hatchery for effluent treatment. These alternatives could not be tested in pilot scale due to the project time and budget constraints. However, a series of bench testing was designed to explore the feasibility of some alternate technologies to compare against the technologies piloted. Some of the technologies tested at bench scale showed promising results but did not reach the required effluent limits necessary at Powder Mill. However, it is anticipated that the performance of these technologies, specifically for filtration, might increase in a larger pilot application. Additionally, given there will be time between the issuance of Berlin's draft NPDES permit and the time in which new TP effluent limits become enforceable, a pilot of these potential technologies may be justified depending upon the TP limits imposed.

7 Paths to Achieve Statewide Production Goals

Based on the high cost of providing advanced effluent treatment at Powder Mill and Berlin, the state's two top production facilities, investments need to be made within the state's other hatcheries to maintain stocking goals and remain in permit compliance. Variables that drive the amount of production at any given site include water supply limits, water quality concerns, receiving stream TP assimilation capacity, and geographic considerations. Because all of the State's facilities have a fairly limited water supply, alternatives are inadequate without considering implementation of recirculating aquaculture systems.

In the development of the statewide alternatives, the goals desired to be achieved include:

- Total target production of 400,000 lbs annually statewide
- A mixture of existing infrastructure and new infrastructure
- The addition of dedicated infrastructure for broodstock

The statewide alternatives developed for evaluation can be briefly described as follows:

- Alternative 1 One Large Facility at New Hampton
- Alternative 2 One Large Facility at New Hampton with Rebuild at Milford
- Alternative 3 Two Large Facilities at New Hampton and Powder Mill
- Alternative 4 One Large Facility at New Hampton with New Northern Facility

These alternatives are shown in Table 7-1, and differ in the fish pounds produced at each facility. Each of these alternatives are described in more detail in the sections that follow. As can be seen, investment in New Hampton is a singular theme among all the alternatives evaluated given its availability of source water, ability to meet existing effluent discharge regulatory compliance, and proximity to a large receiving water body with more assimilative capacity for total phosphorus should it be required in the future. Conversely, Powder Mill's production is greatly reduced to maintain permit compliance focus while still providing much needed fish production at a limited scale. However, Alternative 3 presents the possibility of the construction of a new facility at Powder Mill in the future should it become a viable option.

| Hatchery | Existing | Alt 1 | Alt 2 | Alt 3 | Alt 4 |
|-----------------------|----------|---------|---------|---------|---------|
| Powder Mill | 124,097 | 30,000 | 30,000 | 150,000 | 30,000 |
| Berlin | 74,336 | 64,000 | 64,000 | 64,000 | 64,000 |
| New Hampton | 71,792 | 250,000 | 150,000 | 150,000 | 125,000 |
| Milford | 68,124 | 68,000 | 100,000 | 68,000 | 68,000 |
| Twin | 20,698 | 15,000 | 15,000 | 15,000 | 15,000 |
| Warren | 26,742 | 26,500 | 26,500 | 26,500 | 26,500 |
| New Northern Facility | | | | | 125,000 |
| Total | 385,789 | 453,500 | 385,500 | 473,500 | 453,500 |

 Table 7-1: Summary of Hatchery Production in each Statewide Alternative

The implementation of modifications to the hatcheries under each of these alternatives will inevitably occur in phases. For the phasing approach on all alternatives, it is expected that a reduction in production at Powder Mill is the first to take place. It is important to note that the timing of each phase will be based on a variety of factors including regulatory requirements and funding availability. Thus, no attempt has been made to define how long implementation of the entire alternative will take. Because of this, it is important to note the achievable level of production for each phase of an alternative and if it is below the statewide goals during construction any of the outlined phases is not included. With the current system near carrying capacity for pounds of fish, it's likely that some disruption of annual pounds produced will occur but will be temporary. Once all construction phases are complete, production goals should be met.

7.1 Alternative 1 – One Large Facility at New Hampton

Alternative 1 maximizes the amount of production at New Hampton to achieve statewide goals. This alternative includes the following modifications at each facility:

- Powder Mill Reduction in production to roughly 30,000 lbs to meet effluent TP limits.
- Berlin Slight reduction in production to 64,000 lbs, and operational changes to meet anticipated effluent TP limits.
- New Hampton New RAS facility to accommodate 150,000 lbs in production plus house brook and brown trout broodstock and Landlocked Atlantic Salmon rearing. In a future phase of improvements thein effluent discharge can be relocated to the Pemigewasset River to allow for a potential increase in production up to 250,000 lbs with minimal additional facility improvements.
- Milford Continue operation as is with continued investment in rehabilitation of existing infrastructure.
- Twin Mountain Slight reduction in production to focus on and invest in Rainbow Trout broodstock.
- Warren Continue operation as is with continued investment in rehabilitation of existing infrastructure.

This alternative brings the overall statewide production total to roughly 453,500 lbs. For the phasing approach on all alternatives, it is expected that a reduction in production at Powder Mill and Berlin are the first modifications to take place. For this alternative, phase 2 would likely be the construction and startup of a new RAS facility at New Hampton, and phase 3 is a shift to focus on broodstock at Twin along with moving the outfall at New Hampton to the Pemigewasset River to allow for increased production (see Table 7-2).

| | Existing | Phase 1 | Phase 2 | Phase 3 |
|-------------|----------|---------|---------|---------|
| Powder Mill | 124,097 | 30,000 | 30,000 | 30,000 |
| Belin | 74,336 | 64,000 | 64,000 | 64,000 |
| New Hampton | 71,792 | 71,500 | 150,000 | 250,000 |
| Milford | 68,124 | 68,000 | 68,000 | 68,000 |
| Twin | 20,698 | 20,500 | 20,500 | 15,000 |
| Warren | 26,742 | 26,500 | 26,500 | 26,500 |
| Total | 385,789 | 280,500 | 359,000 | 453,500 |

Table 7-2: Phases of Alternative 1 Production (lbs) by Facility

7.2 Alternative 2 – One Large Facility at New Hampton with Rebuild at Milford

Alternative 2 slightly reduces the amount of production at the new New Hampton RAS facility and invests in a rebuild of the Milford facility to achieve statewide goals. This alternative includes the following modifications at each facility:

- Powder Mill Reduction in production to roughly 30,000 lbs to meet effluent TP limits.
- Berlin Slightly reduction in production to 64,000 lbs and operational changes to meet anticipated effluent TP limits.
- New Hampton New RAS facility to accommodate 150,000 lbs in production plus house Brook Trout and Brown Trout broodstock and egg rearing of Landlocked Atlantic Salmon.
- Milford Rebuild of Milford including source water treatment to reach 100,000 lbs in production.
- Twin Mountain Slight reduction in production to focus on and invest in Rainbow Trout broodstock.
- Warren Continue operation as is with continued investment in rehabilitation of existing infrastructure.

This brings the overall statewide production total to roughly 385,500 lbs. For the phasing approach on all alternatives, it is expected that a reduction in production at Powder Mill and Berlin is the first to take place. For this alternative, phase 2 would likely be the construction and startup of a new RAS facility at New Hampton, and phase 3 is a shift to focus on broodstock at Twin along with the rebuild of Milford (see Table 7-3).

| | Existing | Phase 1 | Phase 2 | Phase 3 |
|-------------|----------|---------|---------|---------|
| Powder Mill | 124,097 | 30,000 | 30,000 | 30,000 |
| Belin | 74,336 | 64,000 | 64,000 | 64,000 |
| New Hampton | 71,792 | 71,500 | 150,000 | 150,000 |
| Milford | 68,124 | 68,000 | 68,000 | 100,000 |
| Twin | 20,698 | 20,500 | 20,500 | 15,000 |
| Warren | 26,742 | 26,500 | 26,500 | 26,500 |
| Total | 385,789 | 280,500 | 359,000 | 385,500 |

Table 7-3: Phases of Alternative 2 Production (lbs) by Facility

7.3 Alternative 3 – Two Large Facilities at New Hampton and Powder Mill

Alternative 3 includes a 150,000 lb RAS facility at New Hampton and a 150,000 lb RAS facility at Powder Mill. This alternative is presented in the event source water issues at other facilities are found to be too difficult to overcome or unanticipated events make this option viable in the future, such as a new method of TP removal that is more economical or regulatory modifications are successful and more affordable effluent treatment system becomes sufficient. This alternative includes the following modifications at each facility:

- Powder Mill New 150,000 lb RAS facility with advanced effluent treatment.
- Berlin Reduction in production to a less than 64,000 lbs, focus on Brook Trout broodstock to meet anticipated effluent TP limits.
- New Hampton New RAS facility to accommodate 150,000 lbs in production plus house brook and brown trout broodstock and Landlocked Atlantic Salmon egg rearing.
- Milford Continue operation as is with continued investment in rehabilitation of existing infrastructure.
- Twin Mountain Slight reduction in production to focus on and invest in Rainbow Trout broodstock.
- Warren Continue operation as is with continued investment in rehabilitation of existing infrastructure.

This brings the overall statewide production total to roughly 473,500 lbs. For the phasing approach on all alternatives, it is expected that a reduction in production at Powder Mill and Berlin are the first modifications to take place. For this alternative, phase 2 would likely be the construction and startup of a new RAS facility at New Hampton, phase 3 is a shift to focus on broodstock at Twin and phase 4 is the construction and startup of a new RAS facility with advanced effluent treatment at Powder Mill (see Table 7-4).

| | Existing | Phase 1 | Phase 2 | Phase 3 | Phase 4 |
|-------------|----------|---------|---------|---------|---------|
| Powder Mill | 124,097 | 30,000 | 30,000 | 30,000 | 150,000 |
| Belin | 74,336 | 64,000 | 64,000 | 64,000 | 64,000 |
| New Hampton | 71,792 | 71,500 | 150,000 | 150,000 | 150,000 |
| Milford | 68,124 | 68,000 | 68,000 | 68,000 | 68,000 |
| Twin | 20,698 | 20,500 | 20,500 | 15,000 | 15,000 |
| Warren | 26,742 | 26,500 | 26,500 | 26,500 | 26,500 |
| Total | 385,789 | 280,500 | 359,000 | 353,500 | 473,500 |

Table 7-4: Phases of Alternative 3 Production (lbs) by Facility

Alternatively, the design production of the facilities at New Hampton and Powder Mill could be increased to 200,000 which serves to allow the flexibility to abandon lower producing hatchery sites should it become desirable in the future to reduce operational expenses.

7.4 Alternative 4 – One Large Facility at New Hampton with New Northern Facility

Alternative 4 is like Alternative 3 with the exception of instead of investing in Powder Mill as a second larger facility the investment is made in a new facility in the northern part of the state. This alternative includes the following modifications at each facility:

- Powder Mill Reduction in production to roughly 30,000 lbs to meet effluent TP limits.
- Berlin Slight reduction in production to 64,000 lbs and operational changes to meet anticipated effluent TP limits.
- New Hampton New RAS facility to accommodate 125,000 lbs in production plus house Brook Trout and Brown Trout broodstock and egg rearing of Landlocked Atlantic Salmon.
- Milford Continue operation as is with continued investment in rehabilitation of existing infrastructure.
- Twin Mountain –Reduction in production to less than 15,000 lbs, focus on and invest in Rainbow Trout broodstock.

- Warren Continue operation as is with continued investment in rehabilitation of existing infrastructure.
- New Facility New facility to accommodate 125,000 lbs in production, this will require determination of the best site and acquisition of land for the new facility.

This brings the overall statewide production total to roughly 453,500 lbs. For the phasing approach on all alternatives, it is expected that a reduction in production at Powder Mill is the first to take place. For this alternative, phase 2 would likely be the construction and startup of a new RAS facility at New Hampton, phase 3 is a reduction at Berlin, and phase 4 is the construction of a new northern facility (see Table 7-5).

| | Existing | Phase 1 | Phase 2 | Phase 3 | Phase 4 |
|--------------|----------|---------|---------|---------|---------|
| Powder Mill | 124,097 | 30,000 | 30,000 | 30,000 | 30,000 |
| Belin | 74,336 | 64,000 | 64,000 | 64,000 | 64,000 |
| New Hampton | 71,792 | 71,500 | 125,000 | 125,000 | 125,000 |
| Milford | 68,124 | 68,000 | 68,000 | 68,000 | 68,000 |
| Twin | 20,698 | 20,5000 | 20,500 | 15,000 | 15,000 |
| Warren | 26,742 | 26,500 | 26,500 | 26,500 | 26,500 |
| New facility | | | | | 125,000 |
| Total | 385,789 | 280,500 | 334,000 | 328,000 | 453,500 |

Table 7-5: Phases of Alternative 4 Production (lbs) by Facility

Alternatively, the design production of the facilities at New Hampton and the new northern facility could be increased to 150,000 lbs which serves to allow even more flexibility to abandon lower producing hatchery sites should it become necessary in the future to reduce operational expenses.

7.5 Discussion and Recommendation

The implementation of modifications to the hatcheries under each of the proposed alternatives will inevitably occur in phases. Phasing will be required to allow NHFGD to secure project funding given that all of the alternatives require significantly more funding than what NHFGD currently has secured. Additionally, given NHFGD has historically been unable to secure funding for basic required maintenance, it is anticipated that a significant campaign to state officials as well as the public will be required to successfully secure the remaining funding required for completion of all phases. Given that the period required to secure this funding is unknown, the achievable production between phases must be looked at closely to see how it will vary. Thus, due to the anticipated extended period in which statewide production goals cannot be met, Alternative 3 and Alternative 4 are not desirable.

Alternative 1 and Alternative 2 are the remaining possible approaches. Both alternatives include the construction of a scalable 150,000 lb RAS facility at New Hampton as Phase 2. The difference then is the decision to either relocate the effluent discharge at the New Hampton RAS facility to

allow for an increase in production of up to 250,000 lbs, or to reinvest in Milford. The decision between these two alternatives is hard to justify given the lack of available information at this time.

It is recommended that further evaluation of these two alternatives be conducted after the first year of operation at the proposed New Hampton RAS facility prior to settling on a course of action. While relocating the outfall at New Hampton may seem like an easier approach, this will require a significant amount of regulatory coordination, construction of an effluent pump station and effluent pipeline. In addition, investment is still required at Milford to keep the facility operating at its current capacity. Most critically, the conditions within the Hatchery Building are unsafe for employees and will require mold removal and remediation. Thus, it is likely that reinvestment in Milford would be the overall lower capital cost alternative. However, this is complicated by the high iron and manganese present in the source water.

Previous cost estimating exercises have shown that the requirement for advanced effluent treatment at Powder Mill is cost prohibitive under current conditions. However, there is a possibility of achieving regulatory relief in the form of the implementation of a dilution zone that can be achieved only if the volume of effluent discharged is reduced significantly using recirculation. Powder Mill is a significant facility in the NHFGD's system due to it being the only facility with plentiful, high quality source water. While significant production at this facility needs to be cut for the time being, it is likely that this site will once again be required to produce at a significant level within the next 15 to 50 years. This will likely be the result of source water issues becoming problematic for other facilities either from quality or quantity.

Alternative 4 would be desirable should regulatory pressures on Berlin become such that a significant reduction in production is required. This is a current concern during its NPDES permit renewal process but will also remain a concern into the future as regulatory requirements are ever changing. Given the significant amount of stocking in the northern region of the state (~95,000 lbs), shifting this production to the central region should Berlin become no longer viable would result in a significant increase in labor and transportation costs for the Department.

Given the significant amount of uncertainty faced by NHFGD from regulatory pressures, source water issues, and funding availability, it is recommended that significant investment to modernize and maximize the production at New Hampton is the best way to continue to meet the state's production needs in the interim. Prior to the implementation of any additional phases, further engineering study should be undertaken to reevaluate the regulatory environment and source water challenges and complete concept advancement for more accurate cost estimating of not just capital requirements but also an evaluation of operational expenses.

7.5.1 Implementation Phasing Approach

After careful consideration and evaluation, it is recommended that significant investment to modernize and maximize the production at New Hampton is the best way to continue to meet the state's production needs in the interim. The overall statewide approach requires modification in production and/or rehabilitation of existing facilities in addition to significant investment in a new

recirculating aquaculture facility at New Hampton. The recommended system-wide long-term plan includes the following phased improvements:

- <u>Phase 1 2025</u>:
 - Powder Mill Reduction in annual production from 118,000 lbs to 30,000 lbs (75% reduction) to meet effluent TP limits.
 - Berlin Slight reduction in annual production from 74,000 lbs to roughly 64,000 lbs (13.5% reduction). If further reduction is deemed necessary after receiving the final EPA discharge permit this facility may shift its focus to Brook Trout broodstock only as a viable alternative to meet new effluent TP limits.
- Phase 2 2025/2026:
 - New Hampton New RAS facility to accommodate 150,000 lbs in production plus house Brook and Brown Trout broodstock and Landlocked Atlantic Salmon egg rearing.
- <u>Phase 3 2026/2027</u>:
 - Twin Mountain Slight reduction in production to focus on Rainbow Trout broodstock.
- <u>Phase 4 2027/2028</u>:
 - Reevaluation of the statewide system will likely be necessary at this time to determine the best way to meet production goals. Possible alternatives for evaluation include:
 - New Hampton Phase 2 Relocation of the effluent discharge from Dickerman Brook to the Pemigewasset River could allow this facility to produce up to 250,000 lbs with minimal rearing improvements by carrying an increased density within the existing rearing units.
 - Milford Rehabilitation Rebuild of Milford including source water treatment to reach 100,000 lbs in production.
 - Powder Mill Re-Evaluation Evaluate use of a dilution zone coupled with recirculating technology. Additional evaluation of less advanced forms of TP removal may also be justified.
 - Berlin/New Northern Facility Depending on the regulatory pressure on Berlin, re-evaluation of a new Northern Facility may be justified.

Additionally, some amount of investment in all the State's facilities is required just to insure they can stay operational given the lack of investment they've received over such a significant period, leaving most existing infrastructure in a state of disrepair and failure. These improvements are deemed as critical, and funding needs to be sought for these items above and beyond the operational funding typically received every year by NHFGD. These improvements are referred to as Mission Critical Improvements and are detailed by facility below.

- Powder Mill:
 - Reduce production to remain in compliance with NPDES permitted limits.
 - Source water treatment including drum filtration and disinfection is recommended to improve bio security.
 - Flow baffles are recommended within rearing units to remain in use to improve movement of fish generated solids towards the drains.
- Berlin:
 - o Reduce production to remain in compliance with NPDES permitted limits.
 - Upgrades to source waters, including either new production wells with backup power to serve as a reliable source without the need for disinfection, or a combination of new wells, existing wells, and surface waters with a new intake building including filtration and disinfection.
 - Hatchery building improvements.
 - Improve predator control systems.
 - Flow baffles for solids transport.
- <u>Milford:</u>
 - Replace backup generators and transfer switches.
 - Remove abandoned electrical systems in the well house.
 - Replace Field Well.
 - Improve predator control systems.
 - Concrete repair on all circular tanks.
 - Rehab the Hatchery Building.
 - Provide epoxy coating on rearing tanks.
 - Replace rusted pipe supports.
 - Replace roof.
 - Replace insulation.
 - Replace doors.
 - Replace exterior finishes.
 - Replace boiler, HVAC systems, and water heaters.
 - Remove or abate asbestos.
 - Remediate black mold.
 - Replace degraded and abandoned electrical systems.
 - Replace abandoned controls with SCADA (PLC) system.
 - Replace fluorescent lights with LEDs.
 - Provide ADA compliant access throughout publicly accessed areas.
- <u>Twin Mountain:</u>
 - Clean vegetation, sediment, and debris out of spring head boxes.
 - Provide or replace spring head box covers and screens.
 - Remove loose or deteriorated concrete and restore the structures to their original dimensions.
 - Replace the well/pump house floor slab and drain.
 - Rehab the Hatch House.

- Replace furnace.
- Replace electrical equipment.
- Patch damaged CMU wall.
- Replace windows.
- Rehab the Storage Garage.
 - Replace Roof.
 - Replace existing temperature-controlled feed storage area.
 - Repair/Replace rotted windowsills.
 - Replace light fixtures with LEDs.
- Rehab the Garage / Office Building.
 - Remove all abandoned equipment.
 - Replace panel board.
 - Replace HVAC systems and water heater.
 - Additional renovations would require a full gut renovation including structural adjustments to bring the entire building up to the current code for its current uses.
- <u>Warren:</u>
 - Replace heaters in the well houses.
 - Evaluate Well #2 for rehab vs replacement including a new backup generator.
 - o Clean reservoirs of vegetation, sediment, and debris.
 - Repair or replace deteriorated concrete in the rearing ponds and control structures.

These Mission Critical improvements will need to be completed at the same time as the implementation of the phased approach presented above. Thus, making the implementation timeline of the recommendations extremely condensed, requiring significant capital investment within the State's hatchery systems over the course of the next five to ten years to maintain production goals.

8 Opinion of Probable Construction Cost

A Conceptual Opinion of Probable Construction Cost (OPCC) was developed for the phasing approach set forth in Section 7.5.1. The OPCCs are based on estimated quantities and unit costs. Each OPCC was generated using a combination of improvement costs referenced from previous studies and industry data, scaled costs from facilities or equipment of similar operations, and unit costs applied to quantities of materials and equipment.

These opinions of probable construction cost were prepared to the standards of the Association for the Advancement of Cost Engineering (AACE) International Class 4 estimate. At the concept development stage, contingencies of 50 percent of the construction value were applied. Contingencies at New Hampton were reduced to 44% to account for economies of scale. Percentages of construction costs were used to represent cost for the items listed below:

- Contractor's Field General Conditions at 12% (10% used for New Hampton).
- Contractor's Mobilization at 2%.
- Contractor's OH&P at 10%.
- Contractor's Bonds and Insurance at 2%.
- Escalation to Midpoint of Construction:
 - 7.43% for 2023 through 2025.
 - 4.00% for 2025 and on.
- Market volatility adjustment factor at 10% (5% used for New Hampton).

The OPCC summaries for each phase set forth in Section 7.5.1 are shown below in Table 8-1 and a detailed breakdown of each OPCC is presented in Appendix D. Mission Critical improvements at Powder Mill are included in Phase 1 as some amount of improvement will be required to implement the reduction in production and Mission Critical rehabilitation should be implemented at the same time to reduce overall construction costs.

Table 8-1: Recommended Interim Plan OPPCs by Phase

| | Phase 1 2025 | Phase 2 2025/2026 | Phase 3 2026/2027 |
|-------------|-----------------|----------------------|----------------------|
| Powder Mill | \$2,800,000 | | |
| Belin | | | |
| New Hampton | | \$50,900,000 | |
| Milford | | | |
| Twin | | | \$ 4,000,000 |
| Warren | | | |
| Total | \$2,800,000 | \$50,900,000 | \$4,000,000 |

Notes: 1. Opinion of Probable Construction Costs do not include required design engineering and design services during construction fees. Determination of project funding requirements will necessitate the inclusion of these fees.

Mission Critical rehabilitation necessary at Berlin, Milford, and Warren to continue operation without significant risk of complete failure should be assessed by NHFGD on a continuing basis as they work to secure additional funding.

9 Conclusion

The six hatcheries in the state operate in unison as one large system supporting the stocking goal of up to 400,000 lbs of stockable fish per year. Three key issues drive achieving 400,000 lbs of production; permit compliance, water supply (quantity and quality), and the condition of the existing infrastructure.

Permit Compliance – The low TP limits already in place for Powder Mill and the potential for similar low limits at Berlin dictate the need for any of the larger hatcheries to include effluent treatment. The scale and complexity of the treatment will be determined by the location of the facility, the amount of treated recirculation water, and existing or potential future limits. Production capabilities have been estimated in this and supporting documents that outline potentials but the ultimate levels of production achievable at each location will be driven by permit compliance.

Water Supply – Powder Mill is the only facility within the state with ample water supply. All other sites have limited water supply that are currently being utilized to the maximum extent for a system designed for flow through with multiple passes. Thus, for any of the other five facilities, treatment and recirculation of the water within the hatchery would be required to increase production.

Infrastructure – Existing infrastructure has been driven to the end of its useful life. Major investments to maintain permit compliance, efficient operation, and address water supply issues should be done in conjunction with modernized rearing facilities to maximize the investment of the state's dollars and protect the production capabilities of the system.

After review of multiple alternatives at all six facilities as well as development and evaluation of statewide alternatives, an approach to the improvements required to continue to meet most of NHFGD's production goals in the interim is clear. Immediate investments should occur at the New Hampton facility to construct a new RAS facility to accommodate 150,000 lbs in production plus house Brook and Brown Trout broodstock and Landlocked Atlantic Salmon egg rearing. The centralized location of the facility, capability to complete major renovation within the existing footprint, and the ability to utilize RAS make the location ideal for major infrastructure investments. At a minimum, production could be increased 108% based on lbs per year with a future potential to increase to between 280% and 350% based on lbs per year with the use of higher rearing densities and a relocation of the effluent discharge to the Pemigewasset River.

Investment to construct a Rainbow Trout broodstock facility at Twin Mountain should be completed in conjunction or shortly after completion of construction at New Hampton. A new biosecure building capable of housing an internal Rainbow Trout program would eliminate the need to import poor quality eggs from other programs outside of New Hampshire, resulting in a huge cost savings in labor and operation in addition to better control of egg quality.

However, these major projects at New Hampton and Twin Mountain are far from the end of the improvements required. Reinvestment into the entire statewide system is necessary. The State's existing hatcheries have provided an enormous environmental, social, and economic impact over their life span. Per year, the New Hampshire Hatchery System produces roughly 1.5 million fish for stocking. Extrapolating that by the average 20-year lifespan of a facility typically assigned in engineering studies, results in roughly 30 million fish! These systems have served New

Hampshire for significantly longer than 20 years, and now need reinvestment to continue to provide these benefits.

Investments to improve the water quality at Milford and Berlin, including the replacement of rearing units should be reviewed. Installing a modern iron removal system followed by new circular rearing units at Milford would allow the facility to increase production above the current 70,000 lb range, significantly improving the production capabilities in the southern portion of the state. Additionally, an allowance should be developed to allow for one well rehabilitation each year. Doing one each year would put the wells on a cycle of every other year individually. It is common in wells with high iron to routinely pull pumps and recharge wells. With regular maintenance and enhanced iron removal, the Milford wells could be a consistent water supply for the program.

Berlin is currently going through its permit renewal cycle and discussions with EPA have indicated that discharge to York Pond will most likely have a lower TP limit to avoid further impairments to this water body. This will result in the loss of production in the east portion of the facility. Furthermore, the main effluent discharge point is also subject to tighter TP effluent limits given the indirect receiving water body, West Branch Upper Ammonoosuc Rive, is classified as an outstanding resource water. Thus, it is anticipated that some reduction in production will be required to meet new TP permit limits. Depending on the amount of reduction required, this may result in huge rippling effects to the states system, like that faced at Powder Mill. While a reduction at Berlin is impactful, the hope is that the newly constructed New Hampton RAS and maximizing production at all the other hatcheries will enable NHFGD to meet most of the state's required production.

Depending on what the future brings, the Warren Hatchery may or may not be required to continue operations. However, its role in the statewide system will be critical throughout implementation of the proposed phasing approach to produce as much stockable fish as possible during disruptions at other facilities. However, this site is becoming more prone to flooding. It is recommended that this risk be monitored and investment in this facility will likely need to be reevaluated over time. It may make sense given the historic significance to set this area up as a museum, or larger visitor's center with minimal showcase production.

It is crucial to understand that the recommended approach is an interim approach and reevaluation should occur in the future given the nature of unknown regulatory compliance issues at Berlin. The future approach to New Hampton requires relocation of the existing outfall to the Pemigewasset River which has a higher TP assimilative capacity than the current receiving stream. This allows for higher TP effluent limits which is critical to being able to reach up to 250,000 lb production The anticipated reduction proposed at Berlin may turn out to be either too aggressive, or not enough. Currently, the anticipated effluent limits are still within a fairly wide range and additional evaluation will need to be completed to determine exactly what the facility will be able to produce once limits are known. Additionally, regulatory issues at the remaining facilities may emerge as permits go through the renewal cycle and need to be monitored to ensure continued viability of the state's facilities.

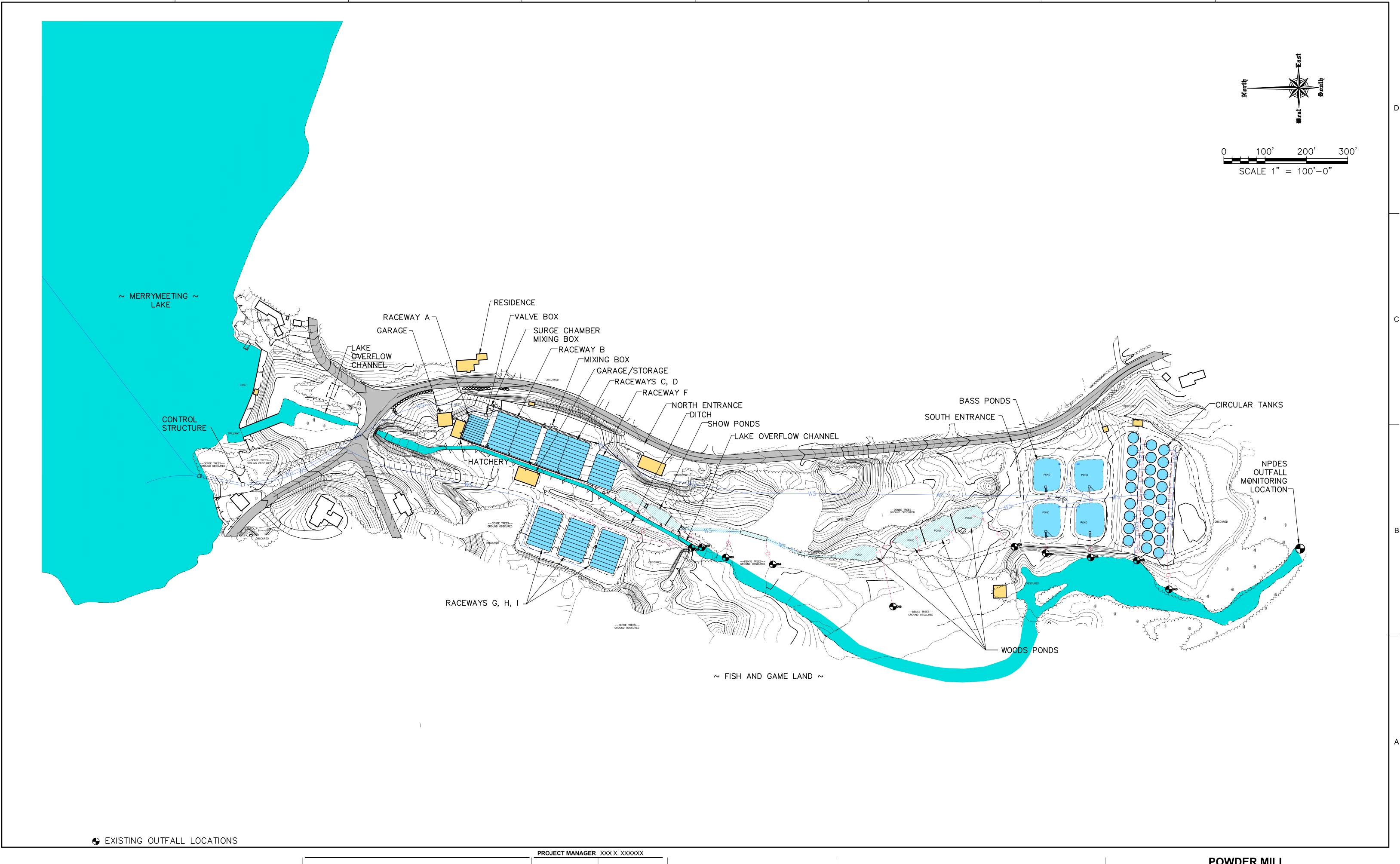
The implementation timeline for the recommended approach is extremely condensed and will require significant capital investment within the State's hatchery systems over the course of the next five years to maintain production goals.

- <u>Phase 1 2025</u>:
 - Powder Mill Reduction in annual production from 118,000 lbs to 30,000 lbs (75% reduction) to meet effluent TP limits.
 - Berlin Slight reduction in annual production from 74,000 lbs to roughly 64,000 lbs (13.5% reduction). If further reduction is deemed necessary after receiving the final EPA discharge permit this facility may shift its focus to Brook Trout broodstock only as a viable alternative to meet new effluent TP limits.
- <u>Phase 2 2025/2026</u>:
 - New Hampton New RAS facility to accommodate 150,000 lbs in production plus house Brook and Brown Trout broodstock and Landlocked Atlantic Salmon egg rearing.
- <u>Phase 3 2026/2027</u>:
 - Twin Mountain Slight reduction in production to focus on Rainbow Trout broodstock.
- <u>Phase 4 2027-2030</u>:
 - Reevaluation of the statewide system will likely be necessary at this time to determine the best way to meet production goals. Possible alternatives for evaluation include:
 - New Hampton Phase 2 Relocation of the effluent discharge from Dickerman Brook to the Pemigewasset River could allow this facility to produce up to 250,000 lbs with minimal rearing improvements by carrying an increased density within the existing rearing units.
 - Milford Rehabilitation Rebuild of Milford including source water treatment to reach 100,000 lbs in production.
 - Powder Mill Re-Evaluation Evaluate use of a dilution zone coupled with recirculating technology. Additional evaluation of less advanced forms of TP removal may also be justified.
 - Berlin/New Northern Facility Depending on the regulatory pressure on Berlin, re-evaluation of a new Northern Facility may be justified.
 - Depending on the approach taken, major rehabilitation at other facilities should be undertaken to maintain production capabilities at existing facilities.

While the recommended approach presented here only gets the State to roughly 359,000 lbs of production, there are multiple pathways still available to meet the overall statewide production goals. Implementing significant improvements to New Hampton will allow NHFGD to continue to effectively carry out its mission of conserving, managing, and protecting the State's fish and wildlife resources and their habitats; informing and educating the public about these resources;

and providing the public with opportunities to use and appreciate these resources until further information is known. Furthermore, reevaluation of the remaining alternatives to reach the State's goal of 400,000lbs ensures that the best overall long-term solution is implemented so that NHFGD can continue to provide the enormous environmental, social, and economic impact in the most cost-effective way.

Appendix A Existing Site Maps and Hydraulic Profiles



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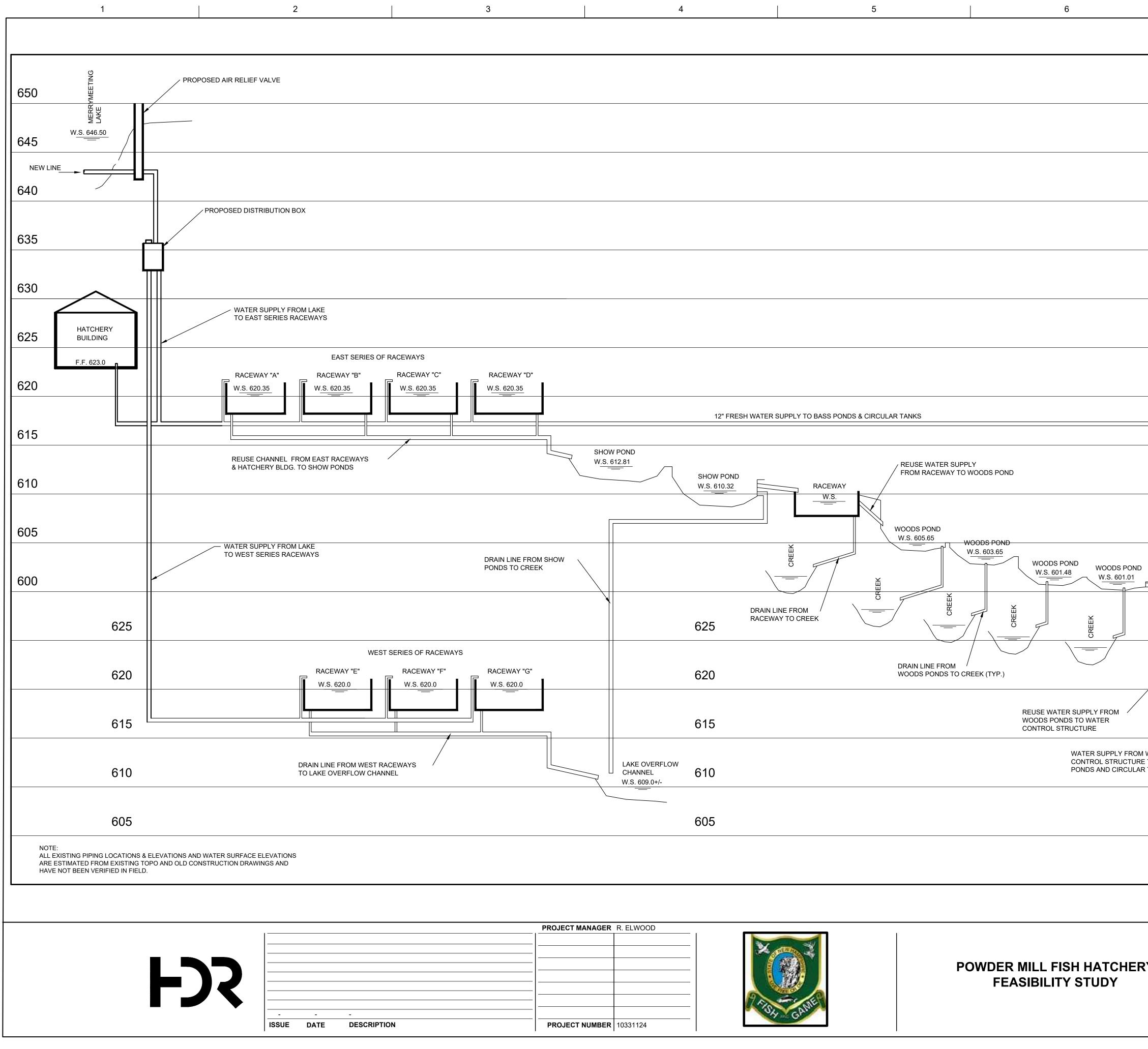
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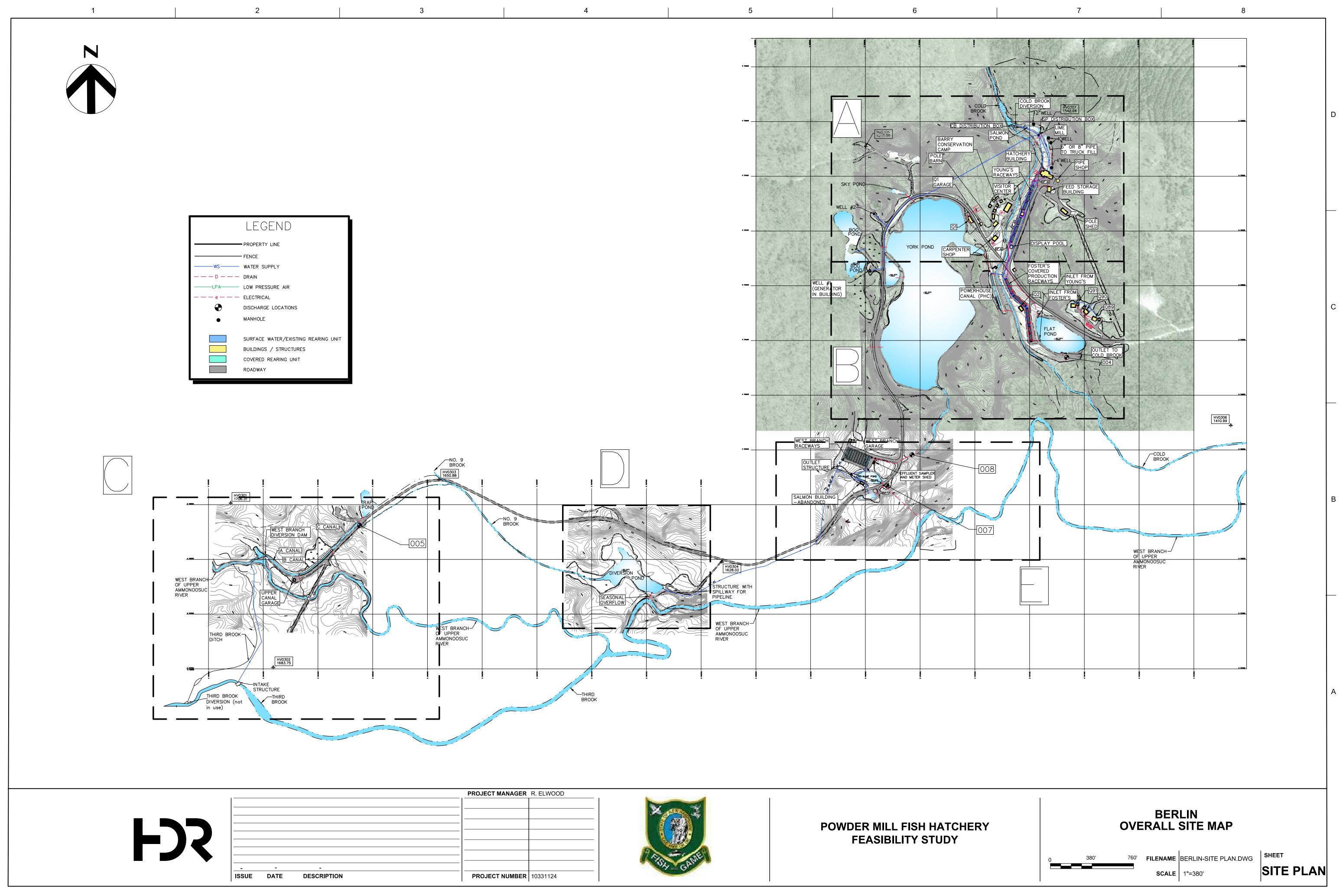
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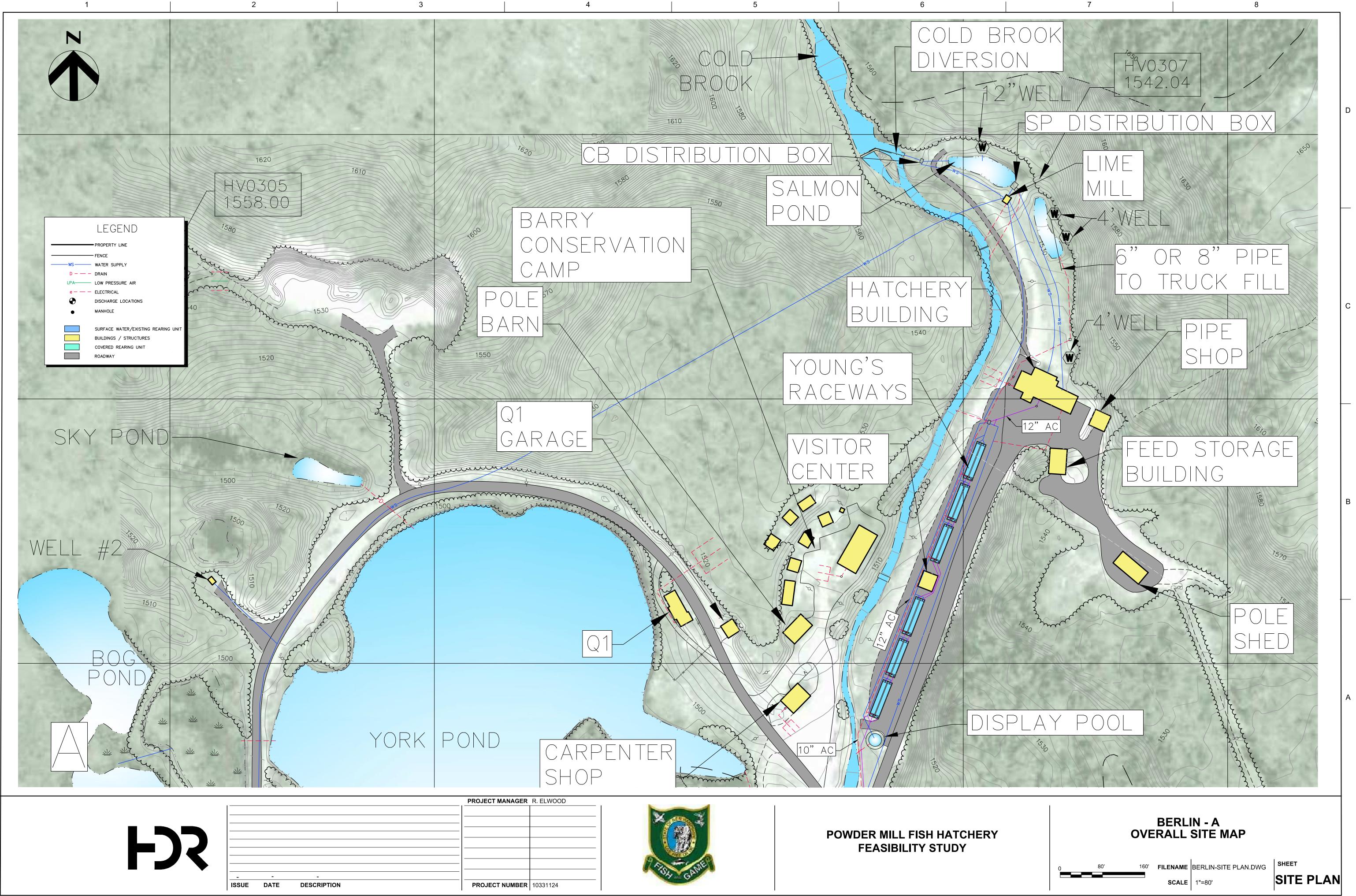
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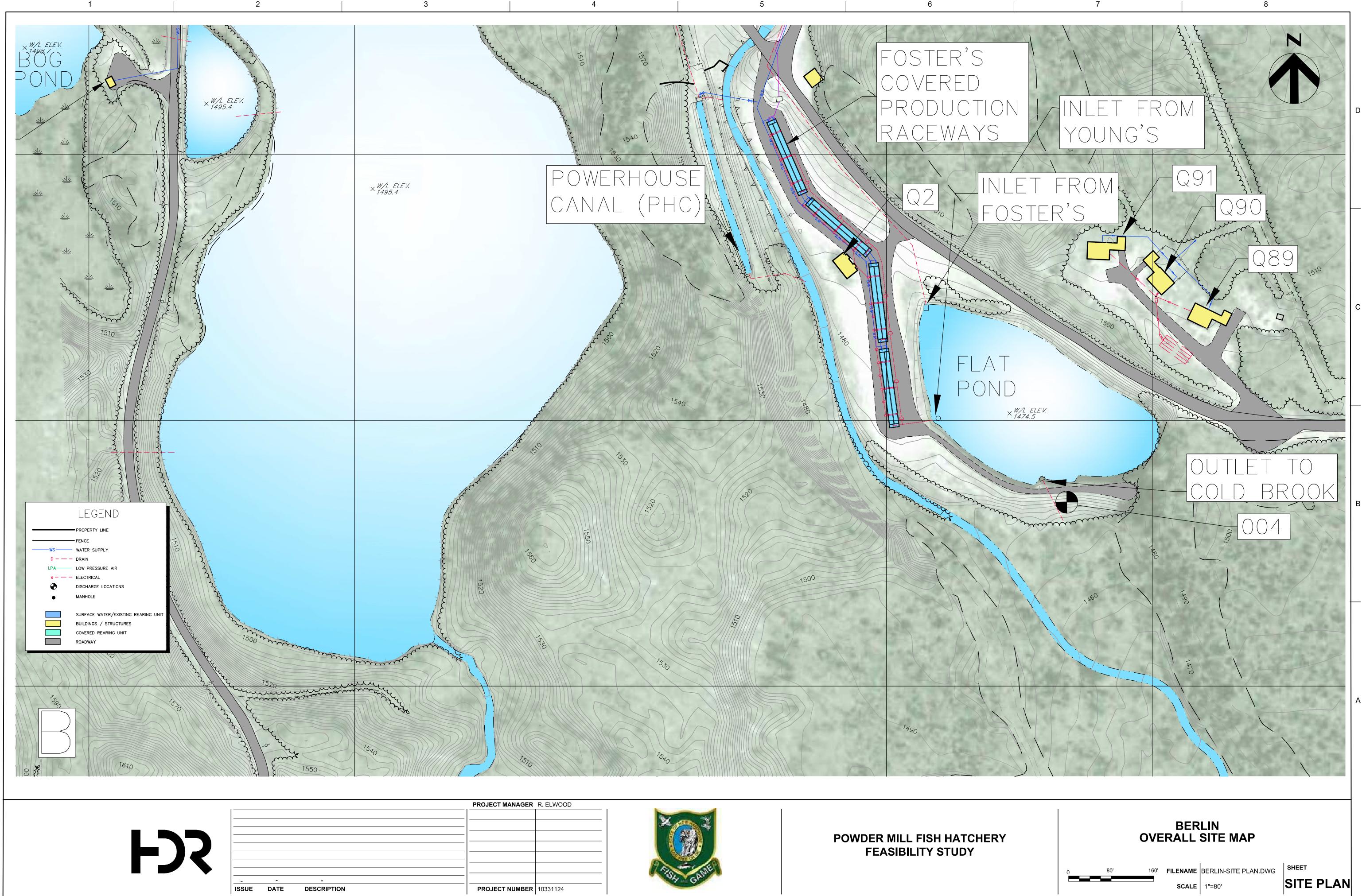


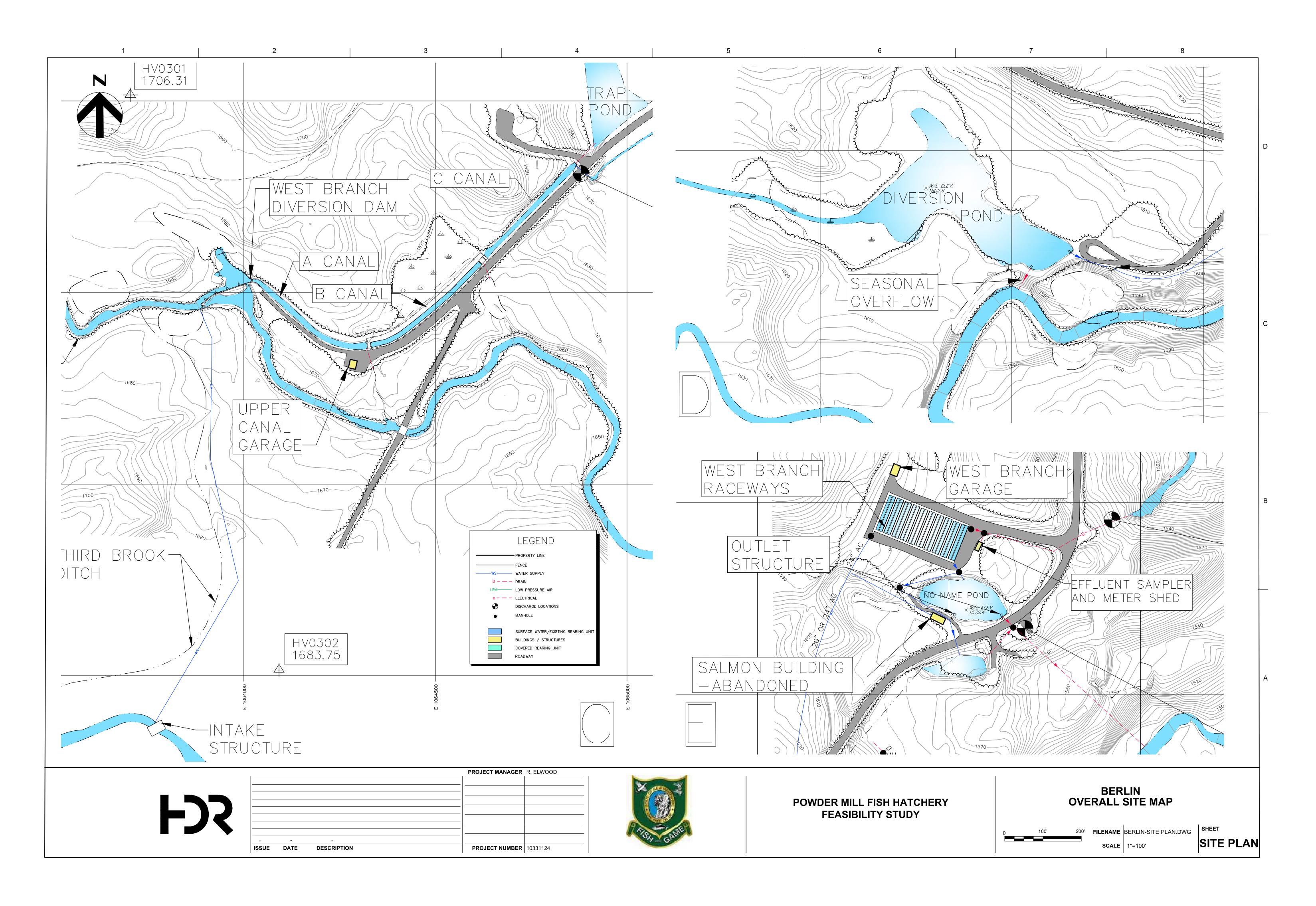
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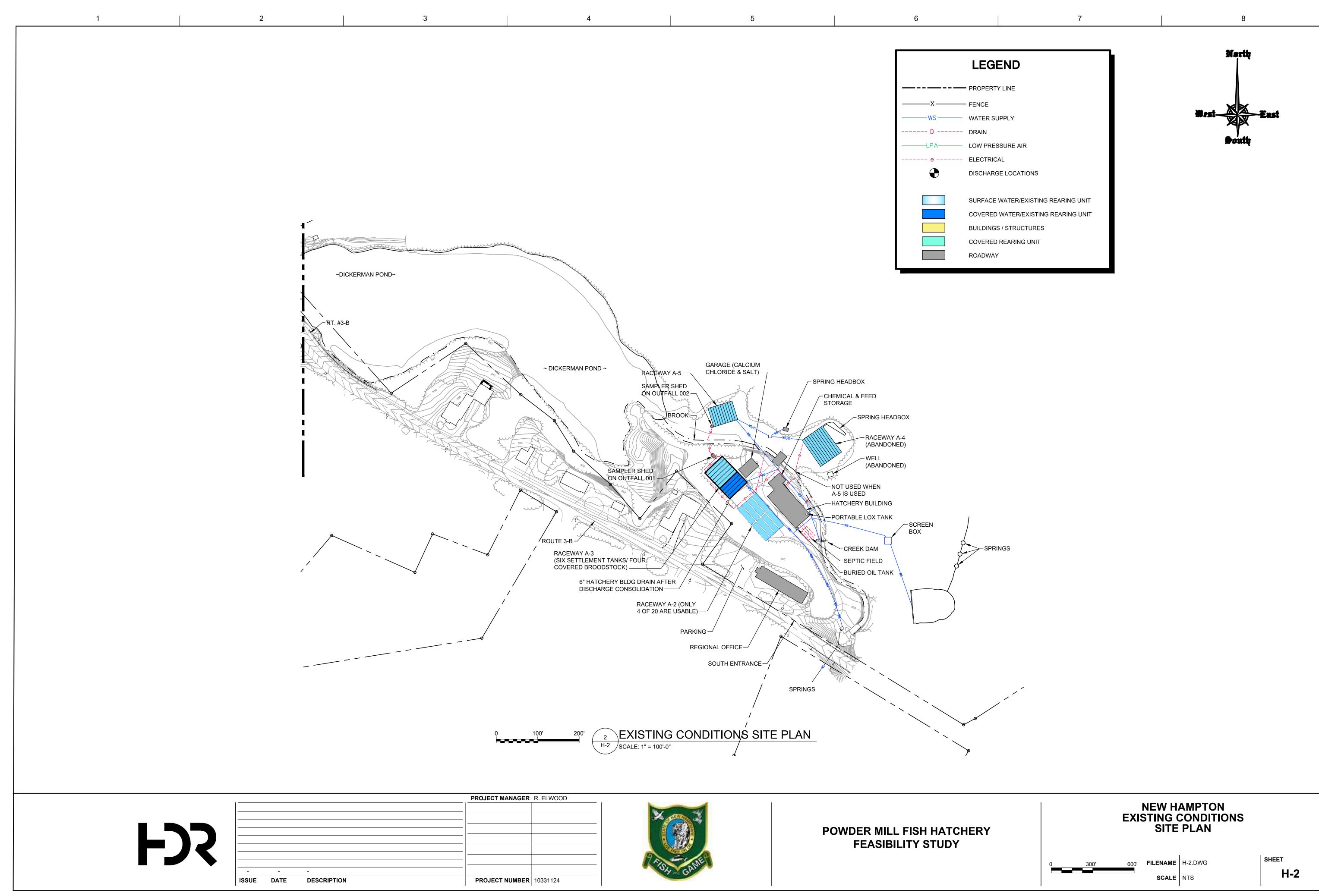


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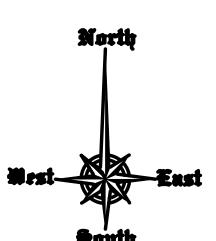


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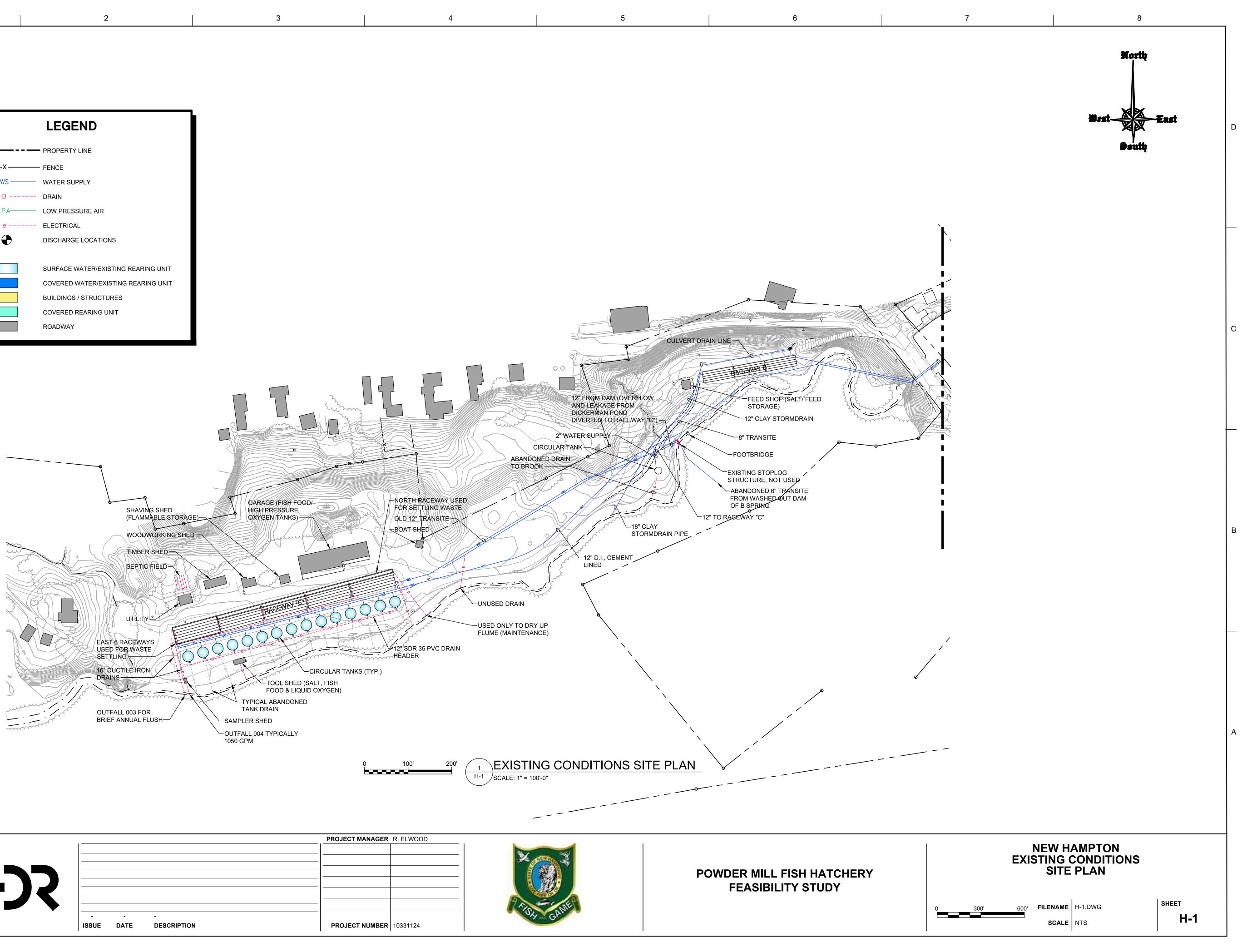


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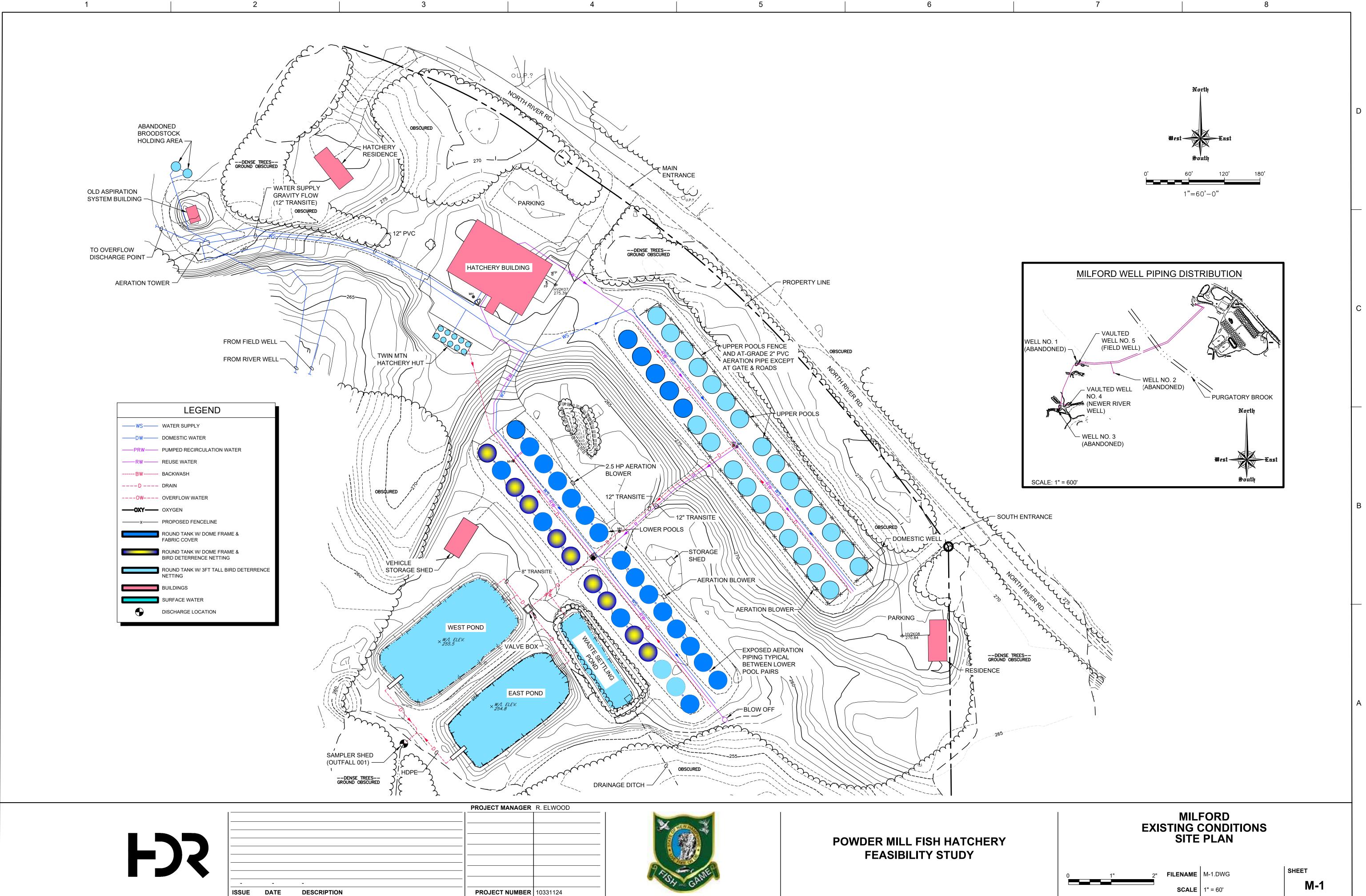
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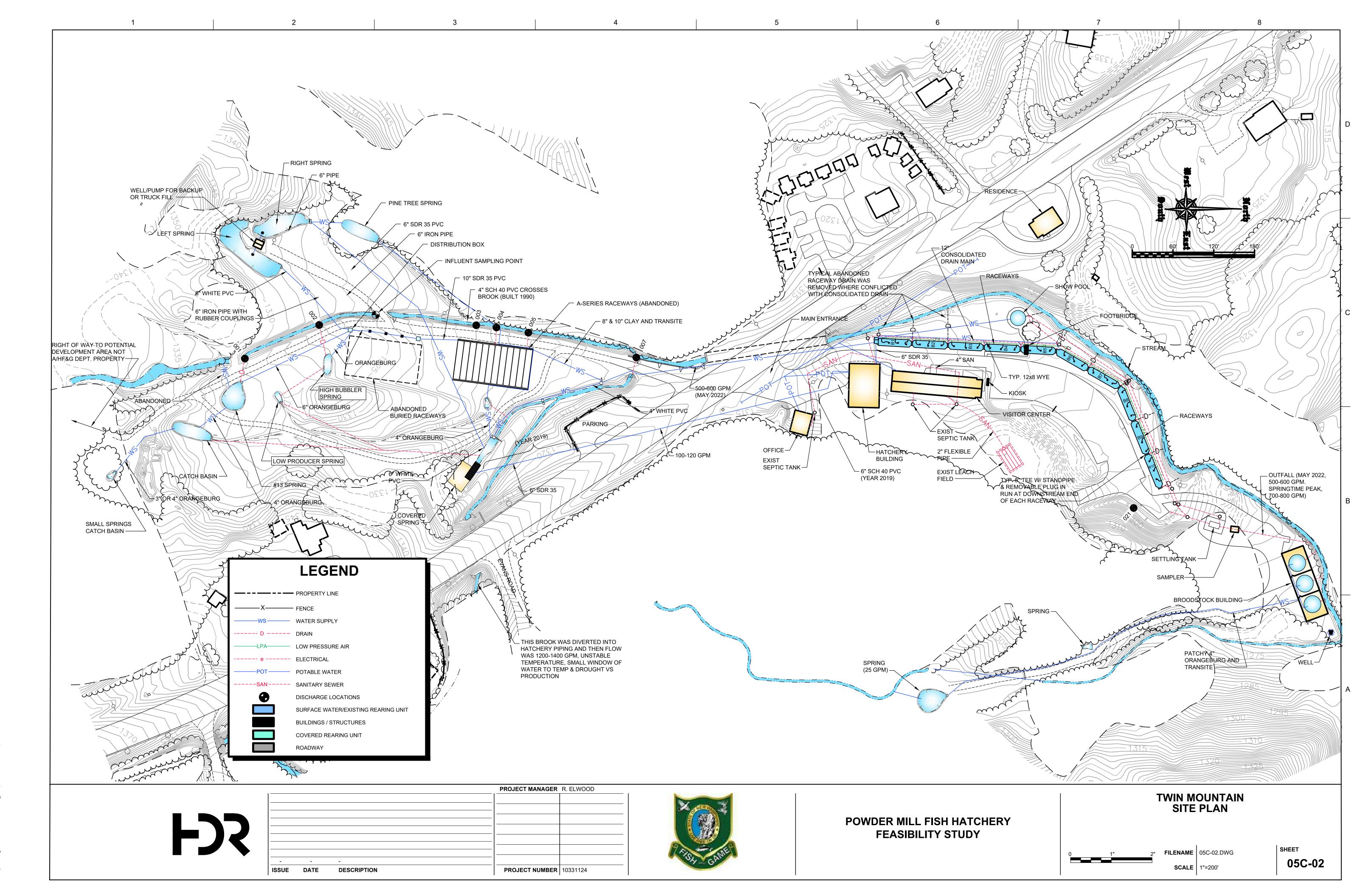
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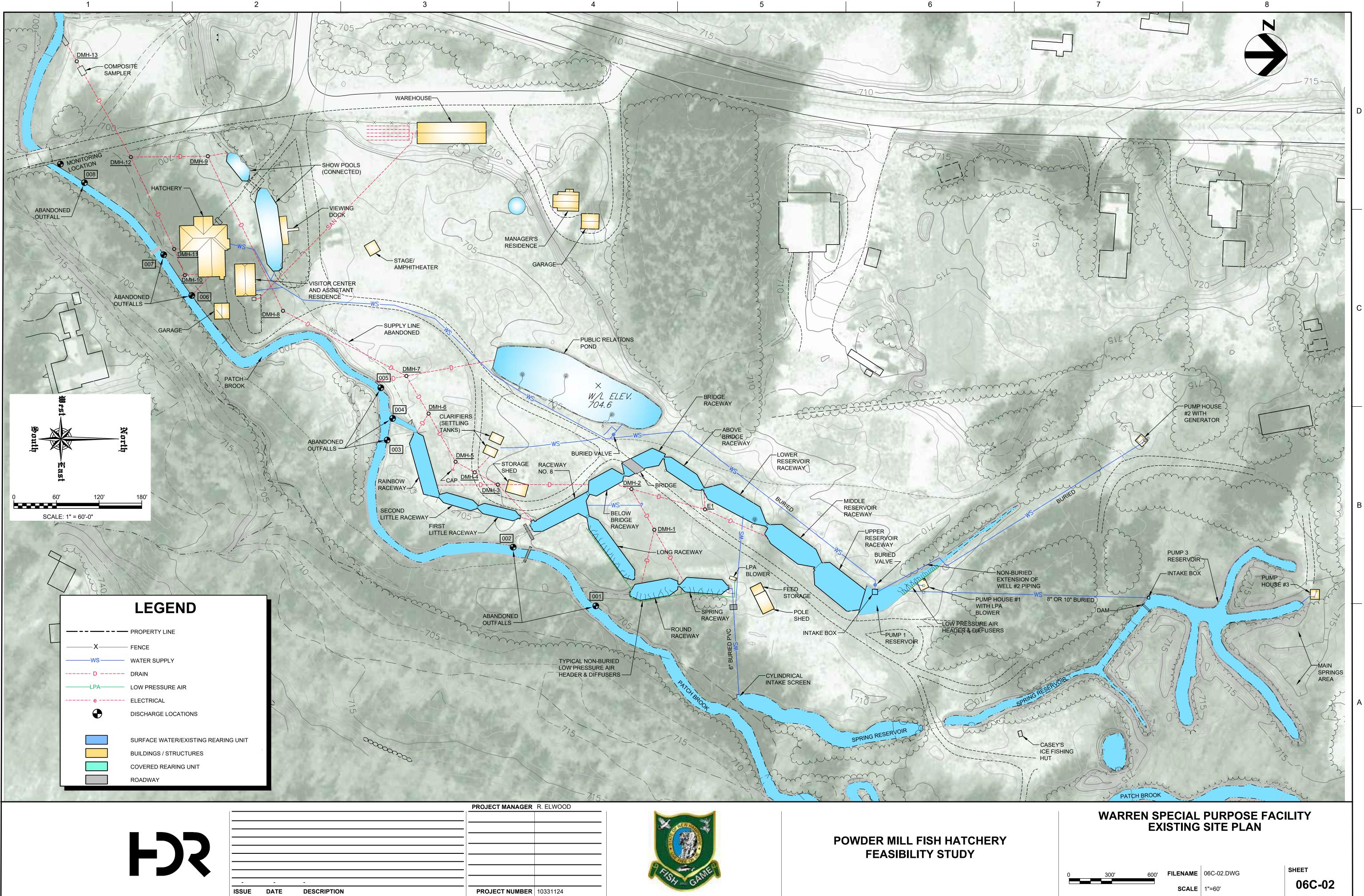
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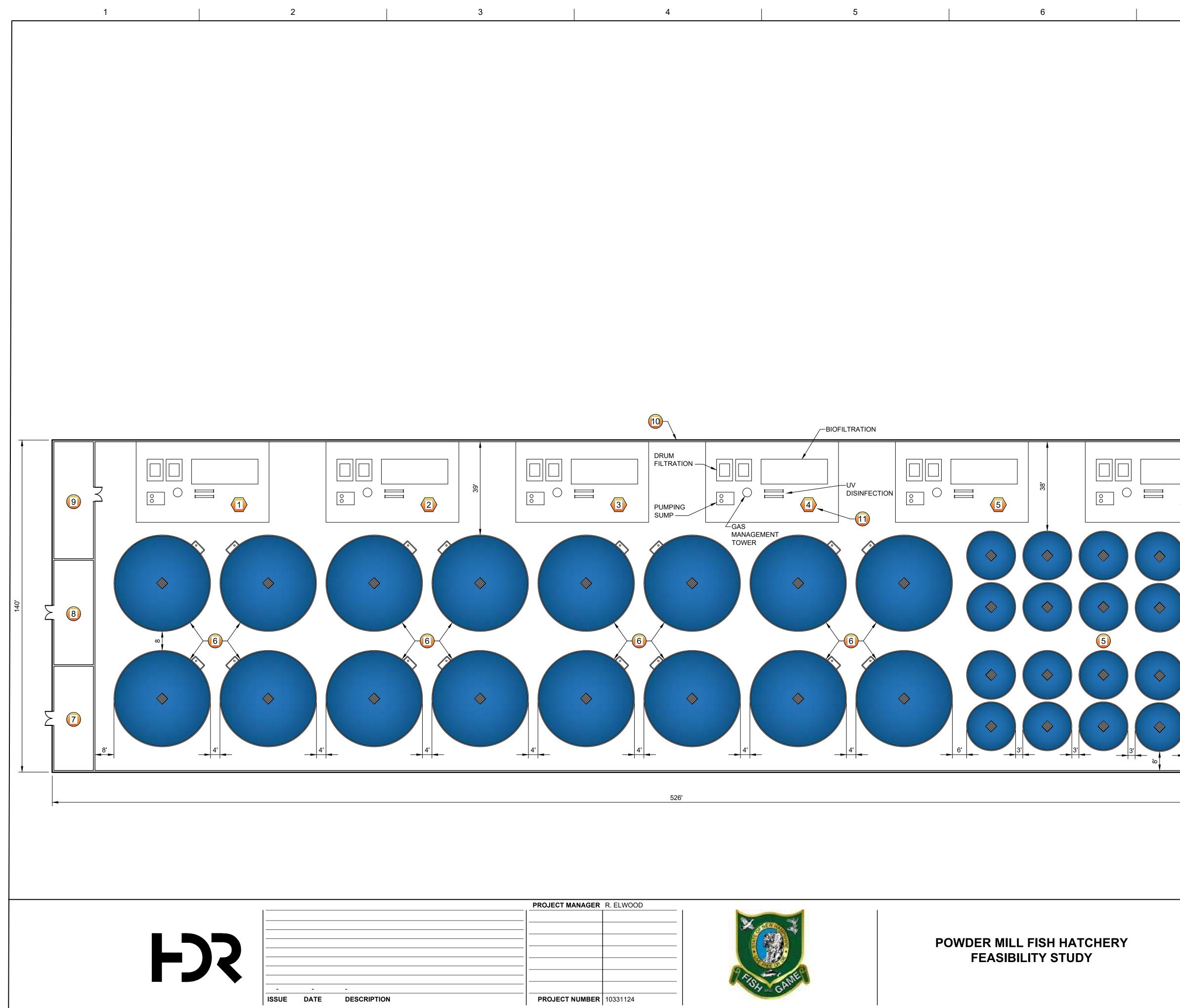






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Appendix B Proposed Site Layouts



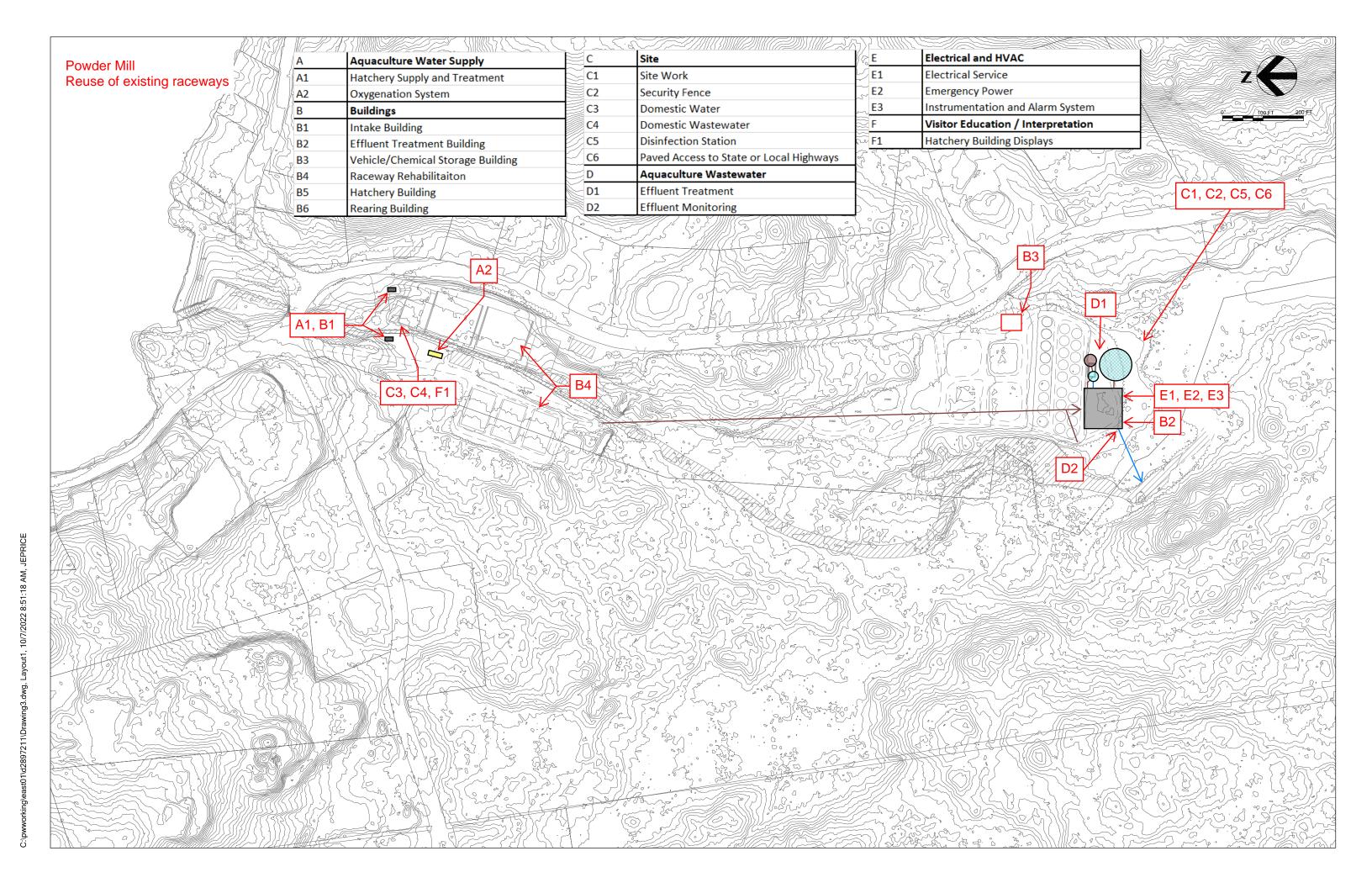
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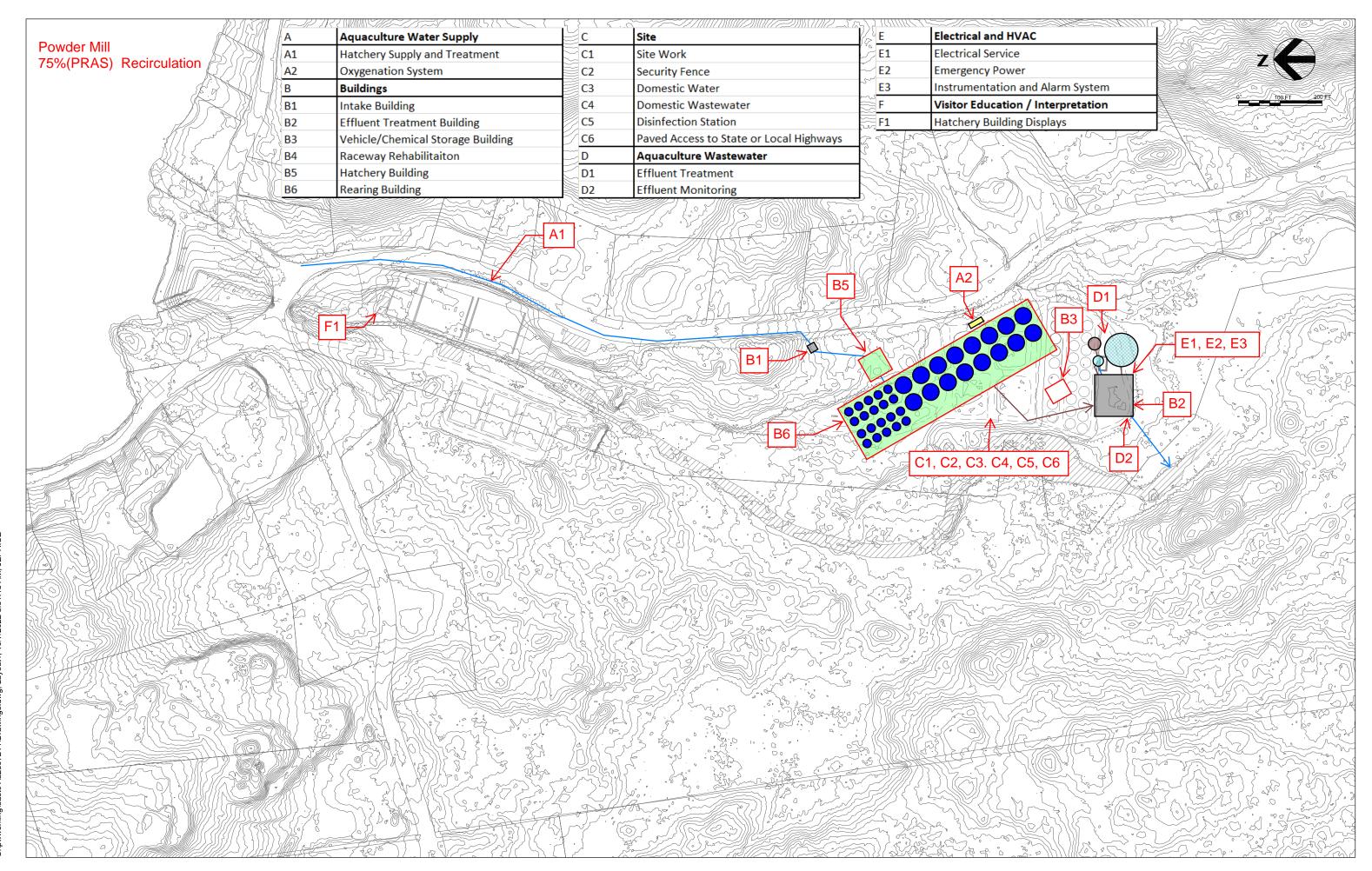


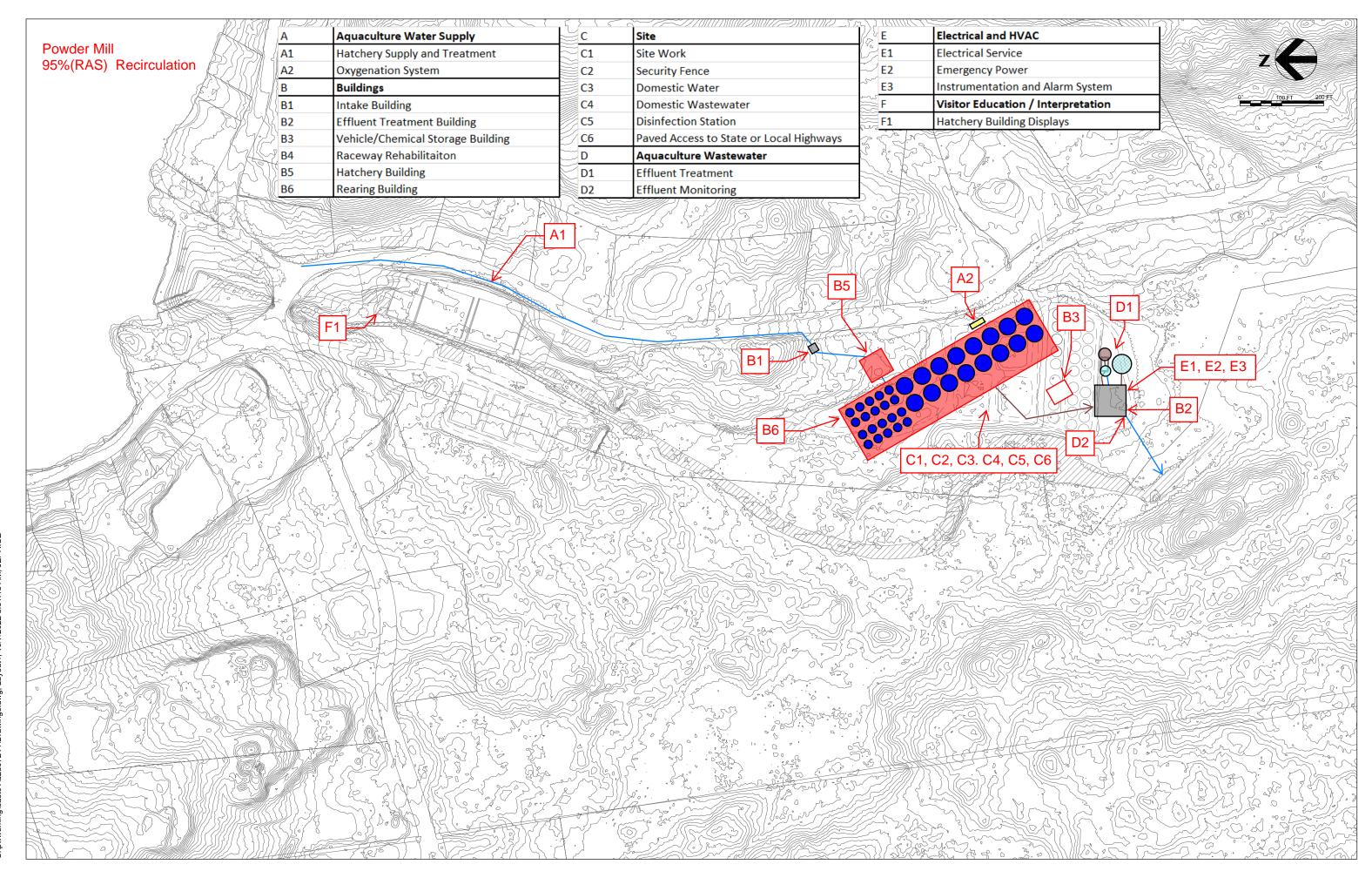
POWDER MILL FISH HATCHERY

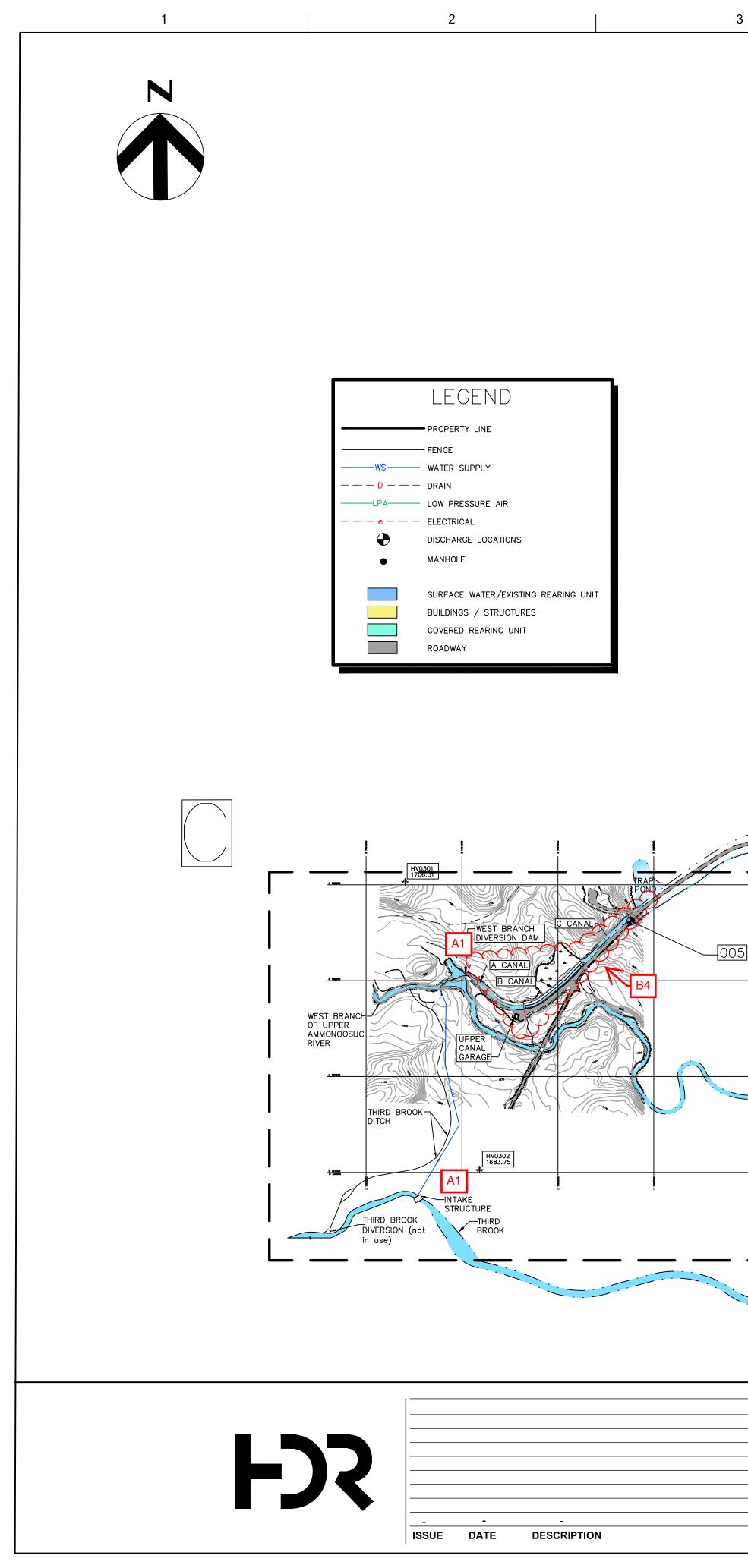
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| | KEYED NOTES: OFFICES AND STAFF SUPPORT SPACES IN INSULATED POWDER MILL RAS PRE-ENGINEERED BUILDING. EGG INCUBATION ROOM INCLUDING BIOSECURITY EGG |
| | WASH AREA, VERTICAL FLOW EGG INCUBATORS AND CIRCULAR FEED TRAINING TANKS. THIS ROOM ON FLOW THROUGH WATER USE ONLY (NOT RAS.) SHALLOW AND DEEP LAKE WATER SUPPLY LINES FOR MAKEUP WATER TO RAS SYSTEM. |
| | 4 PROCESS MECHANICAL ROOM. LAKE WATER FILTRATION, UV DISINFECTION AND MAKE-UP WATER DE-GASSING/ AERATION. SPACE INCLUDES PROCESS WATER HEATING SYSTEMS. |
| | 5 20 FT DIAMETER INTERMEDIATE REARING TANKS WITH MODULAR RAS TREATMENT COMPONENTS. TWO (2) RAS MODULES WITH 10 TANKS PER MODULE. TANKS ARE DUAL DRAIN DESIGN. |
| | 6 40 FT DIAMETER FINAL GROW-OUT TANKS WITH MODULAR RAS TREATMENT COMPONENTS. FOUR (4) RAS MODULES WITH 4 TANKS PER MODULE. TANKS ARE DUAL DRAIN DESIGN. |
| | (7) GENERAL EQUIPMENT STORAGE SPACE. |
| | 8 FEED STORAGE SPACE (AIR CONDITIONED). |
| | 9 ELECTRICAL EQUIPMENT ROOM. ELECTRICAL PANELS AND EMERGENCY ELECTRICAL GENERATOR. PROCESS MONITORING AND INSTRUMENTATION SYSTEM FOR ALL RAS MODULES PROVIDED. |
| | PRE-ENGINEERED INSULATED METAL BUILDING WITH HVAC SYSTEMS. BUILDING SIZE IS APPROXIMATELY 65,745 SQUARE FEET. |
| | RAS MODULES 6 PROVIDED. EACH MODULE INCLUDES: DUAL DRAIN CULTURE TANKS, MICROSCREEN, CIRCULATION PUMPS, BIOFILTRATION TOWER, GAS MANAGEMENT TOWER WITH CO2 & DO GAS MANAGEMENT, UV DISINFECTION, OZONE AND SYSTEM PIPING. SYSTEM IS 95% RECIRCULATION / 5% MAKE-UP BY RATE OF FLOW RAS DESIGN. RAS MODULES CAN OPERATE AS STAND-ALONE INDEPENDENT SYSTEMS |
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| Λ | Aquaculture Water Supply | |
|--------|---|---|
| A1 | Hatchery Supply | |
| A2 | Oxygenation System | |
| В | Buildings | |
| B1 | Cold Brook and Wells Intake Building | |
| B2 | West Branch Intake Building | |
| B3 | Effluent Treatment Building | |
| B4 | Raceways Rehabilitation | |
| B5 | Hatchery Building | H 7980 |
| B6 | Rearing Building | SKY POND |
| B7 | Existing Building Rehab | |
| С | Site | WELL #2 |
| C1 | Site Work | |
| C2 | Domestic Water | POND |
| C3 | Domestic Wastewater | YOF |
| C4 | Disinfection Station | |
| C5 | Paved Access to State or Local Highways | POND |
| D | Aquaculture Wastewater | WELL #1 (GENERATOR B7,E2 |
| D1 | Effluent Treatment | |
| D2 | Effluent Monitoring | |
| D3 | West Branch Pumping | |
| D4 | Young's and Foster's Pumping | |
| E | Electrical | |
| E1 | Electrical Service | |
| E2 | Emergency Power | |
| E3 | Instrumentation and Alarm System | |
| F | Visitor Education / Interpretation | 1 70000 |
| F1 | Vis <mark>itor Center Repairs</mark> | |
| | | |
| | | WEST BRANCH |
| | | B2,E1 |
|) K | | OUTLET STRUCTURE |
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| | | B7 SALMON BUILDING |
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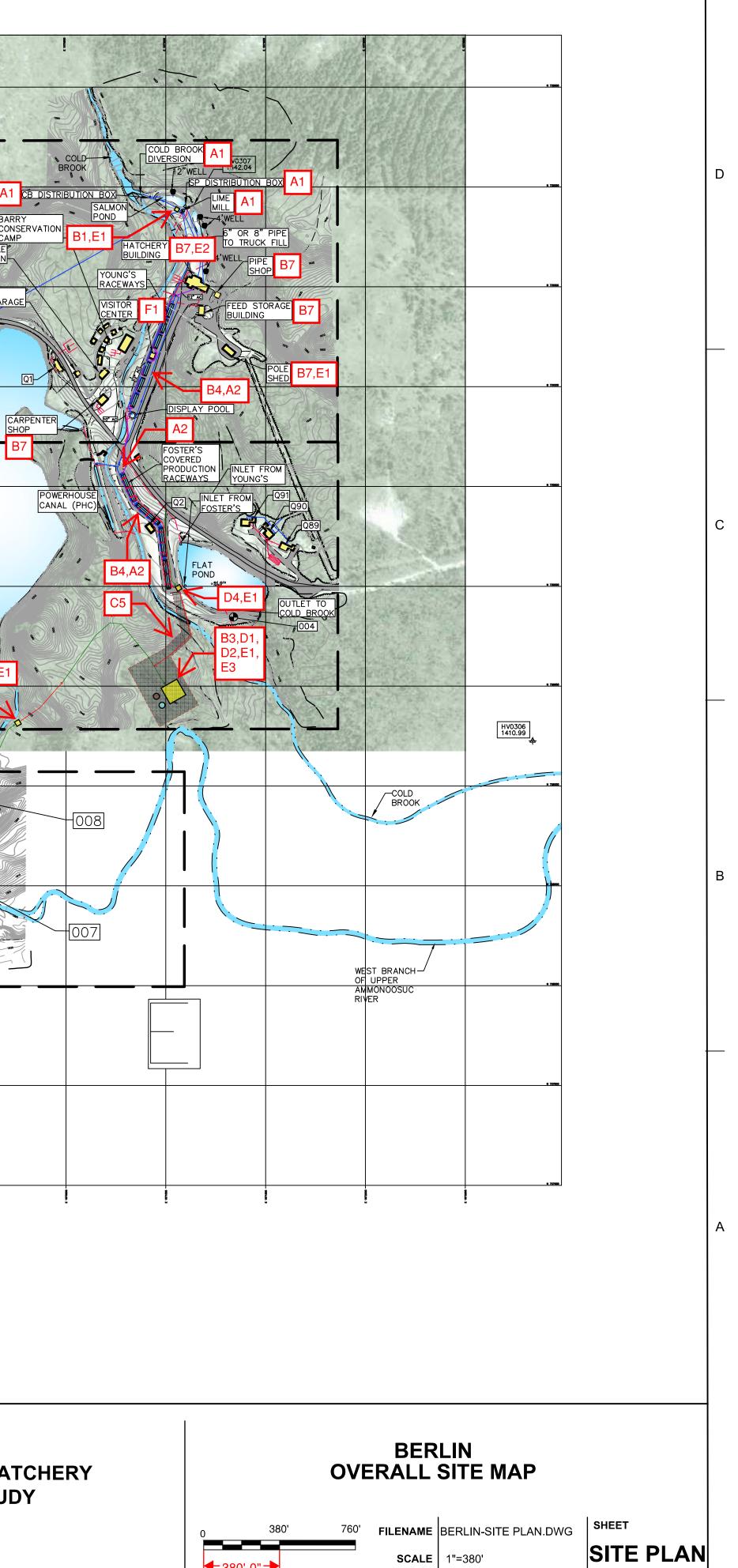
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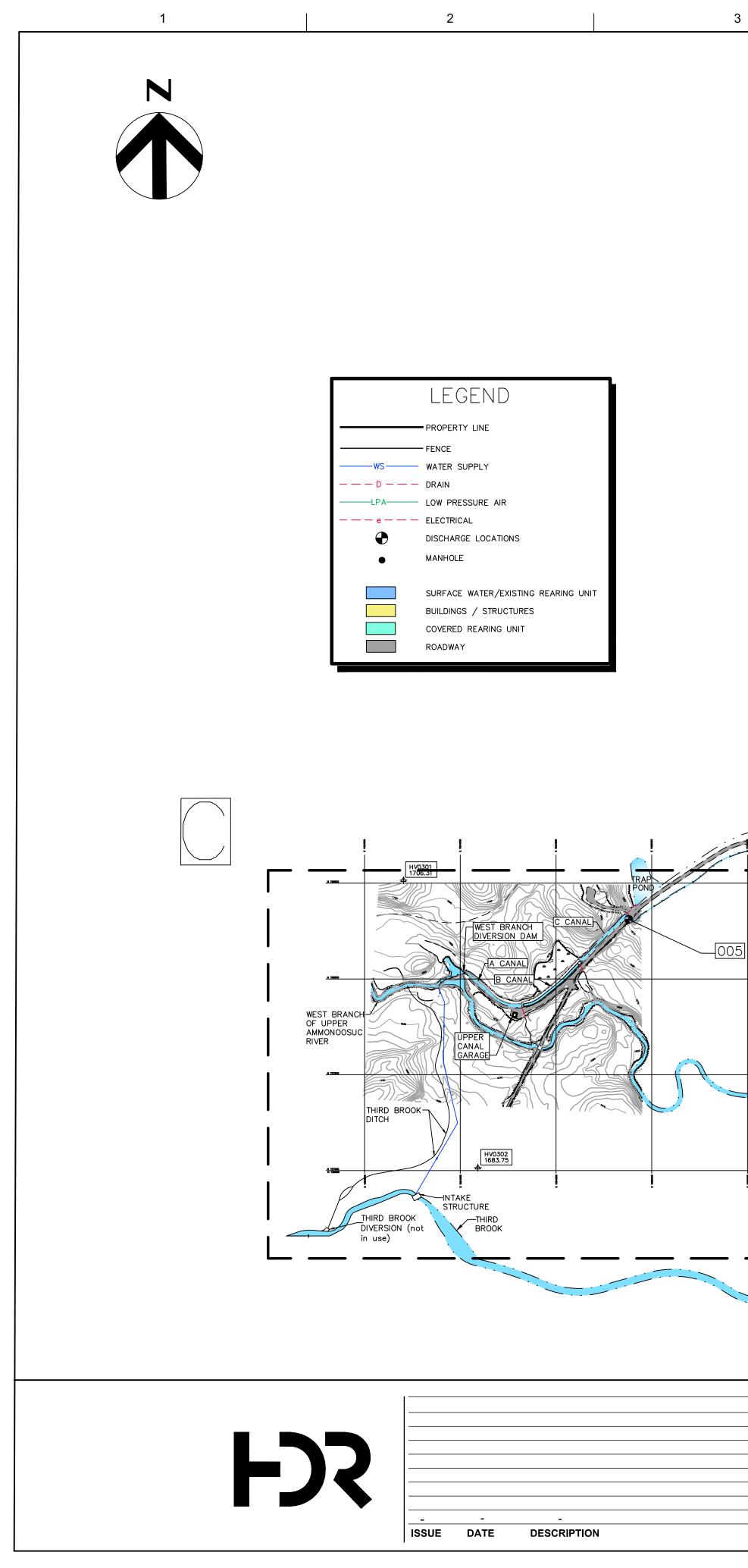
POWDER MILL FISH HATCHERY FEASIBILITY STUDY



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| | A2 | Oxygenation System | | | E The Part of the A | Mary Mary |
| | В | Buildings | 1 | | | |
| | B1 | Cold Brook and Wells Intake Building | 10 | Selle alle | | 1. 1. 1. |
| | B2 | West Branch Intake Building | H 738000 | 2.10.41 | | 1820 7810 |
| | B3 | Effluent Treatment Building | 1 | me & The | | HV0305 1058.00 |
| | B4 | Raceways Rehabilitation | ET. | 101/102 | and the second second | |
| | B5 | Hatchery Building | | - Argar | | 1540 HIL 1650 |
| | B 6 | Rearing Building | 100 | | | 1520 |
| | B 7 | Existing Building Rehab | н 731800 | an anne | | |
| | с | Site | | THE PARTY | SKY PONE | 1500 |
| | C1 | Site Work | | | | · · · · |
| | C2 | Domestic Water | 2 | and and | WELL #2* | |
| | C3 | Domestic Wastewater | | All Star | B7 100 | |
| | C4 | Disinfection Station | и 731000 | A REAL PLAN | BOG | |
| | C5 | Paved Access to State or Local Highways | Star 1 | 四 王治 | | |
| | D | Aquaculture Wastewater | 1 | S. St. C | | YO |
| | D1 | Effluent Treatment | 100 | the spirit | | |
| | D1 D2 | Effluent Monitoring | 146 | Section States | BOGPOND | × Fala Ger |
| | | | н 730800 | (E) - 33 | WELL #1 | |
| | D3 | West Branch Pumping | S. Martin | | (GENERATOR IN BUILLING) B7,E | 2 |
| | D4 | Young's and Foster's Pumping | 0.00 | The sti | A A A A A A A A A A A A A A A A A A A | |
| | E | Electrical | 0.11 | A MAR | | |
| | E1 | Electrical Service | 13 | | | 1910 |
| | E2 | Emergency Power | н 730000 | Ser Phil | | |
| | E3 | Instrumentation and Alarm System | 100 | A SANGO | | |
| | F F1 | Visitor Education / Interpretation Visitor Center Repairs | | 1 and the second | | |
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| | and a second | | | | | |
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| | | | - Tatto | | | the literature of the literatu |
| | | | | | | |
| | | | | | | |
| | | | | | | |
| | | | I 73000 | WESI | BRANCH WAYS | WEST BRANCH GARAGE |
| 9 | | | - 7000 - 7000 | RACE | WAYS | MEST BRANCH GARAGE |
| | | | 1 7860 | RACE | BRANCH WAYS | GARAGE |
| . 9 оок | | | - 7000 | RACE | WAYS | GARAGE |
| | | | - 7000 - 7000 | | WAYS JTLET RUCTURE | GARAGE |
| | | | - Taxio | | WAYS JTLET RUCTURE | GARAGE |
| | | | - Taxo | | WAYS | GARAGE |
| | NO. 9 BROOK | | . 7860 | | WAYS JTLET RUCTURE | GARAGE |
| | NO. 9 BROOK | | I 7300 | | WAYS JTLET RUCTURE | GARAGE |
| | NO. 9 BROOK | | | | WAYS JTLET RUCTURE | GARAGE |
| | NO. 9 BROOK | | . 73000 | | WAYS JTLET RUCTURE | GARAGE |
| | NO. 9 BROOK | | 1 7360 | | WAYS JTLET RUCTURE | GARAGE |
| | NO. 9 BROOK | | # 73000 | | WAYS JTLET RUCTURE | GARAGE |
| | -NO. 9 BROOK | | | | WAYS JTLET RUCTURE | GARAGE |
| | NO. 9 BROOK | NUMBER STOR | UCTURE WITH | | WAYS JTLET RUCTURE | GARAGE |
| | NO. 9 BROOK | | | | WAYS JTLET RUCTURE | GARAGE |
| | NO. 9 BROOK | NUMBER STOR | UCTURE WITH | | WAYS JTLET RUCTURE | GARAGE |
| | NO. 9 BROOK | e e e e e e e e e e e e e e e e e e e | UCTURE WITH LLWAY FOR ELINE | | WAYS JTLET RUCTURE | GARAGE |
| WCH | NO. 9 BROOK | I I I I I I I I I I I I I I I I I I I | UCTURE WITH LWAY FOR ELINE | | WAYS JTLET RUCTURE | GARAGE |
| | NO. 9 BROOK | I I I I I I I I I I I I I I I I I I I | UCTURE WITH LWAY FOR ELINE | | WAYS JTLET RUCTURE | GARAGE |

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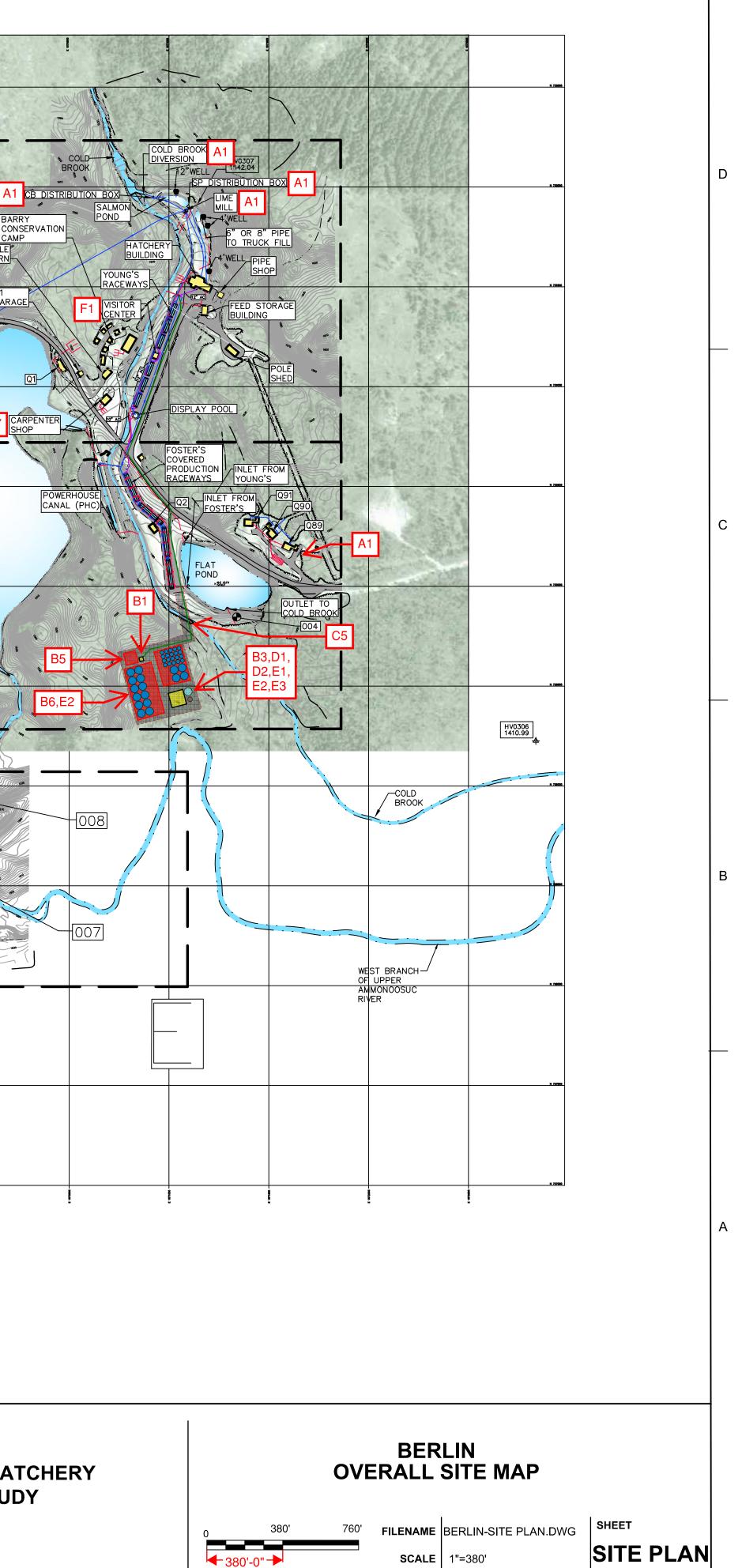
PROJECT MANAGER R. ELWOOD

-THIRD BROOK

| | PROJECT NUMBER | 10331124 |
|---|----------------|----------|
| l | | l |



POWDER MILL FISH HATCHERY FEASIBILITY STUDY

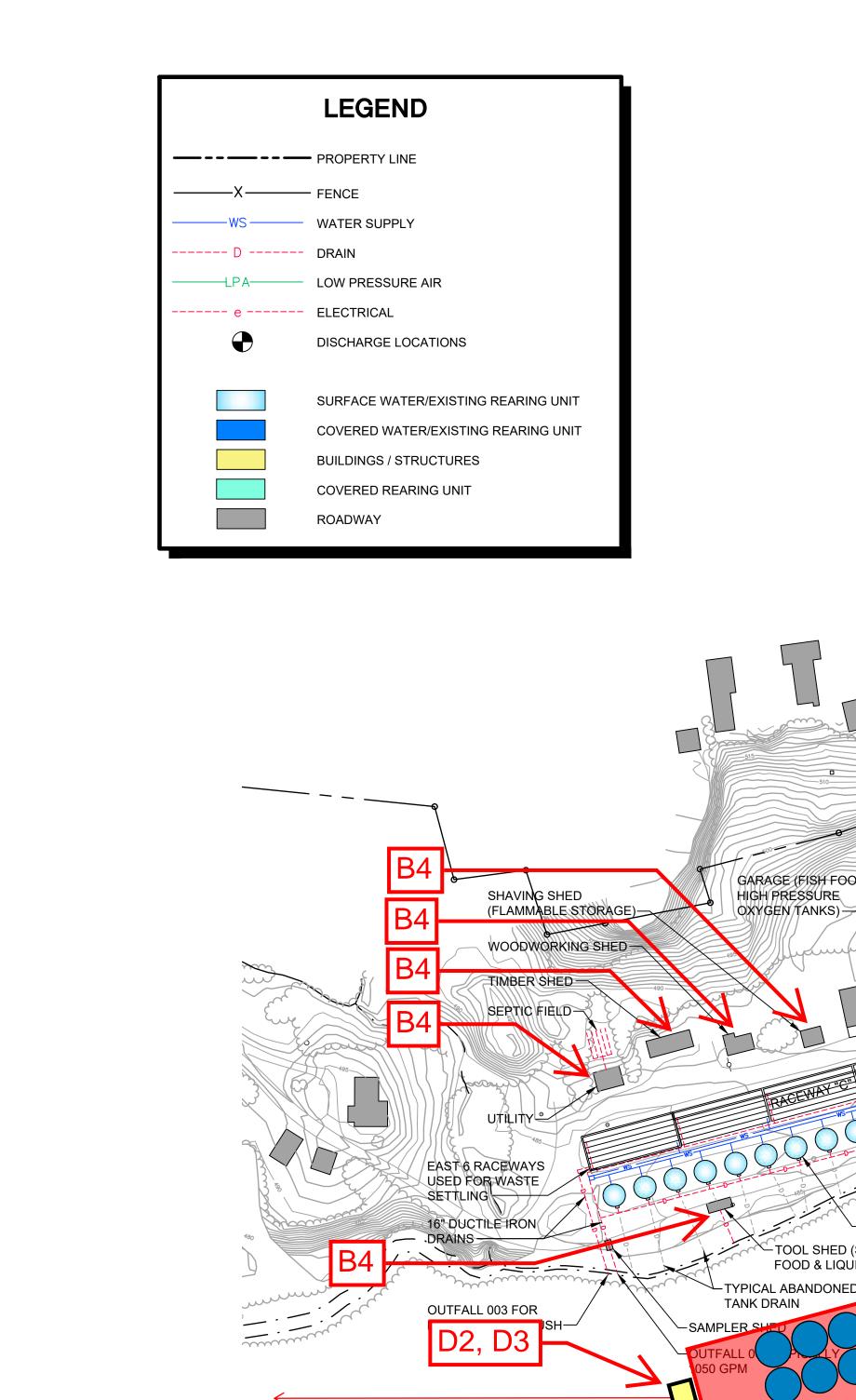


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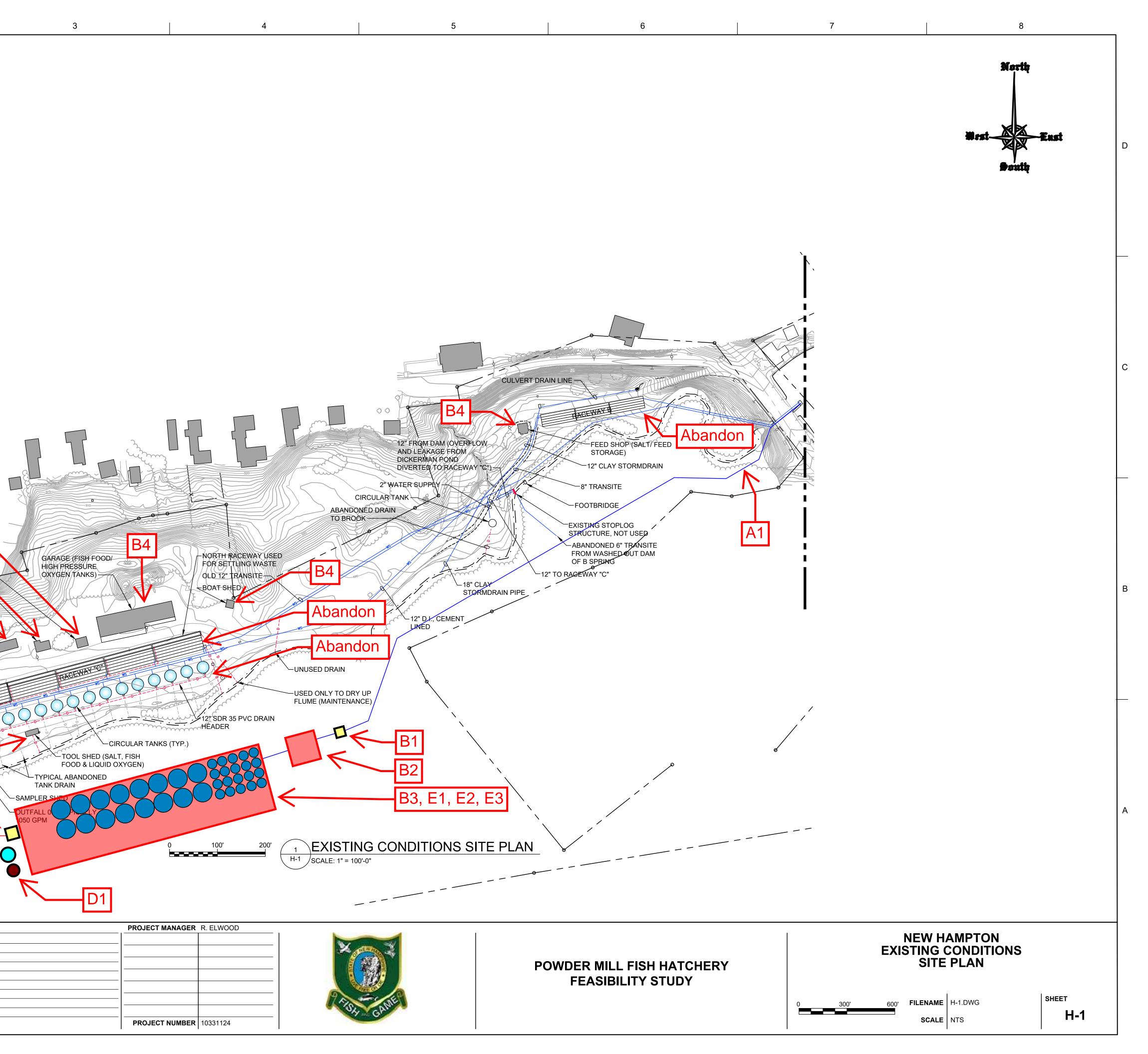


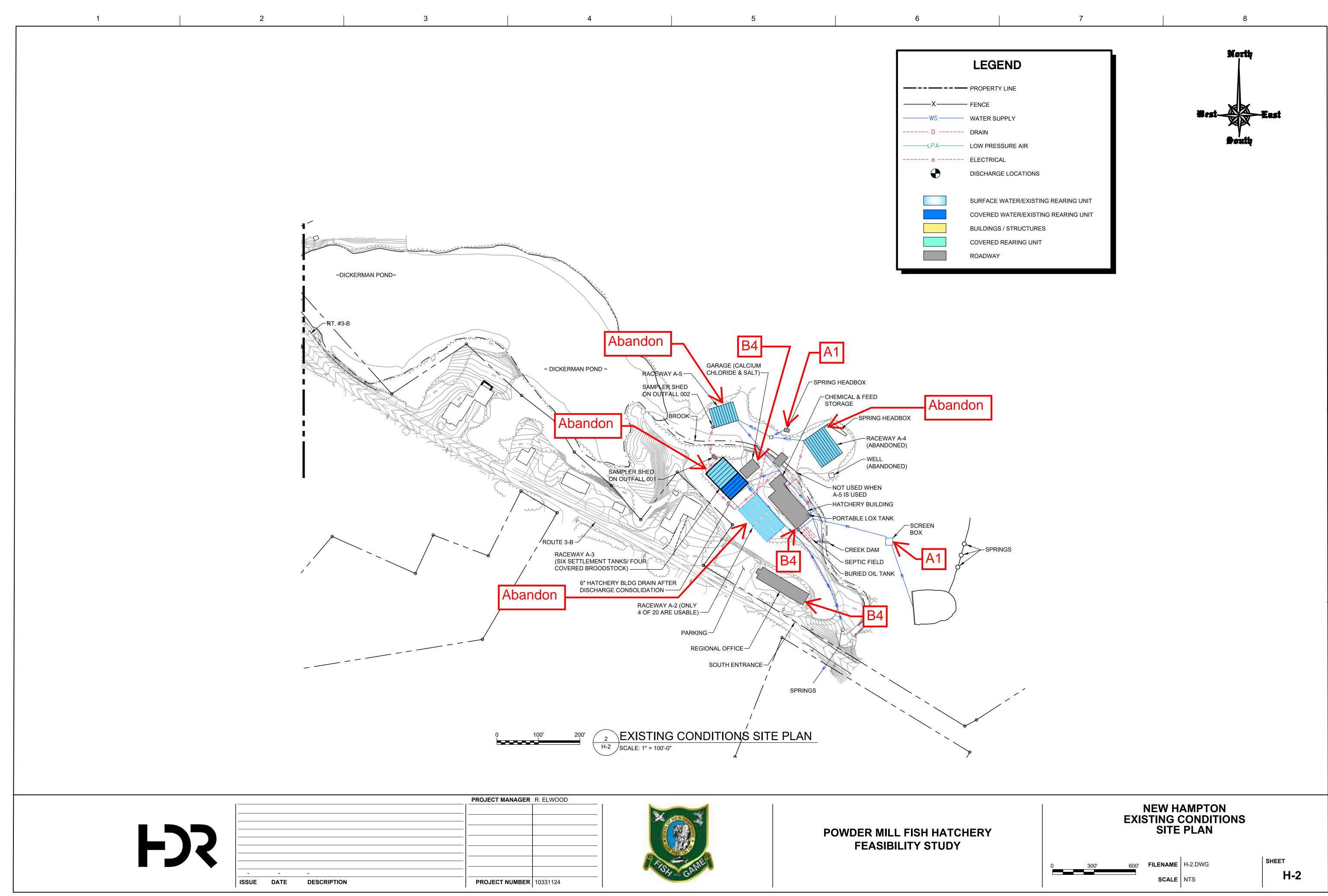
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-ISSUE DATE DESCRIPTION

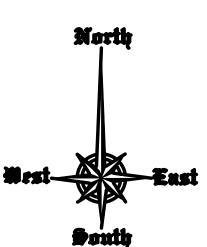
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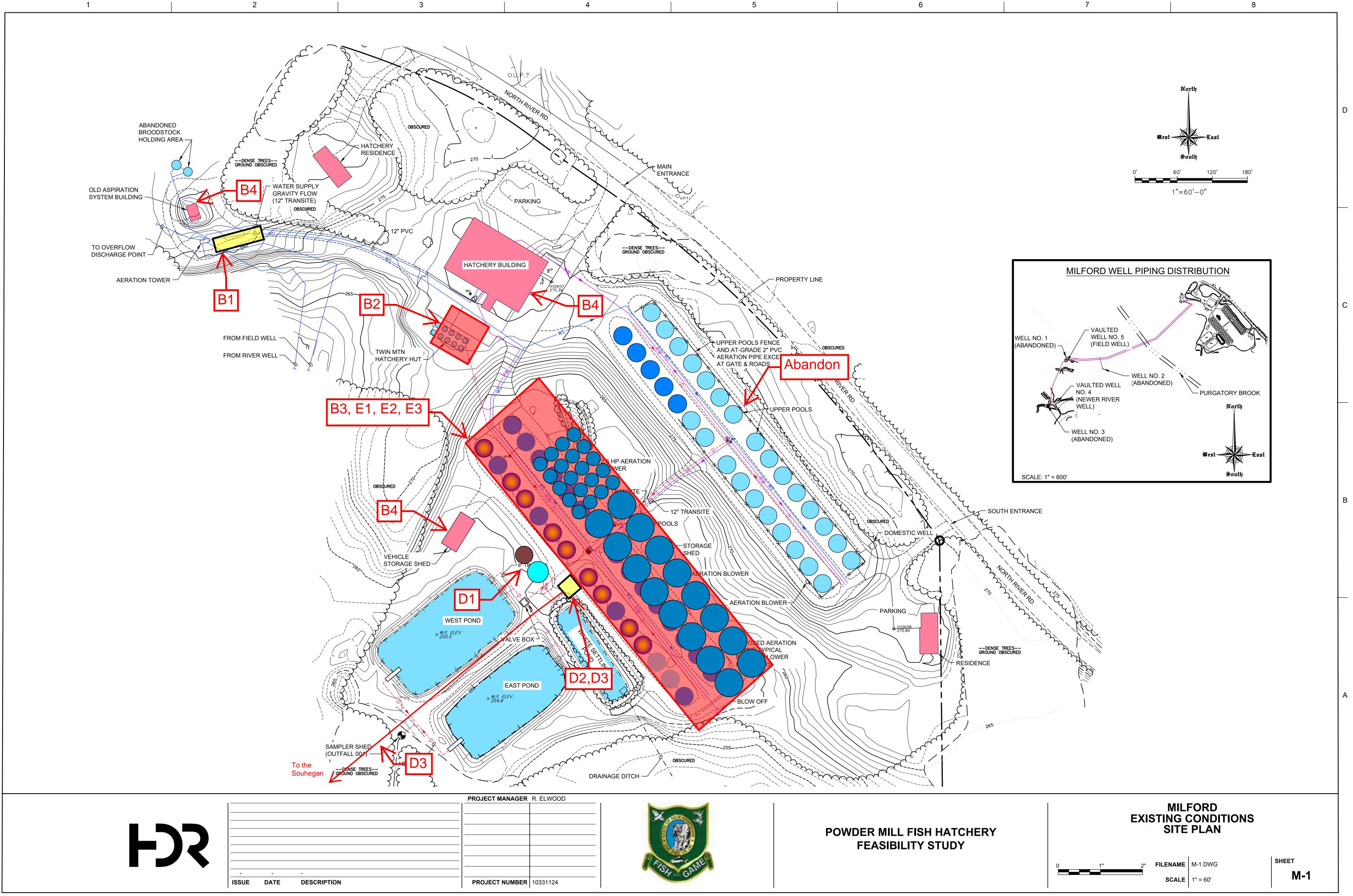






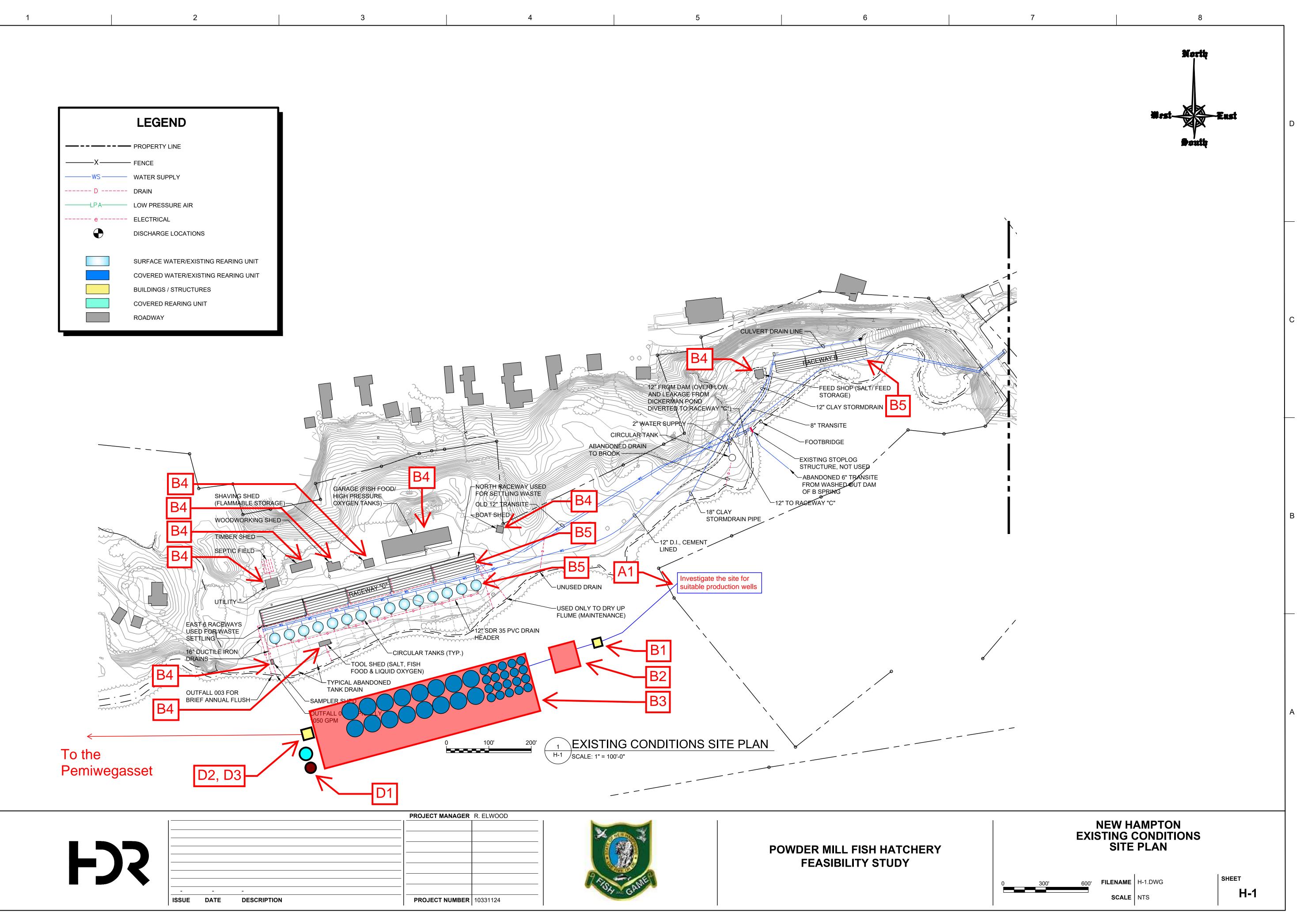


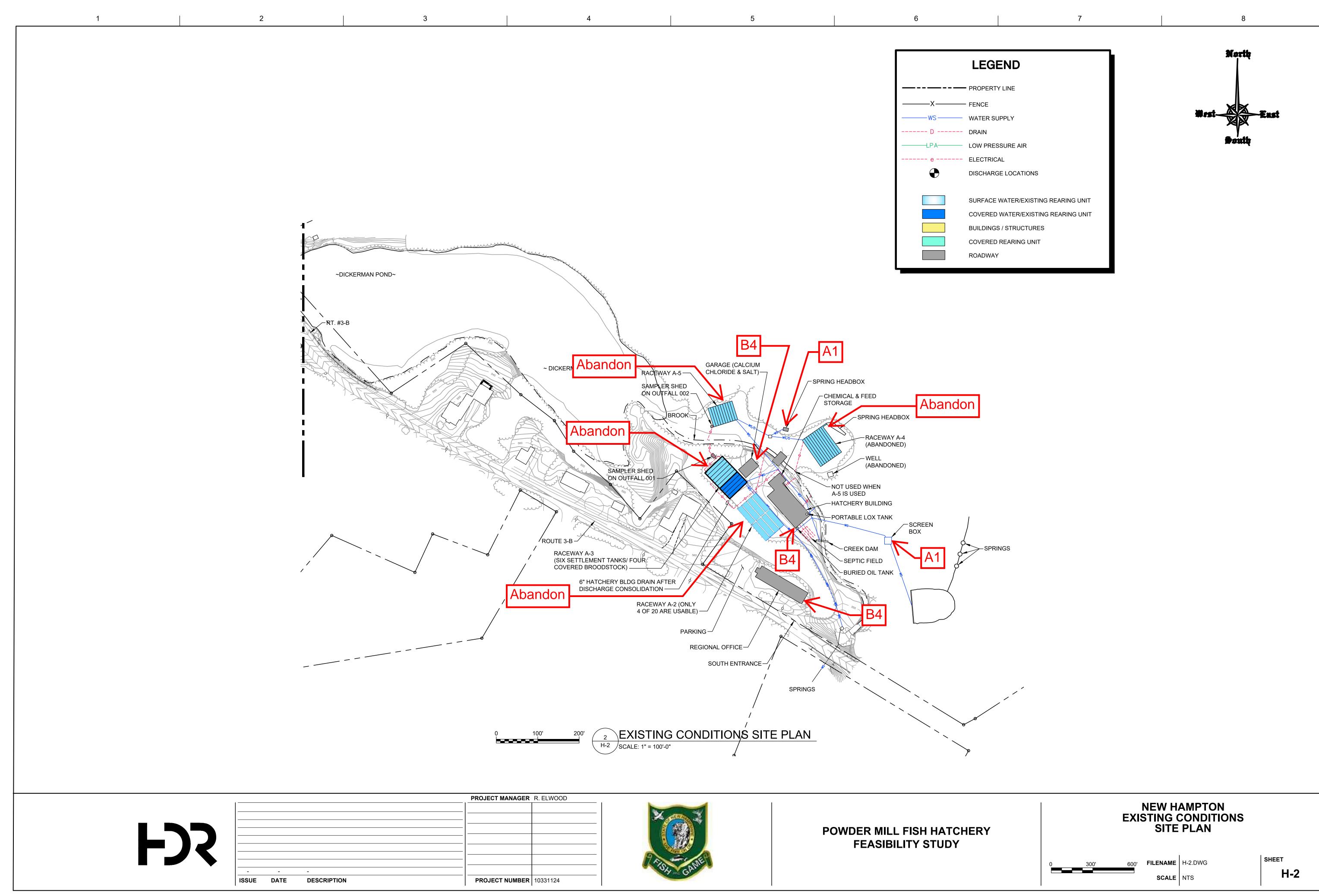
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| | LEGEND |
|------------|-------------------------------------|
| | PROPERTY LINE |
| X | - FENCE |
| WS | WATER SUPPLY |
| D | DRAIN |
| LPA | LOW PRESSURE AIR |
| e | ELECTRICAL |
| \bigcirc | DISCHARGE LOCATIONS |
| | |
| | SURFACE WATER/EXISTING REARING UNIT |
| | COVERED WATER/EXISTING REARING UNIT |
| | BUILDINGS / STRUCTURES |
| | COVERED REARING UNIT |
| | ROADWAY |
| | |
| | |

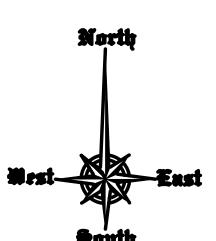








| EGEND |
|-----------------------------------|
| DPERTY LINE |
| ICE |
| TER SUPPLY |
| AIN |
| V PRESSURE AIR |
| CTRICAL |
| CHARGE LOCATIONS |
| |
| RFACE WATER/EXISTING REARING UNIT |
| /ERED WATER/EXISTING REARING UNIT |
| LDINGS / STRUCTURES |
| /ERED REARING UNIT |
| |



А

С

Appendix C Process Calculations

Circular Tank Calculations

Feed Training Tanks when in use are usually on flow thru first-use water only

| Tank Data | | | | | | | | | | Hour | ly Exchange | Rate |
|----------------------|--------|------|-------|---------|---------|---------|------------|---------|-----|-------|-------------|------|
| | Radius | Dia. | Depth | cuft | gallons | # Units | Total cuft | R= | R=1 | R=1.3 | R=2 | R=3 |
| 6' dia. Circular TKS | 3 | 6 | 4 | 113.097 | 846 | 20 | 2,262 | gpm@ | 14 | 19 | 28 | 42 |
| Usable Vol | 3 | 6 | 3 | 84.823 | 634 | 20 | 1,696 | gpm@ | 11 | 16 | 21.1 | 32 |
| | | | CM= | 2.40292 | | | | gpmTot. | 211 | 317 | 423 | 634 |

REARING UNIT DATA

REARING UNIT DATA

| Tank Data | | | | | | | | | | Hour | ly Exchange | Rate |
|------------------------|--------|------|-------|--------|---------|---------|------------|---------|-------|-------|-------------|-------|
| | Radius | Dia. | Depth | cuft | gallons | # Units | Total cuft | R= | R=1 | R=1.3 | R=2 | R=3 |
| 20 ' dia. Circular TKS | 10 | 20 | 4 | 1256.6 | 9,400 | 20 | 25,133 | gpm@ | 157 | 209 | 313 | 470 |
| Usable Vol | 10 | 20 | 3 | 942.5 | 7,050 | 20 | 18,850 | gpm@ | 117 | 176 | 235.0 | 352 |
| | | | CM= | 26.7 | | | | gpmTot. | 2,350 | 3,525 | 4,700 | 7,050 |

REARING UNIT DATA

| Tank Data | | | | | | | | | | Hour | ly Exchange | Rate |
|------------------------|--------|------|-------|---------|---------|---------|------------|---------|-------|--------|-------------|--------|
| | Radius | Dia. | Depth | cuft | gallons | # Units | Total cuft | R= | R=1 | R=1.3 | R=2 | R=3 |
| 40 ' dia. Circular TKS | 20 | 40 | 4 | 5026.55 | 37,599 | 16 | 80,425 | gpm@ | 627 | 836 | 1,253 | 1,880 |
| Usable Vol | 20 | 40 | 3 | 3769.91 | 28,199 | 16 | 60,319 | gpm@ | 470 | 627 | 940 | 1,410 |
| | | | CM= | 106.796 | | | | gpmTot. | 7,520 | 10,026 | 15,039 | 22,559 |

Theoretical Carring Capacity DATA

| | D | D | D | D |
|-----------------|---------|---------|---------|---------|
| | lbs /CF | lbs /CF | lbs /CF | lbs /CF |
| Density Ibs/CF | 2 | 3 | 4 | 5 |
| PER unit LBS= | 170 | 254 | 339 | 424 |
| Total Lbs | 3,393 | 5,089 | 6,786 | 8,482 |
| Loading LBS/GPM | 10.7 | 16.0 | 21.4 | 26.7 |

Theoretical Carring Capacity DATA

| | D | D | D | D |
|-----------------|---------|---------|---------|---------|
| | lbs /CF | lbs /CF | lbs /CF | lbs /CF |
| Density Ibs/CF | 2 | 3 | 4 | 5 |
| PER unit LBS= | 1,885 | 2,827 | 3,770 | 4,712 |
| Total Lbs | 37,699 | 56,549 | 75,398 | 94,248 |
| Loading LBS/GPM | 10.7 | 16.0 | 21.4 | 26.7 |

Theoretical Carring Capacity DATA

| | D | D | D | D |
|-----------------|---------|---------|---------|---------|
| | lbs /CF | lbs /CF | lbs /CF | lbs /CF |
| Density Ibs/CF | 2 | 3 | 4 | 5 |
| PER unit LBS= | 7,540 | 11,310 | 15,080 | 18,850 |
| Total Lbs | 120,637 | 180,956 | 241,274 | 301,593 |
| Loading LBS/GPM | 12.0 | 18.0 | 24.1 | 30.1 |

| | | gpm |
|-------------|------|--------|
| | | 13,551 |
| 95% recirc. | 0.95 | 12,874 |
| 5% makeup | 0.05 | 678 |
| 75% recirc. | 0.75 | 10,163 |
| 25% makeup | 0.25 | 3,388 |

Bio Programming to determine P Load

Option:

10% treatment efficiency, 75% recirc

| Inputs and Constants | | |
|----------------------|--|------------------------------------|
| Total Phos | Parameter | |
| 0.75 | Recirculation Rate (R) | Enter facility recirculation rate |
| 0.10 | Enter treatment removal efficiency | Enter treatment removal efficiency |
| 3464.00 | gpm Flow Rate | Enter total flow rate |
| 0.01 | mg/L Background TP (waste _{new}) | Enter known TP in background |
| 482.00 | lb/day Daily Feed Rate | Enter daily feed in pounds |
| 0.005 | kg TP per kg feed | Enter kg TP produced per kg fed |
| 218.63 | kg/day Daily Feed Rate | Calculated |
| 1.09 | kg/day TP Generated (r _{waste}) | Calculated |
| 1093156.72 | mg/day TP Generated | Calculated |
| 2598 | gpm Q recirc | Calculated gpm recirculated |
| 866.00 | gpm Q makeup | Calculated makeup |

0.19 mg/L (waste_{out})

Calculated TP discharge

| Date Entry Cell |
|--------------------|
| No Data Entry Cell |
| Result Cell |

Option:

10% treatment efficiency, 95% recirc

| Inputs and Constants | | |
|----------------------|--|------------------------------------|
| Total Phos | Parameter | |
| 0.95 | Recirculation Rate (R) | Enter facility recirculation rate |
| 0.10 | Enter treatment removal efficiency | Enter treatment removal efficiency |
| 3464.00 | gpm Flow Rate | Enter total flow rate |
| 0.01 | mg/L Background TP (waste _{new}) | Enter known TP in background |
| 482.00 | lb/day Daily Feed Rate | Enter daily feed in pounds |
| 0.005 | kg TP per kg feed | Enter kg TP produced per kg fed |
| 218.63 | kg/day Daily Feed Rate | Calculated |
| 1.09 | kg/day TP Generated (r _{waste}) | Calculated |
| 1093156.72 | mg/day TP Generated | Calculated |
| 3290.8 | gpm Q recirc | Calculated gpm recirculated |
| 173.20 | gpm Q makeup | Calculated makeup |

0.40 mg/L (waste_{out})

Calculated TP discharge

| Date Entry Cell | |
|--------------------|--|
| No Data Entry Cell | |
| Result Cell | |

Chemical usage and costing calculations

| | Coagulation gal/year chemical usage (4 months of operation from HDR | | | | | | | |
|---|---|-------------|-------|-------------|--|--|--|--|
| | modelling) | | | | | | | |
| | | Alt 1 | Alt 2 | Alt 3 | | | | |
| | Ferric | <u>9977</u> | 23117 | <u>9855</u> | | | | |
| _ | 25% Caustic w Ferric | 13383 | 31268 | 13383 | | | | |
| | Alum | 12045 | 7908 | 8395 | | | | |
| | 25% Caustic w Alum | 10098 | 6570 | 6935 | | | | |

| Membrane Clean gal/year chemical usage (From Membrane Proposal) | | | | | | | | | | |
|---|-------------------|-------|-------|--|--|--|--|--|--|--|
| | Alt 1 Alt 2 Alt 3 | | | | | | | | | |
| Sulfuric | | | | | | | | | | |
| Нуро | 18300 | 18300 | 6900 | | | | | | | |
| Citric | 38500 | 38500 | 14500 | | | | | | | |
| Sodium Bisulfate | 4400 | 4400 | 1700 | | | | | | | |

Г

| | lbs/gal from | \$/lb from | ¢/ml |
|----------------------|--------------|------------|---------|
| | supplier | supplier | \$/gal |
| Ferric | 11.74 | \$ 0.26 | \$ 3.05 |
| 25% Caustic w Ferric | 10.66 | \$ 0.18 | \$ 1.92 |
| Alum | 11.34 | \$ 0.16 | \$ 1.81 |
| 25% Caustic w Alum | 10.66 | \$ 0.18 | \$ 1.92 |
| | | | |
| | | | |
| | | | |
| | | | |
| Sulfuric | 15.3 | \$ 0.16 | \$ 2.45 |
| Нуро | 10.1 | | \$ 2.50 |
| Citric | 10.35 | \$ 0.80 | \$ 8.28 |
| Sodium Bisulfate | 11.34 | \$ 0.30 | \$ 3.40 |

| Annual Coagulation Chemical Costs | | | | | | | | | | |
|-----------------------------------|-------|----------------------|--------------------|----------------------|---------|----------------------|--|--|--|--|
| | Alt : | 1 A | Alt | 2 A | Alt 3 A | | | | | |
| Ferric | \$ | 30,452.78 | \$ | 70,561.31 | \$ | 30,081.40 | | | | |
| 25% Caustic w Ferric | ¢ | 25 670 94 | ¢ | 50 007 68 | ¢ | 25 670 94 | | | | |
| Alum | \$ | 21,854.45 | , \$ | 14,348.88 | \$ | 15,231.89 | | | | |
| 25%Caustic w Alum | \$ | 19,376.68 | \$ | 12,606.52 | \$ | 13,306.88 | | | | |
| Coagulation totals | \$ | 41,231.13 | \$ | 26,955.40 | \$ | 28,538.77 | | | | |

| Annual Membrane Clean Chemical Costs | | | | | | | | | | |
|--------------------------------------|-----|------------|-----|------------|-------------|------------|--|--|--|--|
| | Alt | 1 A & B | Alt | 2 A & B | Alt 3 A & B | | | | | |
| Sulfuric | \$ | - | \$ | - | \$ | - | | | | |
| Нуро | \$ | 45,750.00 | \$ | 45,750.00 | \$ | 17,250.00 | | | | |
| Citric | \$ | 318,780.00 | \$ | 318,780.00 | \$ | 120,060.00 | | | | |
| Sodium Bisulfate | \$ | 14,968.80 | \$ | 14,968.80 | \$ | 5,783.40 | | | | |
| Mebrane Clean Totals | \$ | 379,498.80 | \$ | 379,498.80 | \$ | 143,093.40 | | | | |

Density from a SDS

Alum costs included in report because costs were lower

Cost reported in \$/gal from supplier

Mix and React tank optimization and costing calculations

| AVG Exist | | 3745 | Mixing tanl | volume in ft3 | 15019.04953 | | Alter | native 1A No Rec | circula | tion | |
|--------------|-----------|-------------|-------------|---------------|---------------|---------------|-------|------------------|---------|------------------|----------------|
| Inner Radius | | Inner | Sidewall | Tank cubic | | | | | | | |
| (ft) | Radius ft | Diameter ft | depth ft | yards | Tank Cost | Excavation yd | | vation Cost | | +Excavation Cost | |
| 10 | | | | | | 32610.4 | | 1,630,518.33 | | 2,063,274.98 | |
| 10.5 | | | | | | 25231.9 | | 1,261,596.62 | | 1,680,331.32 | |
| 11 | | | | | | 19852.3 | | 992,615.58 | | 1,399,361.14 | |
| 11.5 | 13.5 | 23 | 38.1 | | | 15864.6 | | 793,231.96 | \$ | 1,189,762.42 | |
| 12 | 14 | 24 | 35.2 | 258.6 | \$ 387,876.35 | 12863.5 | \$ | 643,174.22 | \$ | 1,031,050.57 | |
| 12.5 | 14.5 | 25 | 32.6 | 253.7 | \$ 380,606.32 | 10572.9 | \$ | 528,644.30 | \$ | 909,250.63 | |
| 13 | 15 | 26 | 30.3 | 249.7 | \$ 374,572.23 | 8801.8 | \$ | 440,087.96 | \$ | 814,660.19 | |
| 13.5 | 15.5 | 27 | 28.2 | 246.4 | \$ 369,649.08 | 7415.7 | \$ | 370,784.02 | \$ | 740,433.10 | |
| 14 | 16 | 28 | 26.4 | 243.8 | \$ 365,730.73 | 6318.7 | \$ | 315,934.54 | \$ | 681,665.27 | |
| 14.5 | 16.5 | 29 | 24.7 | 241.8 | \$ 362,726.44 | 5441.4 | \$ | 272,067.58 | \$ | 634,794.03 | |
| 15 | 17 | 30 | 23.2 | 240.4 | \$ 360,558.21 | 4732.8 | \$ | 236,638.73 | \$ | 597,196.94 | |
| 15.5 | 17.5 | 31 | 21.9 | 239.4 | \$ 359,158.58 | 4155.2 | \$ | 207,761.08 | \$ | 566,919.67 | |
| 16 | 18 | 32 | 20.7 | 239.0 | \$ 358,468.98 | 3680.4 | \$ | 184,019.74 | \$ | 542,488.72 | |
| 16.5 | 18.5 | 33 | 19.6 | 239.0 | \$ 358,438.23 | 3286.9 | \$ | 164,342.67 | \$ | 522,780.91 | |
| 17 | 19 | 34 | 18.5 | 239.3 | \$ 359,021.50 | 2958.2 | \$ | 147,909.60 | \$ | 506,931.10 | |
| 17.5 | 19.5 | 35 | 17.6 | 240.1 | \$ 360,179.29 | 2681.7 | \$ | 134,087.08 | \$ | 494,266.38 | |
| 18 | 20 | 36 | 16.8 | 241.3 | \$ 361,876.70 | 2447.6 | \$ | 122,381.68 | \$ | 484,258.38 | |
| 18.5 | 20.5 | 37 | 16.0 | 242.7 | \$ 364,082.75 | 2248.1 | \$ | 112,405.83 | \$ | 476,488.58 | |
| 19 | 21 | 38 | 15.2 | 244.5 | \$ 366,769.89 | 2077.1 | \$ | 103,852.73 | \$ | 470,622.62 | |
| 19.5 | 21.5 | 39 | 14.6 | 246.6 | \$ 369,913.48 | 1929.6 | \$ | 96,477.74 | \$ | 466,391.22 | |
| 20 | 22 | 40 | 14.0 | 249.0 | \$ 373,491.48 | 1801.7 | \$ | 90,084.35 | \$ | 463,575.83 | |
| 20.5 | 22.5 | 41 | 13.4 | 251.7 | \$ 377,484.06 | 1690.3 | \$ | 84,513.72 | \$ | 461,997.78 | |
| 21 | 23 | 42 | 12.8 | 254.6 | \$ 381,873.37 | 1592.7 | \$ | 79,636.60 | \$ | 461,509.97 | Min Total Cost |
| 21.5 | 23.5 | 43 | 12.3 | 257.8 | \$ 386,643.27 | 1506.9 | \$ | 75,347.18 | \$ | 461,990.45 | |
| 22 | 24 | 44 | 11.9 | 261.2 | \$ 391,779.16 | 1431.2 | \$ | 71,558.34 | \$ | 463,337.50 | |
| 22.5 | 24.5 | 45 | 11.4 | 264.8 | \$ 397,267.78 | 1364.0 | \$ | 68,197.96 | \$ | 465,465.73 | |
| 23 | | | | | | 1304.1 | | 65,206.00 | | 468,303.05 | |
| 23.5 | | | | | | 1250.6 | | 62,532.25 | | 471,788.24 | |
| 24 | | | | | | 1202.7 | | 60,134.51 | | 475,869.04 | |
| 24.5 | | | | | | 1159.5 | | 57,977.12 | | 480,500.59 | |
| 25 | | | | | | 1120.6 | | 56,029.85 | | 485,644.23 | |
| | _, | | 510 | _0011 | | | Ŧ | | Ŧ | , | |

| 75% recirc l | Flow (GPM) | 3566.3 | Mixing ta | nk volume ft3 | | 14302.3862 | | Alte | ernative 2A 75% re | ecirc | | |
|--------------|------------|-------------|-----------|---------------|--------|------------|---------------|------|--------------------|-------|------------------|----------------|
| Inner Radius | Outer | Inner | Sidewall | Tank cubic | | | | | | | | |
| (ft) | Radius ft | Diameter ft | Depth ft | yards | Tank C | ost | Excavation yd | Exc | avation Cost | Tank | +Excavation Cost | |
| 10 | 12 | 20 | 47.5 | 276.8 | \$ | 415,238.21 | 28508.6 | \$ | 1,425,430.52 | \$ | 1,840,668.73 | |
| 10.5 | 12.5 | 21 | 43.3 | 268.1 | \$ | 402,122.70 | 22096.2 | \$ | 1,104,809.26 | \$ | 1,506,931.97 | |
| 11 | 13 | 22 | 39.6 | 260.6 | \$ | 390,951.33 | 17417.2 | \$ | 870,857.97 | \$ | 1,261,809.30 | |
| 11.5 | 13.5 | 23 | 36.4 | 254.3 | \$ | 381,477.66 | 13945.9 | \$ | 697,294.63 | \$ | 1,078,772.30 | |
| 12 | 14 | 24 | 33.6 | 249.0 | \$ | 373,498.85 | 11331.1 | \$ | 566,554.33 | \$ | 940,053.18 | |
| 12.5 | 14.5 | 25 | 31.1 | 244.6 | \$ | 366,846.39 | 9333.5 | \$ | 466,676.53 | \$ | 833,522.91 | |
| 13 | 15 | 26 | 28.9 | 240.9 | \$ | 361,379.21 | 7787.5 | \$ | 389,375.80 | \$ | 750,755.02 | |
| 13.5 | 15.5 | 27 | 27.0 | 238.0 | \$ | 356,978.30 | 6576.4 | \$ | 328,820.96 | \$ | 685,799.26 | |
| 14 | 16 | 28 | 25.2 | 235.7 | \$ | 353,542.58 | 5616.9 | \$ | 280,847.37 | \$ | 634,389.95 | |
| 14.5 | 16.5 | 29 | 23.7 | 234.0 | \$ | 350,985.62 | 4848.8 | \$ | 242,439.92 | \$ | 593,425.54 | |
| 15 | 17 | 30 | 22.2 | 232.8 | \$ | 349,233.16 | 4227.8 | \$ | 211,387.77 | \$ | 560,620.93 | |
| 15.5 | 17.5 | 31 | 20.9 | 232.1 | \$ | 348,220.95 | 3721.0 | \$ | 186,050.54 | \$ | 534,271.50 | |
| 16 | 18 | 32 | 19.8 | 231.9 | \$ | 347,893.22 | 3303.9 | \$ | 165,197.49 | \$ | 513,090.70 | |
| 16.5 | 18.5 | 33 | 18.7 | 232.1 | \$ | 348,201.23 | 2957.9 | \$ | 147,895.53 | \$ | 496,096.76 | |
| 17 | 19 | 34 | 17.8 | 232.7 | \$ | 349,102.29 | 2668.6 | \$ | 133,430.31 | \$ | 482,532.59 | |
| 17.5 | 19.5 | 35 | 16.9 | 233.7 | \$ | 350,558.78 | 2425.0 | \$ | 121,249.82 | \$ | 471,808.60 | |
| 18 | 20 | 36 | 16.1 | 235.0 | \$ | 352,537.47 | 2218.5 | \$ | 110,923.79 | \$ | 463,461.25 | |
| 18.5 | 20.5 | 37 | 15.3 | 236.7 | \$ | 355,008.86 | 2042.3 | \$ | 102,114.03 | \$ | 457,122.88 | |
| 19 | 21 | 38 | 14.6 | 238.6 | \$ | 357,946.70 | 1891.1 | \$ | 94,552.66 | \$ | 452,499.37 | |
| 19.5 | 21.5 | 39 | 14.0 | 240.9 | \$ | 361,327.55 | 1760.5 | \$ | 88,025.92 | \$ | 449,353.48 | |
| 20 | 22 | 40 | 13.4 | 243.4 | \$ | 365,130.41 | 1647.2 | \$ | 82,362.01 | \$ | 447,492.41 | |
| 20.5 | 22.5 | 41 | 12.8 | 246.2 | \$ | 369,336.39 | 1548.4 | \$ | 77,421.92 | \$ | 446,758.31 | Min Total Cost |
| 21 | 23 | 42 | 12.3 | 249.3 | \$ | 373,928.50 | 1461.8 | \$ | 73,092.48 | \$ | 447,020.98 | |
| 21.5 | 23.5 | 43 | 11.8 | 252.6 | \$ | 378,891.37 | 1385.6 | \$ | 69,280.98 | \$ | 448,172.35 | |
| 22 | 24 | 44 | 11.4 | 256.1 | \$ | 384,211.09 | 1318.2 | \$ | 65,911.02 | \$ | 450,122.11 | |
| 22.5 | 24.5 | 45 | 11.0 | 259.9 | \$ | 389,875.04 | 1258.4 | \$ | 62,919.32 | \$ | 452,794.36 | |
| 23 | 25 | 46 | 10.6 | 263.9 | \$ | 395,871.72 | 1205.1 | \$ | 60,253.16 | \$ | 456,124.88 | |
| 23.5 | 25.5 | 47 | 10.2 | 268.1 | \$ | 402,190.65 | 1157.4 | \$ | 57,868.40 | \$ | 460,059.05 | |
| 24 | 26 | 48 | 9.9 | 272.5 | \$ | 408,822.27 | 1114.6 | \$ | 55,727.92 | \$ | 464,550.19 | |
| 24.5 | | | 9.6 | 277.2 | \$ | 415,757.81 | 1076.0 | \$ | 53,800.36 | | 469,558.16 | |
| 25 | 27 | 50 | 9.3 | 282.0 | \$ | 422,989.22 | 1041.2 | \$ | 52,059.07 | \$ | 475,048.29 | |
| | | | | | | | | | | | | |

| 95% recirc | Flow gpm | 713.3 | Mixing ta | ink volume ft3 | 2860.637658 | 6 | Alternative 3A | | | |
|--------------|-----------|-------------|-----------|----------------|---------------|---------------|-----------------|-----------|--------------|----------------|
| Inner Radius | Outer | Inner | Sidewall | Tank cubic | | | | | | |
| (ft) | Radius ft | Diameter ft | Depth ft | yards | Tank Cost | Excavation yd | Excavation Cost | Tank+Exca | vation Cost | |
| 10 | 12 | 20 | 11.1 | 90.4 | \$ 135,551.02 | 559.8 | \$ 27,989.98 | \$ | 163,541.00 | |
| 10.5 | 12.5 | 21 | 10.3 | 91.3 | \$ 136,907.07 | 479.7 | \$ 23,984.25 | \$ | 160,891.31 | |
| 11 | 13 | 22 | 9.5 | 92.5 | \$ 138,791.58 | 418.5 | \$ 20,923.81 | \$ | 159,715.40 | |
| 11.5 | 13.5 | 23 | 8.9 | 94.1 | \$ 141,155.28 | 370.9 | \$ 18,544.71 | \$ | 159,699.99 I | Vin Total Cost |
| 12 | 14 | 24 | 8.3 | 96.0 | \$ 143,957.59 | 333.3 | \$ 16,665.94 | \$ | 160,623.53 | |
| 12.5 | 14.5 | 25 | 7.8 | 98.1 | \$ 147,164.82 | 303.2 | \$ 15,160.95 | \$ | 162,325.76 | |
| 13 | 15 | 26 | 7.4 | 100.5 | \$ 150,748.73 | 278.8 | \$ 13,939.59 | \$ | 164,688.32 | |
| 13.5 | 15.5 | 27 | 7.0 | 103.1 | \$ 154,685.54 | 258.7 | \$ 12,936.59 | \$ | 167,622.13 | |
| 14 | 16 | 28 | 6.6 | 106.0 | \$ 158,955.02 | 242.1 | \$ 12,103.95 | \$ | 171,058.96 | |
| 14.5 | 16.5 | 29 | 6.3 | 109.0 | \$ 163,539.88 | 228.1 | \$ 11,405.83 | \$ | 174,945.71 | |
| 15 | 17 | 30 | 6.0 | 112.3 | \$ 168,425.28 | 216.3 | \$ 10,815.17 | \$ | 179,240.45 | |
| 15.5 | 17.5 | 31 | 5.8 | 115.7 | \$ 173,598.36 | 206.2 | \$ 10,311.24 | \$ | 183,909.60 | |
| 16 | 18 | 32 | 5.6 | 119.4 | \$ 179,047.97 | 197.6 | \$ 9,877.98 | \$ | 188,925.95 | |
| 16.5 | 18.5 | 33 | 5.3 | 123.2 | \$ 184,764.36 | 190.1 | \$ 9,502.84 | \$ | 194,267.19 | |
| 17 | 19 | 34 | 5.2 | 127.2 | \$ 190,738.99 | 183.5 | \$ 9,175.88 | \$ | 199,914.87 | |
| 17.5 | 19.5 | 35 | 5.0 | 131.3 | \$ 196,964.33 | 177.8 | \$ 8,889.20 | \$ | 205,853.53 | |
| 18 | 20 | 36 | 4.8 | 135.6 | \$ 203,433.75 | 172.7 | \$ 8,636.40 | \$ | 212,070.15 | |
| 18.5 | 20.5 | 37 | 4.7 | 140.1 | \$ 210,141.33 | 168.2 | \$ 8,412.33 | \$ | 218,553.67 | |
| 19 | 21 | 38 | 4.5 | 144.7 | \$ 217,081.84 | 164.3 | \$ 8,212.75 | \$ | 225,294.59 | |
| 19.5 | 21.5 | 39 | 4.4 | 149.5 | \$ 224,250.58 | 160.7 | \$ 8,034.18 | \$ | 232,284.76 | |
| 20 | 22 | 40 | 4.3 | 154.4 | \$ 231,643.34 | 157.5 | \$ 7,873.73 | \$ | 239,517.07 | |
| 20.5 | 22.5 | 41 | 4.2 | 159.5 | \$ 239,256.36 | 154.6 | \$ 7,728.99 | \$ | 246,985.35 | |
| 21 | 23 | 42 | 4.1 | 164.7 | \$ 247,086.24 | 152.0 | \$ 7,597.94 | \$ | 254,684.17 | |
| 21.5 | 23.5 | 43 | 4.0 | 170.1 | \$ 255,129.89 | 149.6 | \$ 7,478.86 | \$ | 262,608.75 | |
| 22 | 24 | 44 | 3.9 | 175.6 | \$ 263,384.55 | 147.4 | \$ 7,370.32 | \$ | 270,754.86 | |
| 22.5 | 24.5 | 45 | 3.8 | 181.2 | \$ 271,847.67 | 145.4 | \$ 7,271.06 | \$ | 279,118.74 | |
| 23 | 25 | 46 | 3.7 | 187.0 | \$ 280,516.97 | 143.6 | \$ 7,180.04 | \$ | 287,697.02 | |
| 23.5 | 25.5 | 47 | 3.6 | 192.9 | \$ 289,390.35 | 141.9 | \$ 7,096.35 | \$ | 296,486.70 | |
| 24 | 26 | 48 | 3.6 | 199.0 | \$ 298,465.90 | 140.4 | \$ 7,019.18 | \$ | 305,485.08 | |
| 24.5 | 26.5 | 49 | 3.5 | 205.2 | \$ 307,741.85 | 139.0 | \$ 6,947.86 | \$ | 314,689.71 | |
| 25 | 27 | 50 | 3.5 | 211.5 | \$ 317,216.61 | 137.6 | \$ 6,881.79 | \$ | 324,098.40 | |

Mix/React tank constants and costing

1500 \$/cy reinforced concrete tank

50 \$/cy for excavation

2 ft wall thickness

1 ft over excavation

3 water 3 feet above grade.

2 ft freeboard

5 ft of tank above ground

2 2-1 excavation (1 foot down 2 foot out)

30 min of HRT

3.14159 pi

Media Costs and Vessel Requirements

| Design Parameters | | | | Influent s-phosp average – 0.4 m | | 681 833 1 1 1 1 1 10 681 336 681 336 672 10 79 10 4.3 8.7 | |
|---------------------------|---------|---------|---------|-------------------------------------|---------|---|---------|
| Flow Rate | MGD | 5.4 | 5.4 6.5 | | 5.9 | 0.98 | 1.2 |
| Flow Rate | gpm | 3,750 | 4,514 | 3,403 | 4,097 | 681 | 833 |
| Number of Vessels | | 4 | 4 | 3 | 3 | 1 | 1 |
| Redundant Vessels (HDR) | | 2 | 2 | 2 | 2 | 1 | 1 |
| Vessel Diameter | feet | 12 | 12 | 12 | 12 | 10 | 10 |
| Flow per Vessel | gpm | 938 | 1128 | 1134 | 1366 | 681 | 833 |
| Media Volume per vessel | ft3 | 420 | 420 | 420 | 420 | 336 | 336 |
| Media Volume total onsite | ft3 | 3360 | 3360 | 2520 | 2520 | 672 | 672 |
| Vessel Area | ft2 | 113 | 113 | 113 | 113 | 79 | 79 |
| Bed Depth | feet | 3.7 | 3.7 | 3.7 | 3.7 | 4.3 | 4.3 |
| Linear Velocity: | gpm/ft2 | 8.3 | 10 | 10 | 12.1 | 8.7 | 10.6 |
| Specific Flowrate | gpm/ft3 | 2.2 | 2.7 | 2.7 | 3.3 | 2 | 2.5 |
| Empty Bed Contact Time | minutes | 3.4 | 2.8 | 2.8 | 2.3 | 3.7 | 3 |
| Projected throughput | BV | 300,000 | 300,000 | 183,000 | 183,000 | 163,000 | 163,000 |
| Days between exchanges | days | 698 | 580 | 352 | 292 | 418 | 341 |

Based on recent pricing of other projects each vessel is estimated at \$250,000 (HDR)

| Budgetary cost of Vessels (HDR) | \$ 250,000.00 | | \$ 1,500,000.00 | | \$ 1,250,000.00 | | \$ 500,000.00 |
|--|---------------|--------------|-----------------|--------------|-----------------|-------------|---------------|
| Budgetary cost of Ferrix A33E per cu ft | \$500 | | | | | | |
| Cost of initial fill (Media Capital Cost) | | \$1,680,000 | \$1,680,000 | \$1,260,000 | \$1,260,000 | \$336,000 | \$336,000 |
| | | | | | | | |
| Budgetary Cost of RAM300 per cu ft | \$250 | | | | | | |
| cost per regen | | \$420,000 | \$420,000 | \$315,000 | \$315,000 | \$84,000 | \$84,000 |
| | | | | | | | |
| yearly use factor: days use/year | | 0.52 | 0.63 | 1.04 | 1.25 | 0.87 | 1.07 |
| Esimatated cost per year assuming 24/7 operation based on regeneration costs | | \$219,585.56 | \$264,315.95 | \$326,645.19 | \$393,307.47 | \$73,344.87 | \$89,810.05 |
| Assuming 4 months operation (Media Replacement O&M, HDR) | | | \$88,105.32 | | \$131,102.49 | | \$29,936.68 |

Circular Tank Calculations

Feed Training Tanks when in use are usually on flow thru first-use water only

| Tank Data | | | | | | | | | | Hour | ly Exchange | Rate |
|----------------------|--------|------|-------|---------|---------|---------|------------|---------|-----|-------|-------------|------|
| | Radius | Dia. | Depth | cuft | gallons | # Units | Total cuft | R= | R=1 | R=1.3 | R=2 | R=3 |
| 6' dia. Circular TKS | 3 | 6 | 4 | 113.097 | 846 | 20 | 2,262 | gpm@ | 14 | 19 | 28 | 42 |
| Usable Vol | 3 | 6 | 3 | 84.823 | 634 | 20 | 1,696 | gpm@ | 11 | 16 | 21.1 | 32 |
| | | | CM= | 2.40292 | | | | gpmTot. | 211 | 317 | 423 | 634 |

REARING UNIT DATA

REARING UNIT DATA

| Tank Data | | | | | | | | | | Hourly Exchange Rate | | |
|------------------------|--------|------|-------|--------|---------|---------|------------|---------|-------|----------------------|-------|-------|
| | Radius | Dia. | Depth | cuft | gallons | # Units | Total cuft | R= | R=1 | R=1.3 | R=2 | R=3 |
| 20 ' dia. Circular TKS | 10 | 20 | 4 | 1256.6 | 9,400 | 20 | 25,133 | gpm@ | 157 | 209 | 313 | 470 |
| Usable Vol | 10 | 20 | 3 | 942.5 | 7,050 | 20 | 18,850 | gpm@ | 117 | 176 | 235.0 | 352 |
| | | | CM= | 26.7 | | | | gpmTot. | 2,350 | 3,525 | 4,700 | 7,050 |

REARING UNIT DATA

| Tank Data | | | | | | | | | | Hour | Hourly Exchange Rate | | |
|------------------------|--------|------|-------|---------|---------|---------|------------|---------|-------|--------|----------------------|--------|--|
| | Radius | Dia. | Depth | cuft | gallons | # Units | Total cuft | R= | R=1 | R=1.3 | R=2 | R=3 | |
| 40 ' dia. Circular TKS | 20 | 40 | 4 | 5026.55 | 37,599 | 16 | 80,425 | gpm@ | 627 | 836 | 1,253 | 1,880 | |
| Usable Vol | 20 | 40 | 3 | 3769.91 | 28,199 | 16 | 60,319 | gpm@ | 470 | 627 | 940 | 1,410 | |
| | | | CM= | 106.796 | | | | gpmTot. | 7,520 | 10,026 | 15,039 | 22,559 | |

Theoretical Carring Capacity DATA

| | D | D | D | D |
|-----------------|---------|---------|---------|---------|
| | lbs /CF | lbs /CF | lbs /CF | lbs /CF |
| Density Ibs/CF | 2 | 3 | 4 | 5 |
| PER unit LBS= | 170 | 254 | 339 | 424 |
| Total Lbs | 3,393 | 5,089 | 6,786 | 8,482 |
| Loading LBS/GPM | 10.7 | 16.0 | 21.4 | 26.7 |

Theoretical Carring Capacity DATA

| | D | D | D | D |
|-----------------|---------|---------|---------|---------|
| | lbs /CF | lbs /CF | lbs /CF | lbs /CF |
| Density Ibs/CF | 2 | 3 | 4 | 5 |
| PER unit LBS= | 1,885 | 2,827 | 3,770 | 4,712 |
| Total Lbs | 37,699 | 56,549 | 75,398 | 94,248 |
| Loading LBS/GPM | 10.7 | 16.0 | 21.4 | 26.7 |

Theoretical Carring Capacity DATA

| | D | D | D | D |
|-----------------|---------|---------|---------|---------|
| | lbs /CF | lbs /CF | lbs /CF | lbs /CF |
| Density Ibs/CF | 2 | 3 | 4 | 5 |
| PER unit LBS= | 7,540 | 11,310 | 15,080 | 18,850 |
| Total Lbs | 120,637 | 180,956 | 241,274 | 301,593 |
| Loading LBS/GPM | 12.0 | 18.0 | 24.1 | 30.1 |

| | | gpm |
|-------------|------|--------|
| | | 13,551 |
| 95% recirc. | 0.95 | 12,874 |
| 5% makeup | 0.05 | 678 |
| 75% recirc. | 0.75 | 10,163 |
| 25% makeup | 0.25 | 3,388 |

Use this page to enter the required data for each month White fields are required for the model, Yellow fields are optional

| Year | Feed | Flow | Weight Gain | Biomass | Total Fish |
|------|--------|-------|-------------|---------|------------|
| 2020 | (lbs) | (gpm) | (lbs) | (lbs) | (number) |
| Jan | 2,154 | 2570 | | | |
| Feb | 2,318 | 2099 | | | |
| Mar | 3,418 | 2120 | | | |
| Apr | 3,800 | 2992 | | | |
| May | 3,805 | 3044 | | | |
| Jun | 4,957 | 2663 | | | |
| Jul | 7,404 | 1467 | | | |
| Aug | 9,309 | 2882 | | | |
| Sep | 10,538 | 3122 | | | |
| Oct | 6,161 | 3570 | | | |
| Nov | 1,951 | 2724 | | | |
| Dec | 2,026 | 2623 | | | |

| | | Feed | | | Flow | V |
|---------|-----|--------|-------|------|------|------|
| | Y&F | West | Tot | Y&F | West | Tot |
| Jan | 153 | 0 624 | 2154 | 756 | 1814 | 2570 |
| Feb | 164 | 6 672 | 2318 | 551 | 1548 | 2099 |
| Mar | 266 | 1 757 | 3418 | 454 | 1666 | 2120 |
| Apr | 249 | 0 1310 | 3800 | 747 | 2245 | 2992 |
| May | 254 | 7 1258 | 3805 | 891 | 2153 | 3044 |
| Jun | 456 | 4 393 | 4957 | 1041 | 1622 | 2663 |
| Jul | 740 | 4 | 7404 | 1467 | | 1467 |
| Aug | 865 | 8 651 | 9309 | 1312 | 1570 | 2882 |
| Sep | 869 | 2 1846 | 10538 | 1384 | 1738 | 3122 |
| Oct | 330 | 3 2858 | 6161 | 1694 | 1876 | 3570 |
| Nov | 109 | 1 860 | 1951 | 796 | 1928 | 2724 |
| Dec | 145 | 0 576 | 2026 | 696 | 1927 | 2623 |
| Average | | | | 982 | 1826 | 2809 |

* This model estimates the monthly average concentration based on fish feeding data only

Wastewater Generation Model

Blue cells are from Inputs sheet Red cells are for calculated values

teu cells are for calculateu values

| 2020 | | | | | | | | | - | | | _ |
|---|------------|-----------------|-------------|----------------|----------------|------------------|-------------|------------------|-------------|----------|------------------|---------------|
| 2020 | Jan | Feb | Mar | Apr | May | Jun | Jul | Aug | Sep | Oct | Nov | Dec |
| Days in Period | 31 | 28 | 31 | 30 | 31 | 30 | 31 | 31 | 30 | 31 | 30 | 31 |
| English | | | | | | | | | | | | |
| Average Flow (gpm) | 2,570 | 2,099 | 2,120 | 2,992 | 3,044 | 2,663 | 1,467 | 2,882 | 3,122 | 3,570 | 2,724 | 2,623 |
| Number of fish at end of period | | | | | | | | | | | | |
| Pounds of fish at End of Period | | | | | | | | | | | | |
| Weight Gain (Pounds) | | 0.040 | 0.440 | | 0.005 | 4.057 | | | 40 500 | | 4.054 | |
| Lbs of feed | 2,154 | 2,318 | 3,418 | 3,800 | 3,805 | 4,957 | 7,404 | 9,309 | 10,538 | 6,161 | 1,951 | 2,026 |
| Feed Conversion | 1.0 | 1.0 | 1.0 | 1.0 | 1.0 | 1.0 | 1.0 | 1.0 | 1.0 | 1.0 | 1.0 | 1.0 |
| Metric Total Liters | 3.E+08 | 2.E+08 | 2.E+08 | 3.E+08 | 4.E+08 | 3.E+08 | 2.E+08 | 3.E+08 | 4.E+08 | 4.E+08 | 3.E+08 | 3.E+08 |
| Average Flow (Ipm) | 9,727 | 2.E+00 7,945 | 8,024 | | 4.2+00 | 3.E+08 10,079 | | 3.E+08 10,908 | 4.00 | 4.00 | 3.E+00 10,310 | 9,928 |
| Weight Gain (kg) | 9,727 | 7,945 | 0,024 | 11,325 | 11,522 | 10,079 | 5,553 | 10,908 | 11,017 | 13,512 | 10,310 | 9,920 |
| Kg of Fish at End of Period | #VALUE! | #1/411151 | #\/ALLEI | #VALUE! | #VALUE! | #VALUE! | #VALUE! | #VALUE! | #VALUE! | #\/ALLET | #VALUE! | #\/AIIIE |
| Kg of Feed | #VALUE: | #VALUE: | #VALUE: | #VALUE: | #VALUE: | #VALUE: | 3,358 | 4,222 | 4,780 | 2,795 | #VALUE: | #VALUE 919 |
| ING OF FEED | 311 | 1,051 | 1,550 | 1,724 | 1,720 | 2,240 | 3,350 | 4,222 | 4,700 | 2,795 | 005 | 313 |
| Total Phaenharus | | | | | | | | | | | | |
| Total Phosphorus | Jan | Feb | Mar | Apr | Mav | Jun | Jul | Aug | Sep | Oct | Nov | Dec |
| Modeled Total Phosphorus (kg per month) | 3.5 | 3.8 | 5.6 | 6.2 | 6.2 | 8.1 | 12.1 | Aug 15.2 | 5ep 17.2 | 10.1 | 3.2 | 3.3 |
| Modeled Total Phosphorus (kg per month) | 3.5 7.8 | 3.0 8.3 | 5.6 12.3 | 0.2 13.7 | 13.7 | 0.1 17.8 | 26.7 | 33.5 | 37.9 | 22.2 | 3.2 7.0 | 3.3 7.3 |
| Modeled Total Phosphorus (los per month) Modeled Total Phosphorus (Avg. lbs per day) | 0.3 | 0.3 | 0.4 | 0.5 | 0.4 | 0.6 | 26.7 | 33.5 1.1 | 1.3 | 0.7 | 0.2 | 0.2 |
| Modeled TP | 0.3 | 0.3 | 0.4 | 0.5 | 0.4 | 0.027 | 0.9 | 0.045 | 0.048 | 0.024 | 0.2 | 0.2 |
| | 0.012 | 0.017 | 0.022 | 0.018 | 0.017 | 0.027 | 0.070 | 0.045 | 0.040 | 0.024 | 0.010 | 0.011 |
| Organic Phosphorus | | | | | | | | | | | | |
| organic Fliosphorus | Jan | Feb | Mar | Apr | May | Jun | Jul | Aug | Sep | Oct | Nov | Dec |
| Modeled Total Phosphorus (kg per month) | 2.5 | 2.7 | 4.0 | 4.5 | 4.5 | 5.8 | 8.7 | 10.9 | 12.4 | 7.2 | 2.3 | 2.4 |
| Modeled Total Phosphorus (kg per month) | 2.5 | 6.0 | 4.0 8.9 | 4.5 9.8 | 4.5 9.9 | 5.6 12.8 | 0.7 19.2 | 24.1 | 27.3 | 16.0 | 2.3 5.1 | 2.4 |
| Modeled Total Phosphorus (Avg. lbs per day) | 0.1 | 0.0 | 0.9 | 9.8 0.1 | 0.1 | 0.2 | 0.3 | 0.4 | 0.4 | 0.2 | 0.1 | 0.1 |
| Modeled Total Phosphorus (Avg. nos per day) | 0.008 | 0.009 | 0.013 | 0.015 | 0.015 | 0.2 | 0.029 | 0.4 | 0.4 | 0.2 | 0.008 | 0.008 |
| Modeled Total Phospholds (Avg. high) | 0.008 | 0.009 | 0.013 | 0.015 | 0.015 | 0.019 | 0.029 | 0.030 | 0.041 | 0.024 | 0.008 | 0.008 |
| Inorganic Phosphorus | | | | | | | | | | | | |
| norganic Phosphorus | Jan | Feb | Mar | Apr | May | Jun | Jul | Aug | Sep | Oct | Nov | Dec |
| Modeled Total Phosphorus (kg per month) | 0.98 | 1.06 | 1.56 | 1.74 | 1.74 | 2.27 | 3.39 | 4.26 | 4.82 | 2.82 | 0.89 | 0.93 |
| Modeled Total Phosphorus (kg per month) | 2.2 | 2.3 | 3.4 | 3.8 | 3.8 | 5.0 | 7.5 | 9.4 | 10.6 | 6.2 | 2.0 | 2.0 |
| Modeled Total Phosphorus (Avg. Ibs per day) | 0.03 | 0.04 | 0.05 | 0.06 | 0.06 | 0.08 | 0.11 | 0.14 | 0.16 | 0.2 | 0.03 | 0.03 |
| Modeled Total Phosphorus (Avg. mg/l) | 0.003 | 0.004 | 0.005 | 0.006 | 0.006 | 0.008 | 0.011 | 0.014 | 0.016 | 0.009 | 0.003 | 0.003 |
| | | | | | | | | | | | | |
| Total Suspended Solids | | | | | | | | | | | | |
| | Jan | Feb | Mar | Apr | May | Jun | Jul | Aug | Sep | Oct | Nov | Dec |
| Modeled Total Suspended Solids (kg per month) | 293.1 | 315.4 | 465.1 | 517.1 | 517.8 | 674.5 | 1007.5 | 1266.7 | 1434.0 | 838.4 | 265.5 | 275.7 |
| Modeled Total Suspended Solids (kg per month) | 646.2 | 695.4 | 1025.4 | 1140.0 | 1141.5 | 1487.1 | 2221.2 | 2792.7 | 3161.4 | 1848.3 | 585.3 | 607.8 |
| Modeled Total Suspended Solids (Avg. lbs per day) | 20.8 | 24.8 | 33.1 | 38.0 | 36.8 | 49.6 | 71.7 | 90.1 | 105.4 | 59.6 | 19.5 | 19.6 |
| Permitted Total Suspended Solids (Nyg. bs per day) | 216.0 | 216.0 | 216.0 | 216.0 | 216.0 | 216.0 | 216.0 | 216.0 | 216.0 | 216.0 | 216.0 | 216.0 |
| Modeled Total Suspended Solids (Avg. mg/L) | 1.0 | 1.4 | 1.9 | 1.5 | 1.4 | 2.2 | 5.8 | 3.7 | 4.0 | 2.0 | 0.9 | 0.9 |
| Permitted Total Suspened Solids (Avg. Monthly mg/ | | 10.0 | 10.0 | 10.0 | 10.0 | 10.0 | 10.0 | 10.0 | 10.0 | 10.0 | 10.0 | 10.0 |
| Total Ammonia Nitrogen | | | | | | | | | | | | |
| | Jan | Feb | Mar | Apr | May | Jun | Jul | Aug | Sep | Oct | Nov | Dec |
| Modeled Total Ammonia (kg per month) | 38.6 | 41.6 | 61.3 | 68.1 | 68.2 | 88.9 | 132.7 | 166.9 | 188.9 | 110.4 | 35.0 | 36.3 |
| Modeled Total Ammonia (kg per month) | 85.1 | 91.6 | 135.1 | 150.2 | 150.4 | 195.9 | 292.6 | 367.9 | 416.5 | 243.5 | 77.1 | 80.1 |
| Modeled Total Ammonia (Avg. Ibs per day) | 2.7 | 3.3 | 4.4 | 5.0 | 4.9 | 6.5 | 9.4 | 11.9 | 13.9 | 7.9 | 2.6 | 2.6 |
| Modeled Total Ammonia (Avg. ns per day) Modeled Total Ammonia (Avg. mg/l) | 0.1 | 0.2 | 0.2 | 0.2 | 0.2 | 0.3 | 0.8 | 0.5 | 0.5 | 0.3 | 0.1 | 0.1 |
| Carbonaceous Biochemical Oxygen Dema | and | | | | | | | | | | | |
| Carbonaceous Biochemical Oxygen Dema | ano Jan | Feb | Mar | Apr | May | Jun | Jul | Aug | Sep | Oct | Nov | Dec |
| Modeled CBOD5 (kg per month) | 332.2 | 357.5 | 527.1 | 586.0 | 586.8 | 764.5 | 1141.8 | 1435.6 | 1625.2 | 950.2 | 300.9 | 312.5 |
| Modeled CBOD5 (lbs per month) | 732.4 | 788.1 | 1162.1 | 1292.0 | 1293.7 | 1685.4 | 2517.4 | 3165.1 | 3582.9 | 2094.7 | 663.3 | 688.8 |
| Modeled CBOD3 (lbs per month) Modeled CBOD (Avg. lbs per day) | 23.6 | 28.1 | 37.5 | 43.1 | 41.7 | 56.2 | 81.2 | 102.1 | 119.4 | 67.6 | 22.1 | 22.2 |
| Modeled CBOD5 (Avg. mg/l) | 1.1 | 1.6 | 2.1 | 1.7 | 1.6 | 2.5 | 6.6 | 4.2 | 4.6 | 2.3 | 1.0 | 1.0 |
| | | | | | | 2.0 | 5.0 | | | 2.0 | | |

Circular Tank Calculations

Feed Training Tanks when in use are usually on flow thru first-use water only

| Tank Data | | | | | | | | | | Hour | ly Exchange | Rate |
|----------------------|--------|------|-------|---------|---------|---------|------------|---------|-----|-------|-------------|------|
| | Radius | Dia. | Depth | cuft | gallons | # Units | Total cuft | R= | R=1 | R=1.3 | R=2 | R=3 |
| 6' dia. Circular TKS | 3 | 6 | 4 | 113.097 | 846 | 20 | 2,262 | gpm@ | 14 | 19 | 28 | 42 |
| Usable Vol | 3 | 6 | 3 | 84.823 | 634 | 20 | 1,696 | gpm@ | 11 | 16 | 21.1 | 32 |
| | | | CM= | 2.40292 | | | | gpmTot. | 211 | 317 | 423 | 634 |

REARING UNIT DATA

REARING UNIT DATA

| Tank Data | | | | | | | | | | Hour | ly Exchange | Rate |
|------------------------|--------|------|-------|--------|---------|---------|------------|---------|-------|-------|-------------|-------|
| | Radius | Dia. | Depth | cuft | gallons | # Units | Total cuft | R= | R=1 | R=1.3 | R=2 | R=3 |
| 20 ' dia. Circular TKS | 10 | 20 | 4 | 1256.6 | 9,400 | 20 | 25,133 | gpm@ | 157 | 209 | 313 | 470 |
| Usable Vol | 10 | 20 | 3 | 942.5 | 7,050 | 20 | 18,850 | gpm@ | 117 | 176 | 235.0 | 352 |
| | | | CM= | 26.7 | | | | gpmTot. | 2,350 | 3,525 | 4,700 | 7,050 |

REARING UNIT DATA

| Tank Data | | | | | | | | | | Hour | ly Exchange | Rate |
|------------------------|--------|------|-------|---------|---------|---------|------------|---------|-------|--------|-------------|--------|
| | Radius | Dia. | Depth | cuft | gallons | # Units | Total cuft | R= | R=1 | R=1.3 | R=2 | R=3 |
| 40 ' dia. Circular TKS | 20 | 40 | 4 | 5026.55 | 37,599 | 16 | 80,425 | gpm@ | 627 | 836 | 1,253 | 1,880 |
| Usable Vol | 20 | 40 | 3 | 3769.91 | 28,199 | 16 | 60,319 | gpm@ | 470 | 627 | 940 | 1,410 |
| | | | CM= | 106.796 | | | | gpmTot. | 7,520 | 10,026 | 15,039 | 22,559 |

Theoretical Carring Capacity DATA

| | D | D | D | D |
|-----------------|---------|---------|---------|---------|
| | lbs /CF | lbs /CF | lbs /CF | lbs /CF |
| Density Ibs/CF | 2 | 3 | 4 | 5 |
| PER unit LBS= | 170 | 254 | 339 | 424 |
| Total Lbs | 3,393 | 5,089 | 6,786 | 8,482 |
| Loading LBS/GPM | 10.7 | 16.0 | 21.4 | 26.7 |

Theoretical Carring Capacity DATA

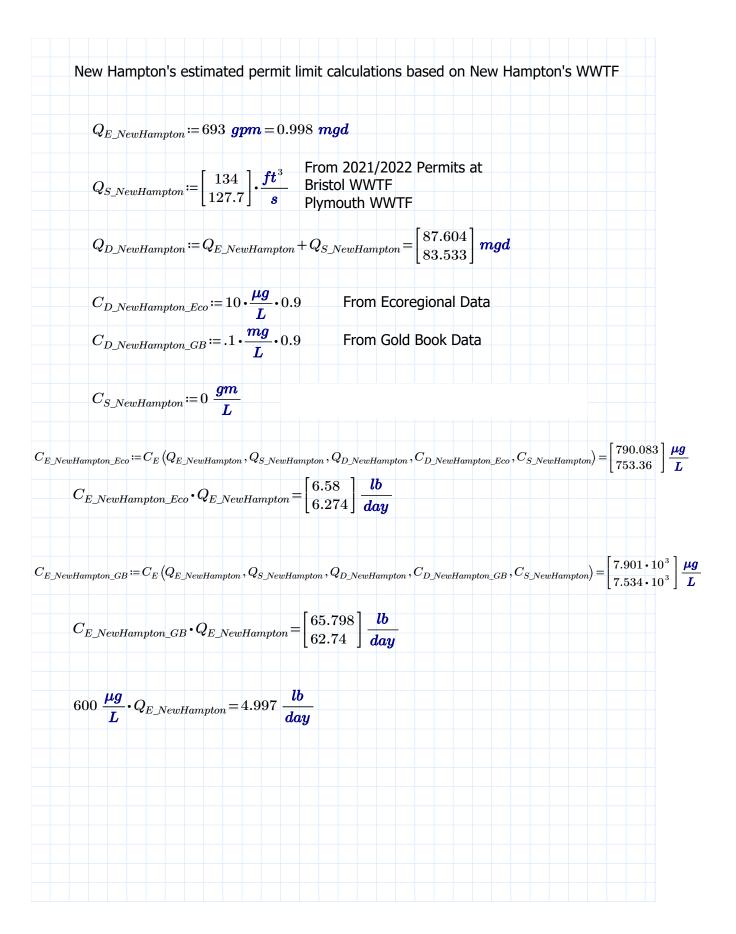
| | D | D | D | D |
|-----------------|---------|---------|---------|---------|
| | lbs /CF | lbs /CF | lbs /CF | lbs /CF |
| Density Ibs/CF | 2 | 3 | 4 | 5 |
| PER unit LBS= | 1,885 | 2,827 | 3,770 | 4,712 |
| Total Lbs | 37,699 | 56,549 | 75,398 | 94,248 |
| Loading LBS/GPM | 10.7 | 16.0 | 21.4 | 26.7 |

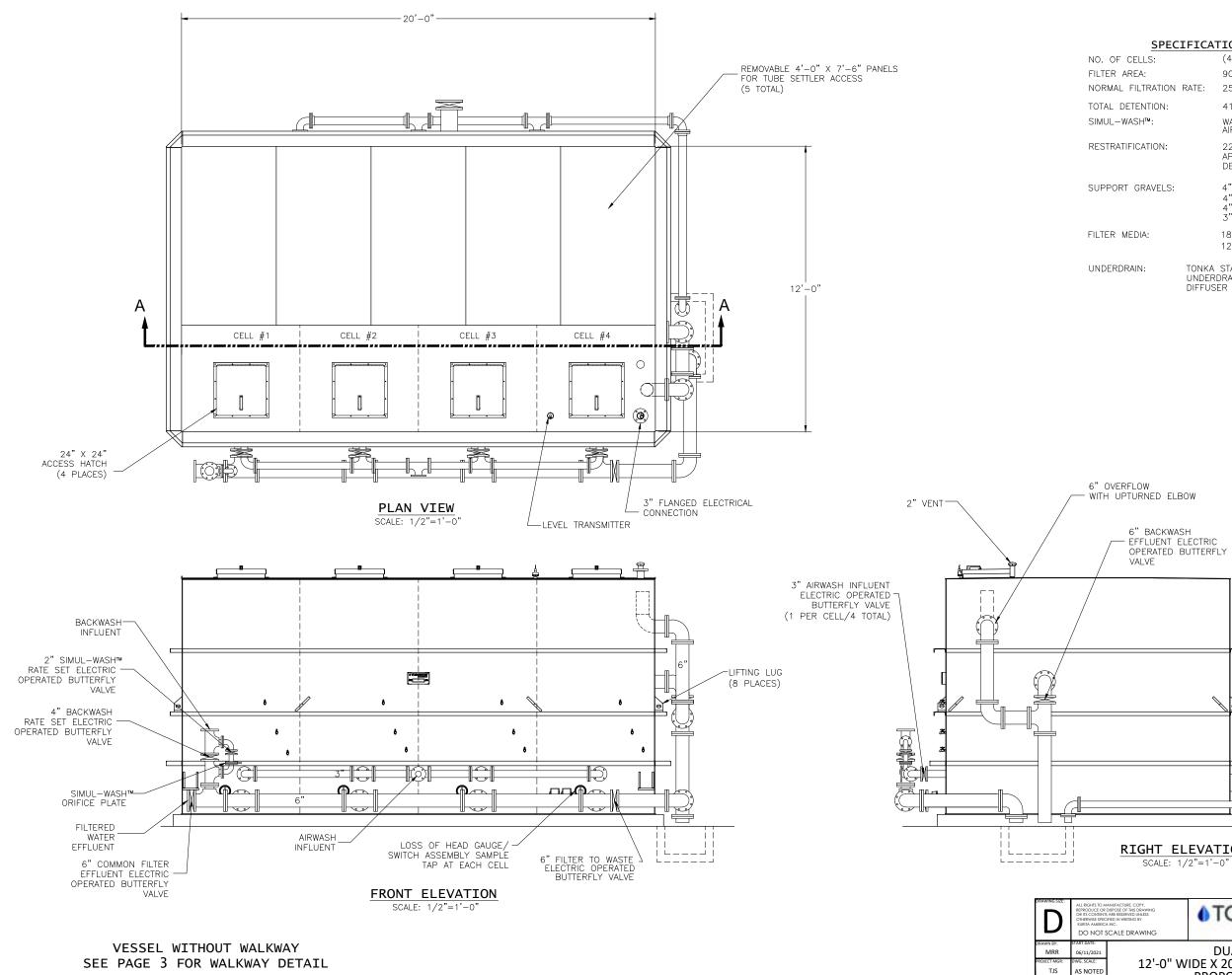
Theoretical Carring Capacity DATA

| | D | D | D | D |
|-----------------|---------|---------|---------|---------|
| | lbs /CF | lbs /CF | lbs /CF | lbs /CF |
| Density Ibs/CF | 2 | 3 | 4 | 5 |
| PER unit LBS= | 7,540 | 11,310 | 15,080 | 18,850 |
| Total Lbs | 120,637 | 180,956 | 241,274 | 301,593 |
| Loading LBS/GPM | 12.0 | 18.0 | 24.1 | 30.1 |

| | | gpm |
|-------------|------|--------|
| | | 13,551 |
| 95% recirc. | 0.95 | 12,874 |
| 5% makeup | 0.05 | 678 |
| 75% recirc. | 0.75 | 10,163 |
| 25% makeup | 0.25 | 3,388 |

| | | $u_{\alpha} = \underline{gm}$ |
|---|--|--|
| | | $\boldsymbol{\mu g} \coloneqq \frac{\boldsymbol{gm}}{10^6}$ |
| $C (Q, Q, Q, C, C) = Q_D$ | $\cdot C_D - Q_S \cdot C_S$ | |
| $C_E \left(Q_E, Q_S, Q_D, C_D, C_S \right) \coloneqq \frac{Q_D}{Q_D}$ | $\overline{Q_E}$ | |
| CE: Effluent total phosphorus c | oncentration | |
| CE. Emdent total phosphorus e | oncentration | |
| QE: Facility design Flow | | |
| QS: 7Q10 Flow upstream of the | e facility | |
| QD: Combined stream flow (7Q | 10+effluent) | |
| CD: Downstream phosphorus c | | |
| CS: Median upstream total pho | sphorus concentration | |
| Milford's estimated permit limit ca | culations based on Milford W | /WTF |
| | | |
| $Q_{E_Milford} \coloneqq 693 \; gpm = 0.998 \; r$ | ngd | |
| $Q_{S_Milford} \coloneqq \begin{bmatrix} 4.15 \\ 3.44 \end{bmatrix} mgd$ | From Milford WW | F's 2020 permit |
| | | |
| O_{-} \cdots $i = O_{-}$ $i = 1 + O_{-}$ | [5.148] mad | |
| $Q_{D_Milford} \coloneqq Q_{E_Milford} + Q_{S_Milford}$ | $ord = \lfloor 4.438 \rfloor$ | |
| $C_{D_Milford} \coloneqq 0.9 \cdot 100 \ \frac{\mu g}{L} = 90 \ \frac{\mu}{L}$ | Gold Book Water Qua | ality Standard |
| L | L Cold Dook Water Que | |
| $C_{D_Milford_2} \coloneqq 0.9 \cdot 10 \frac{\mu g}{L} = 9 \frac{\mu}{L}$ | | Juality Standard |
| | | |
| | | |
| | | |
| $C_{S_Milford} \coloneqq 0 \; \frac{gm}{L}$ | From Milford WW | F's 2020 permit |
| | | |
| | | [464.979] 40 |
| $C_{E_Milford} \coloneqq C_E \left(Q_{E_Milford}, Q_{S_Milj} \right)$ | $C_{ord}, Q_{D_Milford}, C_{D_Milford}, C_{S}$ | $S_{Milford} = \begin{bmatrix} 404.278 \\ 400.245 \end{bmatrix} \frac{\mu g}{T}$ |
| | | |
| [3 867]] | | |
| $C_{E_Milford} \cdot Q_{E_Milford} = \begin{vmatrix} 3.867 \\ 3.333 \end{vmatrix} \frac{l}{dd}$ | <u></u> | |
| [0.000] (((| <i>y</i> | |
| | | [46.428] |
| $C_{E_Milford_2} \coloneqq C_E \left(Q_{E_Milford}, Q_{S_M} \right)$ | $_{ilford}, Q_{D_Milford}, C_{D_Milford_2}$ | $, C_{S_Milford}) = \begin{vmatrix} 10.120 \\ 40.025 \end{vmatrix} \frac{\mu}{4}$ |
| | | |
| [0.387] | lb | |
| $C_{E_Milford_2} \cdot Q_{E_Milford} = \begin{vmatrix} 0.387\\ 0.333 \end{vmatrix}$ | lau | |
| [0.000] | <i>uu y</i> | |



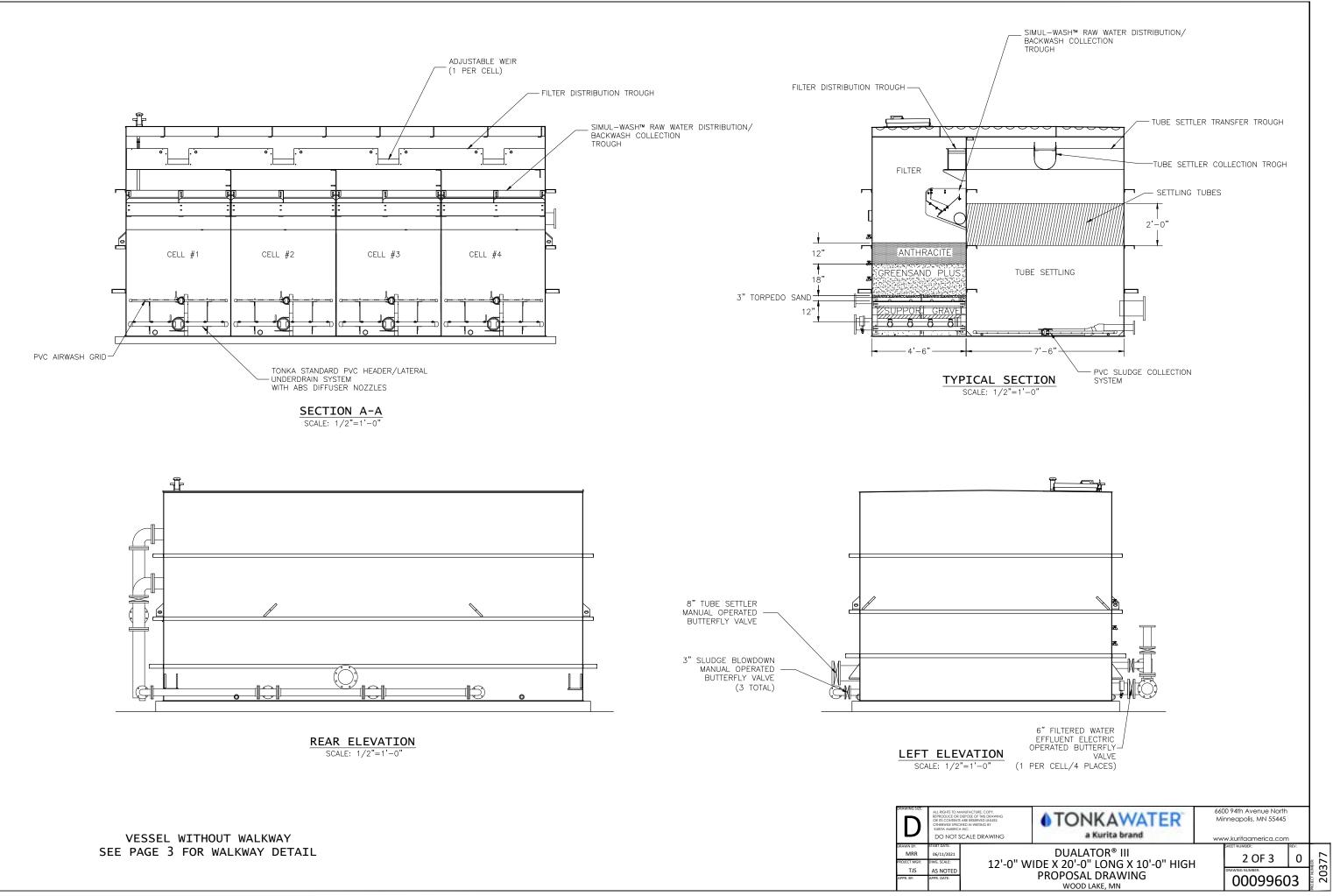


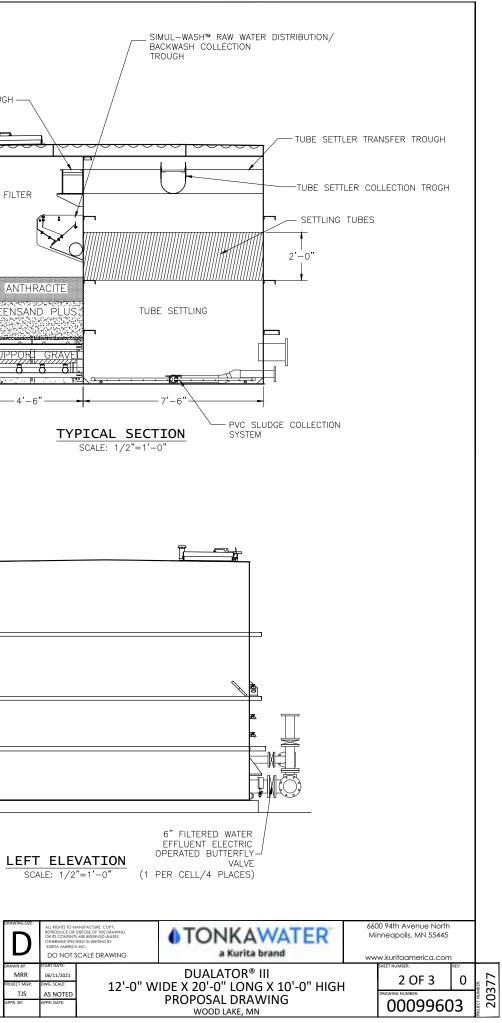
| | EVATION | | |
|---|--|--|-----------------------------|
| URE, COPY, OF THIS DRAWING RVED UNLESS RTING BY DRAWING | | 6600 94th Avenue North Minneapolis, MN 55445 www.kuritaamerica.com | |
| 12'-0" W | DUALATOR® III /IDE X 20'-0" LONG X 10'-0" HIGH PROPOSAL DRAWING wood lake, mn | 1 OF 3 0 DRAWING NUMBER: 00099603 | рео е ст и имв ек: 20377 |
| | | | |

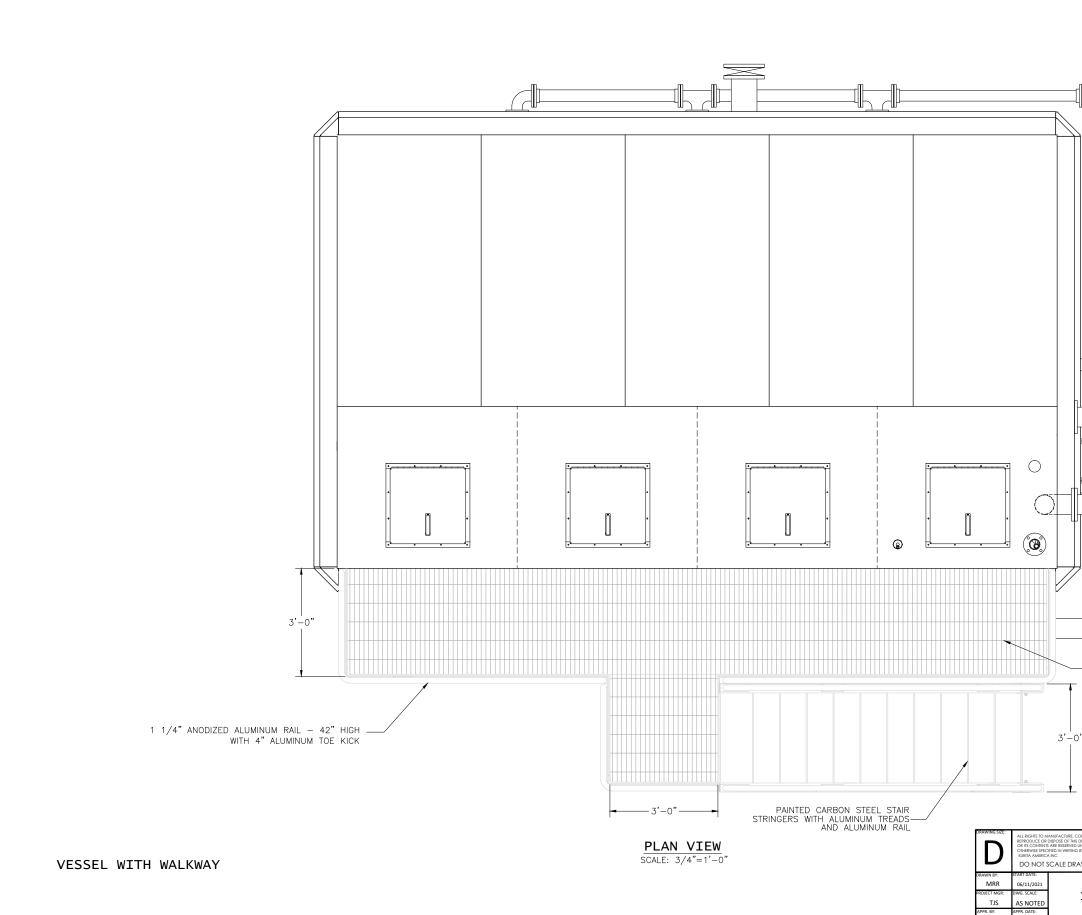
WITH UPTURNED ELBOW

| ELLS: | | (4) FOUR |
|--------------|--------|--|
| REA: | | 90 SQ. FT. – 22.5 SQ. FT./CELL |
| FILTRATION I | RATE: | 250 GPM (3.0 GPM/SQ. FT.) |
| TENTION: | | 41.5 MIN. @ 250 GPM |
| \SH™: | | WATER: 68 GPM (5 GPM/SQ. FT.) AIR: 68 CFM (3 CFM/SQ. FT.) |
| TICATION: | | 225 GPM (10 GPM/SQ. FT.) APPROXIMATE, ACTUAL GPM TO BE DETERMINED IN THE FIELD DURING START-UP |
| GRAVELS: | | 4" – 3/4" x 1/2" GRADED GRAVELS 4" – 1/2" x 1/4" GRADED GRAVELS 4" – 1/4" x 1/8" GRADED GRAVELS 3" – .8 – 1.2 mm TORPEDO SAND |
| EDIA: | | 18" GREENSAND PLUS 12" ANTHRACITE |
| AIN: | UNDERD | STANDARD PVC HEADER/LATERAL RAIN ASSEMBLY WITH TONKA ABS R NOZZLES ON 12" CENTERS |

SPECIFICATIONS:







Appendix D Capital Costs, O&M, and NPV Breakdowns

Client: NHFGD Project:Powder Mill Fish Hatchery Study Project No.: 10331124

Date:10/13/2022Estimator:Matt Cochran & Mario BenischChecked By:Jason HillCheck Date:12/27/2022Revised:-

FX

| Detailed Opinions of Probable Cost | | | | | | | | |
|------------------------------------|-------|-------|----------|-----------------|------------|--|--|--|
| | NO. | UNIT | COST PER | Escalation cost | TOTAL COST | | | |
| Alternative 1 | UNITS | MEAS. | UNIT | to 2022 | 50% CONT. | | | |

| Α. | Aquaculture Water Supply | | | | | | | |
|----------|--|-----|----|---------------|----|--------|----------------|-----------|
| A1 | Hatchery Supply | | | | | | \$ | 8,448 |
| | Water Supply Piping and Accessories | 50 | LF | \$ 85 | \$ | 113 | \$ | 8,448 |
| A2 | Oxygenation System | | | | | | \$ | 321,846 |
| | Bulk LOX Tank, Vaporizer, Port. Tank Fill System | 1 | LS | \$ 70,000 | \$ | 92,767 | \$ | 139,151 |
| | Fence | 200 | LF | \$ 20 | \$ | 27 | \$ | 7,951 |
| | Concrete Pad & Bollards | 1 | LS | \$ 11,000 | \$ | 14,578 | \$ | 21,867 |
| | Buried Copper Oxygen Distribution to Units | 1 | LS | \$ 60,000 | \$ | 79,515 | \$ | 119,272 |
| | Oxygen Electrical | 1 | LS | \$ 3,000 | \$ | 3,976 | \$ | 5,964 |
| | Oxygen Dissolving for Rearing Units- LHO | 6 | EA | \$ 2,500 | \$ | 2,906 | \$ | 26,150 |
| | Oxygen Flow Meter Station (raceways) | 1 | LS | \$ 750 | \$ | 994 | \$ | 1,491 |
| В. В1 | Buildings and Rearing Units Intake Building | | | | | | \$ | 1,623,787 |
| ы | New Intake Building | 400 | SF | \$ 165 | \$ | 218 | ₽ \$ | 131,017 |
| | Drumfilter | 100 | | 100 | Ŷ | 210 | Ŷ | |
| | DRUM FILTERS | 2 | EA | \$ 50,000 | | - | \$ | 150,000 |
| | DRUM SUMP | 1 | LS | \$ 75,000 | | - | \$ | 112,500 |
| | PIPING SYSTEMS (INFLOW, DRAINS) | 1 | LS | \$ 500,000 | | - | \$ | 750,000 |
| | PRIMARY POWER | 1 | LS | \$ 75,000 | | - | \$ | 112,500 |
| | UV System | | 0 | | | | | |
| | UV Channel and Lamp Package | 2 | EA | \$ 60,000 | | - | \$ | 180,000 |
| | | | | | | 10.000 | • | |
| | UV Electrical | 1 | LS | \$ 8,000 | \$ | 10,602 | \$ | 15,903 |

| | ALARMS/CONTROLS/MONITORING/PANEL/HMI | 1 | LS | \$ 100,000 | - | \$ 150,000 |
|------------|--|--------|----|---------------|--------------|-----------------|
| B2 | Effluent Treatment Building | | | | | \$ 3,378,113 |
| | New Effluent treatment building | 9462.5 | SF | \$ 165 | \$ 238 | \$ 3,378,113 |
| B 3 | Vehicle/Chemical Storage Building | | | | | \$ 704,980 |
| | Demo existing storage building (assumed: 51'x30'x20') | | | | | |
| | DEMO CMU BUILDINGS | 30600 | CF | \$ 1 | - | \$ 27,081 |
| | DEMO CONCRETE SLABS - assumed 1.5' W | 53 | CY | \$ 210 | - | \$ 16,800 |
| | DEMO CONCRETE FOOTINGS - assumed 1' W | 57 | CY | \$ 60 | - | \$ 5,100 |
| | New Storage Building (40'x50') | 2000 | SF | \$ 165 | \$ 219 | \$ 655,999 |
| B4 | Raceway Rehabilitation | | | | | \$ 465,000 |
| | Concrete rehab of raceways (B thru G) | 1 | LS | \$ 150,000 | - | \$ 225,000 |
| | Demolish and fill in raceway A | 1 | LS | \$ 60,000 | - | \$ 90,000 |
| | Baffle Allowance | 1 | LS | \$ 100,000 | - | \$ 150,000 |
| C. | Site | | | | | |
| C1 | Site Work | | | | | \$1,003,876.52 |
| | Site Clearing | 2.5 | AC | \$2,000.00 | \$2,650.50 | \$ 9,939 |
| | General Earthwork for Hatchery Complex | 0 | LS | \$75,000.00 | \$99,393.71 | \$ - |
| | General Sitework | 2 | LS | \$250,000.00 | \$331,312.38 | \$ 993,937 |
| | Erosion Control | 0 | AC | \$2,500.00 | \$3,313.12 | \$ - |
| | Seeding | 0 | AC | \$1,250.00 | \$1,656.56 | \$ - |
| | Landscaping | 0 | AC | \$3,000.00 | \$3,975.75 | \$ - |
| | Natural Gas Connection and Distribution (if available) | 0 | LS | \$35,000.00 | \$46,383.73 | \$ - |
| | Stormwater Management System | 0.0 | AC | \$3,500.00 | \$4,638.37 | \$ - |
| C2 | Security Fence | | | \$710.00 | | \$6,042.56 |
| | Site Fencing | 152 | LF | \$20.00 | \$26.50 | \$ 6,043 |
| C3 | Domestic Water | | | \$150.00 | | \$49,696.86 |
| | Domestic Water Supply | 1 | LS | \$25,000.00 | | \$ 49,697 |
| | | | | | | |
| C4 | Domestic Wastewater | | | \$100,000.00 | | \$99,393.71 |

| C5 | Disinfection Station | | | | | \$22,500.00 |
|----|---|---|----|--------------|--------------|-------------|
| | Truck Disinfection Station | 1 | LS | \$15,000.00 | - | \$ 22,500 |
| | Roadway Aggregate | 0 | SY | \$15.00 | - | \$- |
| | Electrical | 0 | LS | \$2,500.00 | - | \$- |
| | Detention Tank | 0 | LS | \$5,000.00 | - | \$- |
| C6 | Paved Access to State or Local Highways | 0 | | \$0.00 | | \$0.00 |
| | Bituminous Paved Road | 0 | LS | \$190,000.00 | \$251,797.41 | \$- |
| | Gravel Roads | 0 | LS | \$55,000.00 | \$72,888.72 | \$- |
| | | | | | | |

| D. / | Aquaculture Wastewater | | | | | | |
|------|---------------------------------------|-----|----|----|---------|---------------|------------------|
| D1 I | Effluent Treatment | | | | | | \$ 31,443,671 |
| | | | | | | | |
| | Drumfilter | | | | | | |
| | DRUM FILTERS | 2 | EA | \$ | 50,000 | - | \$ 150,000 |
| | DRUM SUMP | 1 | LS | \$ | 75,000 | - | \$ 112,500 |
| | PIPING SYSTEMS (INFLOW, PRAS, DRAINS) | 1 | LS | \$ | 500,000 | - | \$ 750,000 |
| | PRIMARY POWER | 1 | LS | \$ | 75,000 | - | \$ 112,500 |
| | Clarifier-30ft | | | | | | |
| (| Clarifier Concrete | 142 | CY | \$ | 1,500 | - | \$ 319,500 |
| (| Clarifer Excavation | 642 | CY | \$ | 50 | - | \$ 48,150 |
| | Clarifier Equipment | 1 | LS | \$ | 108,000 | \$ 170,780 | \$ 256,170 |
| | Clarifier Coatings | 1 | LS | \$ | 12,000 | \$ 18,976 | \$ 28,463 |
| | Finger Weirs | 1 | LS | \$ | 6,000 | \$ 9,488 | \$ 14,232 |
| | Duplex Pump Station | 1 | LS | \$ | 18,000 | \$ 28,463 | \$ 42,695 |
| | 3" Sch 80 PVC Pipe | 100 | LF | \$ | 36 | \$ 57 | \$ 8,539 |
| | 4" Sch 80 PVC Pipe | 250 | LF | \$ | 60 | \$ 95 | \$ 35,579 |
| | 3" Plug Valves | 2 | EA | \$ | 3,000 | \$ 4,744 | \$ 14,232 |
| | 3" Swing Check Valves | 2 | EA | \$ | 2,040 | \$ 3,226 | \$ 9,678 |
| | Telescoping Valves | 2 | EA | \$ | 1,140 | \$ 1,803 | \$ 5,408 |
| | 6 ft precast manhole 6 ft deep | 2 | EA | \$ | 9,000 | \$ 14,232 | \$ 42,695 |
| | 4ft Precast Manhole 4 ft deep | 1 | EA | \$ | 5,040 | \$ 7,970 | \$ 11,955 |
| | Clarifier Equipment Install | 1 | LS | \$ | 21,600 | \$ 34,156 | \$ 51,234 |
| | Sludge Storage-30ft | | | _ | | | |

| Sludge Storage Concrete | 138 | CY | \$ 1,500 | - | \$ 310,500 |
|--|------|----|------------------|--------------|-----------------|
| Sludge storage Excavation | 563 | CY | \$ 50 | - | \$ 42,225 |
| Sludge Mixing Pump | 1 | LS | \$ 10,000 | \$ 15,813 | \$ 23,719 |
| Sludge Mixing Nozzles | 1 | LS | \$ 35,000 | \$ 55,345 | \$ 83,018 |
| 4" Sch 80 PVC Pipe | 300 | LF | \$ 50 | \$ 79 | \$ 35,579 |
| Telescoping Valves | 1 | EA | \$ 950 | \$ 1,502 | \$ 2,253 |
| 3" Plug Valves | 1 | EA | \$ 2,500 | \$ 3,953 | \$ 5,930 |
| 3" Swing Check Valves | 1 | EA | \$ 1,700 | \$ 2,688 | \$ 4,032 |
| Air Release Valve | 2 | EA | \$ 450 | \$ 712 | \$ 2,13 |
| Sludge Mix & Transfer System Install | 1 | LS | \$ 13,210 | \$ 20,889 | \$ 31,33 |
| WW Piping | | | | | |
| WW Piping line | 1500 | LF | \$ 85 | \$ 113 | \$ 253,454 |
| WW Sitework | 1 | LS | \$ 40,000 | \$ 53,010 | \$ 79,51 |
| Phosphorus Removal | | | | | |
| Membrane | | | | | |
| Membrane Filtration System | 1 | EA | \$ 11,480,000 | - | \$ 17,220,00 |
| Chemical Storage Membrane Cleaning | 1 | EA | \$ 8,770 | - | \$ 13,15 |
| Membrane Install (25% of Materials) | 1 | LS | \$ 2,872,193 | - | \$ 4,308,28 |
| Chemical Addition | | | | | |
| Mixing/Reaction Tank Concrete | 255 | CY | \$ 1,500 | - | \$ 573,75 |
| Mixing/Reaction Tank 2:1 Excavation | 1593 | CY | \$ 50 | - | \$ 119,47 |
| Mixing/Reaction Tank MISC Piping | 1 | LS | \$ 40,000 | - | \$ 60,00 |
| Mixing/Reaction Mixing Pumps | 1 | EA | \$ 52,595 | - | \$ 78,89 |
| Chemical Dosing | 1 | EA | \$ 20,000 | - | \$ 30,00 |
| Chemical Storage Coagulation | 1 | EA | \$ 2,520 | - | \$ 3,78 |
| Chemical Addition Install (25% of Materials) | 1 | LS | \$ 124,404 | - | \$ 186,60 |
| Adsorption | | | | | |
| Adsorption Columns | 6 | EA | \$ 250,000 | - | \$ 2,250,00 |
| Adsorption Media | 3360 | CF | \$ 500 | - | \$ 2,520,00 |
| Asorption Install (25% of Materials) | 1 | LS | \$ 795,000 | - | \$ 1,192,50 |
| 2 Effluent Monitoring | | | | | \$ 64,60 |
| Automated Flow Measurement Equipment | 1 | LS | \$ 25,000 | \$ 33,131 | \$ 49,69 |
| Portable Composite Sampler | 1 | LS | \$ 5,000 | \$ 6,626 | \$ 9,93 |

| | · · · · · · · · · · · · · · · · · · · | | | - | | | ¢ | 40,167,523 |
|----|---|-----|----|----|-------------|---------------|----|--------------|
| | Visitor Center Remodel (Gut and Remodel Basement Floor) | 850 | SF | \$ | 150 | - | \$ | 191,250 |
| | Display Materials | 1 | LS | | \$20,000.00 | - | \$ | 30,000 |
| F1 | Hatchery Building - Displays | | | | | | | \$221,250.00 |
| F. | Visitor Education/Interpretation | | 1 | | | | | |
| | Instrumentation, Alarm System & Communication | 1 | LS | \$ | 175,000 | \$ 231,919 | \$ | 347,878 |
| E3 | Instrumentation and Alarm System | | | | | | \$ | 347,878 |
| | | | | | | | | |
| | Fuel Tank | 1 | LS | \$ | 14,000 | \$ 18,553 | \$ | 27,830 |
| | Automatic Transfer Switch | 1 | LS | \$ | 20,000 | \$ 26,505 | \$ | 39,757 |
| | Emergency Generator: 100-200kW | 1 | LS | \$ | 75,000 | \$ 99,394 | \$ | 149,091 |
| E2 | Emergency Power | | | | | | \$ | 216,678 |
| | 3-phase service | 1 | EA | \$ | 100,000 | - | \$ | 150,000 |
| | Security Lighting | 8 | EA | \$ | 2,500 | \$ 3,313 | \$ | 39,757 |
| E1 | Electrical Service | | | | | | \$ | 189,757 |
| E. | Utilities (Electrical, HVAC and Instrumentation) | | | | | | | |
| | | | | | | | | |
| | Electrical | 1 | LS | \$ | 2,500 | \$ 3,313 | \$ | 4,970 |



Effluent Treatment Evaluation

Alternative 1A: No Hatchery Upgrades and Chemical Dosing

Operation and Maintenance

Estimated Annual Electricity Usage Costs

| Component | HP | Quantity | Total HP | Watts | Hours/day | kW-hrs/year | | | |
|-------------------------|-------|----------|----------|---------|---------------|--------------|--|--|--|
| Hatchery Modernization | | | | | | | | | |
| UV System | | 2 | | 56,000 | 24 | 981,120 | | | |
| Drum Filter | 8.0 | 2.0 | 16.00 | 11,931 | 24 | 104,517 | | | |
| Site Lighting | | 1 | | 15,000 | 12 | 65,700 | | | |
| Effluent Treatment | | | | | | | | | |
| Effluent Drums | 8.00 | 2 | 16.00 | 11,931 | 24 | 104,517 | | | |
| Clarifier Mechanism | 0.75 | 1 | 0.75 | 559 | 24 | 4,899 | | | |
| Sludge Pump | 20.00 | 1 | 20.00 | 14,914 | 24 | 130,647 | | | |
| Mixing Tank Mixer | 3.00 | 1.00 | 3.00 | 2,237 | 24 | 19,597 | | | |
| Membrane Process Pumps | 15.00 | 8.00 | 120.00 | 487,000 | 1 | 177,755 | | | |
| Membrane Blowers | 90.00 | 2.00 | 180.00 | 335,000 | 1 | 122,275 | | | |
| Membrane CIP Pumps | 15.00 | 1.00 | 15.00 | 116,000 | 1 | 42,340 | | | |
| Membrane CIP Heaters | NA | | | 800,000 | 1 | 292,000 | | | |
| Membrane Backpulse Pump | 60.00 | 2.00 | 120.00 | 70,000 | 1 | 25,550 | | | |
| Membrane Drain Pump | 15.00 | 1.00 | 15.00 | 116,000 | 1 | 42,340 | | | |
| | | L | <u> </u> | | kW-hrs/year = | 2,113,257 | | | |
| \$/kW-hrs = | | | | | | | | | |
| | | | | | | Annual Cost | | | |
| | | | | | | \$253,590.89 | | | |

| Estimated Annual Replacement Costs | | | | | | Annual Cost |
|------------------------------------|------------------|---------------------|---------------|--------------------|-----------|----------------|
| Annual Equipment Replacement | | | | | | \$1,609,000.00 |
| Estimated Annual Labor Costs | Days per Week | Hours per day | Personnel | Rate | OH/Fringe | Annual Cost |
| Daily Operator Attention | 5 | 8 | 2 | \$ 25.00 | \$ 15.00 | \$104,000 |
| Chemicals | Use (gpd) | Annual Use (gal) | Cost (\$/gal) | Replaceme nt/yr | | Annual Cost |
| Alum | | 12045 | 1.81 | | | \$21,801.45 |
| 25% Caustic | | 10098 | 1.92 | | | \$19,388.16 |
| Нуро | | 18300 | 2.5 | | | \$45,750.00 |
| Citric | | 38500 | 8.25 | | | \$317,625.00 |
| Sodium Bisulfate | | 4400 | 3.4 | | | \$14,960.00 |
| Sulfuric | | | | | | \$0.00 |
| O2 Usage - Tank refill | | 6000 | 0.6 | 4 | | \$14,400 |
| Adsorption Media Regen | | | | | | \$0 |

| Estimated Annual Labor and Replacement Costs | \$1,713,000 |
|---|-------------|
| Estimated Annual Electricity and Chemical Usage Costs | \$687,516 |
| TOTAL | \$2,401,000 |

| | <u>New Hampshire Fish and Game Department</u> <u>Effluent Treatment Evaluation</u> <u>Alternative 1A: No Hatchery Upgrades and Chemical Dosing</u> Life Cycle Cost Analysis | | | | | | | | | | | | | | | | | | | |
|---|--|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|
| | 0 | 1 | 2 | 3 | 4 | 5 | 6 | 7 | 8 | 9 | 10 | 11 | 12 | 13 | 14 | 15 | 16 | 17 | 18 | 19 |
| Total | 2023 | 2024 | 2025 | 2026 | 2027 | 2028 | 2029 | 2030 | 2031 | 2032 | 2033 | 2034 | 2035 | 2036 | 2037 | 2038 | 2039 | 2040 | 2041 | 2042 |
| O&M | | | | | | | | | | | | | | | | | | | | |
| Power and Chemical cost (6%/yr 2023-2026, 3%/yr 2027-2042 escalation) | | , | . , , | . , , | \$2,945,418 | \$3,033,781 | | . , , | | . , , | \$3,516,983 | | . , , | | | | | | | \$4,588,866 |
| R&R Maintenance cost (6%/yr 2023-2026, 4%/yr 2027-2042 escalation) | \$556,170 | \$589,540 | \$624,913 | \$662,407 | \$688,904 | \$716,460 | \$745,118 | | . , | | | | \$942,812 | | . , , | | . , , | | . , , | \$1,240,677 |
| Total O&M Cost | \$2,957,170 | \$3,134,600 | \$3,322,676 | \$3,522,037 | \$3,634,322 | \$3,750,241 | \$3,869,912 | \$3,993,461 | \$4,121,014 | \$4,252,704 | \$4,388,666 | \$4,529,043 | \$4,673,980 | \$4,823,628 | \$4,978,142 | \$5,137,683 | \$5,302,419 | \$5,472,521 | \$5,648,168 | \$5,829,542 |
| Average Annual O&M Cost over 20 years (\$/yr) \$4,367,09 | | | | | | | | | | | | | | | | | | | | |
| Average Annual O&M Cost over 10 years (\$/yr) \$3,655,81 | ÷ | | | | | | | | | | | | | | | | | | | |
| Capital Cost | \$38,236,000 | | | | | | | | | | | | | | | | | | | |
| Equipment Cost | \$18,539,000 | | | | | | | | | | | | | | | | | | | |
| Equipment obst | \$10,000,000 | | | | | | | | | I | | | | | | | | | | |
| Net Present Value (at 5% discount rate) | | | | | | | | | | | | | | | | | | | | |
| 20 Year Net Present Value \$89,800,59 | , | | | | | | | | | | | | | | | | | | | |
| 10 Year Net Present Value \$66,030,00 | 1 | | | | | | | | | | | | | | | | | | | |
| Annual Cost | - | | | | | | | | | | | | | | | | | | | |
| Average Annual Cost (Debt Service + O&M, 20 year basis) \$7,435,25 | 2 | | | | | | | | | | | | | | | | | | | |
| Average Annual Cost (Debt Service + O&M, 10 year basis) \$8,607,55 | | | | | | | | | | | | | | | | | | | | |



Effluent Treatment Evaluation

Alternative 1B: No Hatchery Upgrades and Adsorption Units

Operation and Maintenance

| Component | HP | Quantity | Total HP | Watts | Hours/day | kW-hrs/year |
|-------------------------|-------|----------|----------|---------|---------------|--------------|
| Hatchery Modernization | | | | | | |
| UV System | | 2 | | 56,000 | 24 | 981,120 |
| Drum Filter | 8.0 | 2.0 | 16.00 | 11,931 | 24 | 104,517 |
| Site Lighting | | 1 | | 15,000 | 12 | 65,700 |
| Effluent Treatment | | | 0.00 | 0 | 24 | 0 |
| Effluent Drums | 8.00 | 2 | 16.00 | 11,931 | 24 | 104,517 |
| Clarifier Mechanism | 0.75 | 1 | 0.75 | 559 | 24 | 4,899 |
| Sludge Pump | 20.00 | 1 | 20.00 | 14,914 | 24 | 130,647 |
| Mixing Tank Mixer | 0.00 | 1.00 | 0.00 | 0 | 24 | 0 |
| Membrane Process Pumps | 15.00 | 8.00 | 120.00 | 487,000 | 1 | 177,755 |
| Membrane Blowers | 90.00 | 2.00 | 180.00 | 335,000 | 1 | 122,275 |
| Membrane CIP Pumps | 15.00 | 1.00 | 15.00 | 116,000 | 1 | 42,340 |
| Membrane CIP Heaters | NA | | | 800,000 | 1 | 292,000 |
| Membrane Backpulse Pump | 60.00 | 2.00 | 120.00 | 70,000 | 1 | 25,550 |
| Membrane Drain Pump | 15.00 | 1.00 | 15.00 | 116,000 | 1 | 42,340 |
| | | | | | kW-hrs/year = | 2,093,660 |
| | | | | | \$/kW-hrs = | \$0.12 |
| | | | | | | Annual Cost |
| | | | | | | \$251,239.25 |
| | | | | | | |

| Estimated Annual Replacement Costs | | | | | | Annual Cost |
|------------------------------------|------------------|---------------------|---------------|-------------------|-----------|----------------|
| Annual Equipment Replacement | • | - | | | | \$1,794,000.00 |
| Estimated Annual Labor Costs | Days per Week | Hours per day | Personnel | Rate | OH/Fringe | Annual Cost |
| Daily Operator Attention | 5 | 8 | 2 | \$ 25.00 | \$ 15.00 | \$104,000 |
| Chemicals | Use (gpd) | Annual Use (gal) | Cost (\$/gal) | event per year | | Annual Cost |
| Alum | | 0 | 1.81 | | | \$0 |
| 25% Caustic | | 0 | 1.92 | | | \$0 |
| Нуро | | 18300 | 2.5 | | | \$45,750 |
| Citric | | 38500 | 8.25 | | | \$317,625 |
| Sodium Bisulfate | | 4400 | 3.4 | | | \$14,960 |
| Sulfuric | | | | | | \$0 |
| O2 Usage - Tank refill | | 6000 | 0.6 | 4 | | \$14,400 |
| Adsorption Media Regen | | | | | | \$88,105 |

| | Estimated Annual Labor and Replacement Costs \$ | | | | | | | |
|-------|---|--|--|-------|-------------|--|--|--|
| Estin | Estimated Annual Electricity and Chemical Usage Costs | | | | | | | |
| | | | | TOTAL | \$2,631,000 | | | |

| | | | | | | 1B: No Hatc | Treatment Ev | valuation es and Adso | | | | | | | | | | | | |
|--|--------------|-------------|-------------|-------------|-------------|-------------|--------------|--------------------------|-------------|--------------------------|-------------|-------------|-------------|---------------------|----------------------|-------------|----------------------------|-------------|-------------|-------------|
| | 0 | 1 | 2 | 3 | 4 | 5 | 6 | 7 | 8 | 9 | 10 | 11 | 12 | 13 | 14 | 15 | 16 | 17 | 18 | 19 |
| Total | 2023 | 2024 | 2025 | 2026 | 2027 | 2028 | 2029 | 2030 | 2031 | 2032 | 2033 | 2034 | 2035 | 2036 | 2037 | 2038 | 2039 | 2040 | 2041 | 2042 |
| O&M | | | | | | | | | | | | | | | | | | | | |
| Power and Chemical cost (6%/yr 2023-2026, 3%/yr 2027-2042 escalation) | \$2,631,000 | | \$2,956,192 | , , | \$3,227,570 | \$3,324,397 | | | | | | | | | \$4,337,584 | . , , | \$4,601,743 | | . , , | . , , |
| R&R Maintenance cost (6%/yr 2023-2026, 4%/yr 2027-2042 escalation) | \$620,310 | | \$696,980 | \$738,799 | . , | \$799,085 | \$831,049 | | | \$934,817 \$4,676,455 | | \$1,011,098 | | | | | \$1,230,155 \$5,821,808 | | | |
| Total O&M Cost Average Annual O&M Cost over 20 years (\$/yr) \$4,802 | | \$3,440,309 | \$3,653,172 | \$3,072,302 | \$3,995,921 | \$4,123,482 | \$4,200,170 | \$4,391,143 | \$4,531,521 | \$4,070,455 | \$4,620,097 | \$4,980,602 | \$5,140,131 | \$ 5,304,650 | \$ 5,474,9 31 | \$0,000,003 | \$3,031,090 | \$0,019,150 | \$0,212,323 | \$6,412,206 |
| Average Annual O&M Cost over 20 years (\$/yr) \$4,002 Average Annual O&M Cost over 10 years (\$/yr) \$4,019 | | | | | | | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | | | | | | | |
| Capital Cost | \$43,388,000 | | | | | | | | | | | | | | | | | | | |
| Equipment Cost | \$20,677,000 | | | | | | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | | | | | | | |
| Net Present Value (at 5% discount rate) | | | | | | | | | | | | | | | | | | | | |
| 20 Year Net Present Value \$100,091 | | | | | | | | | | | | | | | | | | | | |
| 10 Year Net Present Value \$73,948 | 000 | | | | | | | | | | | | | | | | | | | |
| Annual Cost | | | | | | | | | | | | | | | | | | | | |
| Average Annual Cost (Debt Service + O&M, 20 year basis) \$8,284 | | | | | | | | | | | | | | | | | | | | |
| Average Annual Cost (Debt Service + O&M, 10 year basis) \$9,638 | 638 | | | | | | | | | | | | | | | | | | | |

Client: NHFGD Project:Powder Mill Fish Hatchery Study Project No.: 10331124

| Estimator: Checked By: | | F |
|---------------------------|------------|----------|
| Check Date: Revised: | 12/27/2022 | |
| | | |

| Detailed Opinions | of Probal | ole Cost | | | |
|-------------------|-----------|----------|----------|-----------------|------------|
| Alternative 2 | NO. | | COST PER | Escalation cost | TOTAL COST |
| | UNITS | MEAS. | UNIT | to 2022 | 50% CONT. |

| Α. | Aquaculture Water Supply | | | | | |
|----|-------------------------------------|------|----|-------|--------|------------|
| A1 | Hatchery Supply | | | | | \$246,695 |
| | Water Supply Piping and Accessories | 1460 | LF | \$ 85 | \$ 113 | \$ 246,695 |
| | | | | | | |

| В. | Buildings and Rearing Units | | | | | |
|----|--------------------------------------|-------|----|---------------|--------------|-----------------|
| B1 | Intake Building | | | | | \$ 1,623,787 |
| | New Intake Building | 400 | SF | \$165.00 | \$ 218 | \$ 131,017 |
| | Drumfilter | | | | | |
| | DRUM FILTERS | 2 | EA | \$ 50,000 | - | \$ 150,000 |
| | DRUM SUMP | 1 | LS | \$ 75,000 | - | \$ 112,500 |
| | PIPING SYSTEMS (INFLOW, DRAINS) | 1 | LS | \$ 500,000 | - | \$ 750,000 |
| | PRIMARY POWER | 1 | LS | \$ 75,000 | - | \$ 112,500 |
| | UV System | | 0 | | | |
| | UV Channel and Lamp Package | 2 | EA | \$ 60,000 | - | \$ 180,000 |
| | UV Electrical | 1 | LS | \$ 8,000 | \$ 10,602 | \$ 15,903 |
| | UV Plumbing | 1 | LS | \$ 11,000 | \$ 14,578 | \$ 21,867 |
| | ALARMS/CONTROLS/MONITORING/PANEL/HMI | 1 | LS | \$ 100,000 | - | \$ 150,000 |
| B2 | Effluent Treatment Building | | | | | \$3,291,093.75 |
| | New Effluent treatment building | 9,219 | SF | \$165.00 | \$ 238 | \$ 3,291,094 |
| | | | | | | |

| B 3 | Vehicle/Chemical Storage Building | | | | | | \$ 655,999 |
|------------|--|--------|----|----|----------|--------------|------------------|
| | New Storage Building (40'x50') | 2000 | SF | \$ | 165 | \$ 219 | \$ 655,999 |
| B5 | Hatchery Building | | | | | | \$4,229,021.87 |
| | New Hatchery Building - Office Space | 3700 | SF | | \$165.00 | \$ 218 | \$ 1,211,910 |
| | POWER AND LIGHTING | 3700 | SF | \$ | 50 | \$103.40 | \$ 573,847 |
| | HVAC | 1 | LS | \$ | 100,000 | \$206,791.77 | \$ 310,188 |
| | EQUIPMENT | | | | | | |
| | FEEDERS (SWEENEY MDL AF7 W/CONTROLLER & SUPPORT) | 72 | EA | \$ | 600 | \$1,240.75 | \$ 134,001 |
| | FG TROUGHS (12'x2'x2') | 42 | EA | \$ | 2,500 | \$5,169.79 | \$ 325,697 |
| | INCUBATION ROOM 30 HEATH STACKS | 12 | EA | \$ | 2,500 | \$5,169.79 | \$ 93,056 |
| | INCUBATION HEAD TROUGHS AND CONTROLS | 2 | LS | \$ | 15,000 | \$31,018.77 | \$ 93,056 |
| | CHILLER SYSTEM AND CONTROLS | 1 | LS | \$ | 250,000 | \$516,979.42 | \$ 775,469 |
| | FORMALIN ROOM | 1 | LS | \$ | 50,000 | \$103,395.88 | \$ 155,094 |
| | BOOT LOCKER ROOM, W/D, BENCHES | 1 | LS | \$ | 50,000 | \$103,395.88 | \$ 155,094 |
| | WATER QUALITY ROOM EQUIP ALLOWANCE | 1 | LS | \$ | 75,000 | \$155,093.83 | \$ 232,641 |
| | Hatchery Building Aeration/Degassing System | | | | | | |
| | Primary Headtank & Aeration/Degassing System | 1 | EA | \$ | 85,000 | \$ 112,646 | \$ 168,969 |
| B6 | Rearing Building | | | | | | \$30,151,818.18 |
| | New Rearing Building | 73.640 | SF | \$ | 165 | \$ 218 | \$ 24,120,276 |
| | ALARMS/CONTROLS/MONITORING/PANEL/HMI | , | LS | \$ | 100.000 | - | \$ 150,000 |
| | VED W/CIRCUIT BREAKER AND FULL CONTACTOR SET | 2 | EA | \$ | 25,000 | - | \$ 75,000 |
| | PANEL/RACK/WIRING/CONDUITS/FEEDER | | EA | \$ | 55,000 | _ | \$ 165,000 |
| | 12" FLOW METER | | EA | \$ | 18,000 | - | \$ 54,000 |
| | EQUIPMENT | | | | | | |
| | 20' dia. SS Culture Tank with Foundation & Floor | 20 | EA | \$ | 35,000 | - | \$ 1,050,000 |
| | 40' dia. SS Culture Tank with Foundation & Floor | 16 | EA | \$ | 50,000 | - | \$ 1,200,000 |
| | Drumfilter | | | | | | |
| | DRUM FILTERS | 6 | EA | \$ | 50,000 | - | \$ 450,000 |
| | DRUM SUMP | 1 | LS | \$ | 75,000 | - | \$ 112,500 |
| | PRIMARY POWER | 1 | LS | \$ | 75,000 | - | \$ 112,500 |
| | UV System | | 0 | 1 | | | |

| UV Channel and Lamp Package | 6 | EA | \$ 60,000 | - | \$ 540,000 |
|---------------------------------------|---|----|---------------|------------|---------------|
| UV Electrical | 1 | LS | \$ 8,000 | \$ 10,602 | \$ 15,903 |
| UV Plumbing | 1 | LS | \$ 11,000 | \$ 14,578 | \$ 21,867 |
| Recirculation | | | | | |
| PIPING SYSTEMS (INFLOW, PRAS, DRAINS) | 1 | LS | \$ 500,000 | - | \$ 750,000 |
| Lift Pump | 6 | EA | \$ 80,000 | - | \$ 720,000 |
| 4ft Precast Manhole 4 ft deep | 6 | EA | \$ 4,200 | \$6,641.45 | \$ 59,773 |
| HVAC | 1 | LS | \$ 100,000 | - | \$ 150,000 |
| GAS MANAGEMENT TOWER CO2 STRIPPER/LHO | 6 | EA | \$ 45,000 | - | \$ 405,000 |
| | | | | | |

| C. | Site | | | | | |
|----|--|------|----|--------------|--------------|---------------|
| C1 | Site Work | | | | | \$835,155.69 |
| | Site Clearing | 2.5 | AC | \$2,000.00 | \$2,650.50 | \$ 9,939 |
| | General Earthwork for Hatchery Complex | 1 | LS | \$75,000.00 | \$99,393.71 | \$ 149,091 |
| | General Sitework | 1 | LS | \$250,000.00 | \$331,312.38 | \$ 496,969 |
| | Erosion Control | 20 | AC | \$2,500.00 | \$3,313.12 | \$ 99,394 |
| | Seeding | 1 | AC | \$1,250.00 | \$1,656.56 | \$ 2,485 |
| | Landscaping | 1 | AC | \$3,000.00 | \$3,975.75 | \$ 5,964 |
| | Natural Gas Connection and Distribution (if available) | 0 | LS | \$35,000.00 | \$46,383.73 | \$ - |
| | Stormwater Management System | 10.3 | AC | \$3,500.00 | \$4,638.37 | \$ 71,315 |
| C2 | Security Fence | | | | | \$3,975.75 |
| | Site Fencing | 100 | LF | \$20.00 | \$26.50 | \$ 3,976 |
| C3 | Domestic Water | | | | | \$49,696.86 |
| | Domestic Water Supply | 1 | LS | \$25,000.00 | \$33,131.24 | \$ 49,697 |
| C4 | Domestic Wastewater | | | | | \$99,393.71 |
| | Domestic Wastewater System | 1 | LS | \$50,000.00 | \$66,262.48 | \$ 99,394 |
| C5 | Disinfection Station | | | | | \$22,500.00 |
| | Truck Disinfection Station | 1 | LS | \$15,000.00 | - | \$ 22,500 |
| | Roadway Aggregate | 0 | SY | \$15.00 | - | \$ - |
| | Electrical | 0 | LS | \$2,500.00 | - | \$ - |

| | Detention Tank | 0 | LS | \$5,000.00 | - | \$ - |
|----|---|---|----|--------------|--------------|---------------|
| C6 | Paved Access to State or Local Highways | | | | | \$377,696.12 |
| | Bituminous Paved Road | 1 | LS | \$190,000.00 | \$251,797.41 | \$ 377,696 |
| | Gravel Roads | 0 | LS | \$55,000.00 | \$72,888.72 | \$ - |
| | | | | | | |
| | | | | | | |

|). | Aquaculture Wastewater | | | | | |
|----|--------------------------------------|-----|----|---------------|---------------|---------------|
| D1 | Effluent Treatment | | | | | \$29,254,369 |
| | | | | | | |
| | Clarifier-40ft | | | | | |
| | Clarifier Concrete | 211 | CY | \$ 1,500 | - | \$ 474,750 |
| | Clarifer Excavation | 898 | CY | \$ 50 | - | \$ 67,350 |
| | Clarifier Equipment | 1 | LS | \$ 144,000 | \$ 227,707 | \$ 341,560 |
| | Clarifier Coatings | 1 | LS | \$ 16,000 | \$ 25,301 | \$ 37,951 |
| | Finger Weirs | 1 | LS | \$ 8,000 | 12,650 | \$ 18,976 |
| | Duplex Pump Station | 1 | LS | \$ 24,000 | \$ 37,951 | \$ 56,927 |
| | 3" Sch 80 PVC Pipe | 100 | LF | \$ 48 | \$ 76 | \$ 11,385 |
| | 4" Sch 80 PVC Pipe | 250 | LF | \$ 80 | \$ 127 | \$ 47,439 |
| | 3" Plug Valves | 2 | EA | \$ 4,000 | \$ 6,325 | \$ 18,976 |
| | 3" Swing Check Valves | 2 | EA | \$ 2,720 | \$ 4,301 | \$ 12,903 |
| | Telescoping Valves | 2 | EA | \$ 1,520 | \$ 2,404 | \$ 7,211 |
| | 6 ft precast manhole 6 ft deep | 2 | EA | \$ 12,000 | \$ 18,976 | \$ 56,927 |
| | 4ft Precast Manhole 4 ft deep | 1 | EA | \$ 6,720 | \$ 10,626 | \$ 15,939 |
| | Clarifier Equipment Install | 1 | LS | \$ 28,800 | \$ 45,541 | \$ 68,312 |
| | Sludge Storage-40ft | | | | | |
| | Sludge Storage Concrete | 215 | CY | \$ 1,500 | - | \$ 483,750 |
| | Sludge Storage Excavation | 976 | CY | \$ 50 | - | \$ 73,200 |
| | Sludge Mixing Pump | 1 | LS | \$ 10,000 | \$ 15,813 | \$ 23,719 |
| | Sludge Mixing Nozzles | 1 | LS | \$ 35,000 | \$ 55,345 | \$ 83,018 |
| | 4" Sch 80 PVC Pipe | 300 | LF | \$ 50 | \$ 79 | \$ 35,579 |
| | Telescoping Valves | 1 | EA | \$ 950 | \$ 1,502 | \$ 2,253 |
| | 3" Plug Valves | 1 | EA | \$ 2,500 | \$ 3,953 | \$ 5,930 |
| | 3" Swing Check Valves | 1 | EA | \$ 1,700 | 2,688 | \$ 4,032 |
| | Air Release Valve | 2 | EA | \$ 450 | \$ 712 | \$ 2,135 |
| | Sludge Mix & Transfer System Install | 1 | LS | \$ 13,210 | \$ 20,889 | \$ 31,333 |

| Phosphorus Removal | | | | | |
|--|------|----|------------------|---|----------------|
| Membrane | | | | | |
| Membrane Filtration System | 1 | EA | \$ 11,480,000 | - | \$ 17,220,0 |
| Chemical Storage Membrane Cleaning | 1 | EA | \$ 8,770 | - | \$ 13,1 |
| Membrane Install (25% of Materials) | 1 | LS | \$ 2,872,193 | - | \$ 4,308,2 |
| Chemcial Addition | | | | | |
| Mixing/Reaction Tank Concrete | 246 | CY | \$ 1,500 | - | \$ 553,5 |
| Mixing/Reaction Tank 2:1 Excavation | 1548 | CY | \$ 50 | - | \$ 116,2 |
| Mixing/Reaction Tank MISC Piping | 1 | LS | \$ 40,000 | - | \$ 60,0 |
| Mixing/Reaction Mixing Pumps | 1 | EA | \$ 52,595 | - | \$ 78,8 |
| Chemical Dosing | 1 | EA | \$ 20,000 | - | \$ 30,0 |
| Chemical Storage Coagulation | 1 | EA | \$ 3,215 | - | \$ 4,8 |
| Chemical Addition Install (25% of Materials) | 1 | LS | \$ 121,203 | - | \$ 181,8 |
| Adsorption | | | | | |
| Adsorption Columns | 5 | EA | \$ 250,000 | - | \$ 1,875,0 |
| Adsorption Media | 2520 | CF | \$ 500 | - | \$ 1,890,0 |
| Asorption Install (25% of Materials) | 1 | LS | \$ 627,500 | - | \$ 941,2 |

| D2 | Effluent Monitoring | | | | | \$64,605.91 |
|----|--------------------------------------|---|----|-------------|-----------------|--------------|
| | Automated Flow Measurement Equipment | 1 | LS | \$25,000.00 | \$ 33,131.24 | \$ 49,697 |
| | Portable Composite Sampler | 1 | LS | \$5,000.00 | \$ 6,626.25 | \$ 9,939 |
| | Electrical | 1 | LS | \$2,500.00 | \$ 3,313.12 | \$ 4,970 |
| | | | | | | |

| E. | Electrical and HVAC | | | | | |
|----|--------------------------------|---|----|-------------|-----------------|---------------|
| E1 | Electrical Service | | | | | \$189,757.49 |
| | Security Lighting | 8 | EA | \$2,500.00 | \$ 3,313.12 | \$ 39,757 |
| | 3-phase service | 1 | EA | \$ 100,000 | - | \$ 150,000 |
| E2 | Emergency Power | | | | | \$216,678.30 |
| | Emergency Generator: 100-200kW | 1 | LS | \$75,000.00 | \$ 99,393.71 | \$ 149,091 |
| | Automatic Transfer Switch | 1 | LS | \$20,000.00 | \$ 26,504.99 | \$ 39,757 |

| | Fuel Tank | 1 | LS | \$14,000.00 | \$ 18,553.49 | \$ 27,830 |
|----|---|---|----|--------------|---------------|---------------|
| | | | | | | |
| E3 | Instrumentation and Alarm System | | | | | \$347,878.00 |
| | Instrumentation, Alarm System & Communication | 1 | LS | \$175,000.00 | \$ 231,918.67 | \$ 347,878 |
| | | | | | | |
| | | | | | | |

| F. | Visitor Education/Interpretation | | | | | |
|----|---|------|----|-------------|---|---------------|
| F1 | Hatchery Building - Displays | | | | | \$817,500.00 |
| | Display Materials | 1 | LS | \$20,000.00 | - | \$ 30,000 |
| | New visitor's center building (Display Area, Public Restrooms, & Mechanical spa | 1500 | SF | \$350.00 | - | \$ 787,500 |
| | | | | - | | \$71,821,623 |



Effluent Treatment Evaluation

Alternative 2A: 75% Recirculation with Chemical Dosing

Operation and Maintenance

| Component | HP | Quantity | Total HP | Watts | Hours/day | kW-hrs/year | | |
|--|------------------|---|---|-------------------------------|--|---|--|--|
| Hatchery Modernization | | | | | | | | |
| UV System | | 8 | | 56,000 | 24 | 3,924,480 | | |
| Drum Filter | 8.0 | 8.0 | 64.00 | 47,725 | 24 | 418,069 | | |
| Recirc. Pump | 15.0 | 6.0 | 90.00 | 67,113 | 24 | 587,910 | | |
| Site Lighting | | 1 | | 15,000 | 12 | 65,700 | | |
| Miscellaneous (SCADA, Meters, etc.) | | 1 | | 15,000 | 24 | 131,400 | | |
| Effluent Treatment | | | | | | | | |
| Clarifier Mechanism | 0.75 | 1 | 0.75 | 559 | 24 | 4,899 | | |
| Sludge Pump | 20.00 | 1 | 20.00 | 14,914 | 24 | 130,647 | | |
| Mixing Tank Mixer | 3 | 1 | 3.00 | 2,237 | 24 | 19,597 | | |
| Membrane Process Pumps | 15.00 | 8.00 | 120.00 | 487,000 | 1 | 177,755 | | |
| Membrane Blowers | 90.00 | 2.00 | 180.00 | 335,000 | 1 | 122,275 | | |
| Membrane CIP Pumps | 15.00 | 1.00 | 15.00 | 116,000 | 1 | 42,340 | | |
| Membrane CIP Heaters | NA | | | 800,000 | 1 | 292,000 | | |
| Membrane Backpulse Pump | 60.00 | 2.00 | 120.00 | 70,000 | 1 | 25,550 | | |
| Membrane Drain Pump | 15.00 | 1.00 | 15.00 | 116,000 | 1 | 42,340 | | |
| | | | | | <w-hrs year="<br">\$/kW-hrs =</w-hrs> | 5,984,962 \$0.12 | | |
| | | | - | | | \$0.12 Annual Cost | | |
| | | · | | | | | | |
| Estimated Annual Replacement Costs | | | | | | \$0.12 Annual Cost | | |
| | | | | | | \$0.12 Annual Cost \$718,195 | | |
| Estimated Annual Replacement Costs Annual Equipment Replacement Estimated Annual Labor Costs | Days per Week | Hours per day | Personnel | Rate | | \$0.12 Annual Cost \$718,195 Annual Cost | | |
| Annual Equipment Replacement Estimated Annual Labor Costs | | day 8 | Personnel 2 | | \$/kW-hrs = | \$0.12 Annual Cost \$718,195 Annual Cost \$1,762,000 | | |
| Annual Equipment Replacement Estimated Annual Labor Costs Daily Operator Attention | Week | day | | Rate | \$/kW-hrs = OH/Fringe | \$0.12 Annual Cost \$718,195 Annual Cost \$1,762,000 Annual Cost | | |
| Annual Equipment Replacement Estimated Annual Labor Costs Daily Operator Attention Chemicals | Week 5 | day 8 Annual Use | 2 | Rate \$ 25.00 event per | \$/kW-hrs = OH/Fringe | \$0.12 Annual Cost \$718,195 Annual Cost \$1,762,000 Annual Cost \$104,000 | | |
| Annual Equipment Replacement Estimated Annual Labor Costs Daily Operator Attention Chemicals Alum | Week 5 | day 8 Annual Use (gal) | 2 Cost (\$/gal) | Rate \$ 25.00 event per | \$/kW-hrs = OH/Fringe | \$0.12 Annual Cost \$718,195 Annual Cost \$1,762,000 Annual Cost \$104,000 Annual Cost | | |
| Annual Equipment Replacement Estimated Annual Labor Costs Daily Operator Attention Chemicals Alum 25% Caustic | Week 5 | day 8 Annual Use (gal) 7908 | 2 Cost (\$/gal) 1.81 | Rate \$ 25.00 event per | \$/kW-hrs = OH/Fringe | \$0.12 Annual Cost \$718,195 Annual Cost \$1,762,000 Annual Cost \$104,000 Annual Cost \$14,313.48 | | |
| Annual Equipment Replacement Estimated Annual Labor Costs Daily Operator Attention Chemicals Alum 25% Caustic Hypo | Week 5 | day 8 Annual Use (gal) 7908 6570 | 2 Cost (\$/gal) 1.81 1.92 | Rate \$ 25.00 event per | \$/kW-hrs = OH/Fringe | \$0.12 Annual Cost \$718,195 Annual Cost \$1,762,000 Annual Cost \$104,000 Annual Cost \$14,313.48 \$12,614.40 \$45,750.00 | | |
| Annual Equipment Replacement Estimated Annual Labor Costs Daily Operator Attention Chemicals Alum 25% Caustic Hypo Citric | Week 5 | day 8 Annual Use (gal) 7908 6570 18300 | 2 Cost (\$/gal) 1.81 1.92 2.5 | Rate \$ 25.00 event per | \$/kW-hrs = OH/Fringe | \$0.12 Annual Cost \$718,195 Annual Cost \$1,762,000 Annual Cost \$104,000 Annual Cost \$14,313.48 \$12,614.40 \$45,750.00 | | |
| Annual Equipment Replacement Estimated Annual Labor Costs Daily Operator Attention Chemicals Alum 25% Caustic Hypo Citric Sodium Bisulfate | Week 5 | day 8 Annual Use (gal) 7908 6570 18300 38500 38500 | 2 Cost (\$/gal) 1.81 1.92 2.5 8.25 | Rate \$ 25.00 event per | \$/kW-hrs = OH/Fringe | \$0.12 Annual Cost \$718,195 Annual Cost \$1,762,000 Annual Cost \$104,000 Annual Cost \$14,313.48 \$12,614.40 \$45,750.00 \$317,625.00 | | |
| Annual Equipment Replacement | Week 5 | day 8 Annual Use (gal) 7908 6570 18300 38500 38500 | 2 Cost (\$/gal) 1.81 1.92 2.5 8.25 | Rate \$ 25.00 event per | \$/kW-hrs = OH/Fringe | \$0.12 Annual Cost \$718,195 Annual Cost \$1,762,000 Annual Cost \$104,000 Annual Cost \$14,313.48 \$12,614.40 \$45,750.00 \$317,625.00 \$14,960.00 | | |

| Estimated Annual Labor and Replacement Costs | \$1,866,000 |
|---|-------------|
| Estimated Annual Electricity and Chemical Usage Costs | \$1,166,658 |
| TOTAL | \$3,033,000 |

| | | | | | | /e 2A: 75% R | Freatment Ev | valuation with Chemic | | | | | | | | | | | | |
|--|---------------------|-------------|-------------|-------------|-------------|--------------|--------------|--------------------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|
| | | | | | | | | | | | | | | | | | | | | |
| Total 2023 2024 2025 2026 2027 2028 2029 2030 2031 2032 2033 2034 2035 2036 2037 2038 2039 2040 2041 204 | | | | | | | | | | | | | | | 2042 | | | | | |
| | O&M | | | | | | | | | | | | | | | | | | | |
| Power and Chemical cost (6%/yr 2023-2026, 3%/yr 2023-2026 | | | | | | | | | | | | | | | ,, . | | | | | |
| R&R Maintenance cost (6%/yr 2023-2026, 4%/yr 2027-2042 escalation) \$609,180 \$645,731 \$684,475 \$725,543 \$754,565 \$784,747 \$816,137 \$848,783 \$892,734 \$919,044 Total O&M Cost \$3,642,180 \$3,860,711 \$4,092,353 \$4,475,287 \$4,617,091 \$4,763,451 \$4,914,516 \$5,3070,440 \$5,397,502 \$5,568,975 \$5,745,974 \$5,928,679 \$6,117,280 \$6,311,967 \$6,512,943 \$6,720,412 \$6,934,588 \$7,155 | | | | | | | | | | | | | | | | | | | | |
| Total O&M Cost | | \$3,860,711 | \$4,092,353 | \$4,337,895 | \$4,475,287 | \$4,617,091 | \$4,763,451 | \$4,914,516 | \$5,070,440 | \$5,231,380 | \$5,397,502 | \$5,568,975 | \$5,745,974 | \$5,928,679 | \$6,117,280 | \$6,311,967 | \$6,512,943 | \$6,720,412 | \$6,934,588 | \$7,155,692 |
| Average Annual O&M Cost over 20 years (\$/yr) \$5,369,966 | | | | | | | | | | | | | | | | | | | | |
| Average Annual O&M Cost over 10 years (\$/yr) \$4,500,530 | | | | | | | | | | | | | | | | | | | | |
| Capital Cost | \$74,218,000 | | | | | | | | | | | | | | | | | | | |
| Equipment Cost | \$20,306,000 | | | | | | | | | | | | | | | | | | | |
| Equipment Cost | \$20,300,000 | | | | | | | | | I | 1 | | | | | | | | | |
| Net Present Value (at 5% discount rate) | | | | | | | | | | | | | | | | | | | | |
| 20 Year Net Present Value \$137,643,717 | | | | | | | | | | | | | | | | | | | | |
| 10 Year Net Present Value \$108,436,000 | | | | | | | | | | | | | | | | | | | | |
| Annual Cost | - | | | | | | | | | | | | | | | | | | | |
| Average Annual Cost (Debt Service + O&M, 20 year basis) \$11,325,410 | | | | | | | | | | | | | | | | | | | | |

Average Annual Cost (Debt Service + O&M, 10 year basis) \$14,112,101



Effluent Treatment Evaluation

Alternative 2B: 75% Recirculation with Adsorption Units

Operation and Maintenance

| Component | HP | Quantity | Total HP | Watts | Hours/day | kW-hrs/year |
|-------------------------------------|------------------|---------------------|---------------|-------------------|--------------------|----------------|
| Hatchery Modernization | | | | | | |
| UV System | | 8 | | 56,000 | 24 | 3,924,480 |
| Drum Filter | 8.0 | 8.0 | 64.00 | 47,725 | 24 | 418,069 |
| Recirc. Pump | 15.0 | 6.0 | 90.00 | 67,113 | 24 | 587,910 |
| Site Lighting | | 1 | | 15,000 | 12 | 65,700 |
| Miscellaneous (SCADA, Meters, etc.) | | 1 | | 15,000 | 24 | 131,400 |
| | | | 0.00 | 0 | 24 | 0 |
| Effluent Treatment | | | | | | |
| Clarifier Mechanism | 0.75 | 1 | 0.75 | 559 | 24 | 4,899 |
| Sludge Pump | 20.00 | 1 | 20.00 | 14,914 | 24 | 130,647 |
| Mixing Tank Mixer | 0 | 1 | 0.00 | 0 | 24 | 0 |
| Membrane Process Pumps | 15.00 | 8.00 | 120.00 | 487,000 | 1 | 177,755 |
| Membrane Blowers | 90.00 | 2.00 | 180.00 | 335,000 | 1 | 122,275 |
| Membrane CIP Pumps | 15.00 | 1.00 | 15.00 | 116,000 | 1 | 42,340 |
| Membrane CIP Heaters | NA | | | 800,000 | 1 | 292,000 |
| Membrane Backpulse Pump | 60.00 | 2.00 | 120.00 | 70,000 | 1 | 25,550 |
| Membrane Drain Pump | 15.00 | 1.00 | 15.00 | 116,000 | 1 | 42,340 |
| | | | | | | |
| | | | | | | |
| | | | | | | |
| | | | | | | |
| | | | ļ | I | ı kW-hrs/year = | 5,965,365 |
| | | | | | \$/kW-hrs = | \$0.12 |
| | | | | | | Annual Cost |
| | | | | | | \$715,843.78 |
| | | | | | | Annual Cost |
| Estimated Annual Replacement Costs | | | | | | Annual Cost |
| Annual Equipment Replacement | | | | | | \$1,915,000.00 |
| Estimated Annual Labor Costs | Days per Week | Hours per day | Personnel | Rate | OH/Fringe | Annual Cost |
| Daily Operator Attention | 5 | 8 | 2 | \$ 25.00 | \$ 15.00 | \$104,000 |
| Chemicals | Use (gpd) | Annual Use (gal) | Cost (\$/gal) | event per year | | Annual Cost |
| Alum | | 0 | 1.81 | | | \$0 |
| 25% Caustic | | 0 | 1.92 | | | \$0 |
| Нуро | | 18300 | 2.5 | | | \$45,750 |
| Citric | | 38500 | 8.25 | | | \$317,625 |
| Sodium Bisulfate | | 4400 | 3.4 | | | \$14,960 |
| Sulfuric | | 1 | | | | \$0 |

| O2 Usage - Tank refill | 6000 | 0.6 | \$ 3,600.00 | 12 | \$43,200.00 |
|------------------------|------|-----|-------------|----|--------------|
| Adsorption Media Regen | | | | | \$131,102.49 |

| Estimated Annual Labor and Replacement Costs | \$2,019,000 |
|---|-------------|
| Estimated Annual Electricity and Chemical Usage Costs | \$1,268,481 |
| TOTAL | \$3,288,000 |

| | | | | | | | re 2B: 75% Re | Freatment Ev | aluation with Adsorpt | | | | | | | | | | | | |
|---|-------------|------------|------|------|------|------|---------------|--------------|--------------------------|------|------|------|------|-------------|---------|------|------|------|------|------|------|
| 0 1 2 3 4 5 6 7 8 9 10 11 12 13 14 15 16 17 18 19 | | | | | | | | | | | | | | | 19 | | | | | | |
| Tot | tal | 2023 | 2024 | 2025 | 2026 | 2027 | 2028 | 2029 | 2030 | 2031 | 2032 | 2033 | 2034 | 2035 | 2036 | 2037 | 2038 | 2039 | 2040 | 2041 | 2042 |
| O&M | | | | | | | | | | | | | | | | | | | | | |
| Comm Power and Chemical cost (6%/yr 2023-2026, 3%/yr 2027-2042 escalation) \$3,288,000 \$3,485,280 \$3,694,397 \$3,916,061 \$4,033,542 \$4,154,549 \$4,279,185 \$4,675,981 \$4,816,261 \$4,960,748 \$5,109,571 \$5,262,858 \$5,750,867 \$5,923,393 \$6,101,095 \$6,284,154,549 | | | | | | | | | | | | | | | , . , . | | | | | | |
| R&R Maintenance cost (6%/yr 2023-2026, 4%/yr 2027-2042 escalation) \$662,040 \$71,325,340 \$4,273,103 \$4,273,103 \$4,273,103 \$4,273,103 \$4,273,103 \$4,273,103 \$4,273,103 \$4,273,103 \$4,273,103 \$4,273,103 \$4,273,103 \$4,273,103 \$4,203,001 \$4,303,011 \$4,303,0 | | | | | | | | | | | | | | | | | | | | | |
| Total O&M Cost \$3,950,040 \$4,187,042 \$4,438,265 \$4,704,561 \$4,853,583 \$5,007,391 \$5,166,141 \$5,329,994 \$5,499,119 \$5,673,686 \$5,853,873 \$6,039,865 \$6,231,853 \$6,430,031 \$6,634,604 \$6,845,780 \$7,063,778 \$7,288,820 \$7,521,139 \$7, | | | | | | | | | | | | | | \$7,760,974 | | | | | | | |
| Average Annual O&M Cost over 20 years (\$/yr) \$5,8 | 324,027 | | | | | | | | | | | | | | | | | | | | |
| Average Annual O&M Cost over 10 years (\$/yr) \$4,8 | 380,982 | | | | | | | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | | | | | | | | |
| Capital Cost | | 78,284,000 | | | | | | | | | | | | | | | | | | | |
| Equipment Cost | \$2 | 22,068,000 | | | | | | | | | | | | | | | | | | | |
| Net Present Value (at 5% discount rate) | | | | | | | | | | | | | | | | | | | | | |
| 20 Year Net Present Value (at 5% discount rate) | 172 365 | | | | | | | | | | | | | | | | | | | | |
| 10 Year Net Present Value \$115,3 | , | | | | | | | | | | | | | | | | | | | | |
| Annual Cost | 33,000 | | | | | | | | | | | | | | | | | | | | |
| | 105,738 | | | | | | | | | | | | | | | | | | | | |
| |) 19,118 | | | | | | | | | | | | | | | | | | | | |
| Average Annual Cost (Debt Service + Okivi, 10 year basis) ϕ (13,0 | 515,110 | | | | | | | | | | | | | | | | | | | | |

| Date: | 10/13/2022 | |
|-----------------|------------------------------|--|
| Estimator: | Matt Cochran & Mario Benisch | |
| Checked By: | Jason Hill | |
| Check Date: | 12/27/2022 | |
| Revised: | - | |
| | | |

| Detailed Opinions of Probable Cost | | | | | | | | | | |
|------------------------------------|-------|-------|----------|-----------------|------------|--|--|--|--|--|
| | NO. | UNIT | COST PER | Escalation cost | TOTAL COST | | | | | |
| Alternative 3 | UNITS | MEAS. | UNIT | to 2022 | 50% CONT. | | | | | |

| Α. | Aquaculture Water Supply | | | | | | |
|----|-------------------------------------|------|----|-------|--------|------|---------|
| A1 | Hatchery Supply | | | | | \$ | 246,695 |
| | Water Supply Piping and Accessories | 1460 | LF | \$ 85 | \$ 113 | \$ 2 | 246,695 |
| | | | | | | | |

| В. | Buildings and Rearing Units | | | | | |
|----|--------------------------------------|-------|----|---------------|--------------|-----------------|
| B1 | Intake Building | | | | | \$ 1,623,787 |
| | New Intake Building | 400 | SF | \$ 165 | \$ 218 | \$ 131,017 |
| | Drumfilter | | | | | |
| | DRUM FILTERS | 2 | EA | \$ 50,000 | - | \$ 150,000 |
| | DRUM SUMP | 1 | LS | \$ 75,000 | - | \$ 112,500 |
| | PIPING SYSTEMS (INFLOW, DRAINS) | 1 | LS | \$ 500,000 | - | \$ 750,000 |
| | PRIMARY POWER | 1 | LS | \$ 75,000 | - | \$ 112,500 |
| | UV System | | 0 | | | |
| | UV Channel and Lamp Package | 2 | EA | \$ 60,000 | - | \$ 180,000 |
| | UV Electrical | 1 | LS | \$ 8,000 | \$ 10,602 | \$ 15,903 |
| | UV Plumbing | 1 | LS | \$ 11,000 | \$ 14,578 | \$ 21,867 |
| | ALARMS/CONTROLS/MONITORING/PANEL/HMI | 1 | LS | \$ 100,000 | - | \$ 150,000 |
| B2 | Effluent Treatment Building | | | | | \$1,959,037.50 |
| | New Effluent treatment building | 5,488 | SF | \$165.00 | \$ 238 | \$ 1,959,038 |
| | | | | | | |

| B 3 | Vehicle/Chemical Storage Building | | | | | | \$ 655,999 |
|------------|--|--------|----------|------------|-----------------|--------------|------------------|
| | New Storage Building (40'x50') | 2000 | SF | F : | \$ 165 | \$ 219 | \$ 655,999 |
| B5 | Hatchery Building | | | | | | \$4,229,021.87 |
| | New Hatchery Building - Office Space | 3700 | SF | F | \$165.00 | \$ 218 | \$ 1,211,910 |
| | POWER AND LIGHTING | 3700 | SF | 5 | \$ 50 | \$103.40 | \$ 573,847 |
| | HVAC | 1 | LS | | \$ 100,000 | \$206,791.77 | \$ 310,188 |
| | EQUIPMENT | | | | | | |
| | FEEDERS (SWEENEY MDL AF7 W/CONTROLLER & SUPPORT) | 72 | EA | | \$ 600 | \$1,240.75 | \$ 134,001 |
| | FG TROUGHS (12'x2'x2') | 42 | EA | | \$ 2,500 | \$5,169.79 | \$ 325,697 |
| | INCUBATION ROOM 30 HEATH STACKS | 12 | EA | | \$ 2,500 | \$5,169.79 | \$ 93,056 |
| | INCUBATION HEAD TROUGHS AND CONTROLS | 2 | LS | | \$ 15,000 | \$31,018.77 | \$ 93,056 |
| | CHILLER SYSTEM AND CONTROLS | 1 | LS | 5 | \$ 250,000 | \$516,979.42 | \$ 775,469 |
| | FORMALIN ROOM | 1 | LS | 5 | \$ 50,000 | \$103,395.88 | \$ 155,094 |
| | BOOT LOCKER ROOM, W/D, BENCHES | 1 | LS | | \$ 50,000 | \$103,395.88 | \$ 155,094 |
| | WATER QUALITY ROOM EQUIP ALLOWANCE | 1 | LS | 5 | \$ 75,000 | \$155,093.83 | \$ 232,641 |
| | Hatchery Building Aeration/Degassing System | | | | | | |
| | Primary Headtank & Aeration/Degassing System | 1 | EA | A : | \$ 85,000 | \$ 112,646 | \$ 168,969 |
| | | | | | | | |
| B6 | Rearing Building | | | | | | \$31,951,818.18 |
| | New Rearing Building (526x140) | 73,640 | SF | | \$ 165 | \$ 218 | \$ 24,120,276 |
| | ALARMS/CONTROLS/MONITORING/PANEL/HMI | | LS | | \$ 100,000 | - | \$ 150,000 |
| | VFD W/CIRCUIT BREAKER AND FULL CONTACTOR SET | | 2 EA | | \$ 25,000 | - | \$ 75,000 |
| | PANEL/RACK/WIRING/CONDUITS/FEEDER | - | EA | | \$ 55,000 | | \$ 165,000 |
| | 12" FLOW METER | 2 | EA | 5 | \$ 18,000 | | \$ 54,000 |
| | EQUIPMENT | | | - | | | |
| | 20' dia. SS Culture Tank with Foundation & Floor | 20 | EA | | \$ 35,000 | - | \$ 1,050,000 |
| | 40' dia. SS Culture Tank with Foundation & Floor | 16 | EA | <u>م</u> : | \$ 50,000 | - | \$ 1,200,000 |
| | | | <u> </u> | | ф <u>го ооо</u> | | 450.000 |
| | DRUM FILTERS | 6 | EA | | \$ 50,000 | - | \$ 450,000 |
| | | 1 | LS | | \$ 75,000 | - | \$ 112,500 |
| | PRIMARY POWER | 1 | LS | | \$ 75,000 | - | \$ 112,500 |
| | UV System | | 0 | | | | |

| UV Channel and Lamp Package | 6 | EA | \$ 60,000 | - | \$ 540,000 |
|---------------------------------------|---|----|---------------|------------|-----------------|
| UV Electrical | 1 | LS | \$ 8,000 | \$ 10,602 | \$ 15,903 |
| UV Plumbing | 1 | LS | \$ 11,000 | \$ 14,578 | \$ 21,867 |
| Recirculation | | | | | |
| PIPING SYSTEMS (INFLOW, PRAS, DRAINS) | 1 | LS | \$ 500,000 | - | \$ 750,000 |
| Lift Pump | 6 | EA | \$ 80,000 | - | \$ 720,000 |
| 4ft Precast Manhole 4 ft deep | 6 | EA | \$ 4,200 | \$6,641.45 | \$ 59,773 |
| Biofilter System | | | | | |
| MBBR | 6 | EA | \$ 200,000 | - | \$ 1,800,000 |
| HVAC | 1 | LS | \$ 100,000 | - | \$ 150,000 |
| GAS MANAGEMENT TOWER CO2 STRIPPER/LHO | 6 | EA | \$ 45,000 | - | \$ 405,000 |
| | | | | | |

| C. | Site | | | | | |
|----|--|------|----|--------------|--------------|---------------|
| C1 | Site Work | | | | | \$835,155.69 |
| | Site Clearing | 2.5 | AC | \$2,000.00 | \$2,650.50 | \$ 9,939 |
| | General Earthwork for Hatchery Complex | 1 | LS | \$75,000.00 | \$99,393.71 | \$ 149,091 |
| | General Sitework | 1 | LS | \$250,000.00 | \$331,312.38 | \$ 496,969 |
| | Erosion Control | 20 | AC | \$2,500.00 | \$3,313.12 | \$ 99,394 |
| | Seeding | 1 | AC | \$1,250.00 | \$1,656.56 | \$ 2,485 |
| | Landscaping | 1 | AC | \$3,000.00 | \$3,975.75 | \$ 5,964 |
| | Natural Gas Connection and Distribution (if available) | 0 | LS | \$35,000.00 | \$46,383.73 | \$ - |
| | Stormwater Management System | 10.3 | AC | \$3,500.00 | \$4,638.37 | \$ 71,315 |
| C2 | Security Fence | | | | | \$3,975.75 |
| | Site Fencing | 100 | LF | \$20.00 | \$26.50 | \$ 3,976 |
| C3 | Domestic Water | | | | | \$49,696.86 |
| | Domestic Water Supply | 1 | LS | \$25,000.00 | \$33,131.24 | \$ 49,697 |
| C4 | Domestic Wastewater | 1 | | \$2,500.00 | | \$99,393.71 |
| | Domestic Wastewater System | 1 | LS | \$50,000.00 | \$66,262.48 | \$ 99,394 |
| C5 | Disinfection Station | | | | | \$22,500.00 |
| | Truck Disinfection Station | 1 | LS | \$15,000.00 | - | \$ 22,500 |

| | Roadway Aggregate | 0 | SY | | \$15.00 | - | \$ - |
|----|---|-----|----|----|--------------|---------------|---------------|
| | Electrical | 0 | LS | | \$2,500.00 | - | \$ - |
| | Detention Tank | 0 | LS | | \$5,000.00 | - | \$ - |
| C6 | Paved Access to State or Local Highways | 0 | | | \$0.00 | | \$377,696.12 |
| | Bituminous Paved Road | 1 | LS | | \$190,000.00 | \$251,797.41 | \$ 377,696 |
| | Gravel Roads | 0 | LS | | \$55,000.00 | \$72,888.72 | \$ - |
|). | Aquaculture Wastewater | | | | | | |
| D1 | Effluent Treatment | | | | | | \$12,232,40 |
| | Clarifier-40ft | | | _ | | | |
| | Clarifier Concrete | 211 | CY | \$ | 1,500 | - | \$ 474,750 |
| | Clarifier Excavation | 898 | CY | \$ | 50 | - | \$ 67,350 |
| | Clarifier Equipment | 1 | LS | \$ | 144,000 | \$ 227,707 | \$ 341,560 |
| | Clarifier Coatings | 1 | LS | \$ | 16,000 | \$ 25,301 | \$ 37,95 |
| | Finger Weirs | 1 | LS | \$ | 8,000 | \$ 12,650 | \$ 18,976 |
| | Duplex Pump Station | 1 | LS | \$ | 24,000 | \$ 37,951 | \$ 56,927 |
| | 3" Sch 80 PVC Pipe | 100 | LF | \$ | 48 | \$ 76 | \$ 11,385 |
| | 4" Sch 80 PVC Pipe | 250 | LF | \$ | 80 | \$ 127 | \$ 47,439 |
| | 3" Plug Valves | 2 | EA | \$ | 4,000 | \$ 6,325 | \$ 18,970 |
| | 3" Swing Check Valves | 2 | EA | \$ | 2,720 | \$ 4,301 | \$ 12,90 |
| | Telescoping Valves | 2 | EA | \$ | 1,520 | \$ 2,404 | \$ 7,21 |
| | 6 ft precast manhole 6 ft deep | 2 | EA | \$ | 12,000 | \$ 18,976 | \$ 56,927 |
| | 4ft Precast Manhole 4 ft deep | 1 | EA | \$ | 6,720 | \$ 10,626 | \$ 15,939 |
| | Clarifier Equipment Install | 1 | LS | \$ | 28,800 | \$ 45,541 | \$ 68,312 |
| | Sludge Storage-25ft | | | | | | |
| | Sudge Storage Concrete | 121 | CY | \$ | 1,500 | - | \$ 272,250 |
| | Sludge Storage Exavation | 725 | CY | \$ | 50 | - | \$ 54,375 |
| | Sludge Mixing Pump | 1 | LS | \$ | 10,000 | \$ 15,813 | \$ 23,719 |
| | Sludge Mixing Nozzles | 1 | LS | \$ | 35,000 | \$ 55,345 | \$ 83,018 |
| | 4" Sch 80 PVC Pipe | 300 | LF | \$ | 50 | \$ 79 | \$ 35,579 |
| | Telescoping Valves | 1 | EA | \$ | 950 | \$ 1,502 | \$ 2,253 |
| | 3" Plug Valves | 1 | EA | \$ | 2,500 | \$ 3,953 | \$ 5,930 |
| | 3" Swing Check Valves | 1 | EA | \$ | 1,700 | \$ 2,688 | \$ 4,032 |

| 1 | LS | | | | | |
|-----|---|---|--|--|---|---|
| | LƏ | \$ | 13,210 | \$ 20,889 | \$ | 31,333 |
| | | | | | | |
| | | | | | | |
| 1 | EA | \$ | 4,480,000 | - | \$ | 6,720,000 |
| 1 | EA | \$ | 7,800 | - | \$ | 11,700 |
| 1 | LS | \$ | 1,121,950 | - | \$ | 1,682,925 |
| | | | | | | |
| 94 | CY | \$ | 1,500 | - | \$ | 211,50 |
| 371 | CY | \$ | 50 | - | \$ | 27,82 |
| 1 | LS | \$ | 40,000 | - | \$ | 60,00 |
| 1 | EA | \$ | 47,802 | - | \$ | 71,70 |
| 1 | EA | \$ | 20,000 | - | \$ | 30,00 |
| 1 | EA | \$ | 2,515 | - | \$ | 3,77 |
| 1 | LS | \$ | 62,829 | - | \$ | 94,24 |
| | | | | | | |
| 2 | EA | \$ | 250,000 | - | \$ | 750,00 |
| 672 | CF | \$ | 500 | - | \$ | 504,00 |
| 1 | LS | \$ | 209,000 | - | \$ | 313,50 |
| | 371 1 1 1 1 1 1 1 2 | 1 EA 1 LS 94 CY 371 CY 1 LS 1 EA 1 CF | 1 EA \$ 1 LS \$ 94 CY \$ 371 CY \$ 1 LS \$ 1 LS \$ 1 EA \$ 2 EA \$ 2 EA \$ 672 CF \$ | 1 EA \$ 7,800 1 LS \$ 1,121,950 94 CY \$ 1,500 371 CY \$ 50 1 LS \$ 40,000 1 EA \$ 20,000 1 EA \$ 2,515 1 LS \$ 62,829 2 EA \$ 250,000 672 CF \$ 500 | 1 EA \$ 7,800 - 1 LS \$ 1,121,950 - 94 CY \$ 1,500 - 371 CY \$ 50 - 1 LS \$ 40,000 - 1 EA \$ 20,000 - 1 EA \$ 2,515 - 1 EA \$ 62,829 - 1 LS \$ 62,829 - 2 EA \$ 250,000 - 672 CF \$ 500 - | 1 EA \$ 7,800 - \$ 1 LS \$ 1,121,950 - \$ 94 CY \$ 1,500 - \$ 94 CY \$ 1,500 - \$ 371 CY \$ 50 - \$ 1 LS \$ 40,000 - \$ 1 EA \$ 47,802 - \$ 1 EA \$ 20,000 - \$ 1 EA \$ 20,000 - \$ 1 EA \$ 20,000 - \$ 1 EA \$ 2,515 - \$ 1 EA \$ 62,829 - \$ 1 LS \$ 62,829 - \$ 2 EA \$ 250,000 - \$ 2 EA \$ 500,000 - \$ 672 CF \$ 500 - \$ |

| D2 | Effluent Monitoring | | | | | \$64,605.91 |
|----|--------------------------------------|---|----|-------------|--------------|--------------|
| | Automated Flow Measurement Equipment | 1 | LS | \$25,000.00 | \$ 33,131.24 | \$ 49,697 |
| | Portable Composite Sampler | 1 | LS | \$5,000.00 | \$ 6,626.25 | \$ 9,939 |
| | Electrical | 1 | LS | \$2,500.00 | \$ 3,313.12 | \$ 4,970 |
| | | | | | | |

| E. | Electrical and HVAC | | | | | |
|----|---------------------|---|----|------------|-------------|---------------|
| E1 | Electrical Service | | | | | \$189,757.49 |
| | Security Lighting | 8 | EA | \$2,500.00 | \$ 3,313.12 | \$ 39,757 |
| | 3-phase service | 1 | EA | \$ 100,000 | - | \$ 150,000 |
| E2 | Emergency Power | | | | | \$216,678.30 |

| | Emergency Generator: 100-200kW | 1 | LS | \$75,000.00 | \$ 99,393.71 | \$ 149,091 |
|----|---|---|----|--------------|------------------|---------------|
| | Automatic Transfer Switch | 1 | LS | \$20,000.00 | \$ 26,504.99 | \$ 39,757 |
| | Fuel Tank | 1 | LS | \$14,000.00 | \$ 18,553.49 | \$ 27,830 |
| | | | | | | |
| E3 | Instrumentation and Alarm System | | | | | \$347,878.00 |
| | Instrumentation, Alarm System & Communication | 1 | LS | \$175,000.00 | \$ 231,918.67 | \$ 347,878 |
| | | | | | | |
| | | | | | | |

| F. | Visitor Education/Interpretation | | | | | |
|----|---|------|----|-------------|---|---------------|
| F1 | Hatchery Building - Displays | | | | | \$817,500.00 |
| | Display Materials | 1 | LS | \$20,000.00 | - | \$ 30,000 |
| | New visitor's center building (Display Area, Public Restrooms, & Mechan | 1500 | SF | \$350.00 | - | \$ 787,500 |
| | | | | | | \$55,267,598 |



Effluent Treatment Evaluation

Alternative 3B: 95% Recirculation and Chemical Dosing

| Component | HP | Quantity | Total HP | Watts | Hours/day | kW-hrs/year |
|-------------------------------------|------------------|---------------------|---------------|----------|---------------|----------------|
| Hatchery Modernization | | | | | | |
| UV System | | 8 | | 56,000 | 24 | 3,924,480 |
| Drum Filter | 8.0 | 8.0 | 64.00 | 47,725 | 24 | 418,069 |
| Recirc. Pump | 15.0 | 6.0 | 90.00 | 67,113 | 24 | 587,910 |
| Site Lighting | | 1 | | 15,000 | 12 | 65,700 |
| Miscellaneous (SCADA, Meters, etc.) | | 1 | | 15,000 | 24 | 131,400 |
| MBBR-Blower | 15.00 | 6 | 90.00 | 67,113 | 24 | 587,910 |
| Effluent Treatment | | | | | | |
| Clarifier Mechanism | 0.75 | 1 | 0.75 | 559 | 24 | 4,899 |
| Sludge Pump | 20.00 | 1 | 20.00 | 14,914 | 24 | 130,647 |
| Mixing Tank Mixer | 2.00 | 1 | 2.00 | 1,491 | 24 | 13,065 |
| Membrane Process Pumps | 15.00 | 3.00 | 45.00 | 115,000 | 1 | 41,975 |
| Membrane Blowers | 90.00 | 1.00 | 90.00 | 123,000 | 1 | 44,895 |
| Membrane CIP Pumps | 15.00 | 1.00 | 15.00 | 44,000 | 1 | 16,060 |
| Membrane CIP Heaters | NA | | | 300,000 | 1 | 109,500 |
| Membrane Backpulse Pump | 60.00 | 1.00 | 60.00 | 40,000 | 1 | 14,600 |
| Membrane Drain Pump | 15.00 | 1.00 | 15.00 | 45,000 | 1 | 16,425 |
| | | | | | kW-hrs/year = | 6,107,534 |
| | | | | | \$/kW-hrs = | \$0.12 |
| | | | | | φ/κνν-1115 – | Annual Cost |
| | | | | | | |
| | | | | | | \$732,904.11 |
| Estimated Annual Replacement Costs | | | | | | Annual Cost |
| Annual Equipment Replacement | | | | | | \$1,007,000.00 |
| Estimated Annual Labor Costs | Days per Week | Hours per day | Personnel | Rate | OH/Fringe | Annual Cost |
| Daily Operator Attention | 5 | 8 | 2 | \$ 25.00 | \$ 15.00 | \$104,000 |
| Chemicals | Use (gpd) | Annual Use (gal) | Cost (\$/gal) | | | Annual Cost |
| Alum | | 8395 | 1.81 | | | \$15,194.95 |
| 25% Caustic | | 6935 | 1.92 | | | \$13,315.20 |
| Нуро | | 6900 | 2.5 | | | \$17,250.00 |
| Citric | | 14500 | 8.25 | | | \$119,625.00 |
| Sodium Bisulfate | | 1700 | 3.4 | | | \$5,780.00 |
| Sulfuric | | | | | | \$0.00 |

| O2 Usage - Tank refill | 6000 | 0.6 | \$ 3,600.00 | 12 | \$43,200.00 |
|------------------------|------|-----|-------------|----|-------------|
| Adsorption Media Regen | | | | | \$0.00 |

| Estimated Annual Labor and Replacement Costs | \$1,111,000 |
|---|-------------|
| Estimated Annual Electricity and Chemical Usage Costs | \$947,269 |
| TOTAL | \$2,059,000 |

| | | | | | | | ve 3A: 95% R | Treatment E | valuation with Chemic | | | | | | | | | | | | |
|---|---------------|------------------------------|-------------------------|-------------|-------------|-------------|--------------|-------------|--------------------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|
| | | 0 | 1 | 2 | 3 | 4 | 5 | 6 | 7 | 8 | 9 | 10 | 11 | 12 | 13 | 14 | 15 | 16 | 17 | 18 | 19 |
| | Total | 2023 | 2024 | 2025 | 2026 | 2027 | 2028 | 2029 | 2030 | 2031 | 2032 | 2033 | 2034 | 2035 | 2036 | 2037 | 2038 | 2039 | 2040 | 2041 | 2042 |
| O&M | | | | | | | | | | | | | | | | | | | | | |
| Power and Chemical cost (6%/yr 2023-2026, 3%/yr 2027-2042 escalation) | | \$2,059,000 | <i>+</i> _, · •_, • · • | \$2,313,492 | \$2,452,302 | \$2,525,871 | \$2,601,647 | | , , , | | | | | . , , | \$3,295,689 | \$3,394,559 | \$3,496,396 | \$3,601,288 | \$3,709,327 | | |
| R&R Maintenance cost (6%/yr 2023-2026, 4%/yr 2027-2042 escalation) | | \$347,910 | \$368,785 | \$390,912 | \$414,366 | . , | \$448,179 | \$466,106 | | . , | . , | . , | . , | \$589,773 | \$613,363 | \$637,898 | \$663,414 | \$689,950 | \$717,548 | \$746,250 | \$776,100 |
| Total O&M Cost | | \$2,406,910 | \$2,551,325 | \$2,704,404 | \$2,866,668 | \$2,956,812 | \$3,049,826 | \$3,145,802 | \$3,244,837 | \$3,347,030 | \$3,452,482 | \$3,561,300 | \$3,673,592 | \$3,789,470 | \$3,909,052 | \$4,032,457 | \$4,159,810 | \$4,291,239 | \$4,426,875 | \$4,566,857 | \$4,711,325 |
| Average Annual O&M Cost over 20 years (\$/yr) | \$3,542,404 | | | | | | | | | | | | | | | | | | | | |
| Average Annual O&M Cost over 10 years (\$/yr) | \$2,972,610 | | | | | | | | | | | | | | | | | | | | |
| Constal Coot | | ¢50.054.000 | | | | | | | | | | | | | | | | | | | |
| Capital Cost Equipment Cost | | \$59,051,000 \$11,597,000 | | | | | | | | | | | | | | | | | | | |
| Equipment 00st | | φ11,537,000 | | | | | | | | | | | | | | | | | | | |
| Net Present Value (at 5% discount rate) | | | | | | | | | | | | | | | | | | | | | |
| 20 Year Net Present Value | \$100,905,261 | | | | | | | | | | | | | | | | | | | | |
| 10 Year Net Present Value | \$81,654,000 | | | | | | | | | | | | | | | | | | | | |
| Annual Cost | | | | | | | | | | | | | | | | | | | | | |
| Average Annual Cost (Debt Service + O&M, 20 year basis) | \$8,280,809 | | | | | | | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | | | | | | | | |

Average Annual Cost (Debt Service + O&M, 10 year basis) \$10,619,984



Effluent Treatment Evaluation

Alternative 3B: 95% Recirculation and Adsorption Units

| Component | HP | Quantity | Total HP | Watts | Hours/day | kW-hrs/year |
|-------------------------------------|------------------|---------------------|---------------|----------|---------------|----------------|
| Hatchery Modernization | | | | | | |
| UV System | | 8 | | 56,000 | 24 | 3,924,480 |
| Drum Filter | 8.0 | 8.0 | 64.00 | 47,725 | 24 | 418,069 |
| Recirc. Pump | 15.0 | 6.0 | 90.00 | 67,113 | 24 | 587,910 |
| Site Lighting | | 1 | | 15,000 | 12 | 65,700 |
| Miscellaneous (SCADA, Meters, etc.) | | 1 | | 15,000 | 24 | 131,400 |
| MBBR-Blower | 15.00 | 6 | 90.00 | 67,113 | 24 | 587,910 |
| Effluent Treatment | | | | | | |
| Clarifier Mechanism | 0.75 | 1 | 0.75 | 559 | 24 | 4,899 |
| Sludge Pump | 20.00 | 1 | 20.00 | 14,914 | 24 | 130,647 |
| Mixing Tank Mixer | 0.00 | 1 | 0.00 | 0 | 24 | 0 |
| Membrane Process Pumps | 15.00 | 3.00 | 45.00 | 115,000 | 1 | 41,975 |
| Membrane Blowers | 90.00 | 1.00 | 90.00 | 123,000 | 1 | 44,895 |
| Membrane CIP Pumps | 15.00 | 1.00 | 15.00 | 44,000 | 1 | 16,060 |
| Membrane CIP Heaters | NA | | | 300,000 | 1 | 109,500 |
| Membrane Backpulse Pump | 60.00 | 1.00 | 60.00 | 40,000 | 1 | 14,600 |
| Membrane Drain Pump | 15.00 | 1.00 | 15.00 | 45,000 | 1 | 16,425 |
| | | | | | | |
| | | | | | | |
| | | | | | | |
| | | 4 | | | √W-hrs/year = | 6,094,470 |
| | | | | | \$/kW-hrs = | \$0.12 |
| | | | | | | Annual Cost |
| | | | | | | \$731,336.35 |
| Estimated Annual Replacement Costs | | | | | | Annual Cost |
| Estimated Annual Replacement Costs | | | | | | Annual Cost |
| Annual Equipment Replacement | | 1 | ! | | 1 | \$1,062,000.00 |
| Estimated Annual Labor Costs | Days per Week | Hours per day | Personnel | Rate | OH/Fringe | Annual Cost |
| Daily Operator Attention | 5 | 8 | 2 | \$ 25.00 | \$ 15.00 | \$104,000 |
| Chemicals | Use (gpd) | Annual Use (gal) | Cost (\$/gal) | | | Annual Cost |
| Alum | | 0 | 1.81 | | | \$0 |
| 25% Caustic | | 0 | 1.92 | | | \$0 |
| Нуро | | 6900 | 2.5 | | | \$17,250 |
| Citric | | 14500 | 8.25 | | | \$119,625 |
| Sodium Bisulfate | | 1700 | 3.4 | | | \$5,780 |
| Sulfuric | | 1 | | | | \$0 |

| O2 Usage - Tank refill | 6000 | 0.6 | \$ 3,600.00 | 12 | \$43,200.00 |
|------------------------|------|-----|-------------|----|-------------|
| Adsorption Media Regen | | | | | \$29,936.68 |

| Estimated Annual Labor and Replacement Costs | \$1,166,000 |
|---|-------------|
| Estimated Annual Electricity and Chemical Usage Costs | \$947,128 |
| TOTAL | \$2,114,000 |

| | | | | | | Effluent ve 3B: 95% R | EFish and Ga Treatment Ev ecirculation ycle Cost An | valuation with Adsorp | | | | | | | | | | | | |
|---|--------------|-------------|-------------|-------------|-------------|--------------------------|--|--------------------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|
| | 0 | 1 | 2 | 3 | 4 | 5 | 6 | 7 | 8 | 9 | 10 | 11 | 12 | 13 | 14 | 15 | 16 | 17 | 18 | 19 |
| Total | 2023 | 2024 | 2025 | 2026 | 2027 | 2028 | 2029 | 2030 | 2031 | 2032 | 2033 | 2034 | 2035 | 2036 | 2037 | 2038 | 2039 | 2040 | 2041 | 2042 |
| O&M | | | | | | | | | | | | | | | | | | | | |
| Power and Chemical cost (6%/yr 2023-2026, 3%/yr 2027-2042 escalation) | \$2,114,000 | \$2,240,840 | \$2,375,290 | \$2,517,808 | \$2,593,342 | \$2,671,142 | \$2,751,277 | \$2,833,815 | \$2,918,829 | \$3,006,394 | \$3,096,586 | \$3,189,484 | \$3,285,168 | \$3,383,723 | \$3,485,235 | \$3,589,792 | \$3,697,486 | \$3,808,410 | \$3,922,663 | \$4,040,342 |
| R&R Maintenance cost (6%/yr 2023-2026, 4%/yr 2027-2042 escalation) | \$367,230 | \$389,264 | \$412,620 | \$437,377 | \$454,872 | \$473,067 | \$491,989 | \$511,669 | \$532,136 | \$553,421 | \$575,558 | \$598,580 | \$622,524 | \$647,425 | \$673,321 | \$700,254 | \$728,265 | \$757,395 | \$787,691 | \$819,199 |
| Total O&M Cost | \$2,481,230 | \$2,630,104 | \$2,787,910 | \$2,955,185 | \$3,048,214 | \$3,144,209 | \$3,243,266 | \$3,345,484 | \$3,450,965 | \$3,559,815 | \$3,672,144 | \$3,788,064 | \$3,907,692 | \$4,031,148 | \$4,158,556 | \$4,290,046 | \$4,425,750 | \$4,565,805 | \$4,710,353 | \$4,859,541 |
| Average Annual O&M Cost over 20 years (\$/yr) \$3,652,774 | | | | | | | | | | | | | | | | | | | | |
| Average Annual O&M Cost over 10 years (\$/yr) \$3,064,638 | | | | | | | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | | | | | | | |
| Capital Cost | \$60,406,000 | | | | | | | | | | | | | | | | | | | |
| Equipment Cost | \$12,241,000 | | | | | | | | | | | | | | | | | | | |
| Net Present Value (at 5% discount rate) | | | | | | | | | | | | | | | | | | | | |
| 20 Year Net Present Value \$103,562,072 | | | | | | | | | | | | | | | | | | | | |
| 10 Year Net Present Value \$83,708,000 | | | | | | | | | | | | | | | | | | | | |
| Annual Cost | | | | | | | | | | | | | | | | | | | | |
| Average Annual Cost (Debt Service + O&M, 20 year basis) \$8,499,908 | | | | | | | | | | | | | | | | | | | | |

Average Annual Cost (Debt Service + O&M, 10 year basis) \$10,887,492

Date:1/12/2023Estimator:Matt Cochran & Mario BenischChecked By:Jason HillCheck Date:-



| Detailed Opinions of Probable Cost | | | | | | | | | | | | |
|------------------------------------|-------|-------|----------|-----------------|------------|--|--|--|--|--|--|--|
| Alternative 1 | NO. | UNIT | COST PER | Escalation cost | TOTAL COST | | | | | | | |
| Alternative 1 | UNITS | MEAS. | UNIT | to 2022 | 50% CONT. | | | | | | | |

| Α. | Aquaculture Water Supply | | | | | |
|----|--|-----|----|---------------|---------------|-----------------|
| A1 | Hatchery Supply | | | | | \$ 229,345 |
| | Water Supply Piping and Accessories | 150 | LF | \$ 85 | \$ 113 | \$ 25,345 |
| | Cold Brook Diversion Dam & Dist. Box Structural Upgrades | 1 | LS | \$ 9,000 | - | \$ 13,500 |
| | Cold Brook Diversion Dam & Dist. Box Process Upgrades | 1 | LS | \$ 35,000 | - | \$ 52,500 |
| | Salmon Pond Outlet Structural Upgrades | 1 | LS | \$ 5,000 | - | \$ 7,500 |
| | Salmon Pond Outlet Process Upgrades | 1 | LS | \$ 15,000 | - | \$ 22,500 |
| | Lime Mill Structural Upgrades | 1 | LS | \$ 1,000 | - | \$ 1,500 |
| | Lime Mill Process Upgrades | 1 | LS | \$ 15,000 | - | \$ 22,500 |
| | Third Brook Intake Structural Upgrades | 1 | LS | \$ 2,500 | - | \$ 3,750 |
| | Third Brook Intake Process Upgrades | 1 | LS | \$ 8,000 | - | \$ 12,000 |
| | West Branch Diversion Dam Structural Upgrades | 1 | LS | \$ 8,000 | - | \$ 12,000 |
| | West Branch Diversion Dam Process Upgrades | 1 | LS | \$ 15,000 | - | \$ 22,500 |
| | No.9 Brook and Diversion Pond Structural Upgrades | 1 | LS | \$ 15,000 | - | \$ 22,500 |
| | No.9 Brook and Diversion Pond Process Upgrades | 1 | LS | \$ 7,500 | - | \$ 11,250 |
| A2 | Oxygenation System | | | | | \$ 1,022,003 |
| | Bulk LOX Tank, Vaporizer, Port. Tank Fill System | 2 | LS | \$ 150,000 | \$ 198,787 | \$ 596,362 |
| | Fence | 400 | LF | \$ 20 | \$ 27 | \$ 15,903 |
| | Concrete Pad & Bollards | 2 | LS | \$ 11,000 | \$ 14,578 | \$ 43,733 |
| | Buried Copper Oxygen Distribution to Units | 2 | LS | \$ 60,000 | \$ 79,515 | \$ 238,545 |
| | Oxygen Electrical | 2 | LS | \$ 5,000 | \$ 6,626 | \$ 19,879 |
| | Oxygen Dissolving for Rearing Units- LHO | 24 | EA | \$ 2,500 | \$ 2,906 | \$ 104,599 |
| | Oxygen Flow Meter Station (raceways) | 2 | LS | \$ 750 | \$ 994 | \$ 2,982 |

| В. | Buildings and Rearing Units | | | | | |
|------------|---|---------|----|---------------|--------------|-----------------|
| B1 | Cold Brook and Wells Intake Building | | | | | \$ 1,588,544 |
| | New Intake Building Cold Brook and Wells | 400 | SF | \$ 165 | \$ 218 | \$ 131,017 |
| | Drumfilter | | | | | |
| | DRUM FILTERS - Cold Brook and wells | 2 | EA | \$ 75,000 | - | \$ 225,000 |
| | DRUM SUMP | 1 | LS | \$ 75,000 | - | \$ 112,500 |
| | PIPING SYSTEMS (INFLOW, DRAINS) | 1 | LS | \$ 500,000 | - | \$ 750,000 |
| | PRIMARY POWER | 1 | LS | \$ 75,000 | - | \$ 112,500 |
| | UV System | | | | | |
| | UV Channel and Lamp Package - Cold Brook and wells | 2 | EA | \$ 50,000 | - | \$ 150,000 |
| | UV Electrical | 1 | LS | \$ 8,000 | \$ 10,602 | \$ 15,903 |
| | UV Plumbing | 1 | LS | \$ 11,000 | \$ 14,578 | \$ 21,867 |
| | Electrical Power and Lighting | 1 | LS | \$ 20,000 | \$ 26,505 | \$ 39,757 |
| | ALARMS/CONTROLS/MONITORING/PANEL/HMI | 1 | LS | \$ 20,000 | - | \$ 30,000 |
| B2 | West Branch Intake Building | | | | | \$ 1,568,666 |
| | New Intake Building West Branch | 400 | SF | \$ 165 | \$ 218 | \$ 131,017 |
| | Drumfilter | | | | | |
| | DRUM FILTERS - West Branch | 2 | EA | \$ 75,000 | - | \$ 225,000 |
| | DRUM SUMP | 1 | LS | \$ 75,000 | - | \$ 112,500 |
| | PIPING SYSTEMS (INFLOW, DRAINS) | 1 | LS | \$ 500,000 | - | \$ 750,000 |
| | PRIMARY POWER | 1 | LS | \$ 75,000 | - | \$ 112,500 |
| | UV System | | | | | |
| | UV Channel and Lamp Package - West Branch | 2 | EA | \$ 50,000 | - | \$ 150,000 |
| | UV Electrical | 1 | LS | \$ 8,000 | \$ 10,602 | \$ 15,903 |
| | UV Plumbing | 1 | LS | \$ 11,000 | \$ 14,578 | \$ 21,867 |
| | Electrical Power and Lighting | 1 | LS | \$ 10,000 | \$ 13,252 | \$ 19,879 |
| | ALARMS/CONTROLS/MONITORING/PANEL/HMI | 1 | LS | \$ 20,000 | - | \$ 30,000 |
| B 3 | Effluent Treatment Building | | | | | \$ 2,943,019 |
| | New Effluent treatment building | 8243.75 | SF | \$ 165 | \$ 238 | \$ 2,943,019 |
| | | | | | | |
| B4 | Raceway Rehabilitation | | | | | \$ 1,353,750 |
| | Concrete rehab of the Young's and Foster's Raceways | 1 | LS | \$ 50,000 | - | \$ 75,000 |
| | Process rehab Young's and Foster Raceways | 1 | LS | \$ 60,000 | - | \$ 90,000 |
| | Concrete rehab of the West Branch Raceways | 1 | LS | \$ 625,000 | - | \$ 937,500 |
| | Process Rehab West Branch Raceways | 1 | LS | \$ 7,500 | - | \$ 11,250 |
| | Demolish and fill in Upper Canals | 1 | LS | \$ 60,000 | - | \$ 90,000 |
| | Baffle Allowance | 1 | LS | \$ 100,000 | - | \$ 150,000 |
| B7 | Existing Building Rehab | | | | | \$ 1,145,725 |
| | Headquarter Office and Hatchery Building | 1 | LS | \$ 237,500 | | \$ 237,500 |
| | Well House 1 (New Well, Well House & Equipment) | 1 | LS | \$ 49,000 | | \$ 49,000 |

| | Well House 2 (New Well, Well House & Equipment) | 1 | LS | \$ 49,000 | | \$ 49,000 |
|----|--|------|----|--------------|--------------|--------------|
| | Feed Storage Building | 1 | LS | \$ 227,250 | | \$ 227,250 |
| | Pipe Shop | 1 | LS | \$ 241,975 | | \$ 241,975 |
| | Carptenters Shop | 1 | LS | \$ 21,000 | | \$ 21,000 |
| | West Branch Garage | 1 | LS | \$ 5,000 | | \$ 5,000 |
| | Salmon Building - Demolish | 1 | LS | \$ 15,000 | | \$ 15,000 |
| | Replace Pole Shed w/ Maintenance & Storage Garage | 2000 | SF | \$ 150 | | \$ 300,000 |
| C. | Site | | | | | |
| C1 | Site Work | | | | | \$506,907.95 |
| | Site Clearing | 2.5 | AC | \$2,000.00 | \$2,650.50 | \$ 9,939 |
| | General Earthwork for Hatchery Complex | 0 | LS | \$75,000.00 | \$99,393.71 | \$ - |
| | General Sitework | 1 | LS | \$250,000.00 | \$331,312.38 | \$ 496,969 |
| | Erosion Control | 0 | AC | \$2,500.00 | \$3,313.12 | \$ - |
| | Seeding | 0 | AC | \$1,250.00 | \$1,656.56 | \$- |
| | Landscaping | 0 | AC | \$3,000.00 | \$3,975.75 | \$- |
| | Natural Gas Connection and Distribution (if available) | 0 | LS | \$35,000.00 | \$46,383.73 | \$- |
| | Stormwater Management System | 0.0 | AC | \$3,500.00 | \$4,638.37 | \$ - |
| C2 | Domestic Water | | | \$150.00 | | \$49,696.86 |
| | Domestic Water Supply | 1 | LS | \$25,000.00 | \$33,131.24 | \$ 49,697 |
| C3 | Domestic Wastewater | | | \$100,000.00 | | \$99,393.71 |
| | Domestic Wastewater System | 1 | LS | \$50,000.00 | \$66,262.48 | |
| C4 | Disinfection Station | | | | | \$45,000.00 |
| | Truck Disinfection Station | 1 | LS | \$30,000.00 | - | \$ 45,000 |
| | Roadway Aggregate | 0 | SY | \$30.00 | - | \$ - |
| | Electrical | 0 | LS | \$5,000.00 | - | \$ - |
| | Detention Tank | 0 | LS | \$10,000.00 | - | \$ - |
| C5 | Paved Access to State or Local Highways | 0 | | \$0.00 | | \$377,696.12 |
| | Bituminous Paved Road | 1 | LS | \$190,000.00 | \$251,797.41 | \$ 377,696 |
| | Gravel Roads | 0 | LS | \$55,000.00 | \$72,888.72 | \$ - |

| D. | Aquaculture Wastewater | | | |
|----|------------------------|--|--|---------------|
| D1 | Effluent Treatment | | | \$ 29,804,245 |
| | | | | |

| DRUM FILTERS DRUM SUMP PIPING SYSTEMS (INFLOW, PRAS, DRAINS) PRIMARY POWER | 2 | EA | \$ 150,000 | - | \$ | 450,0 |
|---|-----|----|---------------|---------------|----|-------|
| PIPING SYSTEMS (INFLOW, PRAS, DRAINS) | 1 | | | | * | 100, |
| | | LS | \$ 75,000 | - | \$ | 112, |
| | 1 | LS | \$ 500,000 | - | \$ | 750, |
| | 1 | LS | \$ 75,000 | - | \$ | 112, |
| Clarifier-30ft | | | | | | |
| Clarifier Concrete | 142 | CY | \$ 1,500 | - | \$ | 319 |
| Clarifer Excavation | 642 | CY | \$ 50 | - | \$ | 48 |
| Clarifier Equipment | 1 | LS | \$ 108,000 | \$ 170,780 | \$ | 256 |
| Clarifier Coatings | 1 | LS | \$ 12,000 | \$ 18,976 | \$ | 28 |
| Finger Weirs | 1 | LS | \$ 6,000 | \$ 9,488 | \$ | 14 |
| Duplex Pump Station | 1 | LS | \$ 18,000 | \$ 28,463 | \$ | 42 |
| 3" Sch 80 PVC Pipe | 100 | LF | \$ 36 | \$ 57 | \$ | 8 |
| 4" Sch 80 PVC Pipe | 250 | LF | \$ 60 | \$ 95 | \$ | 35 |
| 3" Plug Valves | 2 | EA | \$ 3,000 | \$ 4,744 | \$ | 14 |
| 3" Swing Check Valves | 2 | EA | \$ 2,040 | \$ 3,226 | \$ | 9 |
| Telescoping Valves | 2 | EA | \$ 1,140 | \$ 1,803 | \$ | 5 |
| 6 ft precast manhole 6 ft deep | 2 | EA | \$ 9,000 | \$ 14,232 | \$ | 42 |
| 4ft Precast Manhole 4 ft deep | 1 | EA | \$ 5,040 | \$ 7,970 | \$ | 11 |
| Clarifier Equipment Install | 1 | LS | \$ 21,600 | \$ 34,156 | \$ | 51 |
| Sludge Storage-25ft | | | | | | |
| Sudge Storage Concrete | 121 | CY | \$ 1,500 | - | \$ | 272 |
| Sludge Storage Exavation | 725 | CY | \$ 50 | - | \$ | 54 |
| Sludge Mixing Pump | 1 | LS | \$ 10,000 | \$ 15,813 | \$ | 23 |
| Sludge Mixing Nozzles | 1 | LS | \$ 35,000 | \$ 55,345 | \$ | 83 |
| 4" Sch 80 PVC Pipe | 300 | LF | \$ 50 | \$ 79 | \$ | 35 |
| Telescoping Valves | 1 | EA | \$ 950 | \$ 1,502 | \$ | 2 |
| 3" Plug Valves | 1 | EA | \$ 2,500 | \$ 3,953 | \$ | 5 |
| 3" Swing Check Valves | 1 | EA | \$ 1,700 | \$ 2,688 | \$ | 4 |
| Air Release Valve | 2 | EA | \$ 450 | \$ 712 | \$ | 2 |
| Sludge Mix & Transfer System Install | 1 | LS | \$ 13,210 | \$ 20,889 | \$ | 31 |
| WW Piping | | | | | | |
| WW Sitework | 1 | LS | \$ 40,000 | \$ 53,010 | \$ | 79 |
| Electrical Power and Lighting | 1 | LS | \$ 200,000 | \$ 265,050 | \$ | 397 |

| | Membrane | | | | | | | | |
|----------|--|------|----|----------|------------|----|---------|-----------------|-------------|
| | Membrane Filtration System | 1 | EA | \$ | 11,078,500 | | - | \$ | 16,617,750 |
| | Chemical Storage Membrane Cleaning | 1 | EA | \$ | 8,700 | | - | \$ | 13,050 |
| | Membrane Install (25% of Materials) | 1 | LS | \$ | 2,771,800 | | - | \$ | 4,157,700 |
| | Adsorption | | | | | | | | |
| | Adsorption Columns | 1 | LS | \$ | 1,442,600 | | - | \$ | 2,163,900 |
| | Adsorption Media | 1 | LS | \$ | 1,603,000 | | - | \$ | 2,404,500 |
| | Asorption Install (25% of Materials) | 1 | LS | \$ | 761,400 | | - | \$ | 1,142,100 |
| D2 | Effluent Monitoring | | | | | | | \$ | 69,576 |
| | Automated Flow Measurement Equipment | 1 | LS | \$ | 25,000 | \$ | 33,131 | \$ | 49,697 |
| | Portable Composite Sampler | 1 | LS | \$ | 5,000 | \$ | 6,626 | \$ | 9,939 |
| | Electrical | 1 | LS | \$ | 5,000 | \$ | 6,626 | \$ | 9,939 |
| D3 | West Branch Pumping | | | | | | | \$ | 2,619,660 |
| | WW Piping line | 1300 | LF | \$ | 85 | \$ | 113 | \$ | 219,660 |
| | West Branch Pump Station | 1 | LS | \$ | 1,600,000 | | - | \$ | 2,400,000 |
| D4 | Young's and Foster's Pumping | | | | | | | \$ | 2,125,345 |
| | WW Piping line | 150 | LF | \$ | 85 | \$ | 113 | \$ | 25,345 |
| | Young's and Foster's Pump Station | 1 | LS | \$ | 1,400,000 | | - | \$ | 2,100,000 |
| _ | | | | | | | | | |
| E. E1 | Utilities (Electrical, HVAC and Instrumentation) | | | | | | | ¢ | 225,000 |
| EI | 3-phase service - Effluent treatment plant | 1 | LS | ¢ | 100,000 | | - | \$ \$ | 150,000 |
| | New Service Connections - Intakes, Pump Stations, Garage | 1 | LS | \$ \$ | 50,000 | | - | \$ | 75,000 |
| | New Service Connections - Intakes, Fump Stations, Garage | | L3 | φ | 50,000 | | - | φ | 75,000 |
| E2 | Emergency Power | | | | | | | \$ | 297,000 |
| | Emergency Generators: Hatchery and Wells, 100kW | 2 | LS | \$ | 75,000 | | - | \$ | 225,000 |
| | Automatic Transfer Switch | 2 | LS | \$ | 10,000 | | - | \$ | 30,000 |
| | Fuel Tank | 2 | LS | \$ | 14,000 | | - | \$ | 42,000 |
| E3 | Instrumentation and Alarm System | | | | | | | \$ | 298,181 |
| | Instrumentation, Alarm System & Communication | 1 | LS | \$ | 150,000 | \$ | 198,787 | \$ | 298,181 |
| F. | Visitor Education/Interpretation | | I | | | I | | I | |
| F1 | Visitor Center Repairs | | | | | | | | \$53,250.00 |

| Replace egress door on north face | 1 | EA | \$ 2,500 | - | \$ | 3,750 |
|---|------|----|--------------|---|----|--------|
| Fix / replace door sills for ADA compliance | 3 | EA | \$ 1,000 | - | \$ | 4,500 |
| Replace Carpet | 1000 | SF | \$ 5 | - | \$ | 7,500 |
| New Digital Display | 1 | LS | \$ 5,000 | - | \$ | 7,500 |
| Convert Storage Room to Bathroom | 1 | LS | \$ 20,000 | - | \$ | 30,000 |
| | | | | | - | |

\$ 46,422,003

| Powder Mill New Facility Summary Opi | | |
|---|-------------------|-----------------------|
| ITEM | DRAWING I.D. # | ROUNDED TOTAL COST |
| New Facility Features | | |
| Hatchery Supply | A1 | \$230,000 |
| Oxygenation System | A2 | \$1,023,000 |
| Cold Brook and Wells Intake Building | B1 | \$1,589,000 |
| West Branch Intake Building | B2 | \$1,569,000 |
| Effluent Treatment Building | B3 | \$2,944,000 |
| Raceway Rehabilitation | B4 | \$1,354,000 |
| Existing Building Rehab | B7 | \$1,146,000 |
| Site Work | C1 | \$507,000 |
| Domestic Water | C2 | \$50,000 |
| Domestic Wastewater | C3 | \$100,000 |
| Disinfection Station | C4 | \$45,000 |
| Paved Access to State or Local Highways | C5 | \$378,000 |
| Effluent Treatment | D1 | \$29,805,000 |
| Effluent Monitoring | D2 | \$70,000 |
| West Branch Pumping | D3 | \$2,620,000 |
| Young's and Foster's Pumping | D4 | \$2,126,000 |
| Electrical Service | E1 | \$225,000 |
| Emergency Power | E2 | \$297,000 |
| Instrumentation and Alarm System | E3 | \$299,000 |
| Visitor Center Repairs | F1 | \$54,000 |
| Subtotal | | \$46,431,000 |
| Escalation to Midpoint of Const. @ 5%/yr for 5 years | | \$2,322,000 |
| 3% market volatility adjustment | | \$1,392,930 |
| Total Cost | | \$50,146,000 |
| ^a Rounded Total Costs (or Costs needed to Budget) include 50% Class 4 AA Costs do NOT include: Design Reimbursables (Variable); State Agency Adm | | tion or lease. |



Effluent Treatment Evaluation

Alternative 1: No Hatchery Upgrades and Adsorption Units

| Component | HP | Quantity | Total HP | Watts | Hours/day | kW-hrs/year |
|----------------------------|-------|----------|----------|---------|---------------|--------------|
| Hatchery Modernization | | | | | | |
| UV System - Cold Brook | | 2 | | 25,331 | 24 | 443,796 |
| UV System - Diversion Pond | | 2 | | 33,570 | 24 | 588,148 |
| Drum Filter | 8.0 | 4.0 | 32.00 | 23,862 | 24 | 209,035 |
| Site Lighting | | 1 | | 15,000 | 12 | 65,700 |
| Effluent Treatment | | | | | | |
| Effluent Drums | 8.00 | 2 | 16.00 | 11,931 | 24 | 104,517 |
| Clarifier Mechanism | 0.75 | 1 | 0.75 | 559 | 24 | 4,899 |
| Sludge Pump | 20.00 | 1 | 20.00 | 14,914 | 24 | 130,647 |
| Youngs and Fosters Pump | | | | | | 480,000 |
| The West Branch Pump | | | | | | 633,600 |
| Membrane Process Pumps | | | | 465,663 | 1 | 169,967 |
| Membrane Blowers | | | | 322,840 | 1 | 117,837 |
| Membrane CIP Pumps | | | | 111,870 | 1 | 40,833 |
| Membrane CIP Heaters | | | | 771,321 | 1 | 281,532 |
| Membrane Backpulse Pump | | | | 68,279 | 1 | 24,922 |
| Membrane Drain Pump | | | | 111,928 | 1 | 40,854 |
| | | | | | kW-hrs/year = | 3,336,286 |
| | | | | | \$/kW-hrs = | \$0.12 |
| | | | | | | Annual Cost |
| | | | | | | \$400,354.30 |
| | | | | | | |

| Estimated Annual Replacement Costs | | | | | | Annual Cost |
|------------------------------------|------------------|---------------------|---------------|-------------------|--------------|----------------|
| Annual Equipment Replacement | - | - | | - | | \$2,261,000.00 |
| Estimated Annual Labor Costs | Days per Week | Hours per day | Personnel | Rate | OH/Fringe | Annual Cost |
| Daily Operator Attention | 5 | 8 | 2 | \$ 25.00 | \$ 15.00 | \$104,000 |
| Chemicals | Use (gpd) | Annual Use (gal) | Cost (\$/gal) | event per year | | Annual Cost |
| Нуро | | 17646.11603 | 2.5 | | | \$44,115 |
| Citric | | 37123.40216 | 8.25 | | | \$306,268 |
| Sodium Bisulfate | | 4245.132743 | 3.4 | | | \$14,433 |
| Sulfuric | | | | | | \$0 |
| O2 Usage - Tank refill | | 6000 | 0.6 | 3 | | \$10,800 |
| Adsorption Media Regen | | | | | | \$90,157 |
| | | | | | | |
| | | Estimat | ed Annual Lat | oor and Repla | cement Costs | \$2,365,000 |
| | E | Estimated Annu | | | | |
| | | | | | TOTAL | \$3,232,000 |

| | <u>New Hampshire Fish and Game Department</u> <u>Effluent Treatment Evaluation</u> <u>Alternative 1: No Hatchery Upgrades and Adsorption Units</u> Life Cycle Cost Analysis | | | | | | | | | | | | | | | | | | | | |
|--|--|--|--------------------------|--------------------------|---|--------------------------|----------------------------|----------------------------|---------------------------------|---|----------------------------|----------------------------|----------------------------|--------------------------------------|----------------------------|----------------------------|------------------------------|----------------------------|----------------------------|----------------------------|----------------------------|
| | Total | 0 2023 | 1 2024 | 2 2025 | 3 2026 | 4 2027 | 5 2028 | 6 2029 | 7 2030 | 8 2031 | 9 2032 | 10 2033 | 11 2034 | 12 2035 | 13 2036 | 14 2037 | 15 2038 | 16 2039 | 17 2040 | 18 2041 | 19 2042 |
| O&M Power and Chemical cost (6%/yr 2023-2026, 3%/yr 2027-2042 escalation R&R Maintenance cost (6%/yr 2023-2026, 4%/yr 2027-2042 escalation Total O&M Cost | Total | \$3,232,000 \$781,770 \$4,013,770 | \$3,425,920 \$828,676 | \$3,631,475 \$878,397 | \$3,849,364 \$931,101 | \$3,964,845 \$968,345 | \$4,083,790 \$1,007,078 | \$4,206,304 \$1,047,362 | \$4,332,493 \$1,089,256 | \$4,462,468 \$1,132,826 \$5,595,294 | \$4,596,342 \$1,178,139 | \$4,734,232 \$1,225,265 | \$4,876,259 \$1,274,275 | \$5,022,547 \$1,325,246 | \$5,173,223 \$1,378,256 | \$5,328,420 \$1,433,387 | \$5,488,272 \$1,490,722 | \$5,652,920 \$1,550,351 | \$5,822,508 \$1,612,365 | \$5,997,183 \$1,676,860 | \$6,177,099 \$1,743,934 |
| Average Annual O&M Cost over 20 years (\$/yr) Average Annual O&M Cost over 10 years (\$/yr) | \$5,930,564 \$4,962,795 | ψ - ,013,770 | ψ 1 ,204,090 | ψ 1 ,509,072 | ψ - ,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,, | ψ 1 ,303,109 | ψ0,000,000 | ψ0,200,000 | ψ 0, 1 21,749 | ψ 0,030,234 | ψ 0,774,40 1 | ψ0,909,497 | ψ0, 130,334 | ψ 0,0+ 1,1 3 3 | φ0,001,479 | φ0,701,000 | ψ0, <i>01</i> 0, <i>33</i> 4 | <i>ψι,</i> 203,271 | ψι,τ04,073 | φ1,014,043 | ψ1,321,000 |
| Capital Cost Equipment Cost | | \$46,422,000 \$26,059,000 | | | | | | | | | | | | | | | | | | | |
| Net Present Value (at 5% discount rate) 20 Year Net Present Value 10 Year Net Present Value Annual Cost | \$84,152,000 | | | | | | | | | | | | | | | | | | | | |

Average Annual Cost (Debt Service + O&M, 20 year basis)\$9,655,585Average Annual Cost (Debt Service + O&M, 10 year basis)\$10,974,656

| Date: | 10/13/2022 | |
|-----------------|------------------------------|--|
| Estimator: | Matt Cochran & Mario Benisch | |
| Checked By: | Jason Hill | |
| Check Date: | 12/27/2022 | |
| Revised: | - | |

| Detailed Opinions of Probable Cost | | | | | | | | | | | | |
|------------------------------------|-------|-------|----------|-----------------|------------|--|--|--|--|--|--|--|
| | NO. | UNIT | COST PER | Escalation cost | TOTAL COST | | | | | | | |
| Alternative 2 | UNITS | MEAS. | UNIT | to 2022 | 50% CONT. | | | | | | | |

| A. | Aquaculture Water Supply | | | | | | | | |
|----|--|------|----|----|---------|----|--------|----|-----------|
| A1 | Hatchery Supply | | | | | | | | \$488,379 |
| | Water Supply Piping and Accessories | 2300 | LF | \$ | 85 | \$ | 113 | \$ | 388,629 |
| | Cold Brook Diversion Dam & Dist. Box Structural Upgrades | 1 | LS | \$ | 9,000 | - | | \$ | 13,500 |
| | Cold Brook Diversion Dam & Dist. Box Process Upgrades | 1 | LS | \$ | 35,000 | - | | \$ | 52,500 |
| | Salmon Pond Outlet Structural Upgrades | 1 | LS | \$ | 5,000 | - | | \$ | 7,500 |
| | Salmon Pond Outlet Process Upgrades | 1 | LS | \$ | 15,000 | - | | \$ | 22,500 |
| | Lime Mill Structural Upgrades | 1 | LS | \$ | 1,000 | - | | \$ | 1,500 |
| | Lime Mill Process Upgrades | 1 | LS | \$ | 1,500 | - | | \$ | 2,250 |
| | | | | | | | | | |
| | | | | | | | | | |
| В. | Buildings and Rearing Units | | | | | | | | |
| B1 | Cold Brook and Wells Intake Building | | | | | | | \$ | 1,588,544 |
| | New Intake Building | 400 | SF | \$ | 165 | \$ | 218 | \$ | 131,017 |
| | Drumfilter | | | | | | | | |
| | DRUM FILTERS | 2 | EA | \$ | 75,000 | - | | \$ | 225,000 |
| | DRUM SUMP | 1 | LS | \$ | 75,000 | - | | \$ | 112,500 |
| | PIPING SYSTEMS (INFLOW, DRAINS) | 1 | LS | \$ | 500,000 | - | | \$ | 750,000 |
| | PRIMARY POWER | 1 | LS | \$ | 75,000 | - | | \$ | 112,500 |
| | UV System | | | | | | | | |
| | UV Channel and Lamp Package | 2 | EA | \$ | 50,000 | - | | \$ | 150,000 |
| | | 1 | LS | \$ | 8,000 | \$ | 10,602 | \$ | 15,903 |
| | UV Electrical | | LO | Ψ | 0,000 | Ψ | 10,002 | Ψ | 10,000 |

| | Electrical Power and Lighting | 1 | LS | \$ | 20,000 | \$ 26,505 | \$ | 39,757 |
|------------|--|--------|------|----|----------|---------------------------------------|----|-----------------|
| | ALARMS/CONTROLS/MONITORING/PANEL/HMI | 1 | LS | \$ | 20,000 | - | \$ | 30,000 |
| | | | | | | | | |
| B 3 | Effluent Treatment Building | | | | | | | \$1,959,037.50 |
| | New Effluent treatment building | 5,488 | SF | : | \$165.00 | \$ 238 | \$ | 1,959,038 |
| | | | | | | | | |
| B5 | Hatchery Building | | | | | | | \$4,229,021.87 |
| | New Hatchery Building - Office Space | 3700 | SF | : | \$165.00 | \$ 218 | \$ | 1,211,910 |
| | POWER AND LIGHTING | 3700 | SF | \$ | 50 | \$103.40 | \$ | 573,847 |
| | HVAC | 1 | LS | \$ | 100,000 | \$206,791.77 | \$ | 310,188 |
| | EQUIPMENT | | | | | | | |
| | FEEDERS (SWEENEY MDL AF7 W/CONTROLLER & SUPPORT) | 72 | EA | \$ | 600 | \$1,240.75 | \$ | 134,001 |
| | FG TROUGHS (12'x2'x2') | 42 | EA | \$ | 2,500 | \$5,169.79 | | 325,697 |
| | INCUBATION ROOM 30 HEATH STACKS | 12 | EA | \$ | 2,500 | \$5,169.79 | \$ | 93,056 |
| | INCUBATION HEAD TROUGHS AND CONTROLS | 2 | LS | \$ | 15,000 | \$31,018.77 | | 93,056 |
| | CHILLER SYSTEM AND CONTROLS | 1 | LS | \$ | 250,000 | \$516,979.42 | | 775,469 |
| | FORMALIN ROOM | 1 | LS | \$ | 50,000 | \$103,395.88 | | 155,094 |
| | BOOT LOCKER ROOM, W/D, BENCHES | 1 | LS | \$ | 50,000 | \$103,395.88 | | 155,094 |
| | WATER QUALITY ROOM EQUIP ALLOWANCE | 1 | LS | \$ | 75,000 | \$155,093.83 | | 232,641 |
| | Hatchery Building Aeration/Degassing System | | | | - , | · · · · · · · · · · · · · · · · · · · | , | - ,- |
| | Primary Headtank & Aeration/Degassing System | 1 | EA | \$ | 85,000 | \$ 112,646 | \$ | 168,969 |
| | | | | | | | | |
| B6 | Rearing Building | | | | | | | \$33,076,818.18 |
| | New Rearing Building (526x140) | 73,640 | SF | \$ | 165 | \$ 218 | \$ | 24,120,276 |
| | ALARMS/CONTROLS/MONITORING/PANEL/HMI | 1 | I LS | \$ | 50,000 | - | \$ | 75,000 |
| | VFD W/CIRCUIT BREAKER AND FULL CONTACTOR SET | 2 | 2 EA | \$ | 25,000 | - | \$ | 75,000 |
| | PANEL/RACK/WIRING/CONDUITS/FEEDER | | 2 EA | \$ | 55,000 | - | \$ | 165,000 |
| | 12" FLOW METER | 2 | 2 EA | \$ | 18,000 | - | \$ | 54,000 |
| | EQUIPMENT | | | | | | | |
| | 20' dia. SS Culture Tank with Foundation & Floor | 20 | EA | | 35,000 | - | \$ | 1,050,000 |
| | 40' dia. SS Culture Tank with Foundation & Floor | 16 | EA | \$ | 50,000 | - | \$ | 1,200,000 |
| | Drumfilter | | | | | | | |
| | DRUM FILTERS | 6 | EA | \$ | 85,000 | - | \$ | 765,000 |

| - | | | | - | | | - | |
|----|---|------|----|----|---------|------------|----|-----------|
| | DRUM SUMP | 1 | LS | \$ | 75,000 | - | \$ | 112,500 |
| | PRIMARY POWER | 1 | LS | \$ | 75,000 | - | \$ | 112,500 |
| | UV System | | | | | | | |
| | UV Channel and Lamp Package | 6 | EA | \$ | 125,000 | - | \$ | 1,125,000 |
| | UV Electrical | 1 | LS | \$ | 8,000 | \$ 10,602 | \$ | 15,903 |
| | UV Plumbing | 1 | LS | \$ | 11,000 | \$ 14,578 | \$ | 21,867 |
| | Recirculation | | | | | | | |
| | PIPING SYSTEMS (INFLOW, PRAS, DRAINS) | 1 | LS | \$ | 500,000 | - | \$ | 750,000 |
| | Lift Pump | 6 | EA | \$ | 80,000 | - | \$ | 720,000 |
| | 4ft Precast Manhole 4 ft deep | 6 | EA | \$ | 4,200 | \$6,641.45 | \$ | 59,773 |
| | Biofilter System | | | | | | | |
| | MBBR | 6 | EA | \$ | 200,000 | - | \$ | 1,800,000 |
| | HVAC | 1 | LS | \$ | 100,000 | - | \$ | 150,000 |
| | Electrical Power and Lighting | 1 | LS | \$ | 200,000 | - | \$ | 300,000 |
| | GAS MANAGEMENT TOWER CO2 STRIPPER/LHO | 6 | EA | \$ | 45,000 | - | \$ | 405,000 |
| B7 | Existing Building Rehab | | | | | | \$ | 434,000 |
| | Well House 1 (New Well, Well House & Equipment) | 1 | LS | \$ | 49,000 | | \$ | 49,000 |
| | Well House 2 (New Well, Well House & Equipment) | 1 | LS | \$ | 49,000 | | \$ | 49,000 |
| | Salmon Building - Demolish | 1 | LS | \$ | 15,000 | | \$ | 15,000 |
| | Replace Pole Shed w/ Maintenance & Storage Garage | 2000 | SF | \$ | 150 | | \$ | 300,000 |
| | Carpenters Shop | 1 | LS | \$ | 21,000 | | \$ | 21,000 |

| C. | Site | | | | | |
|----|--|------|----|--------------|--------------|---------------|
| C1 | Site Work | | | | | \$835,155.69 |
| | Site Clearing | 2.5 | AC | \$2,000.00 | \$2,650.50 | \$ 9,939 |
| | General Earthwork for Hatchery Complex | 1 | LS | \$75,000.00 | \$99,393.71 | \$ 149,091 |
| | General Sitework | 1 | LS | \$250,000.00 | \$331,312.38 | \$ 496,969 |
| | Erosion Control | 20 | AC | \$2,500.00 | \$3,313.12 | \$ 99,394 |
| | Seeding | 1 | AC | \$1,250.00 | \$1,656.56 | \$ 2,485 |
| | Landscaping | 1 | AC | \$3,000.00 | \$3,975.75 | \$ 5,964 |
| | Natural Gas Connection and Distribution (if available) | 0 | LS | \$35,000.00 | \$46,383.73 | \$ - |
| | Stormwater Management System | 10.3 | AC | \$3,500.00 | \$4,638.37 | \$ 71,315 |
| C2 | Domestic Water | | | | | \$49,696.86 |
| | Domestic Water Supply | 1 | LS | \$25,000.00 | \$33,131.24 | \$ 49,697 |

| C3 | Domestic Wastewater | 1 | | \$2,500.00 | | | \$99,393.71 |
|----|---|-----|----|--------------|--------------|----|-----------------|
| | Domestic Wastewater System | 1 | LS | \$50,000.00 | \$66,262.48 | \$ | 99,394 |
| | | | | | | | |
| C4 | Disinfection Station | | | | | | \$22,500.00 |
| | Truck Disinfection Station | 1 | LS | \$15,000.00 | - | \$ | 22,500 |
| | Roadway Aggregate | 0 | SY | \$15.00 | - | \$ | _ |
| | Electrical | 0 | LS | \$2,500.00 | | \$ | |
| | Detention Tank | 0 | LS | \$5,000.00 | | \$ | _ |
| C5 | Paved Access to State or Local Highways | 0 | 20 | \$0.00 | | Ŷ | \$377,696.12 |
| 00 | Bituminous Paved Road | 1 | LS | \$190,000.00 | \$251,797.41 | \$ | 377,696 |
| | | | | | | | 377,090 |
| | Gravel Roads | 0 | LS | \$55,000.00 | \$72,888.72 | \$ | - |
| D. | Aquaculture Wastewater | | | | | | |
| D1 | Effluent Treatment | | | | | | \$11,733,357 |
| | | | | | | | ¢ : :,: cc,cc : |
| | | | | | | | |
| | Clarifier-40ft | | | | | - | |
| | Clarifier Concrete | 211 | CY | \$ 1,500 | - | \$ | 474,750 |
| | Clarifier Excavation | 898 | CY | \$ 50 | - | \$ | 67,350 |
| | Clarifier Equipment | 1 | LS | \$ 144,000 | \$ 227,707 | \$ | 341,560 |
| | Clarifier Coatings | 1 | LS | \$ 16,000 | \$ 25,301 | \$ | 37,951 |
| | Finger Weirs | 1 | LS | \$ 8,000 | \$ 12,650 | \$ | 18,976 |
| | Duplex Pump Station | 1 | LS | \$ 24,000 | \$ 37,951 | \$ | 56,927 |
| | 3" Sch 80 PVC Pipe | 100 | LF | \$ 48 | \$ 76 | \$ | 11,385 |
| | 4" Sch 80 PVC Pipe | 250 | LF | \$ 80 | \$ 127 | \$ | 47,439 |
| | 3" Plug Valves | 2 | EA | \$ 4,000 | \$ 6,325 | \$ | 18,976 |
| | 3" Swing Check Valves | 2 | EA | \$ 2,720 | \$ 4,301 | \$ | 12,903 |
| | Telescoping Valves | 2 | EA | \$ 1,520 | \$ 2,404 | \$ | 7,211 |
| | 6 ft precast manhole 6 ft deep | 2 | EA | \$ 12,000 | \$ 18,976 | \$ | 56,927 |
| | 4ft Precast Manhole 4 ft deep | 1 | EA | \$ 6,720 | \$ 10,626 | \$ | 15,939 |
| | Clarifier Equipment Install | 1 | LS | \$ 28,800 | \$ 45,541 | \$ | 68,312 |
| | Sludge Storage-25ft | | | | | | |
| | Sudge Storage Concrete | 121 | CY | \$ 1,500 | - | \$ | 272,250 |
| | Sludge Storage Exavation | 725 | CY | \$ 50 | - | \$ | 54,375 |
| | Sludge Mixing Pump | 1 | LS | \$ 10,000 | \$ 15,813 | \$ | 23,719 |
| | Sludge Mixing Nozzles | 1 | LS | \$ 35,000 | \$ 55,345 | \$ | 83,018 |

| 300 | LF | \$ | 50 | \$ 79 | \$ | 35,579 |
|-----|---|---|---|--|---|--|
| 1 | EA | \$ | 950 | \$ 1,502 | \$ | 2,253 |
| 1 | EA | \$ | 2,500 | \$ 3,953 | \$ | 5,930 |
| 1 | EA | \$ | 1,700 | \$ 2,688 | \$ | 4,032 |
| 2 | EA | \$ | 450 | \$ 712 | \$ | 2,13 |
| 1 | LS | \$ | 13,210 | \$ 20,889 | \$ | 31,33 |
| | | | | | | |
| | | | | | | |
| 1 | EA | \$ | 4,480,000 | - | \$ | 6,720,00 |
| 1 | EA | \$ | 7,800 | - | \$ | 11,70 |
| 1 | LS | \$ | 1,121,950 | - | \$ | 1,682,92 |
| | | | | | | |
| 2 | EA | \$ | 250,000 | - | \$ | 750,00 |
| 672 | CF | \$ | 500 | - | \$ | 504,00 |
| 1 | LS | \$ | 209,000 | - | \$ | 313,50 |
| | 1 1 2 1 1 1 1 1 1 1 2 1 1 2 672 | 1 EA 1 EA 1 EA 2 EA 1 LS 1 EA 1 EA 1 LS 1 EA 1 EA 1 EA 1 EA 1 EA 1 LS 2 EA 2 EA 2 EA 672 CF | 1 EA \$ 1 EA \$ 1 EA \$ 2 EA \$ 1 LS \$ 1 EA \$ 1 LS \$ 1 EA \$ 1 LS \$ 1 EA \$ 1 EA \$ 1 EA \$ 1 EA \$ 1 LS \$ 2 EA \$ 672 CF \$ | 1 EA \$ 950 1 EA \$ 2,500 1 EA \$ 1,700 2 EA \$ 450 1 LS \$ 13,210 1 EA \$ 4,480,000 1 EA \$ 7,800 1 EA \$ 1,121,950 2 EA \$ 250,000 672 CF \$ 500 | 1 EA \$ 950 1,502 1 EA \$ 2,500 3,953 1 EA \$ 1,700 2,688 2 EA \$ 450 712 1 LS \$ 13,210 \$ 20,889 1 LS \$ 13,210 \$ 20,889 1 EA \$ 4,480,000 - 1 EA \$ 7,800 - 1 EA \$ 1,121,950 - 1 LS \$ 1,121,950 - 2 EA \$ 250,000 - 2 EA \$ 500 - | 1 EA \$ 950 \$ 1,502 \$ 1 EA \$ 2,500 \$ 3,953 \$ 1 EA \$ 1,700 \$ 2,688 \$ 2 EA \$ 450 \$ 712 \$ 1 LS \$ 13,210 \$ 20,889 \$ 1 EA \$ 4,480,000 - \$ \$ 1 EA \$ 4,480,000 - \$ \$ 1 EA \$ 7,800 - \$ \$ 1 LS \$ 1,121,950 - \$ \$ 2 EA \$ 250,000 - \$ \$ 2 EA \$ 250,000 - \$ <td< td=""></td<> |

| D2 | Effluent Monitoring | | | | | \$64,605.91 |
|----|--------------------------------------|---|----|-------------|-----------------|--------------|
| | Automated Flow Measurement Equipment | 1 | LS | \$25,000.00 | \$ 33,131.24 | \$ 49,697 |
| | Portable Composite Sampler | 1 | LS | \$5,000.00 | \$ 6,626.25 | \$ 9,939 |
| | Electrical | 1 | LS | \$2,500.00 | \$ 3,313.12 | \$ 4,970 |
| | | | | | | |

| E. | Electrical and HVAC | | | | | |
|----|--|---|----|-------------|--------------|---------------|
| E1 | Electrical Service | | | | | \$225,000.00 |
| | 3-phase service - Effluent treatment plant | 1 | LS | \$ 100,000 | - | \$ 150,000 |
| | New Service Connections - Intakes, Pump Stations, Garage | 1 | LS | \$ 50,000 | - | \$ 75,000 |
| | | | | | | |
| E2 | Emergency Power | | | | | \$590,398.67 |
| | Emergency Generator: 100-200kW | 3 | LS | \$75,000.00 | \$ 99,393.71 | \$ 447,272 |
| | Automatic Transfer Switch | 3 | LS | \$10,000.00 | \$ 13,252.50 | \$ 59,636 |
| | Fuel Tank | 3 | LS | \$14,000.00 | \$ 18,553.49 | \$ 83,491 |
| | | | | | | |
| E3 | Instrumentation and Alarm System | | | | | \$397,574.86 |

| Instrumentation, Alarm System & Communication | 1 | LS | \$200,000.00 | \$ 265,049.91 | \$ 397,575 |
|---|---|----|--------------|------------------|---------------|
| | | | | | |

| F. | Visitor Education/Interpretation | | | | | |
|----|---|-------|----|-------------|---|--------------|
| F1 | Visitor Center Repairs | | | | | \$53,250.00 |
| | Replace egress door on north face | 1 | EA | \$2,500.00 | - | \$ 3,750 |
| | Fix / replace door sills for ADA compliance | 3 | EA | \$1,000.00 | - | \$ 4,500 |
| | Replace Carpet | 1,000 | SF | \$5.00 | - | \$ 7,500 |
| | New Digital Display | 1 | LS | \$5,000.00 | - | \$ 7,500 |
| | Convert Storage Room to Bathroom | 1 | LS | \$20,000.00 | - | \$ 30,000 |

\$56,224,430

| ITEM | DRAWING | ROUNDED |
|--|---------|--------------|
| | I.D. # | CONST COST |
| | | |
| New Facility Features | | |
| Hatchery Supply | A1 | \$489,000 |
| Cold Brook and Wells Intake Building | B1 | \$1,589,000 |
| Effluent Treatment Building | B3 | \$1,960,000 |
| Hatchery Building | B5 | \$4,230,000 |
| Rearing Building | B6 | \$33,077,000 |
| Existing Building Rehab | B7 | \$434,000 |
| Site Work | C1 | \$836,000 |
| Domestic Water | C2 | \$50,000 |
| Domestic Wastewater | C3 | \$100,000 |
| Disinfection Station | C4 | \$23,000 |
| Paved Access to State or Local Highways | C5 | \$378,000 |
| Effluent Treatment | D1 | \$11,734,000 |
| Effluent Monitoring | D2 | \$65,000 |
| Electrical Service | E1 | \$225,000 |
| Emergency Power | E2 | \$591,000 |
| Instrumentation and Alarm System | E3 | \$398,000 |
| Visitor Center Repairs | F1 | \$54,000 |
| Subtotal | | \$56,233,000 |
| Escalation to Midpoint of Const. @ 5%/yr for 5 years | | \$2,812,000 |
| 3% market volatility adjustment | | \$1,686,990 |
| Total Cost | | \$60,732,000 |

Powder Mill New Facility Summary Opinions of Probable Cost

Costs do NOT include: Design Reimbursables (Variable); State Agency Administrative Fee; and land acquisition or lease.



Effluent Treatment Evaluation

Alternative 2: 95% Recirculation with Adsorption Units

| Component | HP | Quantity | Total HP | Watts | Hours/day | kW-hrs/year |
|-------------------------------------|------------------|---------------------|---------------|--------------------|---------------|----------------|
| Hatchery Modernization | | | | | | |
| UV System | | 8 | | 56,000 | 24 | 3,924,480 |
| Drum Filter | 8.0 | 8.0 | 64.00 | 47,725 | 24 | 418,069 |
| | | | | | | |
| Recirc. Pumping | 15.0 | 6.0 | 90.00 | 67,113 | 24 | 587,910 |
| Site Lighting | | 1 | | 15,000 | 12 | 65,700 |
| Miscellaneous (SCADA, Meters, etc.) | | 1 | | 15,000 | 24 | 131,400 |
| MBBR-Blower | 15.00 | 6 | 90.00 | 67,113 | 24 | 587,910 |
| Effluent Treatment | | | | | | |
| Clarifier Mechanism | 0.75 | 1 | 0.75 | 559 | 24 | 4,899 |
| Sludge Pump | 20.00 | 1 | 20.00 | 14,914 | 24 | 130,647 |
| | 20.00 | | 20.00 | 14,014 | 27 | 100,047 |
| Membrane Process Pumps | 15.00 | 3.00 | 45.00 | 115,000 | 1 | 41,975 |
| Membrane Blowers | 90.00 | 1.00 | 90.00 | 123,000 | 1 | 44,895 |
| Membrane CIP Pumps | 15.00 | 1.00 | 15.00 | 44,000 | 1 | 16,060 |
| Membrane CIP Heaters | NA | | | 300,000 | 1 | 109,500 |
| Membrane Backpulse Pump | 60.00 | 1.00 | 60.00 | 40,000 | 1 | 14,600 |
| Membrane Drain Pump | 15.00 | 1.00 | 15.00 | 45,000 | 1 | 16,425 |
| | | | | | | |
| | | | | | | |
| | | | | | | |
| | | | | | kW-hrs/year = | 6,094,470 |
| | | | | | \$/kW-hrs = | \$0.12 |
| | | | | | | Annual Cost |
| | | | | | | \$731,336.35 |
| Estimated Annual Replacement Costs | | | | | | Annual Cost |
| Annual Equipment Replacement | | | | | | \$1,403,000.00 |
| Estimated Annual Labor Costs | Days per Week | Hours per day | Personnel | Rate | OH/Fringe | Annual Cost |
| Daily Operator Attention | 5 | 8 | 2 | \$ 25.00 | \$ 15.00 | \$104,000 |
| Chemicals | Use (gpd) | Annual Use (gal) | Cost (\$/gal) | Replacemen t/yr | | Annual Cost |
| Нуро | , | 6900 | 2.5 | | | \$17,250 |
| Citric | | 14500 | 8.25 | | | \$119,625 |
| Sodium Bisulfate | | 1700 | 3.4 | | | \$5,780 |
| Sulfuric | | | | | | \$0 |
| | + | 6000 | 0.6 | 12 | | \$43,200.00 |
| O2 Usage - Tank refill | | 0000 | 0.0 | IZ | | 040,Z00.00 |

| Estimated Annual Labor and Replacement Costs | \$1,507,000 |
|---|-------------|
| Estimated Annual Electricity and Chemical Usage Costs | \$947,128 |
| TOTAL | \$2,455,000 |

New Hampshire Fish and Game Department Effluent Treatment Evaluation Alternative 2: 95% Recirculation with Adsorption Units Life Cycle Cost Analysis

| | 0 | | 0 | • | | 0 | - | 0 | 0 | | | 10 | 40 | | 45 | 10 | 47 | 10 | 10 |
|---|------------------------------|----------------|------------------|-----------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|
| Total | 2023 | 2024 | 2025 2 | 026 2027 | 2028 | 2029 | 2030 | 2031 | 2032 | 10 2033 | 11 2034 | 12 2035 | 13 2036 | 14 2037 | 2038 | 16 2039 | 2040 | 18 2041 | 19 2042 |
| O&M | 2023 | 2024 | 2025 | 026 2027 | 2028 | 2029 | 2030 | 2031 | 2032 | 2033 | 2034 | 2035 | 2036 | 2037 | 2038 | 2039 | 2040 | 2041 | 2042 |
| Power and Chemical cost (6%/yr 2023-2026, 3%/yr 2027-2042 escalation) | \$2.455.000 \$ | 2 602 200 ©2 | ,758,438 \$2,923 | 044 62 044 66 | £2 102 012 | \$2 405 072 | £2 200 025 | £2.200.652 | £2 404 242 | \$2 EOC 002 | \$2 702 OCF | \$2.04E.004 | 62 020 527 | 64 047 400 | £4 460 04E | £4 202 011 | 64 400 700 | \$4 EEE 440 | £4 602 072 |
| | | | | | | | | | | | | | | | | | | | |
| R&R Maintenance cost (6%/yr 2023-2026, 4%/yr 2027-2042 escalation) | | | \$545,025 \$577 | | | \$649,863 | | \$702,892 | \$731,008 | | \$790,658 | \$822,284 | \$855,176 | \$889,383 | \$924,958 | | | \$1,040,452 | |
| Total O&M Cost | \$2,940,070 \$ | 3,116,474 \$3, | ,303,463 \$3,501 | 670 \$3,612,498 | \$3,726,881 | \$3,844,936 | \$3,966,783 | \$4,092,545 | \$4,222,350 | \$4,356,331 | \$4,494,623 | \$4,637,369 | \$4,784,712 | \$4,936,806 | \$5,093,804 | \$5,255,867 | \$5,423,163 | \$5,595,862 | \$5,774,142 |
| Average Annual O&M Cost over 20 years (\$/yr) \$4,334,017 | | | | | | | | | | | | | | | | | | | |
| Average Annual O&M Cost over 10 years (\$/yr) \$3,632,767 | | | | | | | | | | | | | | | | | | | |
| Capital Cost Equipment Cost | \$56,224,000 \$16,169,000 | | | | | | | | | | | | | | | | | | |
| Net Present Value (at 5% discount rate) | | | | | | | | | | | | | | | | | | | |
| 20 Year Net Present Value \$107,415,667 | | | | | | | | | | | | | | | | | | | |
| 10 Year Net Present Value \$83,844,000 | | | | | | | | | | | | | | | | | | | |
| Annual Cost | | | | | | | | | | | | | | | | | | | |

Average Annual Cost (Debt Service + O&M, 20 year basis) \$8,845,577 Average Annual Cost (Debt Service + O&M, 10 year basis) \$10,914,032

| ITEM | DRAWING | ROUNDED CONST COST ^a | ROUNDED CONST COST ^ª | |
|--|---------|------------------------------------|------------------------------------|---------------|
| | I.D. # | New Hampton | Milford | Const cost |
| New Facility Features | | New Hampton | Millord | Combined |
| Hatchery Supply | A1 | \$247,000 | \$34,000 | \$281,000 |
| Intake Building | B1 | \$1,589,000 | \$2,779,000 | \$4,368,000 |
| Hatchery Building | B2 | \$4,230,000 | \$4,230,000 | \$8,460,000 |
| Rearing Building | B3 | \$33,077,000 | \$33,077,000 | \$66,154,000 |
| Rehabilitation of other buildings on site | B4 | \$264,000 | \$828,000 | \$1,092,000 |
| Raceway Rehabiltaiton | B5 | \$0 | \$0 | \$0 |
| Site Work | C1 | \$836,000 | \$836,000 | \$1,672,000 |
| Domestic Water | C2 | \$50,000 | \$50,000 | \$100,000 |
| Domestic Wastewater | C3 | \$100,000 | \$100,000 | \$200,000 |
| Disinfection Station | C4 | \$23,000 | \$23,000 | \$46,000 |
| Paved Access to State or Local Highways | C5 | \$378,000 | \$378,000 | \$756,000 |
| Effluent Treatment | D1 | \$2,055,000 | \$2,055,000 | \$4,110,000 |
| Effluent Monitoring | D2 | \$65,000 | \$65,000 | \$130,000 |
| Effluent Pumping | D3 | \$2,071,000 | \$1,666,000 | \$3,737,000 |
| Electrical Service | E1 | \$300,000 | \$300,000 | \$600,000 |
| Emergency Power | E2 | \$456,000 | \$456,000 | \$912,000 |
| Instrumentation and Alarm System | E3 | \$398,000 | \$398,000 | \$796,000 |
| Visitor Center Repairs | F1 | \$600,000 | \$289,000 | \$889,000 |
| Subtotal | | \$46,739,000 | \$47,564,000 | \$94,303,000 |
| Escalation to Midpoint of Const. @ 5%/yr for 5 years | | \$2,337,000 | \$2,378,000 | \$4,715,000 |
| 3% market volatility adjustment | | \$1,402,170 | \$1,426,920 | \$2,829,090 |
| Total Cost | | \$50,478,000 | \$51,369,000 | \$101,847,000 |

Date: 3/15/2023 Estimator: Checked By: Check Date: Revised: -



| Detailed Opinions of Probable Cost | | | | | | | | | | |
|------------------------------------|-------|-------|----------|-----------------|------------|--|--|--|--|--|
| | NO. | UNIT | COST PER | Escalation cost | TOTAL COST | | | | | |
| New Hampton 1.A | UNITS | MEAS. | UNIT | to 2022 | 50% CONT. | | | | | |

| A. | Aquaculture Water Supply | | | | | |
|-----------|--|------|----|---------------|--------------|-----------------|
| A1 | Hatchery Supply | | | | | \$246,660 |
| | Water Supply Piping and Accessories | 1300 | LF | \$ 85 | \$ 113 | \$ 219,660 |
| | Rehab of Major Spring Conc Structures Above Spring Pond | 1 | LS | \$ 3,000 | \$ 3,000 | \$ 4,500 |
| | Minor Springs Replace Inlet Box at inlet pool and cover inlet pool | 1 | LS | \$ 15,000 | \$ 15,000 | \$ 22,500 |
| В. | Buildings and Rearing Units | | | | | |
| B1 | Intake Building | | | | | \$ 1,588,544 |
| | New Intake Building | 400 | SF | \$ 165 | \$ 218 | \$ 131,017 |
| | Drumfilter | | | | | |
| | DRUM FILTERS | 2 | EA | \$ 75,000 | - | \$ 225,000 |
| | DRUM SUMP | 1 | LS | \$ 75,000 | - | \$ 112,500 |
| | PIPING SYSTEMS (INFLOW, DRAINS) | 1 | LS | \$ 500,000 | - | \$ 750,000 |
| | PRIMARY POWER | 1 | LS | \$ 75,000 | - | \$ 112,500 |
| | UV System | | | | | |
| | UV Channel and Lamp Package | 2 | EA | \$ 50,000 | - | \$ 150,000 |
| | UV Electrical | 1 | LS | \$ 8,000 | \$ 10,602 | \$ 15,903 |
| | UV Plumbing | 1 | LS | \$ 11,000 | \$ 14,578 | \$ 21,867 |
| | Electrical Power and Lighting | 1 | LS | \$ 20,000 | \$ 26,505 | \$ 39,757 |
| | ALARMS/CONTROLS/MONITORING/PANEL/HMI | 1 | LS | \$ 20,000 | - | \$ 30,000 |
| B2 | Hatchery Building | | | | | \$4,229,021.87 |

| | New Hatchery Building - Office Space | 3700 | SF | \$165.00 | \$ 218 | \$ 1,211,910 |
|----|--|--------|----------|---------------|----------------|------------------|
| | POWER AND LIGHTING | 3700 | SF | \$ 50 | \$103.40 | \$ 573,847 |
| | HVAC | 1 | LS | \$ 100,000 | \$206,791.77 | \$ 310,188 |
| | EQUIPMENT | | | | | |
| | FEEDERS (SWEENEY MDL AF7 W/CONTROLLER & SUPPORT) | 72 | EA | \$ 600 | \$1,240.75 | \$ 134,001 |
| | FG TROUGHS (12'x2'x2') | 42 | EA | \$ 2,500 | \$5,169.79 | \$ 325,697 |
| | INCUBATION ROOM 30 HEATH STACKS | 12 | EA | \$ 2,500 | \$5,169.79 | \$ 93,056 |
| | INCUBATION HEAD TROUGHS AND CONTROLS | 2 | LS | \$ 15,000 | \$31,018.77 | \$ 93,056 |
| | CHILLER SYSTEM AND CONTROLS | 1 | LS | \$ 250,000 | \$516,979.42 | \$ 775,469 |
| | FORMALIN ROOM | 1 | LS | \$ 50,000 | \$103,395.88 | 155,094 |
| | BOOT LOCKER ROOM, W/D, BENCHES | 1 | LS | \$ 50,000 | \$103,395.88 | 155,094 |
| | WATER QUALITY ROOM EQUIP ALLOWANCE | 1 | LS | \$ 75,000 | \$155,093.83 | 232,641 |
| | Hatchery Building Aeration/Degassing System | | | | | |
| | Primary Headtank & Aeration/Degassing System | 1 | EA | \$ 85,000 | \$ 112,646 | \$ 168,969 |
| | | | | | | |
| B3 | Rearing Building | | | | | \$33,076,818.1 |
| | New Rearing Building (526x140) | 73,640 | SF | \$ 165 | \$ 218 | \$ 24,120,276 |
| | ALARMS/CONTROLS/MONITORING/PANEL/HMI | 1 | LS | \$ 50,000 | - | \$ 75,000 |
| | VFD W/CIRCUIT BREAKER AND FULL CONTACTOR SET | 2 | EA | \$ 25,000 | - | \$ 75,000 |
| | PANEL/RACK/WIRING/CONDUITS/FEEDER | 2 | EA | \$ 55,000 | - | \$ 165,000 |
| | 12" FLOW METER | 2 | EA | \$ 18,000 | - | \$ 54,000 |
| | EQUIPMENT | | | | | |
| | 20' dia. SS Culture Tank with Foundation & Floor | 20 | EA | \$ 35,000 | - | \$ 1,050,000 |
| | 40' dia. SS Culture Tank with Foundation & Floor | 16 | EA | \$ 50,000 | - | \$ 1,200,000 |
| | Drumfilter | | | | | |
| | DRUM FILTERS | 6 | EA | \$ 85,000 | - | \$ 765,000 |
| | DRUM SUMP | 1 | LS | \$ 75,000 | - | \$ 112,500 |
| | PRIMARY POWER | 1 | LS | \$ 75,000 | - | \$ 112,500 |
| | UV System | | | | | |
| | UV Channel and Lamp Package | 6 | EA | \$ 125,000 | - | \$ 1,125,000 |
| | UV Electrical | 1 | LS | \$ 8,000 | | \$ 15,903 |
| | UV Plumbing | 1 | LS | \$ 11,000 | \$ 14,578 | \$ 21,867 |
| | Recirculation | | | | | |
| | PIPING SYSTEMS (INFLOW, PRAS, DRAINS) | 1 | LS | \$ 500,000 | - | \$ 750,000 |
| | Lift Pump | 6 | EA EA | \$ 80,000 | - *^ ^// // | \$ 720,000 |
| | 4ft Precast Manhole 4 ft deep | 6 | EA | \$ 4,200 | \$6,641.45 | \$ 59,773 |

| | Biofilter System | | | | | |
|-----------|--|------|----|---------------|--------------|-----------------|
| | MBBR | 6 | EA | \$ 200,000 | - | \$ 1,800,000 |
| | HVAC | 1 | LS | \$ 100,000 | - | \$ 150,000 |
| | Electrical Power and Lighting | 1 | LS | \$ 200,000 | - | \$ 300,000 |
| | GAS MANAGEMENT TOWER CO2 STRIPPER/LHO | 6 | EA | \$ 45,000 | - | \$ 405,000 |
| B4 | Rehabilitation of other buildings on site | | | | | \$ 264,000 |
| | Garage Renovations | 1 | LS | \$ 119,500 | | \$ 119,500 |
| | Wood Working Shop Renovations | 1 | LS | \$ 33,500 | | \$ 33,500 |
| | C-Station Office Renovations | 1 | LS | \$ 81,000 | | \$ 81,000 |
| | Demo (Boat Shed, Shavings Shed, Timber Shed, Tools Shed) | 1 | LS | \$ 30,000 | | \$ 30,000 |
| B5 | Raceway Rehabiltaiton | | | | | \$ - |
| | N/A | | | | | |
| C. | Site | | | | | |
| C1 | Site Work | | | | | \$835,155.69 |
| | Site Clearing | 2.5 | AC | \$2,000.00 | \$2,650.50 | \$ 9,939 |
| | General Earthwork for Hatchery Complex | 1 | LS | \$75,000.00 | \$99,393.71 | \$ 149,091 |
| | General Sitework | 1 | LS | \$250,000.00 | \$331,312.38 | \$ 496,969 |
| | Erosion Control | 20 | AC | \$2,500.00 | \$3,313.12 | \$ 99,394 |
| | Seeding | 1 | AC | \$1,250.00 | \$1,656.56 | \$ 2,485 |
| | Landscaping | 1 | AC | \$3,000.00 | \$3,975.75 | \$ 5,964 |
| | Natural Gas Connection and Distribution (if available) | 0 | LS | \$35,000.00 | \$46,383.73 | \$ - |
| | Stormwater Management System | 10.3 | AC | \$3,500.00 | \$4,638.37 | \$ 71,315 |
| C2 | Domestic Water | | | | | \$49,696.86 |
| | Domestic Water Supply | 1 | LS | \$25,000.00 | \$33,131.24 | \$ 49,697 |
| C3 | Domestic Wastewater | 1 | | \$2,500.00 | | \$99,393.71 |
| | Domestic Wastewater System | 1 | LS | \$50,000.00 | \$66,262.48 | \$ 99,394 |
| C4 | Disinfection Station | | | | | \$22,500.00 |
| | Truck Disinfection Station | 1 | LS | \$15,000.00 | - | \$ 22,500 |
| | Roadway Aggregate | 0 | SY | \$15.00 | - | \$ - |
| | Electrical | 0 | LS | \$2,500.00 | - | \$ - |

| | Detention Tank | 0 | LS | | \$5,000.00 | | - | \$ | - |
|----|---|-----|----|----|--------------|---------|---------------------------|----------|-------------|
| C5 | Paved Access to State or Local Highways | 0 | | | \$0.00 | | | | \$377,696.1 |
| | Bituminous Paved Road | 1 | LS | | \$190,000.00 | | \$251,797.41 | \$ | 377,696 |
| | Gravel Roads | 0 | LS | | \$55,000.00 | | \$72,888.72 | \$ | _ |
| | | | | | • , | | · , | • | |
|). | Aquaculture Wastewater | | | | | | | | |
| D1 | Effluent Treatment | | | | | | | | \$2,054,69 |
| | | | | | | | | | |
| | Clarifier-40ft | | | | | | | | |
| | Clarifier Concrete | 211 | CY | \$ | 1,500 | | - | \$ | 474,75 |
| | Clarifer Excavation | 898 | СҮ | \$ | 50 | | _ | \$ | 67,35 |
| | Clarifier Equipment | 1 | LS | \$ | 108,000 | \$ | 170,780 | \$ | 256,17 |
| | Clarifier Coatings | 1 | LS | \$ | 12,000 | \$ | 18,976 | \$ | 28,46 |
| | Finger Weirs | 1 | LS | \$ | 6,000 | ↓ \$ | 9,488 | \$ | 14,23 |
| | Duplex Pump Station | 1 | LS | \$ | 18,000 | Գ \$ | 28,463 | \$ | 42,69 |
| | 3" Sch 80 PVC Pipe | 100 | LU | \$ | 36 | \$ | 20, 4 03 57 | \$ | 8,53 |
| | 4" Sch 80 PVC Pipe | 250 | | \$ | 60 | ≎ \$ | 95 | \$ | 35,57 |
| | 3" Plug Valves | 200 | EA | \$ | 3,000 | \$ | 4,744 | \$ | 14,23 |
| | 3" Swing Check Valves | 2 | EA | \$ | 2,040 | \$ | 3,226 | \$ | 9,67 |
| | Telescoping Valves | 2 | EA | \$ | 1,140 | \$ | 1,803 | \$ | 5,40 |
| | 6 ft precast manhole 6 ft deep | 2 | EA | \$ | 9,000 | \$ | 14,232 | \$ | 42,69 |
| | 4ft Precast Manhole 4 ft deep | 1 | EA | \$ | 5,040 | \$ | 7,970 | \$ | 11,95 |
| | Clarifier Equipment Install | 1 | LS | \$ | 21,600 | \$ | 34,156 | \$ | 51,23 |
| | Sludge Storage-25ft | | | | | | | | |
| | Sudge Storage Concrete | 121 | СҮ | \$ | 1,500 | | | \$ | 272,25 |
| | Sludge Storage Exavation | 725 | CY | \$ | 50 | | - | \$ \$ | 54,37 |
| | Sludge Mixing Pump | 1 | LS | \$ | 10,000 | \$ | 15,813 | \$ | 23,71 |
| | Sludge Mixing Nozzles | 1 | LS | \$ | 35,000 | \$ | 55,345 | \$ | 83,02 |
| | 4" Sch 80 PVC Pipe | 300 | LF | \$ | 50 | \$ | 79 | \$ | 35,57 |
| | Telescoping Valves | 1 | EA | \$ | 950 | \$ | 1,502 | \$ | 2,25 |
| | 3" Plug Valves | 1 | EA | \$ | 2,500 | \$ | 3,953 | \$ | 5,93 |
| | 3" Swing Check Valves | 1 | EA | \$ | 1,700 | \$ | 2,688 | \$ | 4,03 |
| | Air Release Valve | 2 | EA | \$ | 450 | \$ | 712 | \$ | 2,13 |
| | Sludge Mix & Transfer System Install | 1 | LS | \$ | 13,210 | \$ | 20,889 | \$ | 31,33 |
| | WW Sitework | 1 | LS | \$ | 40,000 | \$ | 53,010 | \$ | 79,51 |
| | | I | | φ | +0,000 | Ψ | 55,010 | Ψ | 79,01 |

| | Electrical Power and Lighting | 1 | LS | \$ 200,000 | \$ 265,050 | \$ 397,575 |
|----|--------------------------------------|------|----|--------------|--------------|-----------------|
| | | | | | | |
| D2 | Effluent Monitoring | | | | | \$64,605.91 |
| | Automated Flow Measurement Equipment | 1 | LS | \$25,000.00 | \$ 33,131.24 | \$ 49,697 |
| | Portable Composite Sampler | 1 | LS | \$5,000.00 | \$ 6,626.25 | \$ 9,939 |
| | Electrical | 1 | LS | \$2,500.00 | \$ 3,313.12 | \$ 4,970 |
| D3 | Effluent Pumping | | | | | \$2,070,701.81 |
| | WW Piping line | 3200 | LF | \$ 85 | \$ 113 | \$ 540,702 |
| | New Hampton Pump Station | 1 | LS | \$ 1,020,000 | - | \$ 1,530,000 |

| Е. | Electrical and HVAC | | | | | | |
|----|---|-------|----|--------------|---------------|----|--------------|
| E1 | Electrical Service | | | | | | \$300,000.00 |
| | New 480V utility service | 1 | LS | \$ 100,000 | - | \$ | 150,000 |
| | New 480V distribution | 1000 | LF | \$ 100 | - | \$ | 150,000 |
| E2 | Emergency Power | | | | | | \$455,223.21 |
| | Emergency Generator: 100-200kW | 1 | LS | \$200,000.00 | \$ 265,049.91 | \$ | 397,575 |
| | Automatic Transfer Switch | 1 | LS | \$15,000.00 | \$ 19,878.74 | \$ | 29,818 |
| | Fuel Tank | 1 | LS | \$14,000.00 | \$ 18,553.49 | \$ | 27,830 |
| E3 | Instrumentation and Alarm System | | | | | | \$397,574.86 |
| | Instrumentation, Alarm System & Communication | 1 | LS | \$200,000.00 | \$ 265,049.91 | \$ | 397,575 |
| F. | Visitor Education/Interpretation | | | | | L | |
| F1 | Visitor Center Repairs | | | | | | \$600,000.00 |
| | New Visitor Center Building | 1,000 | SF | \$350.00 | - | \$ | 525,000 |
| | New Displays | 1 | LS | \$50,000.00 | - | \$ | 75,000 |
| i | | | | | | | \$46,732,288 |

\$46,732,288



New Hampshire Fish and Game Department

Effluent Treatment Evaluation

New Hampton 1A: New 95% RAS Building

Operation and Maintenance

| Component | HP | Quantity | Total HP | Watts | Hours/day | kW-hrs/year |
|-------------------------------------|------------------|---------------------|---------------|--------------------|---------------|--------------|
| Influent | | | | | | |
| UV System | | 2 | | 56,000 | 24 | 981,120 |
| Drum Filter | 8.0 | 2.0 | 16.00 | 11,931 | 24 | 104,517 |
| Hatchery Modernization | | | | | | |
| UV System | | 6 | | 56,000 | 24 | 2,943,360 |
| Drum Filter | 8.0 | 6.0 | 48.00 | 35,794 | 24 | 313,552 |
| Recirc. Pumping | 15.0 | 6.0 | 90.00 | 67,113 | 24 | 587,910 |
| Site Lighting | | 1 | | 15,000 | 12 | 65,700 |
| Miscellaneous (SCADA, Meters, etc.) | | 1 | | 15,000 | 24 | 131,400 |
| MBBR-Blower | 15.00 | 6 | 90.00 | 67,113 | 24 | 587,910 |
| Effluent Treatment | | | | | | |
| Clarifier Mechanism | 0.75 | 1 | 0.75 | 559 | 24 | 4,899 |
| Sludge Pump | 20.00 | 1 | 20.00 | 14,914 | 24 | 130,647 |
| Effluent Pumping | | | | | | 192,000 |
| | | | | | kW-hrs/year = | 4,957,377 |
| | | | | | \$/kW-hrs = | \$0.12 |
| | | | | | | Annual Cost |
| | | | | | | \$594,885.28 |
| Estimated Annual Replacement Costs | | | | | | Annual Cost |
| Annual Equipment Replacement | - | 1 | | | | \$789,000.00 |
| Estimated Annual Labor Costs | Days per Week | Hours per day | Personnel | Rate | OH/Fringe | Annual Cost |
| Daily Operator Attention | 5 | 8 | 0 | \$ 25.00 | \$ 15.00 | \$0 |
| Chemicals | Use (gpd) | Annual Use (gal) | Cost (\$/gal) | Replacemen t/yr | | Annual Cost |
| O2 Usage - Tank refill | | 6000 | 0.6 | 12 | | \$43,200.00 |

| Estimated Annual Labor and Replacement Costs | \$789,000 |
|---|-------------|
| Estimated Annual Electricity and Chemical Usage Costs | \$638,085 |
| TOTAL | \$1,428,000 |

| | | | | | | N | | Fish and Os | | | | | | | | | | | | | |
|---|--------------------------------------|--------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|
| | | | | | | Nev | w Hampshire | | - | nt | | | | | | | | | | | |
| | Effluent Treatment Evaluation | | | | | | | | | | | | | | | | | | | | |
| | New Hampton 1A: New 95% RAS Building | | | | | | | | | | | | | | | | | | | | |
| Life Cycle Cost Analysis | | | | | | | | | | | | | | | | | | | | | |
| | | 0 | 1 | 2 | 3 | 4 | 5 | 6 | 7 | 8 | 9 | 10 | 11 | 12 | 13 | 14 | 15 | 16 | 17 | 18 | 19 |
| | Total | 2023 | 2024 | 2025 | 2026 | 2027 | 2028 | 2029 | 2030 | 2031 | 2032 | | 2034 | | 2036 | 2037 | 2038 | 2039 | 2040 | 2041 | 2042 |
| O&M | | | | | | | | | | | | | | | | | | | | | |
| Power and Chemical cost (6%/yr 2023-2026, 3%/yr 2027-2042 escalation) | | \$1,428,000 | \$1,513,680 | \$1,604,501 | \$1,700,771 | \$1,751,794 | | | . , , | | | \$2,091,734 | | | \$2,285,694 | | | \$2,497,639 | | \$2,649,746 | |
| R&R Maintenance cost (6%/yr 2023-2026, 4%/yr 2027-2042 escalation) | | \$272,760 | \$289,126 | \$306,473 | . , | \$337,856 | . , | | | \$395,244 | \$411,053 | . , | \$444,595 | , | \$480,874 | \$500,109 | | \$540,918 | \$562,555 | \$585,057 | \$608,460 |
| Total O&M Cost | | \$1,700,760 | \$1,802,806 | \$1,910,974 | \$2,025,632 | \$2,089,650 | \$2,155,718 | \$2,223,903 | \$2,294,275 | \$2,366,903 | \$2,441,863 | \$2,519,229 | \$2,599,081 | \$2,681,499 | \$2,766,568 | \$2,854,374 | \$2,945,006 | \$3,038,558 | \$3,135,124 | \$3,234,803 | \$3,337,697 |
| Average Annual O&M Cost over 20 years (\$/yr) | \$2,506,221 | | | | | | | | | | | | | | | | | | | | |
| Average Annual O&M Cost over 10 years (\$/yr) | \$2,101,248 | | | | | | | | | | | | | | | | | | | | |
| Capital Cost | | \$50,478,000 | | | | | | | | | | | | | | | | | | | |
| Equipment Cost | | \$9,092,000 | | | | | | | | | | | | | | | | | | | |
| | | \$0,002,000 | | | | | | | | | • | | | | | | | | | | |
| Net Present Value (at 5% discount rate) | | | | | | | | | | | | | | | | | | | | | |
| 20 Year Net Present Value | \$80,082,517 | | | | | | | | | | | | | | | | | | | | |
| | \$66,454,000 | | | | | | | | | | | | | | | | | | | | |
| | | | | | | | | | | | | | | | | | | | | | |
| Annual Cost | ¢6 556 706 | | | | | | | | | | | | | | | | | | | | |

Average Annual Cost (Debt Service + O&M, 20 year basis)\$6,556,706Average Annual Cost (Debt Service + O&M, 10 year basis)\$8,638,380

Client: NHFGD Project:Powder Mill Fish Hatchery Study Project No.: 10331124

Date: 3/15/2023 Estimator: Checked By: Check Date: Revised: -



| Detailed Opinions of Probable Cost | | | | | | | | | | | |
|------------------------------------|-------|-------|----------|-----------------|------------|--|--|--|--|--|--|
| | NO. | UNIT | COST PER | Escalation cost | TOTAL COST | | | | | | |
| Milford 1.A | UNITS | MEAS. | UNIT | to 2022 | 50% CONT. | | | | | | |

| A. | Aquaculture Water Supply | | | | | | | |
|----|--|------|----|----|-----------|----|--------------|-----------------|
| | Hatchery Supply | | | | | | | \$33,794 |
| | Water Supply Piping and Accessories | 200 | LF | \$ | 85 | \$ | 113 | \$ 33,794 |
| | | | | | | | | |
| В. | Buildings and Rearing Units | | | • | | • | | |
| B1 | Intake Building | | | | | | | \$ 2,778,318 |
| | New Intake Building | 1400 | SF | \$ | 165 | \$ | 218 | \$ 458,560 |
| | Iron and Manganese Green Sand Filters | 1 | LS | \$ | 1,500,000 | | - | \$ 2,250,000 |
| | Electrical Power and Lighting | 1 | LS | \$ | 20,000 | \$ | 26,505 | \$ 39,757 |
| | ALARMS/CONTROLS/MONITORING/PANEL/HMI | 1 | LS | \$ | 20,000 | | - | \$ 30,000 |
| B2 | Hatchery Building | | | | | | | \$4,229,021.87 |
| | New Hatchery Building - Office Space | 3700 | SF | | \$165.00 | \$ | 218 | \$ 1,211,910 |
| | POWER AND LIGHTING | 3700 | SF | \$ | 50 | | \$103.40 | \$ 573,847 |
| | HVAC | 1 | LS | \$ | 100,000 | | \$206,791.77 | \$ 310,188 |
| | EQUIPMENT | | | | | | | |
| | FEEDERS (SWEENEY MDL AF7 W/CONTROLLER & SUPPORT) | 72 | EA | \$ | 600 | | \$1,240.75 | \$ 134,001 |
| | FG TROUGHS (12'x2'x2') | 42 | EA | \$ | 2,500 | | \$5,169.79 | \$ 325,697 |
| | INCUBATION ROOM 30 HEATH STACKS | 12 | EA | \$ | 2,500 | | \$5,169.79 | \$ 93,056 |
| | INCUBATION HEAD TROUGHS AND CONTROLS | 2 | LS | \$ | 15,000 | | \$31,018.77 | \$ 93,056 |
| | CHILLER SYSTEM AND CONTROLS | 1 | LS | \$ | 250,000 | | \$516,979.42 | \$ 775,469 |
| | FORMALIN ROOM | 1 | LS | \$ | 50,000 | | \$103,395.88 | \$ 155,094 |

| BOOT LOCKER ROOM, W/D, BENCHES | 1 | LS | \$ 50,000 | \$103,395.88 | \$ | 155,09 |
|--|--------|----|---------------|--------------|----|---------------|
| WATER QUALITY ROOM EQUIP ALLOWANCE | 1 | LS | \$ 75,000 | \$155,093.83 | \$ | 232,64 |
| Hatchery Building Aeration/Degassing System | | | | | | |
| Primary Headtank & Aeration/Degassing System | 1 | EA | \$ 85,000 | \$ 112,646 | \$ | 168,96 |
| | | | | | | |
| 3 Rearing Building | | | | | | \$33,076,818. |
| New Rearing Building (526x140) | 73,640 | SF | \$ 165 | \$ 218 | \$ | 24,120,27 |
| ALARMS/CONTROLS/MONITORING/PANEL/HMI | 1 | LS | \$ 50,000 | - | \$ | 75,00 |
| VFD W/CIRCUIT BREAKER AND FULL CONTACTOR SET | 2 | EA | \$ 25,000 | - | \$ | 75,00 |
| PANEL/RACK/WIRING/CONDUITS/FEEDER | 2 | EA | \$ 55,000 | - | \$ | 165,00 |
| 12" FLOW METER | 2 | EA | \$ 18,000 | | \$ | 54,00 |
| EQUIPMENT | | | | | | |
| 20' dia. SS Culture Tank with Foundation & Floor | 20 | EA | \$ 35,000 | - | \$ | 1,050,00 |
| 40' dia. SS Culture Tank with Foundation & Floor | 16 | EA | \$ 50,000 | - | \$ | 1,200,00 |
| Drumfilter | | | | | + | .,_00,00 |
| DRUM FILTERS | 6 | EA | \$ 85,000 | - | \$ | 765,00 |
| DRUM SUMP | 1 | LS | \$ 75,000 | - | \$ | 112,50 |
| PRIMARY POWER | 1 | LS | \$ 75,000 | - | \$ | 112,50 |
| UV System | | | | | | |
| UV Channel and Lamp Package | 6 | EA | \$ 125,000 | - | \$ | 1,125,00 |
| UV Electrical | 1 | LS | \$ 8,000 | \$ 10,602 | \$ | 15,90 |
| UV Plumbing | 1 | LS | \$ 11,000 | \$ 14,578 | \$ | 21,80 |
| Recirculation | | | | | | |
| PIPING SYSTEMS (INFLOW, PRAS, DRAINS) | 1 | LS | \$ 500,000 | | \$ | 750,00 |
| Lift Pump | 6 | EA | \$ 80,000 | | \$ | 720,0 |
| 4ft Precast Manhole 4 ft deep | 6 | EA | \$ 4,200 | \$6,641.45 | \$ | 59,7 |
| Biofilter System | | | | | | |
| MBBR | 6 | EA | \$ 200,000 | - | \$ | 1,800,0 |
| HVAC | 1 | LS | \$ 100,000 | - | \$ | 150,0 |
| Electrical Power and Lighting | 1 | LS | \$ 200,000 | - | \$ | 300,0 |
| GAS MANAGEMENT TOWER CO2 STRIPPER/LHO | 6 | EA | \$ 45,000 | - | \$ | 405,0 |
| 4 Rehabilitation of other buildings on site | | | | | \$ | 828,0 |
| Hatchery Building Renovations | 1 | LS | \$ 608,000 | | \$ | 608,0 |
| New Maintenance Garage (to replace existing Storage Building) | 1600 | SF | \$ 125 | | \$ | 200,0 |
| Demolish (Storage Building Tent, Twin Mnt Rearing, Storage Shed) | 1 | LS | \$ 20,000 | | \$ | 20,00 |

| B5 | Raceway Rehabiltaiton | | | \$- | |
|----|-----------------------|--|--|-----|--|
| | N/A | | | | |
| | | | | | |

| C. | Site | | | | | |
|----|--|------|----|--------------|--------------|---------------|
| C1 | Site Work | | | | | \$835,155.69 |
| | Site Clearing | 2.5 | AC | \$2,000.00 | \$2,650.50 | \$ 9,939 |
| | General Earthwork for Hatchery Complex | 1 | LS | \$75,000.00 | \$99,393.71 | \$ 149,091 |
| | General Sitework | 1 | LS | \$250,000.00 | \$331,312.38 | \$ 496,969 |
| | Erosion Control | 20 | AC | \$2,500.00 | \$3,313.12 | \$ 99,394 |
| | Seeding | 1 | AC | \$1,250.00 | \$1,656.56 | \$ 2,485 |
| | Landscaping | 1 | AC | \$3,000.00 | \$3,975.75 | \$ 5,964 |
| | Natural Gas Connection and Distribution (if available) | 0 | LS | \$35,000.00 | \$46,383.73 | \$ - |
| | Stormwater Management System | 10.3 | AC | \$3,500.00 | \$4,638.37 | \$ 71,315 |
| C2 | Domestic Water | | | | | \$49,696.86 |
| | Domestic Water Supply | 1 | LS | \$25,000.00 | \$33,131.24 | \$ 49,697 |
| C3 | Domestic Wastewater | 1 | | \$2,500.00 | | \$99,393.71 |
| | Domestic Wastewater System | 1 | LS | \$50,000.00 | \$66,262.48 | \$ 99,394 |
| C4 | Disinfection Station | | | | | \$22,500.00 |
| | Truck Disinfection Station | 1 | LS | \$15,000.00 | - | \$ 22,500 |
| | Roadway Aggregate | 0 | SY | \$15.00 | - | \$ - |
| | Electrical | 0 | LS | \$2,500.00 | - | \$ - |
| | Detention Tank | 0 | LS | \$5,000.00 | - | \$ - |
| C5 | Paved Access to State or Local Highways | 0 | | \$0.00 | | \$377,696.12 |
| | Bituminous Paved Road | 1 | LS | \$190,000.00 | \$251,797.41 | \$ 377,696 |
| | Gravel Roads | 0 | LS | \$55,000.00 | \$72,888.72 | \$ - |
| D. | Aquaculture Wastewater | | | | | |
| D1 | Effluent Treatment | | | | | \$2,054,695 |
| | Clarifier-40ft | | | | | |
| | Clarifier Concrete | 211 | CY | \$ 1,500 | - | \$ 474,750 |

| | Clarifer Excavation | 898 | CY | \$ 50 | - | \$ 67,350 |
|----|--------------------------------------|-----|----|-----------------|-----------------|-----------------|
| | Clarifier Equipment | 1 | LS | \$ 108,000 | \$ 170,780 | \$ 256,170 |
| | Clarifier Coatings | 1 | LS | \$ 12,000 | \$ 18,976 | \$ 28,463 |
| | Finger Weirs | 1 | LS | \$ 6,000 | \$ 9,488 | \$ 14,232 |
| | Duplex Pump Station | 1 | LS | \$ 18,000 | \$ 28,463 | \$ 42,695 |
| | 3" Sch 80 PVC Pipe | 100 | LF | \$ 36 | \$ 57 | \$ 8,539 |
| | 4" Sch 80 PVC Pipe | 250 | LF | \$ 60 | \$ 95 | \$ 35,579 |
| | 3" Plug Valves | 2 | EA | \$ 3,000 | \$ 4,744 | \$ 14,232 |
| | 3" Swing Check Valves | 2 | EA | \$ 2,040 | \$ 3,226 | \$ 9,678 |
| | Telescoping Valves | 2 | EA | \$ 1,140 | \$ 1,803 | \$ 5,408 |
| | 6 ft precast manhole 6 ft deep | 2 | EA | \$ 9,000 | \$ 14,232 | \$ 42,695 |
| | 4ft Precast Manhole 4 ft deep | 1 | EA | \$ 5,040 | \$ 7,970 | \$ 11,955 |
| | Clarifier Equipment Install | 1 | LS | \$ 21,600 | \$ 34,156 | \$ 51,234 |
| | Sludge Storage-25ft | | | | | |
| | Sudge Storage Concrete | 121 | CY | \$ 1,500 | - | \$ 272,250 |
| | Sludge Storage Exavation | 725 | CY | \$ 50 | - | \$ 54,375 |
| | Sludge Mixing Pump | 1 | LS | \$ 10,000 | \$ 15,813 | \$ 23,719 |
| | Sludge Mixing Nozzles | 1 | LS | \$ 35,000 | \$ 55,345 | \$ 83,018 |
| | 4" Sch 80 PVC Pipe | 300 | LF | \$ 50 | \$ 79 | \$ 35,579 |
| | Telescoping Valves | 1 | EA | \$ 950 | \$ 1,502 | \$ 2,253 |
| | 3" Plug Valves | 1 | EA | \$ 2,500 | \$ 3,953 | \$ 5,930 |
| | 3" Swing Check Valves | 1 | EA | \$ 1,700 | \$ 2,688 | \$ 4,032 |
| | Air Release Valve | 2 | EA | \$ 450 | \$ 712 | \$ 2,135 |
| | Sludge Mix & Transfer System Install | 1 | LS | \$ 13,210 | \$ 20,889 | \$ 31,333 |
| | WW Sitework | 1 | LS | \$ 40,000 | \$ 53,010 | \$ 79,515 |
| | Electrical Power and Lighting | 1 | LS | \$ 200,000 | \$ 265,050 | \$ 397,575 |
| D2 | Effluent Monitoring | | | | | \$64,605.91 |
| 02 | Automated Flow Measurement Equipment | 1 | LS | 25,000.00 | \$ 33,131.24 | \$ 49,697 |
| | Portable Composite Sampler | 1 | LS | \$5,000.00 | 6,626.25 | \$ 9,939 |
| | Electrical | 1 | LS | \$2,500.00 | 3,313.12 | \$ 4,970 |
| | | | | | | |
| D3 | Effluent Pumping | | | | | \$1,665,175.45 |
| | WW Piping line | 800 | LF | \$ 85 | \$ 113 | \$ 135,175 |
| | Milford Pump Station | 1 | LS | \$ 1,020,000 | - | \$ 1,530,000 |
| | | | | | | |
| | | | | | | |

| Ε. | Electrical and HVAC | | | | | |
|----|---|-------|----|--------------|------------------|---------------|
| E1 | Electrical Service | | | | | \$300,000.00 |
| | New 480V utility service | 1 | LS | \$ 100,000 | - | \$ 150,000 |
| | New 480V distribution | 1000 | LF | \$ 100 | - | \$ 150,000 |
| E2 | Emergency Power | | | | | \$455,223.21 |
| | Emergency Generator: 100-200kW | 1 | LS | \$200,000.00 | \$ 265,049.91 | \$ 397,575 |
| | Automatic Transfer Switch | 1 | LS | \$15,000.00 | \$ 19,878.74 | \$ 29,818 |
| | Fuel Tank | 1 | LS | \$14,000.00 | \$ 18,553.49 | \$ 27,830 |
| E3 | Instrumentation and Alarm System | | | | | \$397,574.86 |
| | Instrumentation, Alarm System & Communication | 1 | LS | \$200,000.00 | \$ 265,049.91 | \$ 397,575 |
| F. | Visitor Education/Interpretation | | | | | |
| F1 | Visitor Center Repairs | | | | | \$288,750.00 |
| | Gut & Renovate | 1,000 | SF | \$100.00 | - | \$ 150,000 |
| | New Displays | 1 | LS | \$50,000.00 | - | \$ 75,000 |
| | Access Improvements | 1 | LS | \$42,500.00 | - | \$ 63,750 |
| | | | | | - | \$ - |
| | - | - | | | | 647 FF6 410 |

\$47,556,418



New Hampshire Fish and Game Department Effluent Treatment Evaluation Milford 1A: New 95% RAS Building

Operation and Maintenance

| Component | HP | Quantity | Total HP | Watts | Hours/day | kW-hrs/year | | | | |
|-------------------------------------|-------|----------|----------|--------|---------------|--------------|--|--|--|--|
| Hatchery Modernization | | | | | | | | | | |
| UV System | | 6 | | 56,000 | 24 | 2,943,360 | | | | |
| Drum Filter | 8.0 | 6.0 | 48.00 | 35,794 | 24 | 313,552 | | | | |
| Recirc. Pumping | 15.0 | 6.0 | 90.00 | 67,113 | 24 | 587,910 | | | | |
| Site Lighting | | 1 | | 15,000 | 12 | 65,700 | | | | |
| Miscellaneous (SCADA, Meters, etc.) | | 1 | | 15,000 | 24 | 131,400 | | | | |
| MBBR-Blower | 15.00 | 6 | 90.00 | 67,113 | 24 | 587,910 | | | | |
| Effluent Treatment | | | | | | | | | | |
| Clarifier Mechanism | 0.75 | 1 | 0.75 | 559 | 24 | 4,899 | | | | |
| Sludge Pump | 20.00 | 1 | 20.00 | 14,914 | 24 | 130,647 | | | | |
| Effluent Pumping | | | | | | 192,000 | | | | |
| | | | | | | | | | | |
| | | | | | | | | | | |
| | | | | | kW-hrs/year = | 4,957,377 | | | | |
| | | | | | \$/kW-hrs = | \$0.12 | | | | |
| | | | | | | | | | | |
| | | | | | | \$594,885.28 | | | | |
| | | | | | | | | | | |

| Estimated Annual Replacement Costs | | | | | | Annual Cost | | | |
|---|------------------|---------------------|----------------|-------------------|--------------|--------------|--|--|--|
| Annual Equipment Replacement | • | | • | • | | \$952,000.00 | | | |
| Estimated Annual Labor Costs | Days per Week | Hours per day | Personnel | Rate | OH/Fringe | Annual Cost | | | |
| Additional Daily Operator Attention | 5 | 8 | 0 | \$ 25.00 | \$ 15.00 | \$0 | | | |
| Chemicals | Use (gpd) | Annual Use (gal) | Cost (\$/gal) | event per year | | Annual Cost | | | |
| O2 Usage - Tank refill | | 6000 | 0.6 | 12 | | \$43,200.00 | | | |
| | | | | | | | | | |
| | | Estima | ted Annual Lat | por and Repla | cement Costs | \$952,000 | | | |
| Estimated Annual Electricity and Chemical Usage Costs | | | | | | | | | |
| | | | | | TOTAL | \$1,591,000 | | | |

| | | | | | <u>Ne</u> | Effluent Milford 1A | e Fish and G Treatment E : New 95% R Cycle Cost Ar | valuation AS Building | <u>nent</u> | | | | | | | | | | | |
|---|------------------------------|-------------|-------------|-------------|-------------|------------------------|---|--------------------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|-------------|
| | 0 | 1 | 2 | 3 | 4 | 5 | 6 | 7 | 8 | 9 | 10 | | | 13 | | 15 | | 17 | 18 | 19 |
| O&M Total | 2023 | 2024 | 2025 | 2026 | 2027 | 2028 | 2029 | 2030 | 2031 | 2032 | 2033 | 2034 | 2035 | 2036 | 2037 | 2038 | 2039 | 2040 | 2041 | 2042 |
| Power and Chemical cost (6%/yr 2023-2026, 3%/yr 2027-2042 escalation) | \$1,591,000 | \$1 686 460 | \$1,787,648 | \$1 894 906 | \$1.951.754 | \$2.010.306 | \$2 070 615 | \$2.132.734 | \$2,196,716 | \$2,262,617 | \$2 330 496 | \$2 400 411 | \$2,472,423 | \$2 546 596 | \$2,622,994 | \$2.701.684 | \$2.782.734 | \$2.866.216 | \$2,952,203 | \$3,040,769 |
| R&R Maintenance cost (6%/yr 2023-2026, 4%/yr 2027-2042 escalation) | \$329,010 | . , , | | \$391,856 | \$407,530 | \$423,832 | \$440,785 | . , . , . | . , , | \$495,823 | | | . , , | \$580,043 | \$603,245 | \$627,374 | \$652,469 | \$678,568 | \$705,711 | |
| Total O&M Cost | \$1,920,010 | \$2,035,211 | \$2,157,323 | \$2,286,763 | \$2,359,284 | \$2,434,138 | \$2,511,400 | \$2,591,150 | \$2,673,469 | \$2,758,440 | \$2,846,152 | \$2,936,693 | \$3,030,157 | \$3,126,639 | \$3,226,238 | \$3,329,058 | \$3,435,203 | \$3,544,784 | \$3,657,913 | \$3,774,708 |
| Average Annual O&M Cost over 20 years (\$/yr) \$2,831,737 | | | | | | | | | | | | | | | | | | | | |
| Average Annual O&M Cost over 10 years (\$/yr) \$2,372,719 | | | | | | | | | | | | | | | | | | | | |
| Capital Cost Equipment Cost | \$51,369,000 \$10,967,000 | | | | | | | | | | | | | | | | | | | |
| Net Present Value (at 5% discount rate) | | | | | | | | | | | | | | | | | | | | |
| 20 Year Net Present Value \$84,813,145 | | | | | | | | | | | | | | | | | | | | |
| 10 Year Net Present Value \$69,409,000 Annual Cost | | | | | | | | | | | | | | | | | | | | |

Average Annual Cost (Debt Service + O&M, 20 year basis)\$6,953,718Average Annual Cost (Debt Service + O&M, 10 year basis)\$9,025,239

| New Hampton Summary Opinions | s of Probable Cost | |
|---|-----------------------------------|----------------|
| | | |
| ITEM | DRAWING | ROUNDED |
| | I.D. # | TOTAL COST |
| | | |
| New Facility Features | | |
| Hatchery Supply | A1 | \$368,000 |
| Intake Building | B1 | \$1,589,000 |
| Hatchery Building | B2 | \$4,230,000 |
| Rearing Building | B3 | \$33,077,000 |
| Rehabilitation of other buildings on site | B4 | \$264,000 |
| Raceway Rehabilitation | B5 | \$2,052,000 |
| Site Work | C1 | \$507,000 |
| Domestic Water | C2 | \$50,000 |
| Domestic Wastewater | C3 | \$100,000 |
| Disinfection Station | C4 | \$45,000 |
| Paved Access to State or Local Highways | C5 | \$378,000 |
| Effluent Treatment | D1 | \$2,055,000 |
| Effluent Monitoring | D2 | \$70,000 |
| Effluent Pumping | D3 | \$2,071,000 |
| Electrical Service | E1 | \$300,000 |
| Emergency Power | E2 | \$456,000 |
| Instrumentation and Alarm System | E3 | \$398,000 |
| Visitor Center Repairs | F1 | \$600,000 |
| Subtotal | | \$48,610,000 |
| Escalation to Midpoint of Const. @ 5%/yr for 5 years | | \$2,431,000 |
| 3% market volatility adjustment | | \$1,458,300 |
| Total Cost | | \$52,499,000 |
| ^a Rounded Total Costs (or Costs needed to Budget) include 50% Class 4 AA | CE expected accuracy range). | |
| Costs do NOT include: Design Reimbursables (Variable); State Agency Adm | inistrative Fee; and land acquisi | tion or lease. |

Client: NHFGD Project:Powder Mill Fish Hatchery Study Project No.: 10331124

DRUM FILTERS

DRUM SUMP

Date: 3/15/2023 Estimator: Checked By: Check Date: Revised: -



225,000

112,500

\$

\$

-

-

| Detailed Opinions of Probable Cost | | | | | | | | | | |
|------------------------------------|--------------|---------------|------------------|----------------------------|-------------------------|--|--|--|--|--|
| New Hampton 1.B | NO. UNITS | UNIT MEAS. | COST PER UNIT | Escalation cost to 2022 | TOTAL COST 50% CONT. | | | | | |
| | UNITS | WEAS. | UNIT | 10 2022 | 30 % CONT. | | | | | |

| A. | Aquaculture Water Supply | | | | | | |
|----|--|-----|----|-----|-----------|---------------|-----------------|
| A1 | Hatchery Supply | | | | | | \$ 367,966 |
| | Water Supply Piping and Accessories | 150 | LF | \$ | 85 | \$ 113 | \$ 25,345 |
| | Rehab of Major Spring Conc Structures Above Spring Pond | 1 | LS | \$ | 3,000 | - | \$ 4,500 |
| | Repairs/tiedowns at Raceway B and C inlet piping supports | 1 | LS | \$ | 5,000 | - | \$ 7,500 |
| | Minor Springs Replace Inlet Box at inlet pool and cover inlet pool | 1 | LS | \$ | 15,000 | - | \$ 22,500 |
| | Well Water Supply System, 1,000 gpm (1 wells/ 1 back up) | 1 | EA | \$1 | 00,000.00 | \$ 132,525 | \$ 198,787 |
| | Hydrogeological Testing Program & Report | 1 | LS | \$ | 55,000.00 | \$ 72,889 | \$ 109,333 |
| A2 | Oxygenation System | | | | | | \$ 1,014,051 |
| | Bulk LOX Tank, Vaporizer, Port. Tank Fill System | 2 | LS | \$ | 150,000 | \$ 198,787 | \$ 596,362 |
| | Fence | 200 | LF | \$ | 20 | \$ 27 | \$ 7,951 |
| | Concrete Pad & Bollards | 2 | LS | \$ | 11,000 | \$ 14,578 | \$ 43,733 |
| | Buried Copper Oxygen Distribution to Units | 2 | LS | \$ | 60,000 | \$ 79,515 | \$ 238,545 |
| | Oxygen Electrical | 2 | LS | \$ | 5,000 | \$ 6,626 | \$ 19,879 |
| | Oxygen Dissolving for Rearing Units- LHO | 24 | EA | \$ | 2,500 | \$ 2,906 | \$ 104,599 |
| | Oxygen Flow Meter Station (raceways) | 2 | LS | \$ | 750 | \$ 994 | \$ 2,982 |
| | | | | | | | |
| В. | Buildings and Rearing Units | | | | | | |
| B1 | Intake Building | | | | | | \$ 1,588,544 |
| | New Intake Building Cold Brook and Wells | 400 | SF | \$ | 165 | \$ 218 | \$ 131,017 |
| | Drumfilter | | | | | | |

EA

LS

\$

\$

75,000

75,000

2

1

| | PIPING SYSTEMS (INFLOW, DRAINS) | 1 | LS | \$ 500,000 | - | \$ 750,000 |
|------------|--|--------|----|---------------|---------------|------------------|
| | PRIMARY POWER | 1 | LS | \$ 75,000 | - | \$ 112,500 |
| | UV System | | | | | |
| | UV Channel and Lamp Package | 2 | EA | \$ 50,000 | - | \$ 150,000 |
| | UV Electrical | 1 | LS | \$ 8,000 | \$ 10,602 | \$ 15,903 |
| | UV Plumbing | 1 | LS | \$ 11,000 | \$ 14,578 | \$ 21,867 |
| | Electrical Power and Lighting | 1 | LS | \$ 20,000 | \$ 26,505 | \$ 39,757 |
| | ALARMS/CONTROLS/MONITORING/PANEL/HMI | 1 | LS | \$ 20,000 | - | \$ 30,000 |
| B2 | Hatchery Building | | | | | \$4,229,021.87 |
| | New Hatchery Building - Office Space | 3700 | SF | \$165.00 | \$ 218 | \$ 1,211,910 |
| | POWER AND LIGHTING | 3700 | SF | \$ 50 | \$103.40 | \$ 573,847 |
| | HVAC | 1 | LS | \$ 100,000 | \$206,791.77 | \$ 310,188 |
| | EQUIPMENT | | | | | |
| | FEEDERS (SWEENEY MDL AF7 W/CONTROLLER & SUPPORT) | 72 | EA | \$ 600 | \$1,240.75 | \$ 134,001 |
| | FG TROUGHS (12'x2'x2') | 42 | EA | \$ 2,500 | \$5,169.79 | \$ 325,697 |
| | INCUBATION ROOM 30 HEATH STACKS | 12 | EA | \$ 2,500 | \$5,169.79 | \$ 93,056 |
| | INCUBATION HEAD TROUGHS AND CONTROLS | 2 | LS | \$ 15,000 | \$31,018.77 | \$ 93,056 |
| | CHILLER SYSTEM AND CONTROLS | 1 | LS | \$ 250,000 | \$516,979.42 | \$ 775,469 |
| | FORMALIN ROOM | 1 | LS | \$ 50,000 | \$103,395.88 | \$ 155,094 |
| | BOOT LOCKER ROOM, W/D, BENCHES | 1 | LS | \$ 50,000 | \$103,395.88 | \$ 155,094 |
| | WATER QUALITY ROOM EQUIP ALLOWANCE | 1 | LS | \$ 75,000 | \$155,093.83 | \$ 232,641 |
| | Hatchery Building Aeration/Degassing System | | | | | |
| | Primary Headtank & Aeration/Degassing System | 1 | EA | \$ 85,000 | \$ 112,646 | \$ 168,969 |
| | | | | | | |
| B 3 | Rearing Building | | | | | \$33,076,818.18 |
| | New Rearing Building (526x140) | 73,640 | SF | \$ 165 | \$ 218 | \$ 24,120,276 |
| | ALARMS/CONTROLS/MONITORING/PANEL/HMI | 1 | LS | \$ 50,000 | - | \$ 75,000 |
| | VFD W/CIRCUIT BREAKER AND FULL CONTACTOR SET | 2 | EA | \$ 25,000 | - | \$ 75,000 |
| | PANEL/RACK/WIRING/CONDUITS/FEEDER | 2 | EA | \$ 55,000 | - | \$ 165,000 |
| | 12" FLOW METER | 2 | EA | \$ 18,000 | - | \$ 54,000 |
| | EQUIPMENT | | | | | |
| | 20' dia. SS Culture Tank with Foundation & Floor | 20 | EA | \$ 35,000 | - | \$ 1,050,000 |
| | 40' dia. SS Culture Tank with Foundation & Floor | 16 | EA | \$ 50,000 | - | \$ 1,200,000 |
| | Drumfilter | | | | | |

| | DRUM FILTERS | 6 | EA | \$ | 85,000 | - | \$ 765,000 |
|----|--|-----|----|-----|------------|--------------|-----------------|
| | DRUM SUMP | 1 | LS | \$ | 75,000 | - | \$ 112,500 |
| | PRIMARY POWER | 1 | LS | \$ | 75,000 | - | \$ 112,500 |
| | UV System | | | | | | · · · · · |
| | UV Channel and Lamp Package | 6 | EA | \$ | 125,000 | - | \$ 1,125,000 |
| | UV Electrical | 1 | LS | \$ | 8,000 | \$ 10,602 | \$ 15,903 |
| | UV Plumbing | 1 | LS | \$ | 11,000 | \$ 14,578 | \$ 21,867 |
| | Recirculation | | | | | | |
| | PIPING SYSTEMS (INFLOW, PRAS, DRAINS) | 1 | LS | \$ | 500,000 | - | \$ 750,000 |
| | Lift Pump | 6 | EA | \$ | 80,000 | - | \$ 720,000 |
| | 4ft Precast Manhole 4 ft deep | 6 | EA | \$ | 4,200 | \$6,641.45 | \$ 59,773 |
| | Biofilter System | | | | | | |
| | MBBR | 6 | EA | \$ | 200,000 | - | \$ 1,800,000 |
| | HVAC | 1 | LS | \$ | 100,000 | - | \$ 150,000 |
| | Electrical Power and Lighting | 1 | LS | \$ | 200,000 | - | \$ 300,000 |
| | GAS MANAGEMENT TOWER CO2 STRIPPER/LHO | 6 | EA | \$ | 45,000 | - | \$ 405,000 |
| B4 | Rehabilitation of other buildings on site | | | | | | \$ 264,000 |
| | Garage Renovations | 1 | LS | \$ | 119,500 | | \$ 119,500 |
| | Wood Working Shop Renovations | 1 | LS | \$ | 33,500 | | \$ 33,500 |
| | C-Station Office Renovations | 1 | LS | \$ | 81,000 | | \$ 81,000 |
| | Demo (Boat Shed, Shavings Shed, Timber Shed, Tools Shed) | 1 | LS | \$ | 30,000 | | \$ 30,000 |
| B5 | Raceway Rehabilitation | | | | | | \$ 2,051,250 |
| | Concrete rehab of Raceway B series | 1 | LS | \$ | 240,000 | - | \$ 360,000 |
| | Process rehab of Raceway B series | 1 | LS | \$ | 60,000 | - | \$ 90,000 |
| | Concrete rehab of Raceway C series | 1 | LS | \$ | 900,000 | - | \$ 1,350,000 |
| | Process Rehab of Raceway C series | 1 | LS | \$ | 7,500 | - | \$ 11,250 |
| | Demolish and fill in Upper Raceways | 1 | LS | \$ | 60,000 | - | \$ 90,000 |
| | Baffle Allowance | 1 | LS | \$ | 100,000 | - | \$ 150,000 |
| C. | Site | | | | | | |
| C1 | Site Work | | | | | | \$506,907.95 |
| | Site Clearing | 2.5 | AC | | \$2,000.00 | \$2,650.50 | \$ 9,939 |
| | General Earthwork for Hatchery Complex | 0 | LS | \$ | 75,000.00 | \$99,393.71 | \$ - |
| | General Sitework | 1 | LS | \$2 | 50,000.00 | \$331,312.38 | \$ 496,969 |
| | Erosion Control | 0 | AC | | \$2,500.00 | \$3,313.12 | \$ - |
| | Seeding | 0 | AC | | \$1,250.00 | \$1,656.56 | \$ - |
| | Landscaping | 0 | AC | | \$3,000.00 | \$3,975.75 | \$ - |

| | Natural Gas Connection and Distribution (if available) | 0 | LS | \$35,000.00 | \$46,383.73 | \$ - |
|----|--|-----|----|--------------|---------------------------------------|---------------|
| | Stormwater Management System | 0.0 | AC | \$3,500.00 | · · · · · · · · · · · · · · · · · · · | _ |
| | | | | | | |
| C2 | Domestic Water | | | \$150.00 | | \$49,696.86 |
| | Domestic Water Supply | 1 | LS | \$25,000.00 | \$33,131.24 | \$ 49,697 |
| | | | | | | |
| C3 | Domestic Wastewater | | | \$100,000.00 | | \$99,393.71 |
| | Domestic Wastewater System | 1 | LS | \$50,000.00 | \$66,262.48 | \$ 99,394 |
| | | | | | | |
| C4 | Disinfection Station | | | | | \$45,000.00 |
| | Truck Disinfection Station | 1 | LS | \$30,000.00 | - | \$ 45,000 |
| | Roadway Aggregate | 0 | SY | \$30.00 | - | \$ - |
| | Electrical | 0 | LS | \$5,000.00 | - | \$ - |
| | Detention Tank | 0 | LS | \$10,000.00 | - | \$ - |
| C5 | Paved Access to State or Local Highways | 0 | | \$0.00 | | \$377,696.12 |
| | Bituminous Paved Road | 1 | LS | \$190,000.00 | \$251,797.41 | \$ 377,696 |
| | Gravel Roads | 0 | LS | \$55,000.00 | \$72,888.72 | \$ - |

| D. | Aquaculture Wastewater | | | | | |
|----|--------------------------------|-----|----|---------------|---------------|---------------|
| D1 | Effluent Treatment | | | | | \$2,054,695 |
| | | | | | | |
| | Clarifier-40ft | | | | | |
| | Clarifier Concrete | 211 | CY | \$ 1,500 | - | \$ 474,750 |
| | Clarifer Excavation | 898 | CY | \$ 50 | - | \$ 67,350 |
| | Clarifier Equipment | 1 | LS | \$ 108,000 | \$ 170,780 | \$ 256,170 |
| | Clarifier Coatings | 1 | LS | \$ 12,000 | \$ 18,976 | \$ 28,463 |
| | Finger Weirs | 1 | LS | \$ 6,000 | \$ 9,488 | \$ 14,232 |
| | Duplex Pump Station | 1 | LS | \$ 18,000 | \$ 28,463 | \$ 42,695 |
| | 3" Sch 80 PVC Pipe | 100 | LF | \$ 36 | \$ 57 | \$ 8,539 |
| | 4" Sch 80 PVC Pipe | 250 | LF | \$ 60 | \$ 95 | \$ 35,579 |
| | 3" Plug Valves | 2 | EA | \$ 3,000 | \$ 4,744 | \$ 14,232 |
| | 3" Swing Check Valves | 2 | EA | \$ 2,040 | \$ 3,226 | \$ 9,678 |
| | Telescoping Valves | 2 | EA | \$ 1,140 | \$ 1,803 | \$ 5,408 |
| | 6 ft precast manhole 6 ft deep | 2 | EA | \$ 9,000 | \$ 14,232 | \$ 42,695 |
| | 4ft Precast Manhole 4 ft deep | 1 | EA | \$ 5,040 | \$ 7,970 | \$ 11,955 |
| | Clarifier Equipment Install | 1 | LS | \$ 21,600 | \$ 34,156 | \$ 51,234 |
| | | | | | | |

| | Sludge Storage-25ft | | | | | | | |
|----|--|------|----|----------|-------------|------------------|----------|---------------------------|
| | Sudge Storage Concrete | 121 | CY | \$ | 1,500 | - | \$ | 272,250 |
| | Sludge Storage Exavation | 725 | CY | \$ | 50 | - | \$ | 54,375 |
| | Sludge Mixing Pump | 1 | LS | \$ | 10,000 | \$ 15,813 | \$ | 23,719 |
| | Sludge Mixing Nozzles | 1 | LS | \$ | 35,000 | \$ 55,345 | \$ | 83,018 |
| | 4" Sch 80 PVC Pipe | 300 | LF | \$ | 50 | \$ 79 | \$ | 35,579 |
| | Telescoping Valves | 1 | EA | \$ | 950 | \$ 1,502 | \$ | 2,253 |
| | 3" Plug Valves | 1 | EA | \$ | 2,500 | \$ 3,953 | \$ | 5,930 |
| | 3" Swing Check Valves | 1 | EA | \$ | 1,700 | \$ 2,688 | \$ | 4,032 |
| | Air Release Valve | 2 | EA | \$ | 450 | \$ 712 | \$ | 2,135 |
| | Sludge Mix & Transfer System Install | 1 | LS | \$ | 13,210 | \$ 20,889 | \$ | 31,333 |
| | WW Sitework | 1 | LS | \$ | 40,000 | \$ 53,010 | \$ | 79,515 |
| | Electrical Power and Lighting | 1 | LS | \$ | 200,000 | \$ 265,050 | \$ | 397,575 |
| D2 | Effluent Monitoring | | | | | | \$ | 69,576 |
| | Automated Flow Measurement Equipment | 1 | LS | \$ | 25,000 | \$ 33,131 | \$ | 49,697 |
| | Portable Composite Sampler | 1 | LS | \$ | 5,000 | \$ 6,626 | \$ | 9,939 |
| | Electrical | 1 | LS | \$ | 5,000 | \$ 6,626 | \$ | 9,939 |
| D3 | Effluent Pumping | | | | | | \$ | 2,070,702 |
| | WW Piping line | 3200 | LF | \$ | 85 | \$ 113 | \$ | 540,702 |
| | New Hampton Pump Station | 1 | LS | \$ | 1,020,000 | - | \$ | 1,530,000 |
| | | | | | | | | |
| E. | Utilities (Electrical, HVAC and Instrumentation) | | | | | | ۴ | 200.000 |
| E1 | Electrical Service New 480V utility service | 1 | LS | 6 | 100,000 | | \$ ¢ | 300,000 150,000 |
| | New 480V distribution | 1000 | LS | \$ \$ | 100,000 | - | \$ \$ | 150,000 |
| | | 1000 | | Þ | 100 | - | φ | 150,000 |
| E2 | Emergency Power | | | | | | \$ | 455,223 |
| | Emergency Generator: 100-200kW | 1 | LS | \$2 | 200,000.00 | \$ 265,049.91 | \$ | 397,575 |
| | Automatic Transfer Switch | 1 | LS | \$ | \$15,000.00 | \$ 19,878.74 | \$ | 29,818 |
| | Fuel Tank | 1 | LS | 9 | \$14,000.00 | \$ 18,553.49 | \$ | 27,830 |
| E3 | Instrumentation and Alarm System | | | | | | \$ | 397,575 |
| | Instrumentation, Alarm System & Communication | 1 | LS | \$2 | 200,000.00 | \$ 265,049.91 | \$ | 397,575 |
| | | | | | | | | |

| F. | Visitor Education/Interpretation | | | | | |
|----|----------------------------------|-------|----|-------------|---|------------------|
| F1 | Visitor Center Repairs | | | | | \$600,000.00 |
| | New Visitor Center Building | 1,000 | SF | \$350.00 | - | \$ 525,000 |
| | New Displays | 1 | LS | \$50,000.00 | - | \$ 75,000 |
| | | | | | | \$ - |
| | | | | | | \$ 49,618,116 |



New Hampshire Fish and Game Department

Effluent Treatment Evaluation

New Hampton 1B: New 95% RAS Building

Operation and Maintenance

| Component | HP | Quantity | Total HP | Watts | Hours/day | kW-hrs/year |
|-------------------------------------|------------------|---------------------|---------------|--------------------|---------------|--------------|
| Hatchery Modernization | | | | | | |
| UV System | | 8 | | 56,000 | 24 | 3,924,480 |
| Drum Filter | 8.0 | 8.0 | 64.00 | 47,725 | 24 | 418,069 |
| Recirc. Pumping | 15.0 | 6.0 | 90.00 | 67,113 | 24 | 587,910 |
| Site Lighting | | 1 | | 15,000 | 12 | 65,700 |
| Miscellaneous (SCADA, Meters, etc.) | | 1 | | 15,000 | 24 | 131,400 |
| MBBR-Blower | 15.00 | 6 | 90.00 | 67,113 | 24 | 587,910 |
| Effluent Treatment | | | | | | |
| Clarifier Mechanism | 0.75 | 1 | 0.75 | 559 | 24 | 4,899 |
| Sludge Pump | 20.00 | 1 | 20.00 | 14,914 | 24 | 130,647 |
| Effluent Pumping | | | | | | 192,000 |
| | | | | | kW-hrs/year = | 6,043,015 |
| | | | | | \$/kW-hrs = | \$0.12 |
| | | | | | | Annual Cost |
| | | | | | | \$725,161.75 |
| Estimated Annual Replacement Costs | | | | | | Annual Cost |
| Annual Equipment Replacement | • | | | - | | \$789,000.00 |
| Estimated Annual Labor Costs | Days per Week | Hours per day | Personnel | Rate | OH/Fringe | Annual Cost |
| Daily Operator Attention | 5 | 8 | 0 | \$ 25.00 | \$ 15.00 | \$0 |
| Chemicals | Use (gpd) | Annual Use (gal) | Cost (\$/gal) | Replacemen t/yr | | Annual Cost |
| O2 Usage - Tank refill | | 6000 | 0.6 | 12 | | \$43,200.00 |

| Estimated Annual Labor and Replacement Costs | \$789,000 |
|---|-------------|
| Estimated Annual Electricity and Chemical Usage Costs | \$768,362 |
| TOTAL | \$1,558,000 |

| <u>New Hampshire Fish and Game Department</u> <u>Effluent Treatment Evaluation</u> <u>New Hampton 1B: New 95% RAS Building and Rehab Raceways</u> Life Cycle Cost Analysis | | | | | | | | | | | | | | | | | | | | | |
|---|-----------------------------|-----------------------------|------------------------|------------------------|------------------------|------------------------|------------------------|------------------------|-------------|--------------------------|--------------------------|--------------------------|--------------------------|-------------|--------------------------|--------------------------|--------------------------|-------------|--------------------------|--------------------------|-------------|
| _ | | 0 | 1 | 2 | 3 | 4 | 5 | 6 | 7 | 8 | 9 | | 11 | 12 | 13 | 14 | | 16 | 17 | 18 | 19 |
| 0&M | otal | 2023 | 2024 | 2025 | 2026 | 2027 | 2028 | 2029 | 2030 | 2031 | 2032 | 2033 | 2034 | 2035 | 2036 | 2037 | 2038 | 2039 | 2040 | 2041 | 2042 |
| Power and Chemical cost (6%/yr 2023-2026, 3%/yr 2027-2042 escalation) R&R Maintenance cost (6%/yr 2023-2026, 4%/yr 2027-2042 escalation) | | \$768,362 \$299,850 | \$814,463 \$317,841 | \$863,331 \$336,911 | \$915,131 \$357,126 | \$942,585 \$371,411 | \$970,863 \$386,268 | \$999,989 \$401,718 | | \$1,060,888 \$434,499 | \$1,092,714 \$451,879 | \$1,125,496 \$469,954 | \$1,159,261 \$488,752 | | \$1,229,860 \$528,634 | \$1,266,756 \$549,779 | \$1,304,758 \$571,770 | . , , | \$1,384,218 \$618,427 | \$1,425,744 \$643,164 | |
| Total O&M Cost | | \$1,068,212 | \$1,132,304 | \$1,200,243 | \$1,272,257 | \$1,313,996 | \$1,357,130 | \$1,401,707 | \$1,447,775 | \$1,495,386 | \$1,544,593 | \$1,595,450 | \$1,648,013 | \$1,702,340 | \$1,758,494 | \$1,816,535 | \$1,876,529 | \$1,938,542 | \$2,002,645 | \$2,068,909 | \$2,137,407 |
| | ,588,923 ,323,360 | | | | | | | | | | | | | | | | | | | | |
| Capital Cost Equipment Cost | | \$52,499,000 \$9,995,000 | | | | | | | | | | | | | | | | | | | |
| 10 Year Net Present Value \$62, Annual Cost | ,234,523 ,557,000 | | | | | | | | | | | | | | | | | | | | |

 Average Annual Cost (Debt Service + O&M, 20 year basis)
 \$5,801,579

 Average Annual Cost (Debt Service + O&M, 10 year basis)
 \$8,122,221

Twin New Facility Summary Opinions of Probable Cost

| ITEM | DRAWING | ROUNDED |
|--|---------|-------------------------|
| | I.D. # | CONST COST ^a |
| | | |
| New Facility Features | | |
| Pump House & Raceway Rehabiltaiton | B1 | \$518,000 |
| Rehabilitation of Hatch House | B2 | \$124,000 |
| Rehabilitation of Storage Garage | B3 | \$442,000 |
| Rehabilitation of Garage/Office Building | B4 | \$75,000 |
| Subtotal | | \$1,159,000 |
| Escalation to Midpoint of Const. @ 5%/yr for 5 years | | \$58,000 |
| 3% market volatility adjustment | | \$34,770 |
| Total Cost | | \$1,252,000 |

^a Rounded Total Costs (or Costs needed to Budget) include 50% expected accuracy range).

Costs do NOT include: Design Reimbursables (Variable); State Agency Administrative Fee; and land acquisition or lease.

Client: NHFGD Project:Powder Mill Fish Hatchery Study Project No.: 10331124

Date: 3/15/2023 Estimator: Checked By: Check Date: Revised: -



| Detailed Opinions of Probable Cost | | | | | | | | | | | | |
|------------------------------------|-------|-------|----------|-----------------|------------|--|--|--|--|--|--|--|
| Turin | NO. | UNIT | COST PER | Escalation cost | TOTAL COST | | | | | | | |
| l win | UNITS | MEAS. | UNIT | to 2023 | 50% CONT. | | | | | | | |

| A. | Aquaculture Water Supply | | | | | |
|------------|--|-------|----|---------------|---|---------------|
| | N/A | | | | | |
| | | | | | | |
| В. | Buildings and Rearing Units | | | | | |
| B1 | Pump House & Raceway Rehabiltaiton | | | | | \$517,875 |
| | Tension Fabric Over Raceways | 5,000 | SF | \$ 50 | - | \$ 375,000 |
| | Concrete Rehab (Cleaning/Debris) | 1 | LS | \$ 50,000 | - | \$ 75,000 |
| | Concrete Rehab (Replacement) | 1 | LS | \$ 37,250 | - | \$ 55,875 |
| | Well House Slab Rehab | 1 | LS | \$ 8,000 | - | \$ 12,000 |
| B2 | Rehabilitation of Hatch House | | | | | \$ 123,750 |
| | Replace Furnace | 1 | LS | \$ 20,000 | - | \$ 30,000 |
| | Replace Windows | 5 | EA | \$ 1,500 | - | \$ 11,250 |
| | Electrical and Lighting Upgrades | 1 | LS | \$ 55,000 | - | \$ 82,500 |
| B 3 | Rehabilitation of Storage Garage | | | | | \$ 441,300 |
| | Storage Garage Renovations | 1 | LS | \$ 239,000 | - | \$ 358,500 |
| | Storage Garage - Window Replacement | 2 | EA | \$ 1,500 | - | \$ 4,500 |
| | Roof Replacement (with new insulation) | 2,900 | SF | \$ 18 | - | \$ 78,300 |

| B4 | Rehabilitation of Garage/Office Building | | | | | \$ 75,000 |
|----|--|---|----|--------------|---|--------------|
| | Replace HVAC system | 1 | LS | \$ 40,000 | - | \$ 60,000 |
| | Replace Hot Water Heater | 1 | LS | \$ 10,000 | - | \$ 15,000 |
| | | | | | | |
| C. | Site | | | | | |
| | N/A | | | | | |
| | | | | | | |
| D. | Aquaculture Wastewater | | | | | |
| | N/A | | | | | |
| | | | | | | |
| Е. | Electrical and HVAC | | | | | |
| | N/A | | | | | |
| | | | | | | |
| F. | Visitor Education/Interpretation | | | | | |
| | N/A | | | | | |
| | | | | | | |
| | | | | | | \$1,157,925 |

| ITEM | DRAWING | ROUNDED |
|--|---------|-------------------------|
| | I.D. # | CONST COST ^a |
| New Facility Features | | |
| Pump House Rehabiliation | B1 | \$81,000 |
| Block Pond Rehabilitaiton | B2 | \$10,000 |
| Show Pond and PR Pond Rehabilitaiton | B3 | \$555,000 |
| Rehabilitation of Garage and Storage Area | B4 | \$827,000 |
| Visitor Center Repairs | F1 | \$662,000 |
| Subtotal | | \$2,135,000 |
| Escalation to Midpoint of Const. @ 5%/yr for 5 years | | \$107,000 |
| 3% market volatility adjustment | | \$64,050 |
| Total Cost | | \$2,306,000 |

Costs do NOT include: Design Reimbursables (Variable); State Agency Administrative Fee; and land acquisition or lease.

Client: NHFGD Project:Powder Mill Fish Hatchery Study Project No.: 10331124

Date: 3/15/2023 Estimator: Checked By: Check Date: Revised: -



| Detailed Opinions of Probable Cost | | | | | | | | | | | | |
|------------------------------------|-------|-------|----------|-----------------|------------|--|--|--|--|--|--|--|
| 201 | NO. | UNIT | COST PER | Escalation cost | TOTAL COST | | | | | | | |
| Warren | UNITS | MEAS. | UNIT | to 2023 | 50% CONT. | | | | | | | |

| A. | Aquaculture Water Supply | | | | | |
|------------|---|-----|----|---------------|---|---------------|
| | N/A | | | | | |
| | | | | | | |
| В. | Buildings and Rearing Units | | | | | |
| B1 | Pump House Rehabiliation | | | | | \$81,000 |
| | Heater Replacement (Well # 1, Well # 2, and Well # 3) | 1 | LS | \$ 1,000 | - | \$ 1,500 |
| | Pump 1 Reservoir Maintanace/Cleaning | 1 | LS | \$ 50,000 | - | \$ 75,000 |
| | Investigation, Test Well (Well #2) | 1 | LS | \$ 3,000 | - | \$ 4,500 |
| B2 | Block Pond Rehabilitaiton | | | | | \$9,750 |
| | Concrete Epoxy Sealing (Block Ponds 1,2,3) | 650 | LF | \$ 10 | - | \$ 9,750 |
| | | | | | | |
| B 3 | Show Pond and PR Pond Rehabilitaiton | | | | | \$554,625 |
| | Crack Repair | 1 | LS | \$ 18,750 | - | \$ 28,125 |
| | Handle Replacement | 1 | LS | \$ 1,000 | - | \$ 1,500 |
| | PR Pond Concrete Rehabilitation | 1 | LS | \$ 350,000 | - | \$ 525,000 |
| | | | | | | |

| B4 | Rehabilitation of Garage and Storage Area | | | | | | \$826,500 |
|------------|---|-------|----|----|--------|---|---------------|
| | Replace Window (Warehouse) | 12 | EA | \$ | 1,500 | - | \$ 27,000 |
| | Replace Door (Warehouse) | 2 | EA | \$ | 3,500 | - | \$ 10,500 |
| | Replace Overhead Door (Warehouse) | 2 | LS | \$ | 50,000 | - | \$ 150,000 |
| | Install Railing and Handrails (Warehouse) | 1 | LS | \$ | 1,000 | - | \$ 1,500 |
| | Warehous Renovation | 3000 | SF | \$ | 100 | - | \$ 450,000 |
| | Insulation (Warehouse) | 3000 | SF | \$ | 10 | - | \$ 45,000 |
| | Replace HVAC system (Warehouse) | 1 | LS | \$ | 40,000 | - | \$ 60,000 |
| | Replace Electrical and Lighting | 1 | LS | \$ | 55,000 | - | \$ 82,500 |
| C. | Site | | | • | | | |
| | N/A | | | | | | |
| | | | | | | | |
|) . | Aquaculture Wastewater | | | | | | |
| | NA | | | | | | |
| | Electrical and HVAC | | | | | | |
| | N/A | | | | | | |
| | Visitor Education/Interpretation | | | | | | |
| F1 | Visitor Center Repairs | | | | | | \$661,350 |
| | Roof Replacement | 1,300 | SF | \$ | 18 | - | \$ 35,100 |
| | Painting (Exterior, Doors, Window Trim) | 1 | LS | \$ | 15,000 | - | \$ 22,500 |
| | Replace handware (Stainless Steel) | 1 | LS | \$ | 2,500 | - | \$ 3,750 |
| | New Visitor Center Building | 1,000 | SF | \$ | 350 | - | \$ 525,000 |
| | New Displays | 1 | LS | \$ | 50,000 | | \$ 75,000 |
| | | | | | | | |

\$2,133,225

Appendix E Solids Loading Calculations

Clarifier and Sludge storage tank calculation - Alternative 1

Flow and Solid Data:

| Q Cold Brook and wells | 1694 | gpm |
|------------------------------------|--------|------|
| Drum backwash | 5% | |
| Q WAS first Drum - Cold Brook | 84.7 | gpm |
| Q influent to Youngs and Fosters | 1609.3 | gpm |
| Q Diversion Pond | 2245 | gpm |
| Q WAS first Drum - Diversion Pond | 112.3 | gpm |
| Q influent to West brancg Raceways | 2132.8 | gpm |
| | | |
| Q WAS second Drum | 187.1 | gpm |
| SG | 1.05 | |
| Solids % | 5% | |
| Sludge TSS in clarifier | 50000 | mg/L |
| Cold Brook & wells TSS | 3 | mg/L |
| Diversion Pond | 2 | mg/L |
| Drum TSS capture | 62% | |
| Clarifier removal rate | 60% | |
| Feed to TSS | 30% | |
| Note: lake TSS <2mg/l | | |

Mass Captured from Drum Filters:

| Mass captured from Cold brook drum | 1.892 | lb/day |
|--|-------|--------|
| Mass captured from Riversion pond drum | 1.672 | lb/day |

Estimated sludge Volume:

| Youngs a | nd Fosters Race | ways | | We | st Branch Raceways | | | | | | | |
|-----------|-----------------|---------|------------------------|-------|------------------------|-------------------------|------------------------|---------------------------|----------------------------|--|---------------------------|------------------------------------|
| | | Feed | Mass of feed-generated | Feed | Mass of feed-generated | Second Drum WAS capture | Total WAS to clarifier | Mass removed in clarifier | Mass overflow in Clarifier | Mass of sludge from effluent treatment | Sludge Vol from clarifier | Sludge Vol from effluent treatment |
| Month | Days | lbs | lbs/day | lbs | lbs/day | lbs/day | lb/day | lb/day | lb/day | lb/day | gal/mo | lb/day |
| January | 3 | 1 1,530 | 15 | 624 | 6 | 13 | 1 | 6 1 | 6.595 | 14.516 | 700 | 1028 |
| February | 2 | 8 1,646 | 18 | 672 | 7 | 15 | 1 | 9 1 | 7.585 | 17.022 | 728 | 1089 |
| March | 3 | 1 2,661 | 26 | 757 | 7 | 21 | 2 | 4 1 | 9.629 | 22.198 | 1023 | 1572 |
| April | 3 | 0 2,490 | 25 | 1,310 | 13 | 24 | 2 | 7 1 | 10.849 | 25.289 | 1115 | 1733 |
| May | 3 | 1 2,547 | 25 | 1,258 | 12 | 23 | 2 | 6 1 | 10.557 | 24.550 | 1121 | . 1738 |
| June | 3 | 0 4,564 | 46 | 393 | 4 | 31 | 3 | 4 2 | 13.719 | 32.555 | 1410 | 2231 |
| July | 3 | 1 7,404 | 72 | - | 0 | 44 | 4 | 8 2 | 19.195 | 46.423 | 2039 | 3287 |
| August | 3 | 1 8,658 | 84 | 651 | 6 | 56 | 5 | 9 31 | 23.767 | 58.000 | 2524 | 4106 |
| September | 3 | 0 8,692 | 87 | 1,846 | 18 | 65 | 6 | 9 4: | 27.560 | 67.604 | 2832 | 4632 |
| October | 3 | 1 3,303 | 32 | 2,858 | 28 | 37 | 4 | 1 24 | 16.212 | 38.868 | 1722 | 2752 |
| November | 3 | 0 1,091 | 11 | 860 | 9 | 12 | 1 | 6 | 6.264 | 13.678 | 644 | 937 |
| December | 3 | 1 1,450 | 14 | 576 | 6 | 12 | 1 | 6 | 6.288 | 13.738 | 668 | 973 |
| | | | | | | | | | | Total sludge Vol from Clarifier | 16525 | |
| | | | | | | | | | | Total sludge Vol from EFF treatment | | 26076 |
| | | | | | | | | | | Total Sludge Volume | | 42601 |

Clarifier Estimations:

| Solids Flow | | 384.1 | gpm | | | | |
|-------------|--------|----------------|-----------------------------|--------|---------|-------------|-----------|
| | Clarif | Solids det Avg | Overflow rate Hyd load rate | | | | |
| Diameter | | Depth | Surface Ar | Volu | ume | Goal>60 min | Goal<1000 |
| ft | | ft | ft2 | ft3 | gal | min | gpd/ft2 |
| | 25 | 8 | 490.9 | 3927.0 | 29373.9 | 76.5 | 1126.6 |
| | 15 | 8 | 176.7 | 1413.7 | 10574.6 | 27.5 | 3129.5 |
| | 20 | 8 | 314.2 | 2513.3 | 18799.3 | 48.9 | 1760.4 |
| | 30 | 8 | 706.9 | 5654.9 | 42298.4 | 110.1 | 782.4 |

Sludge Storage tank Estimation:

| | Sludge Storage Tank | | | | | | | | | |
|----------|--|--------|---------|-----------|----------|--|--|--|--|--|
| | Operating Depth for vertical wall Total Volume Differenece of Tank Volume and Sludge Volum | | | | | | | | | |
| Diameter | ft | ft3 | gal | Oct-March | Apr-Sep | | | | | |
| 15.0 | 7.4 | 1373.3 | 10272.4 | -3561.1 | -18495.6 | | | | | |
| 20.0 | 7.4 | 2478.2 | 18537.2 | 4703.7 | -10230.7 | | | | | |
| 25.0 | 7.4 | 3929.7 | 29394.4 | 15560.9 | 626.5 | | | | | |

Clarifier and Sludge storage tank calculation - Alternative 2

Flow and Solid Data:

| Q Lake | 713.3 | gpm |
|-------------------------|--------|------|
| | 1.03 | MGD |
| Drum backwash | 5% | |
| Q WAS first Drum | 35.7 | gpm |
| Q WAS first Drum | 0.051 | MGD |
| Q Influent | 677.6 | gpm |
| Q Influent | 0.976 | MGD |
| SG | 1.05 | |
| Solids % | 5% | |
| Sludge TSS in clarifier | 50000 | mg/L |
| Lake TSS | 2 | mg/L |
| Q WAS of rearing system | 677.6 | gpm |
| | 0.9757 | MGD |
| Drum TSS capture | 62% | |
| Clarifier removal rate | 60% | |
| Feed to TSS | 30% | |

Mass Captured from Drum Filters:

| Mass of Influent | 6.511 | lb/day |
|------------------------|--------|--------|
| Mass Influent-captured | 10.622 | lb/day |

Estimated sludge Volume:

| | | Youngs | and Fosters Raceways | West Branc | h Raceways | | | | | | |
|-----------|------|--------|----------------------|------------|--------------|-----------------------|-----------------------------|---------------------------|---------------------------------|--------------------------|-------------------------------|
| | | Feed | Mass generated | Feed | Mass of feed | Mass WAS to Clarifier | Total Mass WAS to Clarifier | Mass removed in Clarifier | Mass overflow in Clarifier | Slude Vol from Clarifier | Sludge Vol from eff treatment |
| Ionth | Days | lbs | lbs/day | lbs | lbs/day | | lb/day | lb/day | lb/day | gal/month | gal/month |
| anuary | 31 | 1,530 | 15 | 624 | 6 | 27.4 | 38.0 | 22.8 | 15.2 | 1613.3 | 25.7 |
| ebruary | 28 | 1,646 | 18 | 672 | 7 | 31.3 | 42.0 | 25.2 | 16.8 | 1610.3 | 33.8 |
| farch | 31 | 2,661 | 26 | 757 | 7 | 39.6 | 50.2 | 30.1 | 20.1 | 2132.9 | 59.1 |
| pril | 30 | 2,490 | 25 | 1,310 | 13 | 44.5 | 55.1 | 33.1 | 22.1 | 2266.5 | 62.7 |
| Лау | 31 | 2,547 | 25 | 1,258 | 12 | 43.3 | 54.0 | 32.4 | 21.6 | 2292.0 | 60.7 |
| une | 30 | 4,564 | 46 | 393 | 4 | 56.1 | 66.7 | 40.0 | 26.7 | 2742.2 | 139.1 |
| uly | 31 | 7,404 | 72 | - | 0 | 78.2 | 88.8 | 53.3 | 35.5 | 3771.6 | 290.6 |
| lugust | 31 | 8,658 | 84 | 651 | 6 | 96.6 | 107.2 | 64.3 | 42.9 | 4554.7 | 410.4 |
| September | 30 | 8,692 | 87 | 1,846 | 18 | 111.9 | 122.5 | 73.5 | 49.0 | 5036.5 | 486.4 |
| October | 31 | 3,303 | 32 | 2,858 | 28 | 66.1 | 76.8 | 46.1 | 30.7 | 3260.6 | 112.1 |
| Vovember | 30 | 1,091 | 11 | 860 | 9 | 26.0 | 36.6 | 22.0 | 14.7 | 1506.4 | 18.3 |
| December | 31 | 1,450 | 14 | 576 | 6 | 26.1 | 36.7 | 22.0 | 14.7 | 1560.7 | 23.5 |
| | | | | | | | · | | Total sludge from Clarifier | 32348 | |
| | | | | | | | | | Total sludge from EFF treatment | | 1722 |
| | | | | | | | | | Total Sludge | | 34070 |

Clarifier Estimations:

| Solids Flow | 713.265 | gpm | | | | |
|-------------|---------|------------------------|----------|----------|----------------|-----------------------------|
| | - | Clrafier Sizing | - | | Solids det Avg | Overflow rate Hyd load rate |
| Diameter | Depth | Surface Area | Volum | e | Goal>60 min | Goal<1000 |
| ft | ft | ft2 | ft3 | gal | min | gpd/ft2 |
| 25 | 8 | 490.87 | 3926.99 | 29373.89 | 41.18 | 2092.39 |
| 15 | 8 | 176.71 | 1413.72 | 10574.60 | 14.83 | 5812.21 |
| 20 | 8 | 314.16 | 2513.27 | 18799.29 | 26.36 | 3269.37 |
| 30 | 8 | 706.86 | 5654.87 | 42298.40 | 59.30 | 1453.05 |
| 35 | 8 | 962.11 | 7696.90 | 57572.83 | 80.72 | 1067.55 |
| 40 | 8 | 1256.64 | 10053.10 | 75197.16 | 105.43 | 817.34 |

Sludge Storage tank Estimation:

| Sludge Storage Tank | | | | | | | | |
|---------------------|-----------------------------------|-----|--------|---------|-----------|----------|--|--|
| | Operating Depth for vertical wall | | | 'olume | Tank \ | /olume | | |
| Diameter | ft | ft3 | | gal | Oct-March | Apr-Sep | | |
| 15.0 | 7.4 | | 1373.3 | 10272.4 | -1684.3 | -11841.0 | | |
| 20.0 | 7.4 | | 2478.2 | 18537.2 | 6580.5 | -3576.2 | | |
| 25.0 | 7.4 | | 3929.7 | 29394.4 | 17437.7 | 7281.0 | | |

Clarifier and sludge Storage Tank Calculation – New Hampton, Alternative 1.A

Flow and Solid Data:

| Q Lake | 693 | gpm |
|-------------------------|--------|------|
| | 1.00 | MGD |
| Drum backwash | 5% | |
| Q WAS first Drum | 34.7 | gpm |
| Q WAS first Drum | 0.050 | MGD |
| Q Raceways | 658.4 | gpm |
| Q Raceways | 0.948 | MGD |
| SG | 1.05 | |
| Solids % | 5% | |
| Sludge TSS in clarifier | 50000 | mg/L |
| Lake TSS | 2 | mg/L |
| Q WAS of rearing units | 677.6 | gpm |
| | 0.9757 | MGD |
| Drum TSS capture | 62% | |
| Clarifier removal rate | 60% | |
| Feed to TSS | 30% | |

Mass captured from Drum Filters in Intake Building:

| Mass of solid in Raceway | 6.325 | lb/day |
|----------------------------|--------|--------|
| Mass Lake-captured by Drum | 10.320 | lb/day |

Estimated Sludge Volume:

| | | Feed | Mass generated | Mass WAS to Clarifier from Rwy | Total Mass WAS to Clarifier | Mass removed in Clarifier | Mass overflow in Clarifier | Slude Vol from Clarifier |
|----------|----|-------|----------------|--------------------------------|-----------------------------|---------------------------|----------------------------|--------------------------|
| Month | | | 0 | | | | | gal/month |
| vionun | | lbs | lbs/day | | lb/day | lb/day | lb/day | gal/monun |
| anuary | 31 | - | - | - | - | - | - | - |
| ebruary | 28 | 2,696 | 28.9 | 35.2 | 45.5 | 27.3 | 18.2 | 1747.0 |
| March | 31 | 3,736 | 36.2 | 42.5 | 52.8 | 31.7 | 21.1 | 2243.0 |
| April | 30 | 743 | 7.4 | 13.8 | 24.1 | 14.4 | 9.6 | 989.7 |
| vlay | 31 | 2,141 | 20.7 | 27.0 | 37.4 | 22.4 | 14.9 | 1587.3 |
| une | 30 | 770 | 7.7 | 14.0 | 24.3 | 14.6 | 9.7 | 1000.8 |
| uly | 31 | - | - | - | - | - | - | - |
| August | 31 | - | - | - | - | - | - | - |
| eptember | 30 | - | - | - | - | - | - | - |
| October | 31 | 7,700 | 74.5 | 80.8 | 91.2 | 54.7 | 36.5 | 3872.6 |
| lovember | 30 | 4,402 | 44.0 | 50.3 | 60.7 | 36.4 | 24.3 | 2493.9 |
| ecember | 31 | 3,084 | 29.8 | 36.2 | 46.5 | 27.9 | 18.6 | 1974.9 |
| | • | | | * | | | Total sludge Clarifier | 15909 |

Clarifier Estimations:

| Solids Flow | 713.2 | gpm | | | | |
|-------------|-------|------------------------|----------------|-----------------------------|-------------|-----------|
| | | Clrafier Sizing | Solids det Avg | Overflow rate Hyd load rate | | |
| Diameter | Depth | Surface Area | Volu | ume | Goal>60 min | Goal<1000 |
| ft | ft | ft2 | ft3 | gal | min | gpd/ft2 |
| 15 | 8 | 176.7 | 1413.7 | 10574.6 | 14.8 | 5803.9 |
| 20 | 8 | 314.2 | 2513.3 | 18799.3 | 26.4 | 3264.7 |
| 30 | 8 | 706.9 | 5654.9 | 42298.4 | 59.4 | 1451.0 |
| 35 | 8 | 962.1 | 7696.9 | 57572.8 | 80.8 | 1066.0 |
| 40 | 8 | 1256.6 | 10053.1 | 75197.2 | 105.6 | 816.2 |

Sludge Storage Tank Estimation:

| | Sludge Storage Tank | | | | | | | | | | | |
|--|---------------------|--------|---------|-----------|---------|--|--|--|--|--|--|--|
| Operating Depth for vertical wall Total Volume Tank Volume | | | | | | | | | | | | |
| Diameter | ft | ft3 | gal | Oct-March | Apr-Sep | | | | | | | |
| 15 | 7.42 | 1373.3 | 10272.4 | -2059.0 | 6694.5 | | | | | | | |
| 20 | 7.42 | 2478.2 | 18537.2 | 6205.8 | 14959.4 | | | | | | | |

Clarifier and sludge Storage Tank Calculation – New Hampton, Alternative 1.B

Flow and Solid Data:

| Q Lake | 693 | gpm |
|-------------------------|--------|------|
| | 1.00 | MGD |
| Drum backwash | 5% | |
| Q WAS first Drum | 34.7 | gpm |
| Q WAS first Drum | 0.050 | MGD |
| Q Raceways | 658.4 | gpm |
| Q Raceways | 0.948 | MGD |
| SG | 1.05 | |
| Solids % | 5% | |
| Sludge TSS in clarifier | 50000 | mg/L |
| Lake TSS | 2 | mg/L |
| Q WAS of rearing units | 677.6 | gpm |
| | 0.9757 | MGD |
| Drum TSS capture | 62% | |
| Clarifier removal rate | 60% | |
| Feed to TSS | 30% | |

Mass captured from Drum Filters in Intake Building:

| Mass of solid in Raceway | 6.325 | lb/day |
|----------------------------|--------|--------|
| Mass Lake-captured by Drum | 10.320 | lb/day |

Estimated Sludge Volume:

| | | Feed | Mass generated | Raceway B&C Feed generated | Mass WAS to Clarifier from Rwy | Total Mass WAS to Clarifier | Mass removed in Clarifier | Mass overflow in Clarifier | Slude Vol from Clarifier |
|-----------|------|-------|----------------|----------------------------|--------------------------------|-----------------------------|---------------------------|----------------------------|--------------------------|
| Vonth | Days | lbs | lbs/day | lbs/day | | lb/day | lb/day | lb/day | gal/month |
| anuary | 31 | - | - | - | - | - | - | - | - |
| ebruary | 28 | 2,696 | 28.9 | 19.3 | 54.5 | 64.8 | 38.9 | 25.9 | 2485.9 |
| March | 31 | 3,736 | 36.2 | 24.1 | 66.6 | 76.9 | 46.1 | 30.8 | 3266.9 |
| April | 30 | 743 | 7.4 | 5.0 | 18.7 | 29.0 | 17.4 | 11.6 | 1193.4 |
| May | 31 | 2,141 | 20.7 | 13.8 | 40.9 | 51.2 | 30.7 | 20.5 | 2174.0 |
| lune | 30 | 770 | 7.7 | 5.1 | 19.2 | 29.5 | 17.7 | 11.8 | 1211.9 |
| luly | 31 | - | - | - | - | - | - | - | - |
| August | 31 | - | - | - | - | - | - | - | - |
| September | 30 | - | - | - | - | - | - | - | - |
| Dctober | 31 | 7,700 | 74.5 | 49.7 | 130.5 | 140.8 | 84.5 | 56.3 | 5982.9 |
| November | 30 | 4,402 | 44.0 | 29.3 | 79.7 | 90.0 | 54.0 | 36.0 | 3700.4 |
| December | 31 | 3,084 | 29.8 | 19.9 | 56.1 | 66.4 | 39.8 | 26.6 | 2820.2 |
| | | | | | • | • | | Total sludge Clarifier | 22835 |

Clarifier Estimations:

| Solids Flow | 713.2 | gpm | | | | |
|-------------|-------|-----------------|----------------|-----------------------------|-------------|-----------|
| | - | Clrafier Sizing | Solids det Avg | Overflow rate Hyd load rate | | |
| Diameter | Depth | Surface Area | Volu | ime | Goal>60 min | Goal<1000 |
| ft | ft | ft2 | ft3 | gal | min | gpd/ft2 |
| 15 | 8 | 176.7 | 1413.7 | 10574.6 | 14.8 | 5803.9 |
| 20 | 8 | 314.2 | 2513.3 | 18799.3 | 26.4 | 3264.7 |
| 30 | 8 | 706.9 | 5654.9 | 42298.4 | 59.4 | 1451.0 |
| 35 | 8 | 962.1 | 7696.9 | 57572.8 | 80.8 | 1066.0 |
| 40 | 8 | 1256.6 | 10053.1 | 75197.2 | 105.6 | 816.2 |

Sludge Storage Tank Estimation:

| | Sludge Storage Tank | | | | | | | | | | | | |
|----------|-----------------------------------|---------|---------|-----------|---------|--|--|--|--|--|--|--|--|
| | Operating Depth for vertical wall | Total V | 'olume | Tank Vol | ume | | | | | | | | |
| Diameter | ft | ft3 | gal | Oct-March | Apr-Sep | | | | | | | | |
| 15 | 7.42 | 1373.3 | 10272.4 | -7983.8 | 5693.1 | | | | | | | | |
| 20 | 7.42 | 2478.2 | 18537.2 | 281.0 | 13957.9 | | | | | | | | |

Clarifier and sludge Storage Tank Calculation – Milford, Alternative 1.A

Flow and Solid Data:

| Q Lake | 693 | gpm |
|-------------------------|--------|------|
| | 1.00 | MGD |
| Drum backwash | 5% | |
| Q WAS first Drum | 34.7 | gpm |
| Q WAS first Drum | 0.050 | MGD |
| Q Raceway | 658.4 | gpm |
| Q Raceway | 0.948 | MGD |
| SG | 1.05 | |
| Solids % | 5% | |
| Sludge TSS in clarifier | 50000 | mg/L |
| Lake TSS | 2 | mg/L |
| Q WAS of rearing system | 677.6 | gpm |
| | 0.9757 | MGD |
| Drum TSS capture | 62% | |
| Clarifier removal rate | 60% | |
| Feed to TSS | 30% | |

Mass captured from Drum Filters in Intake Building:

| Mass of Influent | 6.325 | lb/day |
|------------------------|--------|--------|
| Mass Influent-captured | 10.320 | lb/day |

Estimated Sludge Volume:

| | | Feed | Mass generated | Mass WAS to Clarifier from Rwy | Total Mass WAS to Clarifier | Mass removed in Clarifier | Mass overflow in Clarifier | Slude Vol from Clarifier |
|-----------|------|-------|----------------|--------------------------------|-----------------------------|---------------------------|-----------------------------|--------------------------|
| Month | Days | lbs | lbs/day | | lb/day | lb/day | lb/day | gal/month |
| January | 31 | 7,557 | 73 | 79.5 | 89.8 | 53.9 | 35.9 | 3813.8 |
| February | 28 | 6,721 | 72 | 78.3 | 88.7 | 53.2 | 35.5 | 3401.7 |
| March | 31 | 7,011 | 68 | 74.2 | 84.5 | 50.7 | 33.8 | 3589.3 |
| April | 30 | 5,853 | 59 | 64.9 | 75.2 | 45.1 | 30.1 | 3090.5 |
| May | 31 | 2,402 | 23 | 29.6 | 39.9 | 23.9 | 16.0 | 1694.6 |
| June | 30 | 1,476 | 15 | 21.1 | 31.4 | 18.8 | 12.6 | 1291.1 |
| July | 31 | 2,189 | 21 | 27.5 | 37.8 | 22.7 | 15.1 | 1607.0 |
| August | 31 | 3,237 | 31 | 37.7 | 48.0 | 28.8 | 19.2 | 2037.8 |
| September | 30 | 5,469 | 55 | 61.0 | 71.3 | 42.8 | 28.5 | 2932.6 |
| October | 31 | 7,552 | 73 | 79.4 | 89.7 | 53.8 | 35.9 | 3811.7 |
| November | 30 | 8,724 | 87 | 93.6 | 103.9 | 62.3 | 41.6 | 4270.7 |
| December | 31 | 8,820 | 85 | 91.7 | 102.0 | 61.2 | 40.8 | 4333.0 |
| , | • | | | • | • | · | Total sludge from Clarifier | 35874 |

Clarifier Estimations:

| Solids Flow | 713.2 | gpm | | | | |
|-------------|-------|------------------------|----------------|-----------------------------|-------------|-----------|
| | - | Clrafier Sizing | Solids det Avg | Overflow rate Hyd load rate | | |
| Diameter | Depth | Surface Area | Volu | ime | Goal>60 min | Goal<1000 |
| ft | ft | ft2 | ft3 | gal | min | gpd/ft2 |
| 15 | 8 | 176.7 | 1413.7 | 10574.6 | 14.8 | 5803.9 |
| 20 | 8 | 314.2 | 2513.3 | 18799.3 | 26.4 | 3264.7 |
| 30 | 8 | 706.9 | 5654.9 | 42298.4 | 59.4 | 1451.0 |
| 35 | 8 | 962.1 | 7696.9 | 57572.8 | 80.8 | 1066.0 |
| 40 | 8 | 1256.6 | 10053.1 | 75197.2 | 105.6 | 816.2 |

Sludge Storage Tank Estimation:

| Sludge Storage Tank | | | | | |
|---------------------|-----------------------------------|--------------|---------|-------------|---------|
| | Operating Depth for vertical wall | Total Volume | | Tank Volume | |
| Diameter | ft | ft3 | gal | Oct-March | Apr-Sep |
| 15 | 7.42 | 1373.3 | 10272.4 | -12947.8 | -2381.1 |
| 20 | 7.42 | 2478.2 | 18537.2 | -4683.0 | 5883.7 |
| 25 | 7.42 | 3929.7 | 29394.4 | 6174.2 | 16740.9 |